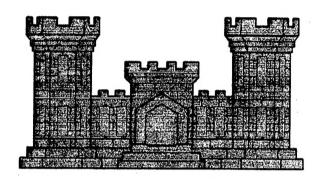
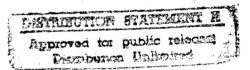
FINAL REPORT

FORT GORDON ENERGY SURVEY & ANALYSIS OF BOILER AND CHILLER PLANTS BUILDING 25910 BUILDING 25330



PROPOSED ENERGY CONSERVATION OPPORTUNITIES FOR SAVANNAH DISTRICT CORPS OF ENGINEERS CONTRACT NUMBER: DACA21-93-C-0110



VOLUME I

3 APRIL 1995

19971016 258

HARRISON AND SPENCER, INC. ENGINEERS - ARCHITECTS - PLANNERS

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DEPARTMENT OF THE ARMY

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Marie Wakef**f**eld,

Librarian Engineering

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Appendix II: Building Heat Load Calculations Data: Ft. Gordon

PROJECT NO. 1

CHILLED WATER NORTH

BUILDING 25910

- Harrison and Spencer, Inc.

GENERAL DESCRIPTION:

Project No. 1 is all of the recommended ECO's combined for the chilled water system in the North area, which is controlled and supplied from Building 25910. The attached project drawing shows an upgrade and general layout of equipment, showing the reuse of the existing cooling towers with new piping from them which will go through a free cooling heat exchanger. There will be pumps at each chiller that will extract the required amount of cooling water through a loop piping arrangement. Chillers 5, 6, and 7 are existing, but new higher efficiency chillers will be added in the size range of one 400 ton and two of 1,250 ton chillers.

Return chilled water will either be run in a loop that will feed any of the chillers which have its new pump "on" to circulate the chilled water through it, or if no pumps are "on", the water will circulate through the new free cooling plate heat exchanger to be located in Building 25910. Teed off of the return chilled water system there will be a pipe that feeds a chilled water storage tank which will be located behind the Plant in the woods. There will be a pump parallel with that line so that if additional pressure is needed to get the water up to the top of the storage tank, that pump will come on. The water in that pipe and water in the pipe leaving at the bottom of the chilled water storage will go back to the Plant. Both of these pipes will have flow in either direction, depending on whether the storage tank is being charged as it will be at night in the summer time, or whether it is being discharged during the peak cooling hours during the day in the summer.

The existing chilled water distribution pumps will remain in operation, but the drives will now be controlled by a single variable speed drive. There will be one variable speed drive for each set of duplicate pumps so that whether one pump or the other back-up pump is running, the variable speed drive will be switched so that it can be controlled to maintain a flow necessary to get buildings the required amount of chilled water. This will be monitored and controlled by the EMCS system.

HOW TO OBTAIN MAXIMUM EFFICIENCY:

Controls and instrumentation added to the EMCS system will allow 24-hour observation of the system and monitoring of equipment operation, temperatures, pressures, flows, amps, etc., to ensure the maximum efficiency is obtained. It will also be the function of the EMCS monitors to compile information so that variations in condenser water flow and chilled water pumping speeds can be monitored, dated, and recorded so that the maximum efficiencies can be obtained and passed onto the next shift for future operations.

The free cooling system will operate primarily in the winter time, and will use cooling towers only to obtain chilled water to be stored at 42°F. This can happen during the night in the winter time. When this happens, not only will the chilled water be circulated to the system as required, which is a year-round requirement, but it can also be stored in the storage tank for use during the day when the temperature rises above the outside ambient temperature not allowing the free cooling system to operate.

Chilled water storage system will operate so that in the low demand times, chilled water can be generated with the chillers and not affect the electrical demand at Fort Gordon. That chilled water will be stored in a 1 million + gallon chilled water storage tank. This stored chilled water can be used during the peak hours in the day to maintain the demand at its lowest possible level. Again, EMCS data will be important in determining when to use the chilled water storage and when to generate chilled water, and how it will affect the overall demand of electricity at Fort Gordon.

COMPILATION OF DATA:

Because all of the ECO's listed under Project No. 1 for the chilled water on the North loop, the cost will be added and an overall simple payback will be determined on the following page.

Simple Payback No. 5.16 SIR for Composite Project 3.02

```
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP)

LIGHTON & LOCATION BETT CORPORT TO LOCATION BETT 
INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3
PROJECT NO. & TITLE: 1 CHILLED WATER NORTH
FISCAL YEAR 1994 DISCRETE PORTION NAME: COMPOSITE
ANALYSIS DATE: 02-19-95 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB
1. INVESTMENT
A. CONSTRUCTION COST $ 2320252.
B. SIOH $ 127614.
C. DESIGN COST $ 139215.
D. TOTAL COST (1A+1B+1C) $ 2587081.
E. SALVAGE VALUE OF EXISTING EQUIPMENT $
F. PUBLIC UTILITY COMPANY REBATE $
                                                                                                                   0.
0.
G. TOTAL INVESTMENT (1D - 1E - 1F)
                                                                                                                                            2587081.
2. ENERGY SAVINGS (+) / COST (-)
DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993
                               UNIT COST SAVINGS ANNUAL $ DISCOUNTED
                              $/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5)
          FUEL
          A. ELECT $ 15.24 18713. $ 285112. 15.61 $ 4450594. B. DIST $ 8.82 0. $ 0. 17.56 $ 0. C. RESID $ 2.73 0. $ 0. 19.97 $ 0. D. NAT G $ 4.50 0. $ 0. 20.96 $ 0. E. COAL $ 1.61 0. $ 0. $ 0. 17.58 $ 0. F. LPG $ 6.34 0. $ 0. 16.12 $ 0. M. DEMAND SAVINGS $ 179970. 14.74 $ 2652758. N. TOTAL 12719. $ 465082. $ 7103352.
 3. NON ENERGY SAVINGS(+) / COST(-)
                                                                                                                                                           $ 3515.
        A. ANNUAL RECURRING (+/-)
                   (1) DISCOUNT FACTOR (TABLE A)
                                                                                                                                   14.74
                   (2) DISCOUNTED SAVING/COST (3A X 3A1)
                                                                                                                                                           $ 51811.
        B. NON RECURRING SAVINGS (+) / COSTS (-)
                                                                      SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4)

$ 657760. 0 1.00 657760.
                                                  COST(-) OC FACTR
(1) (2) (3)
$ 657760. 0 1.00
                                       ITEM
           1. TOTAL
                                                                                                                                                      657760.
                                                                       $ 657760.
           d. TOTAL
         C. TOTAL NON ENERGY DISCOUNTED SAVINGS (+) / COST (-) (3A2+3Bd4)$ 709571.
 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))$ 501485.
                                                                                                                                                                     5.16 YEARS
 5. SIMPLE PAYBACK PERIOD (1G/4)
                                                                                                                                                           $ 7812923.
 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)
 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) =
                                                                                                                                                                    3.02
           (IF < 1 PROJECT DOES NOT QUALIFY)
                                                                                                                                                                    8.96 %
  8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):
```

ECO DATA COMPILATION

TOTAL DISCOUNT SAVINGS	- 4-1	7,812,928
SAVINGS 1st YEAR	27,500 85,278 6,881 7,483 6,834 8,522 40,461 179,970 122,127 16,427	501,483
DEMAND SAVINGS	0 0 0 0 0 179,970 0	179,970
ELECTRICAL SAVINGS MMBTU/YR	0 5,728.48 451.655 162.015 376.38 376.38 2,655.64 0 7,884.48 1,078.17	18,713.20
COST (From LCC)	15,510 440,096 31,190 37,427 145,154 1,968 100,100 660,214 1,086,972 68,456	2,587,087
NON-RECURRING COST (-) SAVINGS (+)	630,000 0 0 22,000 5,760 0 0	657,760
ANNUAL RECURRING COST	4,000 -2,000 0 5,015 0 2,500 0 2,000	3,515
CONSTRUCTION <u>COST</u>	13,910.40 394,703.82 27,972.00 33,566.40 130,183.20 1,765.26 89,775.00 592,118.86 974,862.00 61,394.76	2,320,251.70
DESCRIPTION	Chem Treatment-CHW Variable Speed CHW Pumping Temp Reset Reduce Make-Up Water Cooling Tower Manifolding Cooling Tower Water Treatment Free Cooling CHW Storage Replace Chillers EMCS Controls & Instrumentation	Totals
ECO NO.	6 23 29 33 47 47 51 53 86	

 $\frac{2.587.087}{501,483} = 5.16$ Simple Payback:

 $\frac{7.812.928}{2,587,087} = 3.02$

∺ 1 - 3

ECO NAME:

Treatment of Make-up Water to Chilled Water System

ECO NUMBER:

6

TYPE: BLDG SYSTEM:

Bldg. 25910 Cooling

EXISTING CONDITIONS:

The existing chemical treatment systems serve the condenser side of the chilled water system and are feeding a C-6220 chemical from Industrial Maintenance Corporation into the condenser water system and also adding an A-102 microbiocide by the bucket as the algae begins to build up in the cooling towers. There is no chemical feed on the chilled water side of the system. There is a large volume of make-up water to the chilled water side, which is taken off the fire hose, and is not treated at this time. There isn't any way to treat the make-up water to the chilled water system with the present equipment.

PROPOSED CHANGE:

The proposed system would be to install a coupon system where there are coupon materials located within the contact of the chilled water system to determine what chemicals need to be added to the chilled water system to keep the various coupon materials that may come into contact with the chilled water from corroding. The coupon system is not necessary on the condenser water side because there is actually conductivity meters that are measuring the water on that side, and there is a very limited amount of piping from the cooling towers to the chillers.

CALCULATION & COST METHODOLOGY:

The savings would be the longer life of the chilled water piping system and would be offset by the increased cost in chemicals and installation of the coupons.

Installation of coupon
Materials \$2,000 Labor \$2,000

Chemical feed system
Materials \$3,500 Labor \$2,500

Because chemicals are now being added, the increased cost of chemicals will be \$4,000 per year. All of these costs will be offset by the savings of the life of the chilled water system. Chilled water system piping is \$9,000,000 cost and the life will be 25 years instead of 20 years with chemical treatment. This is computed as a 20-year life with treatment and a 16-year life without chemical treatment. The cost of the chilled water piping system is estimated by scaling the chilled water distribution drawing and multiplying the cost of average pipe sizes by the scaled lengths of that size or nearby sizes.

CONSTRU	CONSTRUCTION COST ESTIMATE				DATE:	23 SEPT 94	SHEET1	OF 1
Project:								
Location:	AUGUSTA, GEORGIA					PROJ. NO.		
	HARRISON AND SPENCER, INC	; .				CODE:	BLDG 25910	
	ECO #6 - TREAT MAKE-UP WATER Estimator: H. TOUB					Checked:		
	ITEM	QUANTIT		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
DESC	RIPTION	QUAN	UNII	UNIT COST	EXTENSION	GINIT COST	EXTENSION	IOIAL
	FEED SYSTEM	1		3500	3500	2500	2500	\$6,000.00
TEST COUP	ON	1	LS	2000	2000	2000	2000	\$4,000.00
		SUBTOTA			5500		4500	
				S TAX	\$275.00	-		
				R TAX			\$765.00	044.040.00
		SUBTOT			\$5,775.00		\$5,265.00	\$11,040.00
				GC ONLY)			-	\$2,208.00 \$13,248.00
		SUBTOTA	AL GC	'S WORK			-	\$13,240.00
		1						
		SUBTOT	Al (G	C & SUBS)		1		\$13,248.00
				PROFIT				
		-		TINGENCY				\$662.40
		TOTAL	1					\$13,910.40

ECO NAME:

Variable Speed Chilled Water Pumping

ECO NUMBER:

23

TYPE: BLDG SYSTEM:

Bldg. 25910 Cooling

EXISTING CONDITIONS:

There are two zones and each zone is served by a set of identical pumps, one backing up the other. Existing pumps all have single speed motors. Buildings on the distribution system, in most cases, have pumps to override the increased pressure drop through the building. 3- way valves are at all of the air handling units and fan coil units in the building.

PROPOSED CHANGE:

The existing pumps shall remain in place, but new variable speed drives should be added to the existing motors in this building. In each building in the chilled water distribution system on the north and the 3-way valves at each of the air handling unit coils will be modified so that the bypass line will be capped off on both directions. (See sketch on following page.) In effect, the 3-way valve will operate as if it were a 2-way valve and reduce flow when chilled water is not required by the coil. The chilled water pump in the building will be operated by the EMCS system so that it will only operate during scheduled chilled water requirements, and will be shut off during times then the building is not in need of cooling. Controls that are tied to the EMCS system will have to be added so that when all the coils shut down for some length of time and when the time is exceeded, the chilled water pump in the building also shuts down. There should also be a time delay so that the pump starts again when enough 3-way valves open to require the chilled water pump to be on. It is expected, in some cases even with the chilled water pump off, there will be sufficient flow in the buildings that are close to the 25910 plant so that the chilled water pump may not be necessary. Because there is no savings on ECO 21 for the primary/ secondary chilled water loop, the cost of the secondary pumps and piping will be included in this ECO.

CALCULATION & COST METHODOLOGY

The cost estimate is as follows:

Six secondary pumps required for the primary/secondary loop:

\$6,000 Materials \$48,000 Labor

20-inch piping as shown on Project No. 1 drawing:

\$20,000 Materials \$10,000

Building controls and EMCS instrumentation for 96 buildings

Labor \$30,000 \$36,000 Materials

One variable speed 200 horsepower drive

\$ 1,000 Material \$17,500 Labor

One set of switches (2) at \$4,340

Labor \$ 3,000 Materials \$ 8,680

Piping changes within all the buildings in the distribution system

\$19,200 \$28,800 Labor Materials Controls and instrumentation in the plant

\$ 2,000 Materials \$ 5,000 Labor

Electrical work

Labor \$10,000 \$ 2,000 Materials

One 300 horsepower variable speed drive

\$ 1,000 Materials \$28,400 Labor

ECO NAME:

Variable Speed Chilled Water Pumping

(Cont'd)

ECO NUMBER:

23

TYPE: BLDG SYSTEM:

Bldg. 25910 Cooling

CALCULATION & COST METHODOLOGY:

One set of two switches at \$4,340 each

Materials

\$ 8,680

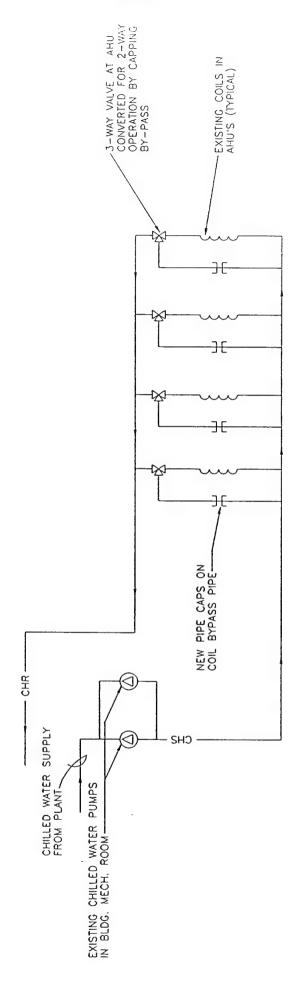
Labor

\$ 3,000

Savings will be the amount saved by having variable speed drives versus constant speed drives for the primary chilled water pumps. The enclosed Bell & Gossett program has been run to show the difference in cost between constant speed and variable speed for the same pumps. Variable speed pumping is obtained by taking the full capacity of the plant as computed and breaking it down into 10% increments of that capacity and then determining the number of hours per bin, and the number of hours on a representative day. From this, the flow can be determined at each speed to come up with the total number of hours that generate flows in the 10% capacity bins allocated. The amount of pumping by each set of pumps is determined based on the pump curves that were available. When this ECO is designed, it would advisable that the designer recheck the actual requirements or demands on the system for each building and the total flow requirements to see that it matches the pump size selected. This will be a confirmation of the existing system. The savings from Pumps 1 and 2 is 434,231.3 KWH and Pumps 3 and 4 is 1,244,198.6 KWH for a total of 1,678,429.9 KWH savings per year. This equates to 1,678,429.9 x 3413 = 5728.48 Million Btu's/year

 10^{6}

CONSTRUCTION COST ESTIMATE					DATE:	23 SEPT 94	SHEET1	OF 1
Project:	FORT GORDON ENERGY STUD	Υ						
Location:	ocation: AUGUSTA, GEORGIA					PROJ. NO.		
Arch/Engr:	HARRISON AND SPENCER, INC.					CODE:	BLDG 25910	
mmary:	ECO #23 - VARAIBLE CHILLED WATER PUMPI	NG	Est	imator:	H. TOUB	Checked:		
	ITEM	QUANTI		MATERIAL		LABOR		
DESC	RIPTION	QUAN	UNIT	UNIT COST	EXTENSION	UNIT COST	EXTENSION	TOTAL
SECONDAR	Y PUMPS	6	EA	8000	48000	1000	6000	\$54,000.00
PIPING		1	LS	10000	10000	20000	20000	\$30,000.00
	& INSTRUMENTAION		LS	36000		30000	30000	\$66,000.00
	PEED DRIVE (200 HP)		LS	17500		1000	1000	\$18,500.00
SWITCHES			EA	4340		1500	3000	\$11,680.00
PIPING CHA			LS	28000		19200	19200	\$47,200.00
	& INSTRUMENTATION IN PLANT		LS	5000		2000	2000	\$7,000.00
ELECTRICAL			LS	2000		10000	10000	\$12,000.00 \$29,400.00
SWITCHES	SPEED DRIVE (300 HP)		LS EA	28400 4340		1000 1500	1000 3000	\$29,400.00
		SUBTOTA			192260		95200	
				S TAX R TAX	\$9,613.00		\$16,184.00	-
		SUBTOT		1700	\$201,873.00		\$111,384.00	\$313,257.0
				SC ONLY)				\$62,651.4
		SUBTOT	AL GC	'S WORK				\$375,908.4
		SUBTOT	AL(GC	& SUBS)				\$375,908.4
		-		PROFIT				
			CON	TINGENCY				\$18,795.4
		TOTAL						\$394,703.8



OPTION #2: ADD VARIABLE SPEED DRIVE TO EXISTING BLDG. CHILLED WATER PUMPS SO THAT MAXIMUM PRESSURE IN CHILLED WATER SUPPLY LEAVING BLDG. PUMPS WILL NOT REACH DEAD—HEAD SETTING.

B&G Pumping System Analysis: SUMMARY OF INPUT DATA: 25910 COOLING Pumps 1+2 2800.00 qpm System peak demand: 71.04 psig) 164.00 ft. (System discharge pressure: Minimum control/Static pressure: 25.00 ft. (10.83 psiq) Standard Efficiency (SE) 60-cycle motor. 1 Pump System: Pump 1: Series VSCS 10X12X13L, Impeller diameter 12.875" Design RPM = 1770.0, Motor HP = 200.00CONSTANT SPEED OPERATION: Hrs Q/Qd,% TGPM TDH,ft BHP Ep,% BHP/HP,m HP,in E,mtr,% kWHR \$/day E,w/w, % 458.1 18.32 12.8 101.21 86.4 10.0 280.0 183.2 87.49 14.8 0.437 6.07 13.28 25.6 86.4 332.1 20.0 560.0 183.2 87.49 29.6 0.437 101.21 4.40 86.4 176.6 7.06 38.3 30.0 840.0 182.8 87.49 44.3 0.437 101.21 2.34 2.99 40.0 1120.0 182.2 95.59 53.9 0.478 90.6 235.2 105.48 9.41 48.8 111.82 8.37 57.3 92.9 209.3 2.51 50.0 1400.0 181.2 103.90 61.6 0.520 93.0 150.2 6.01 63.2 60.0 1680.0 179.7 112.11 68.0 0.561 120.59 1.67 93.0 112.4 4.49 68.1 1.17 -70.0 1960.0 177.3 119.78 73.3 -0.599 -128.80 5.46 72.1 93.0 136.4 1.34 80.0 2240.0 174.1 127.00 77.5 0.635 136.51 99.0 3.96 75.1 90.0 2520.0 170.4 134.27 80.7 - 0.671 144.26 93.1 66.9 2.68 77.3 93.1 0.709 152.14 0.59 100.0 2800.0 166.3 141.70 83.0 COST SUMMARY: 28851.52 Annual Operating Cost @ \$0.04 / kwhr = \$ 8760 hours/year or 100.00% 28851.52 Total annual operating cost = \$ Total kW hours = 721288.04 VARIABLE SPEED OPERATION: (Table 1 of 1) System suction pressure: 0.00 ft. (0.00 psig) Best Efficiency Staging is ON HP, in E, d/m, % kWHR \$/day E, w/w, %. Hrs Q/Qd, % TGPM TDH, ft BHP Ep, % RPM 71.6 2.86 11.8 60.0 15.82 6.07 10.0 280.0 26.4 9.49 19.7 672.3 4.55 12.5 63.4 113.7 20.0 560.0 30.6 21.98 19.7 728.7 34.66 4.40 1.88 29.6 46.9 30.0 840.0 37.5 18.03 44.1 26.90 67.0 2.34 811.1 3.10 38.5 71.8 77.4 40.0 1120.0 47.2 24.92 53.6 919.6 34.72 2.99 83.3 3.33 47.5 77.1 44.52 50.0 1400.0 59.8 34.31 61.6 1041.1 2.51 2.91 54.5 60.0 1680.0 75.0 46.89 67.9 1179.9 58.37 80.3 72.7 1.67 83.1 66.1 2.65 60.8 75.81 70.0 1960.0 93.1 62.98 73.2 1318.8 1.17 3.91 66.0 85.3 97.6 1.34 80.0 2240.0 114.0 83.32 77.4 1457.6 97.71 3.46 69.5 86.3 86.4 90.0 2520.0 137.6 108.64 80.6 1613.8 125.91 0.92 2.82 72.3 70.6 0.59 100.0 2800.0 164.0 139.87 82.9 1752.6 87.2 160.42

Annual Operating Cost @ \$0.04 / kwhr = \$ 11482.27

8760 hours/year or 100.00%

Total kW hours = 287056.74

COST SUMMARY:

ction Pressure : 0.0 psig rcent of Year : 100%

Percent of Year Hours/Year Hours/Year : 8760

Annual Operating Cost: \$11482.27

Total hours/year = 8760 Total annual operating cost = \$11482.27

B&G Pumping System Analysis: Pumps 3+4 25910 COOLING SUMMARY OF INPUT DATA: map 00.0008 System peak demand: 47.65 psig) 110.00 ft. (System discharge pressure: 10.83 psiq) 25.00 ft. (Minimum control/Static pressure: Standard Efficiency (SE) 60-cycle motor. 1 Pump System: Pump 1: Series HSCS 14X16X17, Impeller diameter 13.400" Design RPM = 1785.0, Motor HP = 250.00CONSTANT SPEED OPERATION: O/Od.% TGPM TDH.ft BHP Ep,% BHP/HP,m HP,in E,mtr,% kWHR \$/day E.w/w, % Hrs 10.0 800.0 182.4 295.24 12.5 1.181 314.37 93.9 1423.0 56.92 11.7 6.07 93.9 1031.5 41.26 22.9 314.37 20.0 1600.0 178.5 295.24 24.4 1.181 4.40 93.9 544.5 21.78 33.9 30.0 2400.0 174.4 293.12 36.1 1.172 312.04 2.34 27.66 44.1 94.0 691.4 1.165 310.10 2.99 40.0 3200.0 169.2 291.36 46.9 23.06 53.4 1.158 94.0 576.5 50.0 4000.0 162.8 289.46 56.8 308.01 2.51 15.22 61.5 305:47 94.0 380.4 60.0 4800.0 155.0 287.15 65.4 1.149 1.67 70.0 5600.0 145.9 284.68 72.5 1.139 302.75 94.0 264.1 10.57 68.1 1.17 11.96 73.1 299.0 80.0 6400.0 135.4 281.51 77.7 1.126 299.26 94.1 1:34 8.10 76.1 94.1 202.4 1.111 295.00 90.0 7200.0 123.4 277.63 80.8 0.92 127.1 5.08 77.0 94.2 1.088 288.78 0.59 100.0 8000.0 110.0 271.95 81.7 COST SUMMARY: 80882.08 Annual Operating Cost @ \$0.04 / kwhr = \$ 8760 hours/year or 100.00% Total annual operating cost = \$ 80882.08 Total kW hours = 2022051.95VARIABLE SPEED OPERATION: (Table 1 of 1) 0.00 psig) 0.00 ft. (System suction pressure: Best Efficiency Staging is ON \$7day E, w/w, % HP, in E, d/m, % kWHR Hrs Q/Qd, TGPM TDH, ft BHP Ep, 8 RPM682.2 121.01 60.3 547.7 21.91 4.3 25.9 72.93 7.2 6.07 800.0 9.67 15.6 743.9 73.69 63.8 241.8 4.40 20.0 1600.0 28.4 47.01 24.4 5.68 24.3 67.6 141.9 81.31 32.7 54.99 36.0 832.2 2.34 30.0 2400.0 8.23 33.8 92.26 72.2 205.7 2.99 40.0 3200.0 38.6 66.64 46.8 938.0 7.96 44.0 198.9 2.51 50.0 4000.0 46.3 82.45 56.7 1061.5 106.26 77.6 6.39 52.5 60.0 4800.0 55.6 103.22 65.3 1193.9 128.37 80.4 159.9 1.67 83.2 136.6 5.46 60.2 66.7 130.25 72.4 1335.0 156.59 70.0 5600.0 1.17 7.73 66.3 85.4 193.3 79.4 165.15 77.7 1485.0 193.46 80.0 6400.0 1.34 6.72 69.7 86.3 167.9 244.78 0.92 90.0 7200.0 93.8 211.33 80.7 1635.0

Annual Operating Cost @ \$0.04 / kwhr = \$ 8760 hours/year or 100.00%

0.59 100.0 8000.0 110.0 272.56 81.5 1780.6

5.50 71.2

87.3

312.32

31114.13

137.4

Total kW hours = 777853.32

COST SUMMARY:

retion Pressure : 0.0 psignature : 100%

Hours/Year : 8760

Annual Operating Cost: \$31114.13

Total hours/year = 8760 Total annual operating cost = \$31114.13

ECO NAME:

Controls For Supply CHW Regulations/Reset Temperature

ECO NUMBER:

29

TYPE: BLDG SYSTEM:

Bldg. 25910 Cooling

EXISTING CONDITIONS:

Although the chillers are set to maintain a constant chilled water supply temperature, some water is bypassed through non-operating chillers and the temperature actually varies. The system is set to operate at a constant supply water temperature of approximately 42°F.

PROPOSED CHANGE:

Wire the chilled water supply setpoint to existing EMCS controls so that the chilled water temperature setpoint can be adjusted as conditions require. This will allow the temperature to vary upwards, and the savings of 1.5% of the chiller usage can be obtained for every 1° of reset temperature. Although the savings is available to be had, it is recommended that variable speed pumping also be implemented so that flow reduction will be reduced as building loads are reduced, but the chilled water temperature is still increased to 45°F to save additional energy. Each building will still have the full humidity control at 45°F chilled water.

CALCULATION & COST METHODOLOGY

Total chiller usage is determined by the hours each bin of capacity is shown on Table 3A using .75KW/ton-hour.

```
450 tons x 2262 hours x .75 = 747,900 KW hours

900 tons x 1605 hours x .75 = 1,083,375 KW hours

1350 tons x 853 hours x .75 = 863,663 KW hours

1800 tons x 1092 hours x .75 = 1,474,200 KW hours

2250 tons x 916 hours x .75 = 1,545,750 KW hours

2700 tons x 610 hours x .75 = 1,235,250 KW hours

3150 tons x 428 hours x .75 = 1,011,150 KW hours

3600 tons x 486 hours x .75 = 1,320,300 KW hours

4050 tons x 336 hours x .75 = 1,020,600 KW hours

4500 tons x 215 hours x .75 = 725,625 KW hours

11,027,813 KW per year
```

For the available savings,

Multiply 1.5% of 11,027,813 x 50% for all temperatures above 43°F Multiply 1.5% x 11,027,813 x 20% for all temperatures above 44°F Multiply 11,027,813 by 10% for all temperatures above 45°F

Total of above equals the total savings.

Above 43°F
Above 44°F
Above 45°F

Above 45°F

16541.72 KWH
132333.76 KWH x 3413 = 451.655 Million Btu's/Yr

Cost:

Controls:

Materials

\$10,000

Labor

\$10,000

CONSTRU	ICTION COST ESTIMATE				DATE:	23 SEPT 94	SHEET1	OF 1
Project:	FORT GORDON ENERGY STUD	ΟY						
Location:	AUGUSTA, GEORGIA					PROJ. NO.		
	HARRISON AND SPENCER, INC).				CODE:	BLDG 25910	
	ECO #29 - CHW TEMP RESET		Est	imator:	H. TOUB	Checked:		
	ITEM CRIPTION	QUANTI		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
DE9	SRIFTION							
CONTROLS		1	LS	10000	10000	10000	10000	\$20,000.00
			1-1-1-1					
								· ·
					-			
		SUBTOT			10000		10000	
				STAX	\$500.00		\$1,700,00	
U -		SUBTO		OR TAX	\$10,500.00		\$1,700.00 \$11,700.00	\$22,200.00
				GC ONLY)	\$10,500.00		\$11,700.00	\$4,440.00
				C'S WORK				\$26,640.00
							-	
		0115		2 0 01/50				£26 640 00
			_	C & SUBS)				\$26,640.00
				PROFIT TINGENCY				\$1,332.00
	A STATE OF THE STA	TOTAL	CON	TINGENCT		1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		\$27,972.00

ECO NAME:

Reduce Make-Up Chilled Water

ECO NUMBER:

33

TYPE: BLDG SYSTEM:

Bldg. 25910 Cooling

EXISTING CONDITIONS:

There are water meters on the chilled water Zones 1 and 2 to measure the make-up water. In addition to the metered make-up water, there is a fire hose connected, which is unmetered, that supplies water to the chilled water system to maintain a certain supply pressure through the chillers to the various zones. From tests run shutting off pumps, turning valves, and measuring make-up water flow to Zones 1 and 2 chilled water, the leaks are determined to most likely be in the distribution system. Based on HTW meter readings, the leakage rates vary over the course of the year as leaks are found, repaired and developed again. Accurate determination of the make-up water is not possible because the fire hose is connected into the chilled water system, which is unmetered. During field observations it was noted that 29 gpm was expected with flows separately measured from each zone with zones not cross-connected. When they were cross-connected, the flow averaged 12 gpm. Total loss measured for 24 hour period with a 1-1/4 inch branch closed between the make-up water systems was 16,634 gallons, which was less than what was recorded for previous days on the log with the 1-1/4 inch branch open.

PROPOSED CHANGE:

Although a permanent fix to all of the leaks is not possible, the effort should be made using permanent flow meters, measuring actual supplies, and determining flow rates within the buildings will help reduce the leakage. The leakage amounts to a large expense due to the chilling required on lost water and the cost of water itself.

CALCULATION & COST METHODOLOGY:

The savings consists of water savings and the cost of chilling replacement water. The cost of permanent flow recorders and temperature recording input with wiring of both to the EMCS is included in this ECO, but the EMCS wiring and software changes are shown in the ECO 86 for EMCS controls for this project. Any repair work required to reduce the water leaks is covered by work orders and is not a capital expense for this ECO.

```
16634 gallons/day
16634 \times 8.34 \text{ lb/gpm } \times (\Delta T = 60^{\circ}-45^{\circ}) = 2,080,913 \text{ Btu/day}
                                                        173 tons
          at 12,000 Btu/ton
          Cooling cost at .75 KWH/ton
          .75/KWH/ton x 173 tons
                130 KWH/day saving
            x 365 day
          47,470 \text{ KWH/year or } 47470 \times 3413 = 162.015 \text{ Million Btu's.yr}
Water Savings:
```

 $16.634 \text{ Kgal at } \$.826/\text{Kgal x } 365 \text{ days/yr} = \frac{\$5,015}{\text{year}}$

CONSTRU	CTION COST ESTIMATE			DATE:	23 SEPT 94	SHEET1	OF 1
Project:	FORT GORDON ENERGY STUD						
_ocation:	AUGUSTA, GEORGIA		PROJ. NO.	2			
	HARRISON AND SPENCER, INC		CODE:				
	ECO #33 - REDUCE MAKE-UP CHW		stimator:	H. TOUB	Checked:		
	ITEM RIPTION	QUANTITY QUAN UN	MATERIAL	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
FLOW METE	RS	6 EA			1000	6000	\$15,000.00
TEMP RTD IN	I DISTRIBUTION PIPE	6 EA	500	3000	1000	6000	\$9,000.00
							1 1100
							44.7
		SUBTOTAL		12000		12000	
		-	LES TAX	\$600.00			
			BOR TAX	0.10.000.00		\$2,040.00	#20 040 00
		SUBTOTAL		\$12,600.00		\$14,040.00	\$26,640.00 \$5,328.00
			GC'S WORK				\$31,968.00
							1400-
			GC & SUBS)				\$31,968.00
			C'S PROFIT				\$1,598.40
		TOTAL	ONTINGENCY				\$33,566.40

ECO NAME:

Common Manifolding of Cooling Towers

ECO NUMBER:

43

TYPE: BLDG SYSTEM: Bldg. 25910 Cooling

EXISTING CONDITIONS:

Chillers 1, 2, 3, 4A, and 4B have dedicated cooling towers and although the towers are similarly sized for 700 and 750 ton chillers, there is no means of using an alternate cooling tower with a desired chiller. Chillers 5, 6, and 7 are centrifugal chillers that replaced two absorption chillers. The cooling towers were not replaced so that two cooling towers are cross-connected for use with three centrifugal chillers. It is not possible to maintain a fixed condenser water flow for three chillers with two cooling towers. The fact that the chilled water flow is only constant through all chillers if the same pumps are "On", no chillers are valved "Off", and the pressure drop through the chilled water distribution systems remain constant does not make a fixed condensate water flow any more likely.

PROPOSED CHANGE:

Because the plans for Project 1 calls for eliminating chillers 1, 2, 3, 4A, and 4B and replacing them with three new chillers, of which the tonnage is not matched up with any of the cooling towers, we are going to revise the piping from all cooling towers so that we can establish the correct condenser water flow to any chiller regardless of the cooling towers that are used. The proposed piping and pump arrangement is shown on the drawings for Project No. 1. Each chiller will have its own pump to take water off the loop established by flow through any of the cooling towers in operation. Valving will be available so that the correct flow can be determined, and measured as part of the additional controls that are added. Existing chillers 5, 6, and 7 do not match up with their cooling towers as they are now. The same general approach will apply to them and that pumping and pipes will be added or modified to chillers 5, 6, and 7, similarly to that shown for chiller nos. 1, 2 and 3.

CALCULATIONS AND COST METHODOLOGY:

- 1. With this ECO and ECO 23 which allows for each individual chillers to be piped out of a loop on the chilled water side we now have the ability to isolate any cooling tower or any chiller to do maintenance work as required. By making repairs when they are necessary instead of when the equipment is available, it can improve the life of the chillers one year. This is the difference between a 19-year life and a 20-year life.
- With new pumps and valves, the condenser water flow to each chiller can be controlled to optimum conditions. This will allow us to supply water as required and as monitored by the EMCS system to determine what the best efficiency is for that chiller in operation.
- 3. The condenser water temperature can be controlled by bringing on more cooling towers to bring the temperature down by circulating more water through greater cooling tower capacity. If on hot days we can reduce the condenser water temperature 2 degrees by circulating water through the cooling towers, we can save 1% of yearly cooling tower operating cost of 11,027,813 KW/yr. This equals 110,278KW x 3,413 = 376.38 million Btu's/yr. savings.

There will be some additional cost of pumping the condenser water through the cooling towers to obtain this saving, but the extra pumping cost will be offset by the reduced pumping cost that can be obtained during the cool weather periods when an efficient condenser water temperature can be obtained with less pumping. Because these savings are marginal and in need of experimental data, the EMCS system will monitor efficiencies of chillers with various condenser water flows, as wells as chilled water flows. The EMCS system controls added in this project will allow the operators to obtain the efficiencies indicated in this ECO. Costs for implementing this ECO are the additional pipe costs.

CONSTRU	CTION COST ESTIMATE			DATE:	23 SEPT 94	SHEET 1	OF 1
Project:	FORT GORDON ENERGY STUD	Υ					
ocation:	AUGUSTA, GEORGIA		PROJ. NO.	1			
	HARRISON AND SPENCER, INC).			CODE:	BLDG 25910	
nmary:	ECO #43 - COOLING TOWER MANIFO	H. TOUB	Checked:				
200	ITEM	QUANTITY	stimator: MATERIAL		LABOR		
DESC	RIPTION	QUAN UN	IT UNIT COST	EXTENSION	UNIT COST	EXTENSION	TOTAL
PIPING MAT	FRIALS	1 LS	30000	30000	30000	30000	\$60,000.00
CONDENSER	WATER PUMPS	6 EA	4000		1000	6000	\$30,000.00
ELECTRICAL		1 LS	1500	1500	2500	2500	\$4,000.00
					4.26.46.7		
							4000
		SUBTOTAL		55500		38500	
			LES TAX	\$2,775.00			
		17% LA	BOR TAX			\$6,545.00	
		SUBTOTAL	S	\$58,275.00		\$45,045.00	\$103,320.00
		20% OF	(GC ONLY)				\$20,664.00
		SUBTOTAL	GC'S WORK				\$123,984.00

		CLIPTOTAL	GC & SUBS)				\$123,984.0
			C'S PROFIT				ψ120,007.00
<u> </u>			ONTINGENCY				\$6,199.20
		TOTAL	MINGENCI		1.00		\$130,183.20

ECO NAME:

Cooling Tower Water Treatment

ECO NUMBER:

47

TYPE: BLDG SYSTEM: Bldg. 25910 Cooling

EXISTING CONDITIONS:

Current water treatment is based on a conductivity meter of the cooling tower water, but biocide is added manually by the scoopful only as needed.

PROPOSED CHANGE:

This cooling tower chemical feed is adequate except for the method of feeding biocides. Proper maintenance and observation of the cooling towers is insufficient without the addition of new equipment. The cost of new equipment is \$1000 with \$300 for installation labor.

CALCULATION & COST METHODOLOGY:

Savings amount to the increased life of the cooling tower and improved cooling by keeping it clean. Because chemicals are now being added, there is no increased cost of chemicals. Any improvements in the cooling water chemical treatment will be positive; a potential maintenance cost reduction of \$2,500/year total, and the life of the cooling tower extended for two years (with treatment, the life of the cooling tower is 20 years, without treatment it is 18 years). The cost of a new cooling tower is \$20,000 in materials and \$4,000 in labor for each of six towers in Building 25910. The total cost is therefore \$144,000 for six new cooling towers.

The efficiency improvement of the chillers will be 1% if the cooling tower water can be cooled two degrees F more than it is cooled in a algea laden cooling tower. Based on ECO 29 calculation and cost methodology, the chillers use 11,027,813 KW/year.

1% of 11,027,813 KW/yr = 110,278 KW/yr

 $110,278 \times \frac{3413}{10^6} = 376.38 \text{ million BTU's/yr.}$

CONSTRUCTION COST ESTIMATE	CONSTRUCTION COST ESTIMATE				SHEET1	OF 1
Project: FORT GORDON ENERGY	STUDY					
Location: AUGUSTA, GEORGIA				PROJ. NO.	1	
Arch/Engr: HARRISON AND SPENCE						
mmary: ECO #47 WATER TREATMENT		Estimator:	H. TOUB	Checked:		
ITEM DESCRIPTION	QUANTITY QUAN UI		EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
CHEMICAL FEED	1 LS	1000	1000	300	300	\$1,300.00
	SUBTOTAL		1000 \$50.00		300	
		ALES TAX ABOR TAX	\$50.00	-	\$51.00	
	SUBTOTAL		\$1,050.00		\$351.00	\$1,401.00
	20% O	H (GC ONLY)				\$280.20
	SUBTOTAL	. GC'S WORK				\$1,681.20
		(GC & SUBS)				\$1,681.20
		C'S PROFIT ONTINGENCY				\$84.06
	TOTAL	ONTINGENCT				\$1,765.26

ECO NAME:

Free Cooling In Lieu of Chiller Operation

ECO NUMBER:

51

TYPE: BLDG SYSTEM: Bldg. 25910 Cooling

EXISTING CONDITIONS:

All of the chillers in Building 25910 are either Carrier or York and are not internally convertible to free cooling unless a heat exchanger is added externally.

PROPOSED CHANGE:

Add a plate heat exchanger to allow the cooling tower to provide the necessary cooling for the chilled water system in the winter months. With new valves and pumps to be added to each chiller in Project No. 1, flow will not go through the chiller pumps that are not turned on. When the piping is designed, the new variable speed drives should be made to have a lower pressure drop through the heat exchanger than the chillers if possible.

CALCULATION & COST METHODOLOGY:

Free cooling with non-Trane chillers is based on the KWH of 193,759 KW hours at \$.052 per KW hours which equals \$10,075.47. The cost is based on adding piping and one plate heat exchanger, which cost \$20,000 in material and \$25,000 in labor. Additional savings will be obtainable in winter days when chilled water that is made with this free cooling system is stored in the chilled water storage tank. This will eliminate running the chillers during the winter days when the cooling load is low and free cooling is not available.

TABLE 2

Month	Time Period	Operating Hours	Free Cooling Avg. Tons	Ton Hrs.	KW/Ton EFF	KWH Saved
	01-08	21	66	1386	.66	915
Oct	09-16	0	1069	0	.66	0
	17-24	4	580	2320	.66	1531
	01-08	78	60	4680	.66	3089
Nov	09-16	4	903	3612	.66	2384
	17-24	30	546	16380	.66	10811
	01-08	166	46	7636	.66	5040
Dec	09-16	64	798	51072	.66	33708
200	17-24	116	448	51968	.66	34299
	01-08	170	29	4930	.66	3254
Jan	09-16	78	660	51480	.66	33977
-	17-24	118	386	45548	.66	30062
	01-08	93	40	3720	.66	2455
Feb	09-16	20	619	12380	.66	8171
	17-24	38	387	14707	.66	9706
	01-08	63	57.	3591	.66	2370
Mar	09-16	7	910	6370	.66	4204
17101	17-24	17	576	9792	.66	6463
	01-08	13	104	1352	.66	892
Apr	09-16	0	1210	0	.66	0
- 47	17-24	1	648	648	.66 Total KWH	$\frac{428}{193,759}$

Converting free cooling to millions of Btu's/Yr. \rightarrow 193,759 KW x $\frac{3413}{10^6}$ = 661.3 Million Btu's/Yr.

ECO NAME:

Free Cooling In Lieu of Chiller Operation

(Cont'd)

ECO NUMBER:

51

TYPE: BLDG SYSTEM:

Bldg. 25910 Cooling

CALCULATION & COST METHODOLOGY:

Storage capacity is 7378 ton hours for a 1,061,547 gallon storage tank.

The total cooling tonnage for each month per Table 2A is:

October = 27,432 ton hours

February = 16,714 ton hours, which is the lowest monthly load for chilling

From Table 2 above, the free cooling available in February is:

93 hrs @ 40 tons = 3,720 ton hours 20 hrs @ 619 tons = 12,380 ton hours 38 hrs @ 387 tons = 4,707 ton hours 151 hrs = 30,807 ton hours

In February there are $28 \text{ days } \times 24 \text{ hrs/day} = 672 \text{ hours}$. Since only 151 hours are available for free cooling, the remaining hours are too warm outside for free cooling so a chiller may be required.

If 7378 ton hours are available each day from the chilled water storage, then 30,807 ton hours can be used directly and 7378 \times 28 day/mo = 206,584 ton hours are available from storage with free cooling if every night has some time when the outside temperature is low enough to make chilled water for storage and to supply the distribution system demand. The total cooling required in February is 16,714 ton/hrs/day \times 28 = 467,992 ton hrs/mo.

Since each day chilled water can be supplied with the free cooling system as follows:

Direct Usage 30,807 ton hrs. Storage 206,584 ton hrs

237,391 ton hrs.

<u>237,391</u> = 50% of February's full load can be met by free cooling with the use of the storage tank.

We will assume that a full storage tank can be made from the free cooling heat exchanger every night in December, January, and February and half of November and March

120 days \times 7378 ton hrs. \times .66 KW/ton = 584,338 KWH which is saved in addition to the 193,759 KWH shown in Table 2.

Total Savings:

193,759 + 584,338 = 778,097 KWH

Converted to Btu x 106:

778,097 x $\frac{3413}{10^6}$ = 2655.64 Million Btu's/Yr.

CONSTRUC	TION COST ESTIMATE				DATE:	23 SEPT 94	SHEET1	OF 1
Project:	FORT GORDON ENERGY STUDY							
Location:	AUGUSTA, GEORGIA PROJ. NO. 1							
	HARRISON AND SPENCER, IN	C.				CODE:	BLDG 25910	
Summary:	ECO #51 - FREE COOLING		Est	imator:	H. TOUB	Checked:	X	
	ITEM CRIPTION	QUANTIT	ΓY	MATERIAL	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
MODIFY COO	LING TOWER W/ HEAT EXCHANGER	1	LS	40000	40000	25000	25000	\$65,000.00
		SUBTO	ΓALS 1		\$40,000.00		\$25,000.00	\$65,000.00
		5%	SALE	S TAX	\$2,000.00			\$2,000.00
		17%	LABO	OR TAX			\$4,250.00	\$4,250.00
		SUBTO	TALS 2	2	\$42,000.00		\$29,250.00	\$71,250.00
		20%	GC C	H & PROFIT				\$14,250.00
		SUBTO	TAL G	C WORK				\$85,500.00
		TOTAL	SUB V	VORK				
				SUB PROFIT				
		5%	CON	TINGENCY O	N JOB			\$4,275.00
		TOTAL						\$89,775.00

ECO NAME:

Chilled Water Storage

ECO NUMBER:

53

TYPE: BLDG SYSTEM:

Bldg. 25910 Cooling

EXISTING CONDITIONS:

As the chilled water system requires chilling, the only way to satisfy this now is by the chillers to operate

PROPOSED CHANGE:

Chilled water storage tanks should be obtained and installed in back of the plant and piped accordingly. Storage capacity will be slightly over 1 million gallons which will allow the existing chiller system to not go over 2,900 tons. According to calculations, the present capacity indicates the capacity would exceed 4,400 tons on a peak day in June. Piping to and from the tank will be as shown on Project No. 1 drawing, and the concept will be that water coming in from the return of the system will come into the high side of the tank, and the water leaving will be on the low side. During the discharging of the stored chilled water, the flow in the piping will be reversed when chilled water is being stored in the tank. Through stratification, the temperatures will vary from the top to the bottom of the tank. The size of the tank will be approximately 50 feet high with a 60 foot diameter. There will be a pump added in case the return pressure from the chilled water system is not sufficient to get to the height of the top of the tank, which will only be used if necessary to get the flow into the tank when required. This will have to be a controlled pump operation.

CALCULATION & COST METHODOLOGY:

Table 2A included with ECO 85, each month by the hour, is broken down by tonnage supplied to the distribution system. This tonnage is calculated based on our field investigation which involved heat gain calculations on all of the buildings and totalizing them. It does not take into account any line loss because the temperature difference in the chilled water system is minimal with direct exchange with the earth. Maximum calculated tonnage occurs at 1500 hours on June, which is 4426 tons. All other hours are less than this. Roughly, 4400 tons of chiller capacity would be needed to meet all demands on the system as it currently is now. The intent of this ECO is to supply chilled water so that less chilling capacity is actually installed and needed than the amount of tonnage required for the period of any day where it exceeds 2900 tons. The difference in tonnage between the maximum demand and the installed capacity of the chillers will be supplied by the chilled water storage system. 2900 tons was selected because this number includes most hours in the summer time in the peak demand for electricity. Below 2900 hours, the cooling demand falls off rapidly so that for every hundred tons less than 2800, Fort Gordon will not have any more time when operating the chilled water storage system to meet Georgia Power's interruptible rate requests. Creating the demand savings will only be a matter of controlling the demand by maintaining enough chilled water in the storage system to get through the peak. As you will see from ECO 51 for free cooling, the storage system is also used in the winter time so that if funds are available to increase the storage size, there are still some possibilities that it would pay for itself from additional free cooling in the winter and from reducing the demand slightly in the summer. In accordance with Table 2A calculations, June being the worst month, the hours where it exceeds 2900 is taken:

ECO NAME:

Chilled Water Storage

(Cont'd)

ECO NUMBER:

53

TYPE: BLDG SYSTEM:

Bldg. 25910 Cooling

CALCULATION & COST METHODOLOGY:

	Demand Above
Hours	2900 Tons
0010	174
0011	485
0012	792
0013	1045
0014	1335
0015	1526
0016	727
0017	757
0018	_437
	7378 ton hrs.

Since the chilled water storage tank will be charged to 42°F water, it will be ready for use in the morning starting at 1000 hours. The capacity of the tank will be based on 10°F difference from 42°F to 52°F. Converting this to the Btu's required to get 7,378 ton hour, the following method is calculated:

1 ton hour = 12,000 Btu/hr = 1,200 lbs. water x 10°F Δ t 1,200 lbs. ÷ 8.34 lbs/gal. = 143.88 gal./ton hr. 1,200 lbs ÷ 62.4 lbs/cu. ft. = 19.23 cu. ft./ton hr. 7378 ton hr x 143.88 gal/ton hr. = 1,061,547 gal. capacity 7378 ton hours x 19.23 cu. ft./ton hr. = 141,885 cu. ft. Tank size with diameter roughly equals to height $\Pi D^2 = V$

Where H = D,
$$D^3 = \frac{V \times 4}{\Pi} = 141,885 \times 4 \div \Pi$$

$$D^3 = 180,654, D = 56.5$$

The above calculation was for 2900 tons of chiller demand capacity with a 7,378 ton hour capacity. Basis of selection therefore indicates that a 60 ft. diameter tank at 50 ft. high would satisfy the 2900 tons of chiller demand. Another 300,000 gal. of capacity, that would be necessary to reduce the electrical demand to 2700 tons of chiller capacity, would require that the 60 ft. diameter tank be 10 feet taller. We would only get 200 tons of additional chiller capacity which would minimally affect the time that electrical demand would have to be reduced to meet the Power company's curtailment. EMCS building controls would reduce usage before this 200 ton hour demand decrease would influence electric building. The additional 200 ton hour will only be cost effective if a new low demand can be set for the Georgia Power interruptible rate.

The cost of chilled water storage: The rough cost that seems to work is \$60/ton hr. \$60/ton hr x 7,378 ton hrs. = \$442,680. Of this total, the labor portion of this is roughly \$42,680.

ECO NAME:

Chilled Water Storage

(Cont'd)

ECO NUMBER:

53

TYPE: BLDG SYSTEM: Bldg. 25910 Cooling

CALCULATION & COST METHODOLOGY:

The current arrangement with Georgia Power and Fort Gordon is that the demand charge is at a rate of \$106.20, but there is a \$45/KW rebate if they can meet an interruptible rate when asked by Georgia Power to reduce their demand, in the summer time and usually at the peak couple of hours during the day. Adding the peak demand of \$106.20 to the \$45/KW rebate is a savings of \$151.20/KW if the demand can be reduced, which it can be in this case. Existing chiller operating cost is .66 KW/ton for the chiller, and .12 KW/ton for the fans and pumps on the cooling towers, which would not have to operate with stored chilled water. The total demand savings is a total of .78 KW/ton. Difference in demand between the full chiller capacity of 4426 tons and 2900 tons is 1526 tons for the maximum cooling day in June.

1,526 x .78 KW/ton = 1,190.28 KW demand 1,190.28 KW x \$151.20 = \$179,970.34 savings for demand reduction

CONSTRUC	CTION COST ESTIMATE				DATE:	23 SEPT 94	SHEET	1 OF 1	
Project:	FORT GORDON ENERGY STUD	Y							
cation:	AUGUSTA, GEORGIA PROJ. NO.				1				
	HARRISON AND SPENCER, INC.			CODE: BLDG 25910					
Summary:	ECO #53 - Chilled Water Storage					Checked:			
	ITEM CRIPTION	QUANTIT QUAN	Υ	MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL	
INSTALL UND	ERGROUND CHILLED WATER TANK	1	LS	400000	400000	42650	42680	\$442,680.00	
								-	
		SUBTOT	ΛI Q 1		\$400,000.00	1	\$42,680.00	\$442,680.00	
				STAX	\$20,000.00		¥ 12,000.00	\$20,000.00	
		-		R TAX	\$20,000.00		\$7,255.60	\$7,255.60	
		SUBTOT			\$420,000.00		\$49,935.60	\$469,935.60	
				H & PROFIT	V (25,000.00			\$93,987.12	
	SUB-CONTRACTORS			C WORK				\$563,922.72	
		TOTAL S	SUB V	VORK					
		10% GC SUB PROFIT							
		5% CONTINGENCY ON JOB				\$28,196.14			
	TOTAL				\$592,118.86				

ECO NAME:

Replace Chillers in Plants for Higher Efficiency and the Best Sizing

ECO NUMBER:

85

TYPE: BLDG SYSTEM: Bldg. 25910 Cooling

EXISTING CONDITIONS:

See Figure 1A for the existing chilled water schematic for Building 25910. Chillers 1, 2, and 3 are the oldest; chillers 4A and 4B are next in age and next to lowest in efficiency; chillers 5, 6, and 7 were recently added to the Plant to be replaced in lieu of the absorption chillers which have been removed and are the most efficient. Chillers 1, 2, and 3 are 700 ton capacity; chillers 4A and 4B are both 750 ton capacity.

PROPOSED CHANGE:

Replace all five chillers that are the oldest, 1, 2, 3, 4A and 4B with new chillers of high efficiency in the following capacities: One 400 ton chiller and two 1250 ton chillers. This will give the capacity of 2900 tons, which is what is required with the chilled water storage being put in to maintain the full demand of 4426 tons, which will occur at the highest peak demand in one hour in June. The remaining existing chillers 5, 6, and 7 are the newest and will remain in place, to act as a back-up in case there is any failure in the new chillers being installed. When these new chillers are installed, there will be piping changes for the incoming condenser water, as well as the chilled water entering and leaving the chillers, but the piping cost and piping identification will occur in other ECO's in this Project No. 1.

CALCULATION & COST METHODOLOGY: The new chillers are more efficient than the existing chillers. This information is shown on the sheet that shows chiller efficiencies. Bin limits and the chillers that are operating for those various capacities are shown on Page 2 of this ECO. Page 3 and 4 show the cost of operating the new chillers under Savings No. I of Page 3, and under Savings No. II the existing chiller operating cost is shown. The existing chiller cost is based on most efficient operation of the existing chillers. This is a conservative approach because (1) it is not known how the operators are going to operate which chiller at which time, and (2) the information available about the efficiencies of the chillers is sketchy based on previous reports by GEC Jenson which are the basis of this report. Only three of the 8 chillers have been tested, and the report of the efficiency is widely varied. I have chosen the best efficiencies to operate most of the time, and I have assumed that all chillers that were not tested operated at these best efficiencies. III on Page 4 of this ECO shows that there is a savings of 2,310,133 KWH/yr, which translates into 7,884.48 million Btu's. Because new chillers are replacing old, the maintenance costs will decrease by \$2,000/yr.

ECO NAME:

Replace Chillers in Plants for Higher Efficiency and the Best Sizing

(Cont'd)

ECO NUMBER:

85

TYPE: BLDG SYSTEM:

Bldg. 25910 Cooling

CALCULATION & COST METHODOLOGY:

New

1250 Ton Unit (Based on Trane Information)

Capacity	Electric Usage
100%	.54 KW/ton
75%	.49 KW/ton
50%	.48 KW/ton
25%	.55 KW/ton

400 Ton Unit

Capacity	Electric Usage
100%	.58 KW/ton
95%	.53 KW/ton
50%	.52 KW/ton
25%	.59 KW/ton

Existing

750 Tons, Chillers 4A and 4B

Electric Usage		
13.80		
13.52		
12.27		
12.00		

700 Ton Chillers 1, 2, and 3, 5647

Capacity	Electric Usage		
100%	18.51		
80%	19.07		
65%	19.31		
50%	19.18		

ECO NAME:

Replace Chillers in Plants for Higher Efficiency and the Best Sizing

(Cont'd)

ECO NUMBER:

85

TYPE: BLDG

Bldg. 25910

SYSTEM:

Cooling

CALCULATION & COST

METHODOLOGY:

Chiller Cooling Summary - Project No. 1 (See Table 3A for Plant Cooling Load Summary)

	New			
Existing	Chiller			
Chiller	Capacity			
Operating	Operating	c/o Plant	BIN Limit	Hours
(Quantity)	(Tons)	Capacity	<u>Tons</u>	Per BIN
Qty of 7	Chillers $1,2,3,=2900$	100	4500	215
Qty of 6	Plus Storage	90	4050	336
Qty of 5	Plus Storage	80	3600	489
Qty of 5	Plus Storage	70	3150	428
Qty of 4	Plus Storage	60	2700	610
Qty of 4	Chillers 2 and 3	50	2250	916
Qty of 3	Chillers 2 and 3	40	1800	1092
Qty of 2	Chillers 1 and 3	30	1350	853
Qty of 2	Chiller 3	20	900	1605
Oty of 1	Chiller 3	10	450	2216

New		Existing	
Chiller 1 = Chiller 2 = Chiller 3 =	1250 tons	Chiller 2 = Chiller 3 = Chiller 5 = Chiller 6 =	

ECO NAME:

Replace Chillers in Plants for Higher Efficiency and the Best Sizing

(Cont'd)

ECO NUMBER:

85

TYPE: BLDG

Bldg. 25910

SYSTEM:

Cooling

CALCULATION & COST METHODOLOGY:

I. <u>SAVINGS</u>: (Cost of Operating New Chillers)

% CAP	HRS.	TONS	KW/TON	<u>KWH</u>
100%	1468	2500	.54	1,981,800
thru 70%		400	.58	340,576
60%	610	2500	.54	823,500
		200	.52	63,440
50%	916	1250	.54	618,300
		1000	.50	458,000
40%	1092	1800	.49	963,144
30%	853	950	.49	397,072
		400	.58	197,896
20%	1605	900	.49	707,805
10%	2216	450	.52	518,544
			Total	7,070,077

ECO NAME:

Replace Chillers in Plants for Higher Efficiency and the Best Sizing

(Cont'd)

ECO NUMBER:

85

TYPE: BLDG

Bldg. 25910

SYSTEM:

Cooling

CALCULATION & COST METHODOLOGY:

II. <u>SAVINGS</u>: - Existing Chiller Operating Cost

Α	В	С	D MBTU/HR	E	F KW/HR
% CAP	<u>HRS</u>	<u>TONS</u>	TONS X 12	<u>EER</u>	(BXD/E)
100%	215	4,200	50,400	18.51	585,413
		300	3,600	12.00	64,500
90%	336	4,050	48,600	18.51	882,204
80%	489	3,600	43,200	18.93	1,115,943
70%	428	3,150	37,800	18.78	861,470
60%	610	2,700	33,400	18.55	1,065,445
50%	916	2,250	27,000	19.07	1,296,906
40%	1,092	1,800	21,600	18.93	1,246,022
30%	853	1,350	16,200	18.55	744,938
20%	1,605	900	10,800	19.31	897,670
10%	2,216	450	5,400	19.31	619,700
			•		9,380,210

III. TOTAL SAVINGS - New High Efficiency Chiller vs. Existing chillers Operating at Best Efficiency

Difference from I and II above

9,380,210

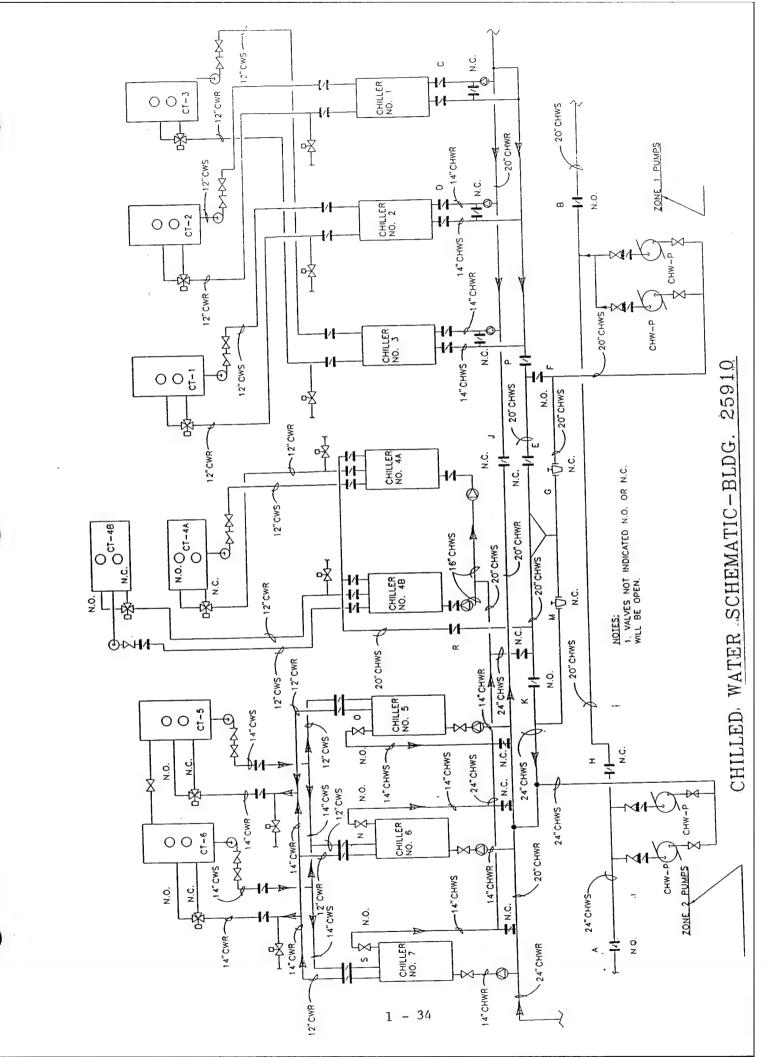
(7,070,077)

2,310,133 KWH Savings/Yr.

Annual Savings in Million Btu's

 $2,310,133 \times 3,413 = 7,884.48$ Million Btu

 10^{6}



CONSTRUCTION COST ESTIMATE				DATE:	23 SEPT 94	SHEET	1 OF 1
Project: FORT GORDON ENERGY STU	IDY						
ocation: AUGUSTA, GEORGIA					PROJ. NO.	2	
Arch/Engr: HARRISON AND SPENCER, IN	IC.				CODE:	BLDG 25910	
mmary: ECO #85 - REPLACE CHILLERS			imator:	H. TOUB	Checked:		
ITEM DESCRIPTION	QUANTI QUAN	TY UNIT	MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
NEW 400 TON CHILLER INSTALLATION	1	LS	110,000	110,000	20,000	20,000	\$130,000.00
NEW 1250 TON CHILLER	2		280,000	560,000	20,000	40,000	\$600,000.00
	SUBTOT	·Al		670,000		60,000	
			S TAX	\$33,500.00			
			R TAX			\$10,200.00	
	SUBTO	TALS		\$703,500.00		\$70,200.00	\$773,700.00
	20%	OH (0	GC ONLY)				\$154,740.00
	SUBTOT	AL GC	'S WORK				\$928,440.00
	SUBTO	TAL(GO	2 & SUBS)				\$928,440.00
			PROFIT				
	5%	CON	TINGENCY				\$46,422.00
	TOTAL						\$974,862.00

ECO NAME:

EMCS Controls and Instrumentation for New Project No. 1

ECO NUMBER:

86

TYPE: BLDG SYSTEM: Bldg. 25910 Cooling

EXISTING CONDITIONS:

Existing automatic or manual controls that are within the plant are not remotely operable by the EMCS by design. The EMCS office which is manned 24 hours a day has very few, if any, instrumentation readouts from the plant, and no control of the plant with the EMCS. Because EMCS personnel are aware of what is happening in many buildings, they are also aware of conditions and demands in the chilled water system. Currently, the boiler operators are making boiler pressure changes, HTW changes, bringing on and off chillers, cooling towers, and many manual valving operations. However, they are not performing the functions that an EMCS office can to control energy and to improve the operating efficiency of the plant.

PROPOSED CHANGE:

It is proposed that the instrumentation discussed in other ECO's related to this Project No. 1 be wired as part of this ECO. Controls that are necessary to obtain maximum operating efficiency will be included in the EMCS software if it is not already there. The wiring from the instrumentation that is referred to in other ECO's and the connections to the EMCS system computer will be included in this ECO computation. Proposed additions or revisions to the EMCS program are as follows:

<u>DESCRIPTION</u>	NO. POINTS	<u>DOLLARS</u>
Software for computing chiller efficiency with BTU measurement		\$ 10,000
Wiring for flow meters at distribution pipe locations	10	5,000
Wiring of temperature sensors at distribution pipe locations	10	5,000
Operating controls for chillers, pumps and valves and indications that they are on	14	4,200
Temperature of chilled water, condenser water, etc.	6	1,200
Free cooling valve positions	4	800
Flow directions to and from chilled water storage	4	6,000
Amps on chillers	7	2,800
Pressures on chilled water supply return and piping to storage	6	1,800
Variable speed pump controls with switches	7	2,500
Chiller pump controls	7	2,500
Condenser water pump controls	6	2,000
Total		\$43,800

This assumes that no additional manpower will be required by EMCS personnel, nor will there be any reduction of personnel in the plant to operate the valves. However, the change that will occur is that EMCS personnel will actually have either physical control or the ability to tell people in the Plant to change valve positions or start equipment.

CALCULATION & COST METHODOLOGY:

It is conservatively estimated that at least 3% of the operating cost for chillers, cooling towers, fans, and pumps, can be saved if the EMCS system is properly controlled and valves properly switched, pumps properly operated, and if the supervision of operating personnel within the Plant is the responsibility of the EMCS personnel using controls and instrumentation to operate plant

ECO NAME:

EMCS Controls and Instrumentation for New Project No. 1

(Cont'd)

ECO NUMBER:

86

TYPE: BLDG SYSTEM: Bldg. 25910 Cooling

CALCULATION & COST METHODOLOGY:

equipment either automatically or by directing the on-site operator by telephone. Savings will be obtained from chiller operation by optimizing the free cooling system so that the chilled water can be stored in the winter, in addition to operating free cooling when ambient temperatures are proper for free cooling, and from locating water leaks in the system using new instrumentation to be installed and monitored by EMCS equipment. From Table 2A, we can count 44 hours listed where the tonnage required per hour is greater than 2900 tons, and for the rest of the hours per year some chilled water, less than 2900 tons, is required. The average tonnage in all hours per year when the full capacity is not required is 1300 tons/hr.

44 hours x 30 days/mo. = 1,320 hrs x 2900 tons x .78 KW/ton = 2,985,840 KW (8760 - 1320 hrs.) x 1,300 tons(average) x .78 KW/ton = 7,544,160 KW Total = 10,530,000 KW

10,530,000 KW x \$.052/KW = \$547,560 1% of \$547,560 = \$5,476

2% of \$547,560 = \$10,951.20 3% of \$547,560 = \$16,426.80

The actual KW saved is 10,530,000 KW \times .03 = 315,900 KW 315,900 KW \times 3.413 = 1078.17 million Btu's 10^6

The costs of the instrumentation are identified in the table under Proposed Changes.

JONS I RUC	TION COST ESTIMATE				DATE:	23 SEPT 94	<u> </u>	OF 1
Project:	FORT GORDON ENERGY STUI	ΣΥ						
ocation:	AUGUSTA, GEORGIA					PROJ. NO.	2	
:h/Engr:	HARRISON AND SPENCER, INC) .				CODE:	BLDG 25910	
Summary:	ECO #86 - EMCS CONTROLS		Est	imator:	H. TOUB	Checked:		
	ITEM RIPTION	QUANTI QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
ייוו ו כם כככוו	ENCY SOFT WARE	1	LS			10000	10000	\$10,000.0
	SYSTEM FLOW METERS	1	LS	3000	3000	2000	2000	\$5,000.0
	SYSTEM FLOW METERS		LS	3000	3000	2000	2000	\$5,000.0
	ONTROLS - CHILLERS, VALVES		LS	3500	3500	700	700	\$4,200.0
	COND WATER		LS	200	200	1000	1000	\$1,200.0
	G VALVE INDICATORS		LS	400	400	400	400	\$800.0
	HES - CHW STORAGE		LS	5200	5200	800	800	\$6,000.0
CHILLER AM			LS	2000	2000	800	800	\$2,800.0
	CHW RET, SUPPLY AND STORAGE		LS	900	900	900	900	\$1,800.0
	PEED & SWITCH CONTROL		LS	1000	1000	1500	1500	\$2,500.0
CHILLER PUM			LS	1000		1500	1500	\$2,500.0
	PUMP CONTROLS		LS	800		1200	1200	\$2,000.0
		SUBTO	ALS 1		\$21,000.00		\$22,800.00	\$43,800.0
		5%	SALE	S TAX	\$1,050.00			\$1,050.0
		17%	LABO	R TAX			\$3,876.00	\$3,876.0
		SUBTO			\$22,050.00		\$26,676.00	\$48,726.0
		20%	GC O	H & PROFIT				\$9,745.2
	SUB-CONTRACTORS	+		WORK				\$58,471.2
		TOTAL	SUB W	/ORK				
				UB PROFIT				
				TINGENCY ON	JOB			\$2,923.
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COOLING

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	<u>. </u>	48.7	35.4	23.0	17.9	13.3	9.0	6.2	211.6	288.3	325.2	356.2	390.7	420.4	450.2	475.0	452.3	463.0	408.7	200.6	6.09	127.9	180	61.0	84.6
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	3.0	13.7	11.6	9.5	7.7	8.0	4	3.7	3.9	69.2	94.6	99.7	110.7	119.0	124.2	18	32.3	8	44.7	38.7	30.6	26.7	229	19.4	18.5
	8	19.1	16.2	124	10.0	7.7	6.6	4.7	161.3	186.2	194.3	206.7	219.9	231.2	238.3	244.0	69.8	89.6	53.5	47.3	4.14	36.4	31.5	26.7	9 C C
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	•	828	68.1	5.65	46.6	36.2	8	23.2	293.7	374.1	414.0	447.4	480.2	516.3	543,8	569.9	552.9	4.899	570.3	24.7	185.2	160 3	8	118.2	07.8
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TONNAGE PROFILE BY MONTH

DAY HOUR	JAN	FEB	MAR	APR	MAY	JUN	JUL	AUG	SEP	OCT	NOV	DEC
1	0.1	114.9	169.7	321.2	546.8	755.1	682.2	723.3	557.4	186.6	169.7	134.2
2	82.6	93.2	94.9	224.8	433.7	634.5	572.0	602.3	447.5	140.9	132.9	105.9
3	61.0	69.2	102.8	152.0	332.6	528.9	475.1	503.8	349.4	109.3	102.2	87.9
4	42.4	48.8	84.0	104.9	241.8	439.7	394.9	417.3	262.8	85.0	84.3	60.9
5	27.6	32.9	71.7	72.1	170.1	361.2	325.5	343.5	197.0	71.3	74.4	41.1
6	22.8	29.1	55.4	54.9	114.1	294.6	265.7	281.2	137.7	63.3	62.5	30.5
7	18.0	27.6	37.7	84.1	193.9	488.2	470.8	438.8	218.2	55.3	42.7	27.4
8	200.6	223.8	295.7	653.1	1053.8	1594.7	1643.6	1536.2	1129.9	340.8	293.2	241.7
9	420.1	438.0	855.2	1409.3	1841.2	2640.7	2760.4	2582.6	2037.7	1054.2	849.1	573.5
10	796.7	791.9	1204.1	1831.2	2200.2	3074.2	3195.8	2951.5	2465.2	1444.9	1222.0	1061.6
11	1130.7	1067.1	1540.5	2204.4	2523.8	3384.8	3494.4	3242.5	2807.6	1890.3	1510.6	1280.4
12	1330.0	1206.6	1833.4	2464.5	2821.7	3692.5	3853.1	3606.6	3126.6	2279.6	1829.2	1620.1
13	1570.6	1433.7	2146.4	2720.4	3139.7	3945.6	4100.7	3943.5	3407.4	2537.2	2156.0	1888.8
14	1732.9	1631.3	2385.4	2981.6	3455.5	4234.8	4261.6	4165.8	3725.5	2709.0	2142.9	2176.7
15	1955.9	1782.3	2492.8	3147.5	3633.2	4426.3	4345.9	4349.1	3887.3	2853.2	2572.4	2280.1
16	1607.9	1540.9	2094.4	2599.0	3039.6	3627.2	3593.9	3632.4	3260.5	2338.3	2169.2	1875.2
17	1574.4	1528.9	2105.2	2392.5	3043.2	2657.2	3553.3	3552.4	3241.1	2280.4	2118.7	1814.8
18	1306.6	1308.8	1838.7	2316.7	2784.6	3336.6	3227.1	3287.1	2945.7	1689.2	1803.8	1509.3
19	762.7	761.3	1553.2	1536.4	1879.3	2247.1	2151.4	2095.9	1925.6	1269.1	1135.4	903.3
20	624.4	619.4	999.7	1339.1	2537.0	1961.4	1909.2	1895.2	1747.0	1102.0	990.3	756.4
21	550.1	548.6	857.6	117.8	1508.8	1783.9	1690.7	1739.1	2338.4	929.2	843.8	636.0
22	509.4	510.5	735.0	1038.7	1357.9	1638.6	1539.3	1595.0	1386.7	790.3	722.5	563.8
23	417.0	467.8	599.2	880.9	1186.7	1480.5	1359.5	1433.0	1218.2	647.4	595.4	501.1
24	423.5	437.3	519.5	746.7	1018.9	1264.4	1180.1	1229.7	1040.3	565.4	516.9	474.7

Table 2A

BUILDING 25910 PLANT COOLING SUMMARY **HOURS PER** CAPACITY % PLANT BIN HOURS REPDAY CAPACITY LIMIT-TONS **PERBIN** TONS 2216 6.07 10 450 4500 20 4.40 900 1605 2.34 30 1350 853 1092 2.99 1800 40 2250 916 2.51 50 60 2700 610 1.67 3150 428 1.17 70 1.34 489 80 3600 336 0.92 4050 90 4500 215 0.59 100

Table 3A

ROWLAND
01!Fort Gordon
P1CARLTON SHUFORD
P2DSN 780-6376
P3ATZH-DIC-E
/RECALL F 000045553 S 03

ECIP PROJECT 1: UPGRADE CHILLER PLANT BUILDING 25910 - FORT GORDON

03A !DESCRIPTION OF PROPOSED CONSTRUCTION

***Upgrade chillers, accessories and the chilled water distribution system at the Central Utility Plant, North side of the Ft. Gordon Installation. Several innovative modifications to the central chilled water system are required to meet current and future cooling requirements for all building on the northern half of the facility. Replacement of obsolete equipment with new high efficiency systems will reduce energy requirements significantly while increasing the net cooling capacity for the barracks, classrooms and administrative buildings.

03B !REMARKS

ECO NO.

***This Energy conservation measure to replace the existing chilled water system consists of ten ECO's, which were combined to create one comprehensive ECIP. Each ECO was developed from field studies of the North Side Central Utility Plant. The economics of incorporating all ten ECO's is explained in the economic justification section of this document. The ten ECO's are described below to provide extra insight into the comprehensive approach taken.

6	Chilled water chemical treatment to prolong chillers life.
23	New variable speed chilled water pumping system.
29	Addition of control to permit chilled water temperature adjustment.
33	Reduce make-up water for the chilled water system.
43	Common manifolding of cooling tower water system.
47	Cooling Tower Water treatment automation/instrumentation.
51	Add free cooling capability to chilled water system.
53	Chilled water storage system
85	Replace five inefficient Chillers with three new units.
86	Install instrumentation for Energy Management System

DESCRIPTION

ECO DATA COMPILATION

ECO NO.	DESCRIPTION	COST (FROM LCC)	SAVINGS 1ST YEAR	TOTAL DISCOUNT SAVINGS
6	Chem Treatment-CHW	15,510	27,500	571,040
23	Variable Speed CHW Pumping	440,096	82,278	1,332,935
29	Temp Reset	31,190	6,881	107,418
33	Reduce Make-Up Water	37,427	7,483	112,453
43	Cooling Tower Manifolding	145,154	6,834	111,515
47	Cooling Tower Water Treatment	1,968	8,522	132,125
51	Free Cooling	100,100	40,461	631,596
53	CHW Storage	660,214	179,970	2,652,763
85	Replace Chillers	1,086,972	122,127	1,904,660
86	EMCS Controls & Instrum.	68,456	16,427	256,423
	Totals	2,587,087	501,483	7,812,928

Simple Payback: 2,587,087 = 5.16

501,483

SIR: 7.812.928 = 3.02

2,587,087

03C !PROJECT DESCRIPTION

***This Energy conservation measure provides the plan to design the required upgrade to the Central Utility Plant, North. Removal and replacement of five inefficient chillers with three new ones properly sized to provide incremental increase in the chilled water capacity as the site load varies. The five old chillers being replaced include 3-700 ton units and 2-750 ton units for a combined capacity of 3,600 tons. The three new chillers have capacity of 1-400 ton chiller and 2-1,250 ton chillers for a combined total of 2,900 tons. The new units are sized to match the load change throughout the day, and have the capacity to replenish the chilled water storage system at night. The chilled water storage system will provide the capacity to make up the difference between the older units 3,600 tons and the capacity of the newer unit of 2,900 tons, or 700 tons. Since the peak demand for chilled water occurs over a short t period of time, the chilled water storage system will provide a capacity to meet a peak demand of 4,400 tons of refrigeration. This exceeds current demand by 800 tons and allows for less chiller capacity to meet current and future needs. Repiping of both the chilled water system and condenser water system will provide flexibility in selecting equipment to run. Current piping makes manual selection of equipment difficult and requires excessive manpower to change over as site loads vary. Consequently, it is easier for chilled water to run through all chillers than to try to control valves and pumps to meet load requirements. In addition to providing a new efficient piping design that is easy to operate, variable speed pumps will be introduced to further allow for energy efficient operation under all load conditions. With the addition of instrumentation and control, all chilled water control functions could be handled from a central location reducing the need for plant operators by fifty percent.

03D !REQUIREMENT (Why is it needed now)

****The chilled water system is not meeting current cooling requirements for the buildings served on the north side of the facility. New construction and renovations will increase the capacity on this system to meet current and future requirements. New CFC regulations for chiller refrigerants will require replacement of older chillers, and require system redesign of chilled water distribution by 1997.

If not implemented now, cooling capacity will not meet current or future needs.

03E !CURRENT SITUATION (How is the need currently being met)

***ECO 6

Existing chemical treatment systems serves the condenser side of the chilled water system and are feeding a C-6220 chemical from Industrial Maintenance Corporation into the condenser water system and also adding an A-102 microbiocide by the bucket as the algae begins to build up in the cooling towers. There is no chemical feed on the chilled water side of the system. There is a large volume of make-up water to the chilled water side, which is taken off the fire hose, and is not treated at this time. There isn't any way to treat the make-up water to the chilled water system with the present equipment.

ECO 23

There are two zones and each zone is served by a set of identical pumps, one backing up the other. Existing pumps all have single speed motors. Buildings on the distribution system, in most cases, have pumps to override the increased pressure drop through the building. 3- way valves are at all of the air handling units and fan coil units in the building.

ECO 29

Although the chillers are set to maintain a constant chilled water supply temperature, some water is bypassed through non-operating chillers and the temperature actually varies. The system is set to operate at a constant supply water temperature of approximately 42°F. Actual supply water temperature was measured at 47°F as a result of return water being bypassed through chillers that are not being operated.

ECO 33

There are water meters on the chilled water Zones 1 and 2 to measure the make-up water. In addition to the metered make-up water, there is a fire hose connected, which is unmetered, that supplies water to the chilled water system to maintain a certain supply pressure through the chillers to the various zones. From tests run shutting off pumps, turning valves, and measuring make-up water flow to Zones 1 and 2 chilled water, the leaks are determined to most likely be in the distribution system. Based on HTW meter readings, the leakage rates vary over the course of the year as leaks are found, repaired and developed again. Accurate determination of the make-up water is not possible because the fire hose is connected into the chilled water system, which is unmetered. During field observations it was noted that 29 gpm was expected with flows separately measured from each zone with zones not cross-connected. When they were cross-connected, the flow averaged 12 gpm. Total loss measured for 24 hour period with a 1-1/4 inch branch closed between the make-up water systems was 16,634 gallons, which was less than what was recorded for previous days on the log with the 1-1/4 inch branch open.

ECO 43

Chillers 1, 2, 3, 4A, and 4B have dedicated cooling towers and although the towers are similarly sized for 700 and 750 ton chillers, there is no means of using an alternate cooling tower with a desired chiller. Chillers 5, 6, and 7 are centrifugal chillers that replaced two absorption chillers. The cooling towers were not replaced so that two cooling towers are cross-connected for use with three centrifugal chillers. It is not possible to maintain a fixed condenser water flow for three chillers with two cooling towers. The fact that the chilled water flow is only constant through all chillers if the same pumps are "On", no chillers are valved "Off", and the pressure drop through the chilled water distribution systems remain constant does not make a fixed condensate water flow any more likely.

ECO 47

There is currently water treatment based on a conductivity meter of the cooling tower water, but biocide is added manually by the scoopful only as needed. There is no water treatment for the chilled water loop and this will cause deterioration of the entire chilled water system.

ECO₅₁

All of the chillers in Building 25910 are either Carrier or York and are not internally convertible to free cooling unless a heat exchanger is added externally.

ECO 53

As the chilled water system requires chilling, the only way to satisfy this now is for the chillers to operate. A chilled water storage system would enable optimization of chiller operation.

ECO 85

See Figure 1A for the existing chilled water schematic for Building 25910. Chillers 1, 2, and 3 are the oldest; chillers 4A and 4B are next in age and next to lowest in efficiency; chillers 5, 6, and 7 were recently added to the Plant to be replaced in lieu of the absorption chillers which have been removed and are the most efficient. Chillers 1, 2, 3, 5, 6, and 7 are 700 ton capacity; chillers 4A and 4B are both 750 ton capacity.

ECO 86

Existing plant controls that are automatic or manual within the plant are not operable remotely by the EMCS by design. EMCS office which is manned 24 hours a day has very few, if any, instrumentation readouts from the plant, and no controllability of the plant with the EMCS. Because EMCS personnel are aware of what is happening in many buildings, they are also aware of what is happening in the chilled water system pertaining to conditions and demands. Currently, the boiler operators are making boiler pressure changes, HTW changes, bringing on and off chillers, cooling towers, and many manual valving operations. However, they are not performing the functions that an EMCS office can to control energy and to improve the operating efficiency of the plant.

03F !IMPACT IF NOT PROVIDED

***If this project is not accomplished, Fort Gordon will continue to use excessive energy to supply chilled

water to the buildings on the north side of the facility. Because of old inefficient chillers and a distribution system that does not respond to reduced load conditions, all equipment must run all the time to provide adequate cooling. The existing system requires high electrical consumption at all times and high demand for electricity during the entire cooling season.

03G !ADDITIONAL

***New construction and renovation projects on the base will increase demand on the chilled water distribution system to respond to new loading conditions. The old chillers use CFC refrigerant which require changes to the old chillers that are cost prohibitive.

03I !RELATED PROJECTS

***ECIP - 45554 - Chilled Water System to Central Utility Plant - Building 25330 South Side

ECIP - 45555 - High Temperature Water Systems North Plant - Building 25910

ECIP - 45556 - High Temperature Water System South Plant - Building 25330

07A !GENERAL JUSTIFICATION DATA

***This ECIP project is required to support the Army wide effort to reduce energy consumption. The project will provide new chillers and variable speed pumps in addition to renovations to the existing piping layout, which will permit better control of the plant. New instrumentation will allow connection to the existing EMCS system.

The project has been coordinated with the installation physical security plan and no security improvements are required.

The project includes ten ECO's combined to provide a comprehensive upgrade to the facility chilled water system. The following justification overview lists the ECO's along with the economic justification.

PROJECT NO. 1 - CHILLED WATER NORTH

TOTAL DISCOUNT SAVINGS

571,040 1,332,935 107,418 112,453 111,515 132,125 631,596 2,652,763 1,904,660 256,423

7,812,928

27,500 85,278 6,881	7,483 6,834	8,522 40,461 179,970	122,127	501,483
000	00	0 0 179,970	0 0	179,970
0 5,728.48 451.655	162.015 376.38	376.38 2,655.64 0	7,884.48	18,713.20
15,510 440,096 31,190	37,427 145,154	1,968 100,100 660,214	1,086,972	2,587,087
630,000	22,000	5,760 0 0	000	657,760
4,000 -2,000	5,015 0	2,500 0	2,000	3,515
13,910.40 394,703.82	33,566.40 130,183.20	1,765.26 89,775.00 592,118.86	974,862.00 61,394.76	2,320,251.70
Chem Treatment-CHW Variable Speed CHW Pumping	Temp Reset Reduce Make-Up Water Cooling Tower Manifolding	Cooling Tower Water Treatment Free Cooling	CLIW Storage Replace Chillers EMCS Controls & Instrumentation	Totals
23	33 43 43	51	85 86	
	Chem Treatment-CHW 13,910.40 4,000 630,000 15,510 0 0 0 Variable Speed CHW Pumping 394,703.82 -2,000 0 440,096 5,728.48 0 0 31.190 451.655 0	Chem Treatment-CHW 13,910.40 -4,000 630,000 15,510 0 0 Variable Speed CHW Pumping 394,703.82 -2,000 0 440,096 5,728.48 0 Temp Reset 0 0 31,190 451.655 0 Reduce Make-Up Water 33,566.40 5,015 0 37,427 162.015 0 Cooling Tower Manifolding 130,183.20 0 22,000 145,154 376.38 0	Chem Treatment-CHW 13,910.40 -4,000 630,000 15,510 0 0 Variable Speed CHW Pumping 394,703.82 -2,000 0 440,096 5,728.48 0 Temp Reset 27,972.00 0 31,190 451.655 0 Reduce Make-Up Water 33,566.40 5,015 0 37,427 162.015 0 Cooling Tower Manifolding 130,183.20 0 22,000 145,154 376.38 0 Cooling Tower Water Treatment 1,765.26 2,500 5,760 1,968 376.38 0 Free Cooling 89,775.00 0 100,100 2,655.64 0 Free Cooling 660.214 0 179.970	Chem Treatment-CHW 13,910.40 4,000 630,000 Variable Speed CHW Pumping 394,703.82 -2,000 0 Temp Reset 27,972.00 0 0 Reduce Make-Up Water 33,566.40 5,015 0 Cooling Tower Manifolding 130,183.20 0 22,000 Cooling Tower Water Treatment 1,765.26 2,500 5,760 Free Cooling 89,775.00 0 0 CHW Storage 592,118.86 0 0 Replace Chillers 974,862.00 2,000 0 EMCS Controls & Instrumentation 61,394.76 0 0

NOTE: See section 7C for detailed cost breakdown.

 $\frac{7.812.928}{2,587,087} = 3.02$

SIR:

Simple Payback:

 $\frac{2.587,087}{501,483} = 5.16$

07B !TRAFFIC ANALYSIS

*** There will be no changes to pedestrian or vehicular traffic as a result of implementing this ECIP.
/*

08B | PRESENT ACCOMMODATIONS AND DISPOSITION

***The physical plant building 25910 housing the chilled water system is adequate to accommodate the new chillers, once the old chillers are removed. The chilled water storage tank will be located outside in a vacant field adjacent to the cooling towers.

09D !RPMA DISCUSSION

***This ECIP will reduce the amount of Real Property Maintenance Required.
/*

10A !ANALYSIS OF DEFICIENCIES

***1) Treatment of makeup water is not being performed on the CHW system. This will shorten the Life of each chiller as well as the pumping and piping systems by 4 years for a total savings of \$630,000.

2) Existing constant speed pumping systems do not meet the needs of dynamic changes to the site A/C loads. The pumps generally are set to run continuously to be certain that capcity is available when needed. A variable speed pumping system designed to meet the dynamic conditions prevailing at the facility will save \$107,418.00 annually.

3) The chilled water system is currently run manually. There is little instrumentation and none of the equipment is connected to the existing on site energy management control system(EMCS). The process of operating the plant is labor intensive and susceptable to inefficient operation. By connecting the central plant to the EMCS sustem an annual savings of \$107,418 will be achieved.

4) Excessive makeup water for the chilled water loop is required because of the existing piping design. Changes to the piping system will reduce the excess, conserve water reduce water treatment requirements and simplify the

plant operation. Annual savings of \$73,921 was calculated

5) The cooling tower condenser water pipe installation dedicates each cooling tower to a specific chiller. By manifolding the condenser water system at the towers, advantage can be taken of selecting the combination of chiller and cooling tower that fits current load conditions will save \$ 36,800 annually. This condition will also be advantageous for the free cooling cycle.

7) The chilled water and condenser water systems are not capable of free cooling operation. Changes to the piping system and the addition of an appropriate heat exchanger will make free cooling possible, thus reducing the requirements for running chillers during off peak season conditions (fall, winter, spring). An annual savings of

\$40,461 will be realized.

8) The existing chilled water system meets peak demand conditions with all chillers running near their maximum capacity. This produces peak electrical demand conditions. To reduce the demand conditions, a chilled water storage system will be installed to retain chilled water to be used instead of a chiller during peak demand conditions. An annual savings of \$179,970 due to reduce demand charges will be achieved.

9) Four of the eight chillers are at the end of their usefull life. Due to the increasing requirementss for chilled water at facility, the four older chillers will be replace with three new hi efficiency chillers. This will result in an annual

savings of \$ 122,127.00.

10) The central plant currently is not equipped with sensors or controls to allow interfacing to the existing Energy management and control system. Connection to the EMCS is required because there is a need to coordinate the operation of the chilled water system with the requirements being monitored by the EMCS. Reducing equipment run time and setpoint control will save \$ 16427.00 annually.

11D !DECISION ANALYSIS

***The decision analysis was based on grouping the following ECO's together because of their interrelationships to each other. The benefit of each of the ECO's however was determined separately and no attempt was made to determine any additional benefit when all were combined as a whole. The savings and ROI therefore are conservative figures and additional savings can be anticipated by the cumulative affect.

			1st Yr	Payback		
ECO#	Descrition	Cost	Savings	Years	SIR	AIRR
6	CHW Chem Trt.	15,410	27,500	.56	36.82	
23	VAR Sp Pmps	440,096	85,278	5.16	3.03	8.97
29	Temp Reset	31,190	6,881	4.53	3.44	9.68
33	Make-up H2O	37427	7,483	5.00	3.00	8.93
43	Tower repipe	145,154	6,834	21.24	.77	1.75
47	CW chem trt	1,968	2,788	.71	21.65	
51	Free Cooling	100,100	40,461	2.47	6.31	13.05
53	CHW Storage	660,214	179,970	3.67	4.02	10.52
85	New Chillers	1,086,972	122,127	8.9	1.75	6.03
86	EMCS control	68,456	16,427	4.17	3.75	10.14
то	DTAL	2,587,087	495,749	5.22	2.98	•

^{***}The following is a detailed cost breakdown of each of the ECO's. Refer to the table in 7A General Justification Data which summarizes these costs.

ECO 6 - LCCA

1.	Investi	ment	
	A.	Construction Cost	\$ 13,910.00
	B.	SIOH	\$ 765.00
	C.	Design Cost	\$ 835.00
	D.	Total Cost $(1A + 1B + 1C)$	\$ 15,510.00
2.	Energy	y Savings	\$ -5,994.00
3.		nergy Savings	\$ 571,040.00
4.		Year Dollar Savings	\$ 27,500.00
5.		e Payback Period	\$.56 Years
6.		Net Discounted Savings	\$ 571,040.00
7.		gs to Investment Ratio	\$ 36.82

ECO 23 - LCCA

1.	Investment		
	A. Construction Cost	\$	394,704.00
	B. SIOH	\$	21,709.00
	C. Design Cost	\$	23,683.00
	D. Total Cost $(1A + 1B + 1C)$	\$	440,096.00
2.	Energy Savings	\$	-266.00
3.	Non Energy Savings	\$	-29,480.00
4.	First Year Dollar Savings	\$	85,278.00
5.	Simple Payback Period	\$	5.16 Years
6.	Total Net Discounted Savings	\$	1,332,935.00
7.	Savings to Investment Ratio	\$	3.03
ECO	29 - LCCA		
1.	Investment		
	A. Construction Cost	\$	27,972.00
	B. SIOH	\$ \$ \$ \$	1,539.00
	C. Design Cost	\$	1,679.00
	D. Total Cost $(1A + 1B + 1C)$	\$	31,190.00
2.	Energy Savings	\$	-5,542.00
3.	Non Energy Savings	\$	0.00
4.	First Year Dollar Savings	\$ \$ \$	6,881.00
5.	Simple Payback Period	\$	4.53 Years
6.	Total Net Discounted Savings		107,418.00
7.	Savings to Investment Ratio	\$	3.44
ECO	33 - LCCA		
1.	Investment	c	22.566.00
	A. Construction Cost	\$	33,566.00
	B. SIOH	\$ \$ \$	1,847.00
	C. Design Cost	3	2,014.00
	D. Total Cost $(1A + 1B + 1C)$		37,427.00
2.	Energy Savings	\$	-4,833.00
3.	Non Energy Savings	\$	73,921.00
4.	First Year Dollar Savings	\$	7,483.00
5.	Simple Payback Period	\$ \$	5.00 Years
6.	Total Net Discounted Savings	\$	112,453.00
7.	Savings to Investment Ratio	\$	3.00

ECO 43 - LCCA

1. 2. 3. 4. 5. 6. 7.	Investment A. Construction Cost B. SIOH C. Design Cost D. Total Cost (1A + 1B + 1C) Energy Savings Non Energy Savings First Year Dollar Savings Simple Payback Period Total Net Discounted Savings Savings to Investment Ratio	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$	130,183.00 7,160.00 7,811.00 145,145.00 -5,618.00 22,000.00 6,834.00 21.24 Years 111,515.00 .77
ECO	47 - LCCA		
1. 2. 3. 4. 5. 6. 7.	Investment A. Construction Cost B. SIOH C. Design Cost D. Total Cost (1A + 1B + 1C) Energy Savings Non Energy Savings First Year Dollar Savings Simple Payback Period Total Net Discounted Savings Savings to Investment Ratio	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	1,765.00 97.00 106.00 1,968.00 -5,994.00 42,610.00 2,788.00 .71 Years 42,610.00 21.65
1. 2. 3. 4. 5. 6. 7.	Investment A. Construction Cost B. SIOH C. Design Cost D. Total Cost (1A + 1B + 1C) Energy Savings Non Energy Savings First Year Dollar Savings Simple Payback Period Total Net Discounted Savings Savings to Investment Ratio	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	89,775.00 4,938.00 5,387.00 100,100.00 -3,338.00 0.00 40,461.00 2.47 Years 631,596.00 6.31

ECO 53 - LCCA

1. 2. 3. 4. 5. 6. 7.	Investment A. Construction Cost B. SIOH C. Design Cost D. Total Cost (1A + 1B + 1C) Energy Savings Non Energy Savings First Year Dollar Savings Simple Payback Period Total Net Discounted Savings Savings to Investment Ratio	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	592,119.00 32,567.00 35,528.00 660,214.00 -5,994.00 0.00 179,970.00 3.67 Years 2,652,763.00 4.02
ECO	85 - LCCA		
1. 2. 3. 4. 5. 6. 7.	Investment A. Construction Cost B. SIOH C. Design Cost D. Total Cost (1A + 1B + 1C) Energy Savings Non Energy Savings First Year Dollar Savings Simple Payback Period Total Net Discounted Savings Savings to Investment Ratio	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	974,862.00 53,618.00 58,492.00 1,086,972.00 1,890.00 29,480.00 122,127.00 8.90 Years 1,904,660.00 1.75
2. 3. 4. 5. 6. 7.	Investment A. Construction Cost B. SIOH C. Design Cost D. Total Cost (1A + 1B + 1C) Energy Savings Non Energy Savings First Year Dollar Savings Simple Payback Period Total Net Discounted Savings Savings to Investment Ratio	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$	61,395.00 3,377.00 3,684.00 68,456.00 -3,917.00 0.00 16,427.00 4.17 Years 256,423.00 3.75

11E !ECONOMIC ANALYSIS ***ECO 6

ITEM DESCRIPTION	QUAN' QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Chemical Feed System Test Coupon	1	LS LS	3,500 2,000	3,500 2,000	2,500 2,000	2,500 2,000	\$6,000.00 \$4,000.00
				SI 20% OH (G SUBTOTAL G	UBTOTAL GC ONLY) C'S WORK		\$11,040.00 \$2,208.00 \$13,248.00
				SUBTOTAL (GO 5% CONT	C & SUBS) INGENCY TOTAL		\$13,248.00 \$662.40 \$13910.40
ECO 23							
ITEM DESCRIPTION	QUAN QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Secondary Pumps Piping Controls & Instrumentation Variable Speed Drive (200HP) Switches for 200HP Drive Piping Changes in Bldgs (96) Controls & Instr. in Plant Electrical Work Variable Speed Drive (300HP) Switches for 300HP Drive	2 1 1 1	EA LS LS EA LS LS LS EA	8,000 10,000 36,000 17,500 4,340 28,000 5,000 2,000 28,400 4,340	20% OH (SUBTOTAL G SUBTOTAL (G		20,000 30,000 1,000 3,000 19,200 2,000 10,000 1,000 3,000	\$54,000.00 \$30,000.00 \$66,000.00 \$18,500.00 \$11,680.00 \$47,200.00 \$7,000.00 \$12,000.00 \$29,400.00 \$11,680.00 \$313,257.00 \$62,651.40 \$375,908.40 \$18,795.42 \$394,703.82
ECO 29							
ITEM DESCRIPTION	QUAN QUAN	TITY UNIT	MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Controls	1	LS	10,000	10,000	10,000	10,000	\$20,000.00
					SUBTOTAL GC ONLY) GC'S WORK		\$22,200.00 \$4,440.00 \$26,640.00
				SUBTOTAL (G 5% CONT	C & SUBS) TINGENCY TOTAL		\$26,640.00 \$1,332.00 \$27,972.00

ECO 33

ITEM DESCRIPTION	QUAN QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Flow Meters Temp RTD in Distribution Pip	9 e 6	LS EA	1,500 500	9,000 3,000	1,000 1,000	6,000 6,000	\$15,000.00 \$9,000.00
					UBTOTAL GC ONLY) C'S WORK		\$26,640.00 \$5,328.00 \$31,968.00
				SUBTOTAL (GO 5% CONT	C & SUBS) INGENCY TOTAL		\$31,968.00 \$1,598.40 \$33,566.40
ECO 43							
ITEM DESCRIPTION	QUAN' QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Piping Materials Condenser Water Pumps Electrical	1 6 1	LS EA LS	30,000 4,000 1,500	30,000 24,000 1,500	30,000 1,000 2,500		\$60,000.00 \$30,000.00 \$4,000.00
					UBTOTAL GC ONLY) C'S WORK		103,320.00 \$20,664.00 123,984.00
				SUBTOTAL (G 5% CONT	C & SUBS) TNGENCY TOTAL		\$123,984.00 \$6,199.20 \$130,183.20
ECO 47							
ITEM DESCRIPTION	QUAN' QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Chemical Feed	1	LS	1,000	1,000	300	300	\$1,300.00
					UBTOTAL GC ONLY) C'S WORK		\$1,401.00 \$280.20 \$1,681.20
				SUBTOTAL (G 5% CONT	C & SUBS) TINGENCY TOTAL		\$1,681.20 \$84.06 \$1,765.26

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ITEM	QUANT		MATERIAL	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
DESCRIPTION	QUAN	UNII	UNIT COST	EXTENSION	OMI COSI	Littlitoron	TOTAL
Modify Cooling Tower w/ Heat Exchange	1	LS	40,000	40,000	25,000	25,000	\$65,000.00
				5% SA 17% LA SUI 20% GC OH			\$65,000.00 \$2,000.00 \$4,250.00 \$71,250.00 \$14,250.00
				SUBTOTAL	GC WORK		\$85,500.00
				5% CONT	INGENCY TOTAL		\$4,275.00 \$89,775.00
ECO 53							
ITEM DESCRIPTION	QUAN' QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Install Underground Chilled Water Tank	1	LS	400,000	400,000	42,650	42,650	\$442,650.00
				5% S 17% L			\$442,650.00 \$20,000.00 \$7,250.50 \$469,950.50 \$93,980.10 \$563,880.60
				5% CON	TINGENCY TOTAL		\$28,194.03 \$592,074.63
ECO 85							
ITEM DESCRIPTION	QUAN QUAN	TITY UNIT	MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSIO1	N TOTAL
New 400 Ton Chiller Installat New 1250 Ton Chiller	tion 1	LS	110,000 280,000	110,000 560,000	20,000 20,000	20,000 40,000	\$130,000.00 \$600,000.00
				5% S 17% L SU 20% GC OF SUBTOTAL	JBTOTAL 1 SALES TAX ABOR TAX JBTOTAL 2 H & PROFIT , GC WORK TINGENCY TOTAL		\$730,000.00 \$33,500.00 \$10,200.00 \$773,700.00 \$154,740.00 \$928,440.00 \$46,422.00 \$974,862.00

ECO 86

ITEM	QUAN QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
DESCRIPTION	QUAIN	ONL	OMIT COST	EXILIBION	01111 0001	E2t1B1\0101\	10111
Chiller Efficiency Software	1	LS			10,000	10,000	\$10,000.00
Distribution System Flow Meter	s 1	LS	3,000	3,000	2,000	2,000	\$5,000.00
Distribution System Flow Meter		LS	3,000	3,000	2,000	2,000	\$5,000.00
Operate. Controls-Chillers, Valv		LS	3,500	3,500	700	700	\$4,200.00
Temps-CHW, Cond Water	1	LS	200	200	1,000	1,000	\$1,200.00
Free Cooling Valve Indicators	1	LS	400	400	400	400	\$800.00
Flow Switches-CHW Storage	1	LS	5,200	5,200	800	800	\$6,000.00
Chillers Amps	1	LS	2,000	2,000	800	800	\$2,800.00
Pressures-CHW, RET, Supply							
and Storage	1	LS	900	900	900	900	\$1,800.00
Variable Speed & Switch Contr	ol 1	LS	1,000	1,000	1,500	1,500	\$2,500.00
Chiller Pump Controls	1	LS	1,000	1,000	1,500	1,500	\$2,500.00
Condenser Pump Controls	1	LS	800	800	1,200	1,200	\$2,000.00
				SU	BTOTAL 1		\$43,800.00
					ALES TAX		\$1,050.00
					ABOR TAX		\$3,876.00
					BTOTAL 2		\$48,726.00
	20% GC OH & PROFIT				\$9,745.20		
				SUBTOTAL			\$58,471.20
				5% CONT	INGENCY		\$2,923.56
				3,7000113	TOTAL		\$61,394.76

12A !CRITERIA FOR PROPOSED CONSTRUCTION

***Construction will conform to existing guidelines of architectural design and building construction, specifically the AEI Design Guide (March 1987), the Corps of Engineers Guide Specifications CEGS 13947 thru 13949 for EMCS, and TM 5-812-2.

13B !FURNISHINGS AND EQUIPMENT DISCUSSION

- ***1) Four chillers will be replaced with three new chillers.
- 2) Two variable speed pumps will be added to serve the primary chilled water loop.
- 3) Rerouting of existing pipes will permit more efficient operation and utilization of new and existing equipment.
- 4) New sensors and controls will be installed to automate the chilled water system functions.

14B !SURVIVAL MEASURES

This project will upgrade the existing chilled water system and is not suitable for inclusion as a protective shelter.

15A !ENVIRONMENTAL DOCUMENTATION

***The refrigerant in four old chillers will need to be reclaimed. Permits will be required. The refrigerants have market value and can be disposed of by selling at current market value. There are no other environmental issues.

15B1 !SUMMARY OF ENVIRONMENTAL CONSEQUENCES

***We have reviewed this project and determined that an environemental impact staement, pursuant to PL 91-190, is not required. We have assessed this project and determined that it will not contribute significantly to air and/or water pollution.

16A1 'EVALUATION OF FLOOD HAZARDS

***The renovation is to an existing plant. No history of flooding has been recorded.

19A !SUMMARY OF ENERGY REQUIREMENTS

***The existing electric utility system in adequate to support the modifications, upgrades and new equipment recommendations. No changes will be required to meet the requirements and modifications. Peak load requirements will actually be reduced. Equipment operation will reflect the changing load requirements throughout the day allowing chillers and pumps to be scheduled more efficiently, thus reducing electric consumption and demand.

The engineering study reports electric consumption reduction to be 15,586,741 KWH and a demand reduction of 2,981.78 from first order effects to reducing equipment use, and chilled water storage. A total discounted savings of \$7,723,413 will be realized.

19B !SUMMARY OF UTILITY SUPPORT

***The central utility plant connected load will be reduced by 15%. The existing electric utilities supplied to the central plant is adequate and will not require additional capacity to be added.

20B !HAZARDS TO HANDICAPPED PERSONS

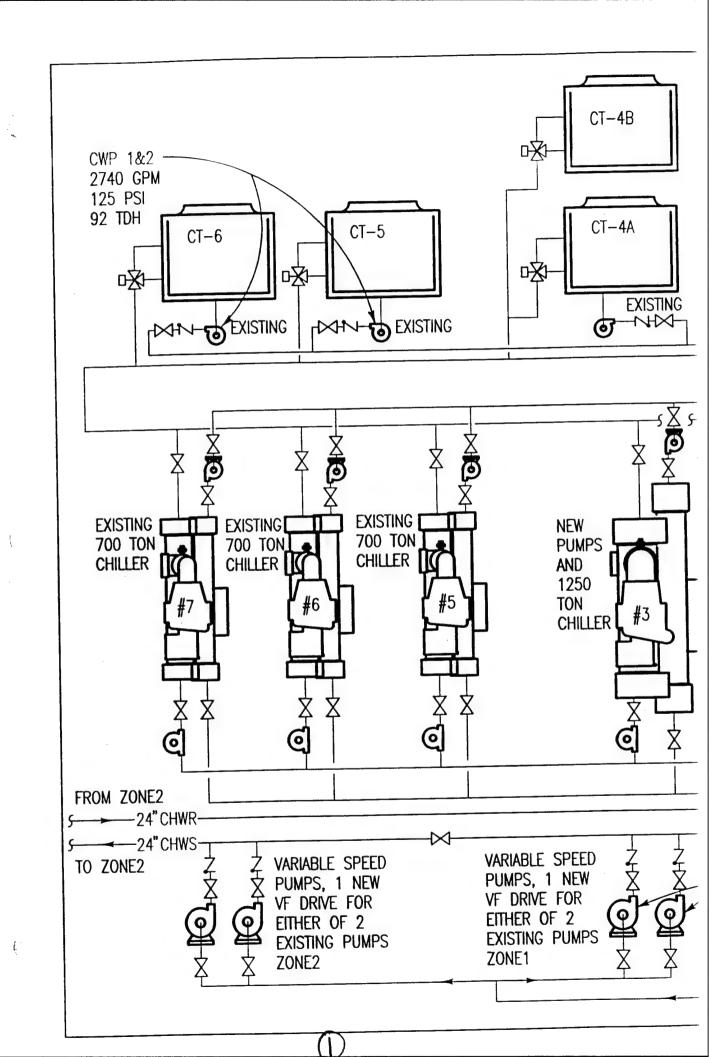
***Existing conditions within the physical plant is considered hazardous to unauthorized personnel. Signs and warnings are posted to alert unauthorized personnel access is restricted to authorized personnel and visitors with prior approval.

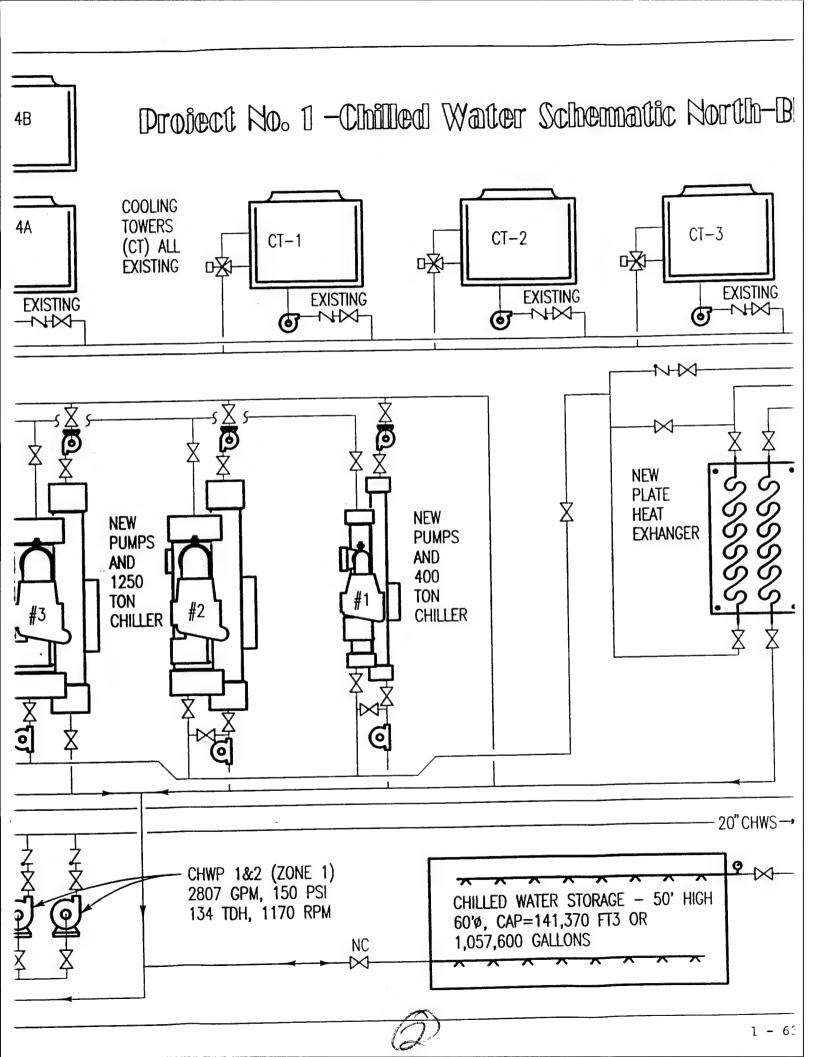
20C !HANDICAP PROVISIONS

***In accordance with Public Law 90-480, no provisions for the handicapped will be made in the project since the facility is used and operated solely by able bodied personnel. However, the main floor of the facility is at ground level and is handicap accessible.

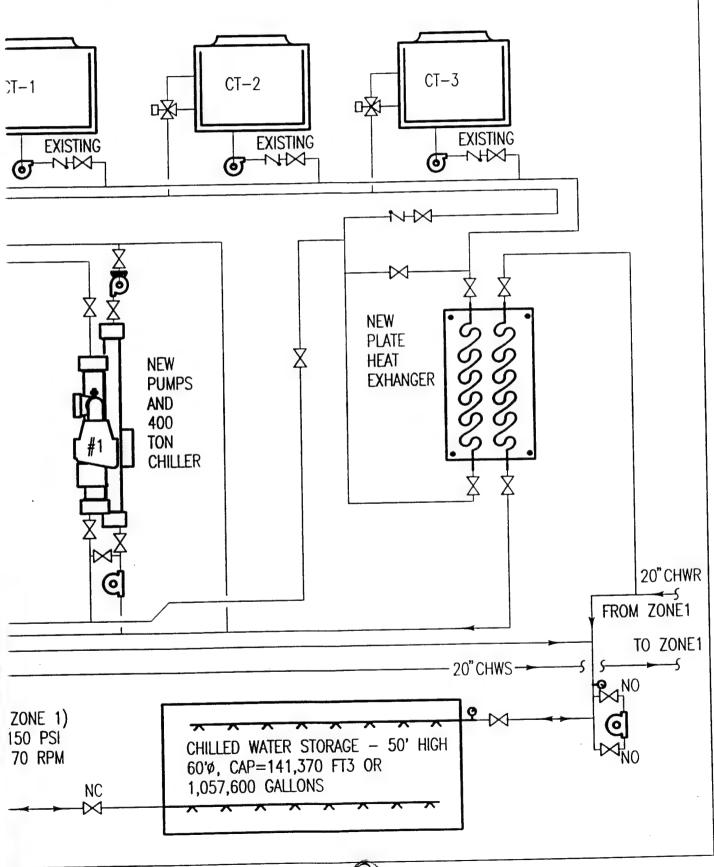
22B !PHYSICAL SECURITY

***Project is not considered for commercial activity. The physical plant upgrade to the existing Central Utility Plant will serve the north side of Ft. Gordon. Provisions of DA circular 235-1 are not applicable to this project.





Do 1 - Chilled Water Schematic North-Bldg. 25910



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ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080 INSTALLATION & LOCATION: FT. GORDON, AUREGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: ECO006 BOILER/CHILLER ENERGY STUDY FISCAL YEAR 1994 DISCRETE PORTION NAME: CHW CHEMICAL TREATMENT ANALYSIS DATE: 09-08-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 13910. \$ 765. B. SIOH C. DESIGN COST \$
D. TOTAL COST (1A+1B+1C) \$ 835. 15510. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ F. PUBLIC UTILITY COMPANY REBATE 0. 15510. G. TOTAL INVESTMENT (1D - 1E - 1F) 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 DISCOUNT DISCOUNTED UNIT COST SAVINGS ANNUAL \$ FACTOR (4) SAVINGS (5) \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FUEL 0. 0. 0. 15.61 A. ELECT \$ 15.24 0. 0. 0. 17.56 0. B. DIST \$ 8.82 0. C. RESID \$ 2.73 D. NAT G \$ 4.50 19.97 0. 20.96 0. 17.58 E. COAL \$ 1.61 0. 0. 16.12 F. LPG \$ 6.34 0. 14.74 0. M. DEMAND SAVINGS 0. 0. -5994. N. TOTAL 3. NON ENERGY SAVINGS (+) / COST(-) -4000. A. ANNUAL RECURRING (+/-) 14.74 (1) DISCOUNT FACTOR (TABLE A) -58960. (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS (+) / COSTS (-) SAVINGS (+) YR DISCNT DISCOUNTED COST(-) SAVINGS(+)/ OC FACTR (3) SAVINGS(+), COST(-)(4) ITEM (1) (2) \$9,000,000. 16 (2) 5490000. 1. CHW PIPING 16 YRS -4860000. .54 2. CHW PIPING 20 YRS \$ -9,000,000. 20 \$ 0. 630000. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 571,040. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd /(YRS ECONOMIC LIFE))\$ YEARS 5. SIMPLE PAYBACK PERIOD (1G/4) 571040. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) (SIR) = (6 / 1G) = 36.827. SAVINGS TO INVESTMENT RATIO (IF < 1 PROJECT DOES NOT QUALIFY)

STUDY: ECO006

N/A

LIFE CYCLE COST ANALYSIS SUMMARY

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8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

* Project does not qualify for ECIP funding; 4,5,6 for information only.

LIFE CYCLE COST ANALYSIS SUMMARY
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP)

STUDY: EC0023
LCCID 1.080 INSTALLATION & LOCATION: FT.GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 1 CHILLED WATER NORTH FISCAL YEAR 1994 DISCRETE PORTION NAME: VARIABLE SPEED PUMPING ANALYSIS DATE: 09-17-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 394704.

B. SIOH \$ 21709.

C. DESIGN COST \$ 23683.

D. TOTAL COST (1A+1B+1C) \$ 440096. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0.

F. PUBLIC UTILITY COMPANY REBATE \$ 0.

G. TOTAL INVESTMENT (1D - 1E - 1F) \$ 440096. 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) 0 . . 3. NON ENERGY SAVINGS(+) / COST(-) -2000. A ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) (1) DISCOUNT FACTOR (TABLE A)
(2) DISCOUNTED SAVING/COST (3A X 3A1)

\$ -29480. B. NON RECURRING SAVINGS (+) / COSTS (-) SAVINGS(+) / COSTS(-)

SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4) ITEM \$ 0. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ -29480. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 85278. 5.16 YEARS 5. SIMPLE PAYBACK PERIOD (1G/4) \$ 1332935. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 3.03 (IF < 1 PROJECT DOES NOT QUALIFY) 8.97 % 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

LIFE CYCLE COST ANALYSIS SUMMARY STUDY: EC0029
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080 INSTALLATION & LOCATION: FORT GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: BOILER/CHILLER ENERGY STUDY FISCAL YEAR 1994 DISCRETE PORTION NAME: CONTROLS ANALYSIS DATE: 06-15-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 27972.

B. SIOH \$ 1539.

C. DESIGN COST \$ 1679.

D. TOTAL COST (1A+1B+1C) \$ 31190. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$
F. PUBLIC UTILITY COMPANY REBATE \$ 0. 0. \$ 31190. G. TOTAL INVESTMENT (1D - 1E - 1F) 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) 3. NON ENERGY SAVINGS (+) / COST(-) A. ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) 0. (1) DISCOUNT FACTOR (TABLE A) 14.74
(2) DISCOUNTED SAVING/COST (3A X 3A1) \$ 0. B. NON RECURRING SAVINGS (+) / COSTS (-) SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4) ITEM \$ 0. 0. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 0. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 6881. 4.53 YEARS 5. SIMPLE PAYBACK PERIOD (1G/4) 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) \$ 107418. 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 3.44 (IF < 1 PROJECT DOES NOT QUALIFY) 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR): 9.68 %

LIFE CYCLE COST ANALYSIS SUMMARY
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP)

STUDY: EC0033
LCCID 1.080 INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 1 CHILLED WATER NORTH FISCAL YEAR 1994 DISCRETE PORTION NAME: MAINTENANCE ANALYSIS DATE: 09-17-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 33566. B. SIOH \$ 1847. C. DESIGN COST \$ 2014. D. TOTAL COST (1A+1B+1C) \$ 37427. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$
F. PUBLIC UTILITY COMPANY REBATE \$
G. TOTAL INVESTMENT (1D - 1E - 1F) 0. \$ 37427. 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNTED FUEL \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) A. ELECT \$ 15.24 162. \$ 2468. 15.61 \$ 38532. B. DIST \$ 8.82 0. \$ 0. 17.56 \$ 0. C. RESID \$ 2.73 0. \$ 0. 19.97 \$ 0. D. NAT G \$ 4.50 0. \$ 0. 20.96 \$ 0. E. COAL \$ 1.61 0. \$ 0. 17.58 \$ 0. F. LPG \$ 6.34 0. \$ 0. 17.58 \$ 0. M. DEMAND SAVINGS N. TOTAL -4833. \$ 2468. \$ 38532. 3. NON ENERGY SAVINGS(+) / COST(-) 14.74 5015. (1) DISCOUNT FACTOR (TABLE A) A. ANNUAL RECURRING (+/-) \$ 73921. (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS(+) / COSTS(-) SAVINGS(+) / COSTS(-)

SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4) ITEM \$ 0. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 73921. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 7483. 5.00 YEARS 5. SIMPLE PAYBACK PERIOD (1G/4) \$ 112453. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 3.00 (IF < 1 PROJECT DOES NOT QUALIFY) 8.93 % 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 1 CHILLED WATER NORTH FISCAL YEAR 1994 DISCRETE PORTION NAME: CONDENSER PIPING ANALYSIS DATE: 09-17-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 130183.

B. SIOH \$ 7160.

C. DESIGN COST \$ 7811.

D. TOTAL COST (1A+1B+1C) \$ 145154. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0. F. PUBLIC UTILITY COMPANY REBATE \$ 0. s - 145154. G. TOTAL INVESTMENT (1D - 1E - 1F) 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) FUEL A. ELECT \$ 15.24 376. \$ 5734. 15.61 \$ 89515. B. DIST \$ 8.82 0. \$ 0. 17.56 \$ 0. C. RESID \$ 2.73 0. \$ 0. 19.97 \$ 0. D. NAT G \$ 4.50 0. \$ 0. 20.96 \$ 0. E. COAL \$ 1.61 0. \$ 0. 17.58 \$ 0. F. LPG \$ 6.34 0. \$ 0. 16.12 \$ 0. M. DEMAND SAVINGS \$ 0. 16.12 \$ 0. N. TOTAL 5618. \$ 5734. \$ 89515. E. COAL \$ 1.61 3. NON ENERGY SAVINGS(+) / COST(-) \$ 14.74 A. ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) 0. (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS (+) / COSTS (-) SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)

(1) (2) (3) COST(-)(4)

\$1100000. 19 .56 616000.

\$-1,100,000 20 .54 -594000. ITEM 1. CHILLERS 19 YRS 2. CHILLERS 20 YRS 0. 22000. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 22000. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd /(YRS ECONOMIC LIFE))\$ YEARS 5. SIMPLE PAYBACK PERIOD (1G/4) 111515. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = .77 (IF < 1 PROJECT DOES NOT QUALIFY) 1.75 % 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

LIFE CYCLE COST ANALYSIS SUMMARY
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP)

STUDY: ECO043
LCCID 1.080

LIFE CYCLE COST ANALYSIS SUMMARY STUDY: ECO047 ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080 LIFE CYCLE COST ANALYSIS SUMMARY INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 1 CHILLED WATER NORTH FISCAL YEAR 1994 DISCRETE PORTION NAME: WATER TREATMENT ANALYSIS DATE: 01-13-95 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$
B. SIOH \$
C. DESIGN COST \$ 1765. 97. 106. D. TOTAL COST (1A+1B+1C) \$ 1968. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$
F. PUBLIC UTILITY COMPANY REBATE \$ 0. 0. G. TOTAL INVESTMENT (1D - 1E - 1F) 1968. 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) FUEL A. ELECT \$ 15.24 376. \$ 5734. 15.61 \$ 89515. B. DIST \$ 8.82 0. \$ 0. 17.56 \$ 0. C. RESID \$ 2.73 0. \$ 0. 19.97 \$ 0. D. NAT G \$ 4.50 0. \$ 0. 20.96 \$ 0. E. COAL \$ 1.61 0. \$ 0. 17.58 \$ 0. F. LPG \$ 6.34 0. \$ 0. 16.12 \$ 0. M. DEMAND SAVINGS \$ 0. 16.12 \$ 0. N. TOTAL -5618. \$ 5734. \$ 89515. 3. NON ENERGY SAVINGS (+) / COST (-) 2500. A. ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) 14.74 \$ 36850. (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS (+) / COSTS (-) SAVINGS(+) YR DISCNT DISCOUNTED

ITEM COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4)

1. COOLING TOWER 20 YRS \$-144000. 20 .54 -77760.

2. COOLING TOWER 18 YRS \$ 144000. 18 .58 83520. d. TOTAL 0. 5760. C. TOTAL NON ENERGY DISCOUNTED SAVINGS (+) / COST (-) (3A2+3Bd4)\$ 42610. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd4/(YRS ECONOMIC LIFE))\$.23 YEARS 5. SIMPLE PAYBACK PERIOD (1G/4)

7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 67.13 (IF < 1 PROJECT DOES NOT QUALIFY)

6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)

8. ADJUSTED INTERNAL RATE OF RETURN (AIRR): 27.23 %

\$ 132125.

LIFE CYCLE COST ANALYSIS SUMMARY STUDY: E ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 1 CHILLED WATER NORTH FISCAL YEAR 1994 DISCRETE PORTION NAME: FREE COOLING ANALYSIS DATE: 09-17-94 ECONOMIC LIFE 20 YEARS PREPARED BY: F	3
1. INVESTMENT A. CONSTRUCTION COST \$ 89775. B. SIOH \$ 4938. C. DESIGN COST \$ 5387. D. TOTAL COST (1A+1B+1C) \$ 100100. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0. F. PUBLIC UTILITY COMPANY REBATE \$ 0. G. TOTAL INVESTMENT (1D - 1E - 1F) \$ 100100	
FUEL \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4)	DISCOUNTED SAVINGS(5)
B. DIST \$ 8.82	\$ 631596. \$ 0. \$ 0. \$ 0. \$ 0. \$ 0. \$ 0. \$ 631596.
3. NON ENERGY SAVINGS(+) / COST(-)	
A. ANNUAL-RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) (2) DISCOUNTED SAVING/COST (3A X 3A1)	\$ 0. \$ 0.
TTEM COST(-) OC FACTR SAVIN	OUNTED NGS (+) / (-) (4)
d. TOTAL- \$ 0.	0.
C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4))\$ 0.
4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 40461.
5. SIMPLE PAYBACK PERIOD (1G/4)	2.47 YEAR
6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)	\$ 631596.
7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = (1F < 1 PROJECT DOES NOT QUALIFY)	6.31
8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):	13.05 %

LIFE CYCLE COST ENERGY CONSERVATION INSTALLATION & LOCATION: PROJECT NO. & TITLE: 1 FISCAL YEAR 1994 DISC ANALYSIS DATE: 09-18-94	INVESTMENT PF FT.GORDON CHILLED WATER RETE PORTION 1	ROGRAM (REGION R NORTH NAME: CH	ECIP) NOS. W STOR	LCCID 4 CENSUS: AGE	1. 3	.080
1. INVESTMENT A. CONSTRUCTION COST B. SIOH C. DESIGN COST D. TOTAL COST (1A+1B+1C) E. SALVAGE VALUE OF EXIS F. PUBLIC UTILITY COMPAN G. TOTAL INVESTMENT (1D	TING EQUIPMEN' Y REBATE	r \$ \$	0. 0.	\$ 66021	4.	
2. ENERGY SAVINGS (+) / DATE OF NISTIR 85-3273-X UNIT COST FUEL \$/MBTU(1)	USED FOR DISC SAVINGS MBTU/YR(2)	ANNUAL SAVINGS	\$ S (3) ⁻	DISCOUNT FACTOR (4)		SCOUNTED VINGS (5)
A. ELECT \$ 15.24 B. DIST \$ 8.82 C. RESID \$ 2.73 D. NAT G \$ 4.50 E. COAL \$ 1.61 F. LPG \$ 6.34 M. DEMAND SAVINGS N. TOTAL	0. 0. 0. 0. 0.	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	0. 0. 0. 0. 0. 970.	15.61 17.56 19.97 20.96 17.58 16.12 14.74	444444444	0.
3. NON ENERGY SAVINGS(+)	/ COST(-)					
A. ANNUAL RECURRING ((1) DISCOUNT FACT (2) DISCOUNTED SA	+/-) OR (TABLE A) VING/COST (3A	. X 3A1)		14.74	\$ \$	0.
B. NON RECURRING SAVI	SAVINGS(+ COST(-)	OC (2)	FACTF	SAV.	INGS	S (+ ⁻) /
d. TOTAL	\$ 0.					0.
C. TOTAL NON ENERGY I	DISCOUNTED SAV	INGS(+)	/COST(-	-) (3A2+3Bd	1)\$	0.
4. FIRST YEAR DOLLAR SAV	/INGS 2N3+3A+((3Bd1/(Y	RS ECO	NOMIC LIFE))\$	179970.
5. SIMPLE PAYBACK PERIOR	(1G/4)					3.67 YEARS
6. TOTAL NET DISCOUNTED	SAVINGS (2N5-	-3C)			\$	2652763.
7. SAVINGS TO INVESTMENT (IF < 1 PROJECT DOE:	r RATIO S NOT QUALIFY)	(SIR)	= (6 / 3	1G) =		4:.02
8. ADJUSTED INTERNAL RA	TE OF RETURN	(AIRR):				10.52 %

ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP)

LCCID 1.080 INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 1 CHILLED WATER NORTH FISCAL YEAR 1994 DISCRETE PORTION NAME: REPLACE CHILLERS ANALYSIS DATE: 09-17-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 974862.

B. SIOH \$ 53618.

C. DESIGN COST \$ 58492.

D. TOTAL COST (1A+1B+1C) \$ 1086972. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0.
F. PUBLIC UTILITY COMPANY REBATE \$ 0. 0. G. TOTAL INVESTMENT (1D - 1E - 1F) 1086972. 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS (5) FUEL A. ELECT \$ 15.24 7884. \$ 120127. 15.61
B. DIST \$ 8.82 0. \$ 0. 17.56
C. RESID \$ 2.73 0. \$ 0. 19.97
D. NAT G \$ 4.50 0. \$ 0. 20.96
E. COAL \$ 1.61 0. \$ 0. 17.58
F. LPG \$ 6.34 0. \$ 0. 16.12
M. DEMAND SAVINGS
N. TOTAL 1890. \$ 120127. 1875180. 0. 17.56 \$ 19.97 \$ 20.96 \$ 0. 0. 0. 16.12 \$ 14.74 \$ 0 . \$ 0. \$ 1875180. 3. NON ENERGY SAVINGS(+) / COST(-) 2000. A. ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) 14.74 29480. (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS (+) / COSTS (-) SAVINGS (+) YR DISCNT DISCOUNTED

COST (-) OC FACTR SAVINGS (+) /

(1) (2) (3) COST (-) (4) COST(-) OC (1) (2) ITEM 0. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 29480. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 122127. :8.90 YEAR: 5. SIMPLE PAYBACK PERIOD (1G/4) \$ 1904660. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 1.75 (IF < 1 PROJECT DOES NOT QUALIFY) 6.03 % 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

LIFE CYCLE COST ANALYSIS SUMMARY

STUDY: ECO085

INSTALLATION & LOCATION: FT.GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 1 CHILLED WATER NORTH FISCAL YEAR 1994 DISCRETE PORTION NAME: EMCS CONTROLS ANALYSIS DATE: 09-18-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 61395.

B. SIOH \$ 3377.

C. DESIGN COST \$ 3684.

D. TOTAL COST (1A+1B+1C) \$ 68456. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$
F. PUBLIC UTILITY COMPANY REBATE \$ 68456. G. TOTAL INVESTMENT (1D - 1E - 1F) 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) A. ELECT \$ 15.24 1078. \$ 16427. 15.61 \$ 256423.

B. DIST \$ 8.82 0. \$ 0. 17.56 \$ 0.

C. RESID \$ 2.73 0. \$ 0. 19.97 \$ 0.

D. NAT G \$ 4.50 0. \$ 0. 20.96 \$ 0.

E. COAL \$ 1.61 0. \$ 0. 17.58 \$ 0.

F. LPG \$ 6.34 0. \$ 0. 16.12 \$ 0.

M. DEMAND SAVINGS \$ 0. 14.74 \$ 0.

N. TOTAL -3917. \$ 16427. \$ 256423. 3. NON ENERGY SAVINGS(+) / COST(-) \$ 0. A. ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) 14.74 0. (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS (+) / COSTS (-) (+) / COSTS(-)
SAVINGS(+) YR DISCNT DISCOUNTED
COST(-) OC FACTR SAVINGS(+)/
(1) (2) (3) COST(-)(4) ITEM 0.. \$ 0. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 16427. 4.17 YEAR 5. SIMPLE PAYBACK PERIOD (1G/4) \$ 256423. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 3.75 (IF < 1 PROJECT DOES NOT QUALIFY) 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR): 10.14 %

LIFE CYCLE COST ANALYSIS SUMMARY

ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080

STUDY: ECO086

PROJECT NO. 2
CHILLED WATER SOUTH
BUILDING 25330

Harrison and Spencer, Inc. -

GENERAL PROJECT NO. 2

GENERAL DESCRIPTION:

See the drawing of Project No. 2 - Chilled Water Schematic South - Building 25330 for new and existing equipment and piping to make this project work. Each ECO defines the necessary equipment modification with a savings justification for its implementation. Existing chillers are low efficiency. Two of the existing chillers will be replaced with new high efficiency chillers, and the newest two chillers that are existing will remain for backup. With the new chilled water storage system, no more than 900 tons will be required at any time from the chillers, which will set a new lower load demand for the plant. This project is similar to Project No. 1 for the larger Building 25910 with the following exceptions:

- 1. The chillers are smaller.
- 2. There is one cooling tower per chiller, so the piping is a lot less.
- 3. The chilled water storage system is less.
- 4. Because the cooling equipment is shut down in the winter time, there is no need for the free cooling heat exchanger that is used as an energy saver in Project No. 1.
- 5. Because there is not much make-up water loss, the ECO to reduce make-up water is in Project No. 1, but not Project No. 2.

SUMMARY:

The composite of all of these ECO's for Project No. 2 are totaled up on the following page. We have computed the cost of the first year savings and the total discounted savings which allows us to compute the SIR of 4.37 in a simple payback of 3.60 years.

LIFE CYCLE COST ANALYSIS SUMMARY STUDY: PROJO02 ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080 INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 2 CHILLED WATER SOUTH FISCAL YEAR 1994 DISCRETE PORTION NAME: COMPOSITE ANALYSIS DATE: 02-19-95 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUR 1. INVESTMENT A. CONSTRUCTION COST \$ 1011653.

B. SIOH \$ 55641.

C. DESIGN COST \$ 60700.

D. TOTAL COST (1A+1B+1C) \$ 1127994. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0.

F. PUBLIC UTILITY COMPANY REBATE \$ 0.

G. TOTAL INVESTMENT (1D - 1E - 1F) \$ 1127994. 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) FUEL A. ELECT \$ 15.24 14053. \$ 214114. 15.61 \$ 3342326. B. DIST \$ 8.82 0. \$ 0. 17.56 \$ 0. C. RESID \$ 2.73 0. \$ 0. 19.97 \$ 0. D. NAT G \$ 4.50 0. \$ 0. 20.96 \$ 0. E. COAL \$ 1.61 0. \$ 0. 17.58 \$ 0. F. LPG \$ 6.34 0. \$ 0. 16.12 \$ 0. M. DEMAND SAVINGS \$ 75868. 14.74 \$ 1118294. N. TOTAL 8059. \$ 289982. \$ 4460621. 3. NON ENERGY SAVINGS (+) / COST (-) ANNUAL RECURRING (+/-) \$
(1) DISCOUNT FACTOR (TABLE A) 14.74
\$ A. ANNUAL RECURRING (+/-) 2000. 29480. B. NON RECURRING SAVINGS (+) / COSTS (-) SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4)

\$ 434184. 0 1.00 434184. ITEM 1. TOTAL d. TOTAL \$ 434184. 434184. C. TOTAL NON ENERGY DISCOUNTED SAVINGS (+) / COST (-) (3A2+3Bd4)\$ 463664. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 313692. 3.60 YEARS 5. SIMPLE PAYBACK PERIOD (1G/4) \$ 4924285. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 4.37 (IF < 1 PROJECT DOES NOT QUALIFY)

8. ADJUSTED INTERNAL RATE OF RETURN (AIRR): 10.98 %

PROJECT NO. 2 - CHILLED WATER SOUTH

ECO DATA COMPILATION

	TOTAL	DISCOUNT	SAVINGS	361,040	2,427,680	787,309	37,351	48,033	64,061	1,118,298	80,516	4,924,288	
		SAVINGS	1st YEAR	17,000	155,632	50,436	2,393	3,037	4,167	75,868	5,158	313,691	
	DEMAND	SAVINGS	ક્કા	0	0	0	0	0	0	75,868	0	75,868	
	NAT GAS	SAVINGS	MMBTU/YR	0	0	0	0	0	0	0	Ol	0	
	ELECTRICAL	SAVINGS	MMBTU/YR	0	1,008.60	3,310.36	157.05	32.9	130.87	0	338.54	14,053.32	
		COST	(From LCC)	15,510	412,620	318,126	15,596	34,139	1,968	281,121	48,917	1,127,997	
NON- RECURRING	DISCOUNTED	COST (-)	SAVINGS (+)	420,000	0	0	0	10,728	3,456	0	0	434,184	
	ANNUAL	RECURRING	COST	4,000	2,000	0	0	2,000	2,000	0	0	2,000	
		CONSTRUCTION	COST	13,910.40	370,062.00	285,314.40	13,986.00	30,618.00	1,765.26	252,126.00	43,870.68	1,011,652.70	
ECO DATA COMPLIATION			DESCRIPTION	Chem Treatment-CHW	Chiller Renjacement	Variable Speed Pumping	CHW Temperature Riser	Cooling Tower Manifolding	Condenser Water Chemical Treatment	Chilled Water Storage	FMCS Controls and Instrumentation	Totals	
D D		ECO	NO.	7	20	24	30	44	. 84	54	. 60		

Simpler Payback: 1,127,997 =

 $\frac{1,127,997}{313,691} = 3.60 \text{ years}$

 $\frac{4,924,288}{1,127,997} = 4.37$

2 - 3

ECO NAME:

Treatment of Make-up Water to Chilled Water System

ECO NUMBER:

7

TYPE: BLDG SYSTEM: Bldg. 25330 Cooling

EXISTING CONDITIONS:

The existing chemical treatment system serves the condenser side of the chilled water system and is feeding a C-6220 chemical from Industrial Maintenance Corporation into the condenser water system. Additionally an A-102 microbicide is added to each cooling tower by the bucket as the algae begins to build up in the cooling towers. There is no chemical feed on the chilled water side of the system. Since there is a fairly large volume of make-up water to the chilled water side, water that is fed into the system is not treated water at this time, nor is there any way to treat the water with the present equipment.

PROPOSED CHANGE:

The proposed change is a coupon system where various materials are located in contact with the chilled water and to determine what chemicals need to be added to the chilled water system to keep the various coupon materials that may come into contact with the chilled water in the distribution piping from corroding. The coupon system is not necessary on the condenser water side because there is actually conductivity meters that are measuring the water quality on that side, and there is a relatively small amount of piping from the cooling towers to the chillers.

CALCULATION & COST METHODOLOGY:

The savings would be the increased life of the chilled water piping system and would be offset by the increased cost in chemicals and installation of the coupons.

Costs:

Installation of Coupon

Materials \$2,000 Labor \$2,000

Chemical Feed System

Materials \$3,500 Labor \$2,500 chilled water side only.

Because chemicals are not being added, the increased cost of chemicals will be \$4,000 per year. All of these costs will be offset by the savings of the life of the chilled water system. Replacement cost is \$6 million. Life of piping will be extended from 20 years to 25 years with chemical treatment which is the equivalent of 16 year and 20 year lives for analysis purposes.

CONSTRUC	TION COST ESTIMATE				DATE:	23 SEPT 94	SHEET1	OF 1
Project:	FORT GORDON ENERGY STUD	ΟY						
Location:	AUGUSTA, GEORGIA					PROJ. NO.	2	
Arch/Engr:	HARRISON AND SPENCER, INC).				CODE:	BLDG 25330	
mmary:	ECO #7 - TREAT MAKE-UP WATER E		Esti	mator:	H. TOUB	Checked:		
	ITEM	QUANTI	ΓY	MATERIAL		LABOR		
DESC	RIPTION	QUAN	UNIT	UNIT COST	EXTENSION	UNIT COST	EXTENSION	TOTAL
CHEMICAL F	FEED SYSTEM	1	LS	3500	3500	2500	2500	\$6,000.00
TEST COUP	ON		LS	2000	2000	2000	2000	\$4,000.00
		-						
		SUBTOT	AL.		5500		4500	
			SALES		\$275.00			
		17%	LABO	R TAX			\$765.00	
		SUBTOT	ALS		\$5,775.00		\$5,265.00	\$11,040.00
				C ONLY)				\$2,208.00
		SUBTOT	AL GC	S WORK				\$13,248.00
				,				
		SUBTOT	AL(GC	& SUBS)				\$13,248.00
		10%	GC'S	PROFIT				
		5%	CONT	INGENCY				\$662.40
		TOTAL						\$13,910.40

ECO NAME:

Replace Chillers 1 and 2 With High Efficiency Chillers

ECO NUMBER:

20

TYPE: BLDG SYSTEM:

Bldg. 25330 Cooling

EXISTING CONDITIONS:

See Figure 1B - Existing Chilled Water Schematic-Building 25330. Chillers 1 and 2 are the oldest chillers. Chillers 3 and 4 are the next in age. All chillers are 500 ton capacity.

PROPOSED CHANGE:

Replace two 500 ton Carrier chillers with two 450 ton high efficiency chillers. The two newer chillers numbers 3 and 4 shall remain in service.

CALCULATION & COST METHODOLOGY

The chiller load for the plant is determined by totaling the loads for the entire building on the chilled water distribution system and adding losses of the distribution piping. Table 1B shows the load for each hour and each month. Totalized tonnages are given in Table 2B. Required plant capacity is a percentage of the maximum calculated load of 1,600 tons shown in Table 3B. Table 3B shows how many hours per year the plant capacity will operate at a given tonnage range. New chiller sizes with best available efficiency are selected to best meet the expected plant loads. Cost and efficiency data were obtained from a representative of the chiller manufacturer. Cost of chiller is \$112,000 for materials and \$25,000 for labor for each of two chillers. New chillers will require less maintenance for a yearly savings of \$2,000 per year.

ECO NAME:

Replace Chillers 1 and 2 With High Efficiency Chillers

(Cont'd)

ECO NUMBER:

20

TYPE: BLDG

Bldg. 25330 Cooling

SYSTEM:

ENERGY SAVINGS CALCULATIONS:

Existing Chillers 1 and 2:

<u>% CAP</u>	HRS	MBTU/HR	EER	<u>KWHR</u>
100%	367	12,000	22.4	196,607
80%	948	9,600	22.6	402,690
65%	1282	7,800	14.0	714,257
50%	6163	6,000	8.6	4,299,767
		•		5,613,321 KWH

@ \$0.052/KWH

Annual Operating Cost = \$291,893/yr

New Chiller:

<u>HRS</u>	TONS	KW/TON	KWH
367	1,000	.58	212,860
948	800	.53	401,952
1282	650	.53	441,649
6163	500	.52	<u>1,602,380</u> 2,658,841 KWH
	367 948 1282	367 1,000 948 800 1282 650	367 1,000 .58 948 800 .53 1282 650 .53

@ \$0.052/KWH

Annual Operating Cost = \$140,498/yr Annual Savings = \$151,395/yr

Annual Savings = 2,954,480 KWH

 $\frac{2,954,480 \times 3413}{10^6}$ = 10,083.6 Million Btu's

Cost:

New Chillers \$224,000 Labor \$ 50,000

CHILLED WATER SCHEMATIC-BLDG. 25330

CONSTRU	CTION COST ESTIMATE				DATE:	23 SEPT 94	SHEET	1 OF 1		
Project:	FORT GORDON ENERGY STUD	Υ								
Location:	AUGUSTA, GEORGIA					PROJ. NO.				
arch/Engr:	HARRISON AND SPENCER, INC	: .				CODE: BLDG 25330				
	ECO #20 - REPLACE CHILLERS	H. TOUB	Checked:							
	ITEM CRIPTION	QUANTIT QUAN (MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL		
500 TON CH	HILLER	2 E	Α	112000	224000	25000	50000	\$274,000.00		
		CUPTOTA			224000		50000			
		SUBTOTA		S TAX	224000 \$11,200.00		50000			
				R TAX	\$11,200.00		\$8,500.00			
		SUBTOTA		IC IPOC	\$235,200.00		\$58,500.00	\$293,700.00		
				SC ONLY)				\$58,740.00		
		SUBTOTA	L GC	'S WORK				\$352,440.00		
			··········							
		SUBTOTA	AL(GC	& SUBS)				\$352,440.00		
		-		PROFIT				0.17.000.00		
		5% (CON	TINGENCY				\$17,622.00 \$370,062.00		

ECO NAME:

Variable Speed Chilled Water Pumping

ECO NUMBER:

24

TYPE: BLDG SYSTEM:

Bldg. 25330 Cooling

EXISTING CONDITIONS:

This building has one chilled water loop with duplicate constant speed pumps circulating the water throughout this distribution loop. Buildings on the distribution loop all have 3way valves and some have chilled water pumps within the building. The constant speed pumps have 350 horsepower motors, and the voltage used to drive them is 2300 volts.

PROPOSED CHANGE:

The existing pump motors will be removed and replaced with 480 volt motors. There will be a transformer added if necessary to convert the 2300 volts to 480 volts, then routed through a variable speed drive with switching to go to either one of the new motors for the existing pumps. Within each building on the distribution system, the 3-way valves will have the bypasses capped off so that they will operate as 2-way valves. See sketch and description in ECO 23 for Project No. 1. The chilled water pumps will be operated by the EMCS system on a schedule determined by EMCS operating personnel with their knowledge of all the building usages. The pump will come on and off as required to satisfy the space temperature conditions within the building, which will be monitored and controlled by the EMCS.

CALCULATION & COST METHODOLOGY

The cost estimate is as follows:

Materials

Secondary Pumps: \$ 4,000 \$32,000 Labor Materials 20-inch piping \$ 1,500 Materials \$ 3,000 Labor Building controls and EMCS instrumentation \$15,000 Materials \$15,000 Labor One variable speed drive \$ 1,500 \$40,300 Labor Material One set of vacuum contractors Labor \$ 1,000 \$ 6,500 Materials One 2300 volt/480 volt transformer for 350 kva \$ 1,500 Materials \$11,200 Labor Two 350 horsepower 480 volt motors each at \$17,700 \$35,400 Labor \$ 2,000 Materials Piping changes within the buildings Labor \$14,000 \$14,000 Materials Building 25330 controls Materials \$ 3,000 Labor \$ 1,500 Electrical Work \$ 4,000 Labor \$ 2,000

ECO NAME:

Variable Speed Chilled Water Pumping

(Cont'd)

ECO NUMBER:

24

TYPE: BLDG SYSTEM:

Bldg. 25330

Cooling

CALCULATION & COST METHODOLOGY:

Savings will be obtained by determining the bins for which variable speed pumping will operate at each 10% increment, then apply this to a Bell & Gossett variable speed pumping program, which will determine the savings between constant speed with the same motors and drives with variable speed pumping and new motors, but the same pumps. The savings is the difference in KWH of 1,568,886.23 and 598,959.47 which is

969,926.73 KWH or

 $969,926.73 \times 3413 = 3310.36 \text{ Million Btu's}$

 10^{6}

CONSTRUC	TION COST ESTIMATE	DATE:	23 SEPT 94	SHEET1	OF 1					
Project:	FORT GORDON ENERGY STUD	Υ								
Location:	AUGUSTA, GEORGIA					PROJ. NO.	2			
Arch/Engr:	HARRISON AND SPENCER, INC	.				CODE:	BLDG 25330	DG 25330		
nmary:	ECO #24 - CHILLED WATER PUMPING Estimator:				H. TOUB	Checked:				
	ITEM	QUANTI	TY	MATERIAL		LABOR				
DESC	RIPTION	QUAN	UNIT	UNIT COST	EXTENSION	UNIT COST	EXTENSION	TOTAL		
MATERIALO			Ε.Δ.	9000	32000	1000	4000	\$36,000.00		
MATERIALS PIPING)		EA LS	8000 3000		1500	1500	\$4,500.00		
	& EMCS INSTRUMENTATION		LS	15000	15000	15000	15000	\$30,000.00		
	SPEED DRIVE		LS	40300	40300	1500	1500	\$41,800.00		
	ONTACTORS		LS	6500	6500	1000	1000	\$7,500.00		
TRANSFOR			LS	11200	11200	1500	1500	\$12,700.00		
480 VOLT N			EA	17700	35400	2000	4000	\$39,400.00		
PIPING CHA		1	LS	14000	14000	14000	14000	\$28,000.00		
CONTROLS			LS	3000	3000	1500	1500	\$4,500.00		
ELECTRICAL			LS	4000	4000	2000	2000	\$6,000.00		
		SUBTOT		S TAX	164400 \$8,220.00		46000			
		-		R TAX	\$5,225.55		\$7,820.00			
		SUBTO			\$172,620.00		\$53,820.00	\$226,440.00		
				GC ONLY)				\$45,288.00		
				'S WORK				\$271,728.00		
		SUBTOT	AL(G(C & SUBS)				\$271,728.00		
				PROFIT				, , , , , , , , , , , , , , , , , , , ,		
				TINGENCY				\$13,586.40		
		TOTAL						\$285,314.40		

B&G Pumping System Analysis:

```
SUMMARY OF INPUT DATA: 25330 cooling fumes 1+2
System peak demand: 3840.00 gpm
```

System discharge pressure: 198.00 ft. (85.77 psig)
Minimum control/Static pressure: 25.00 ft. (10.83 psig)

Standard Efficiency (SE) 60-cycle motor.

1 Pump System:

Pump 1: Series VSCS 12X14X17.5L, Impeller diameter 14.875" Design RPM = 1770.0, Motor HP = 300.00

CONSTANT SPEED OPERATION:

```
Q/Qd,% TGPM TDH,ft BHP Ep,% BHP/HP,m HP,in E,mtr,% kWHR
                                                     26.75 9.3
                                           95.7 668.6
     10.0 384.0 221.5 220.03
                              0.733
                                    229.91
                          9.8
3.90
                                           95.7 1119.5
                                                     44.78 18.7
                                    229.91
    20.0 768.0 221.5 220.03 19.5
                              0.733
6.53
                                                     29.28 28.0
                                                732.1
     30.0 1152.0 221.0 220.03 29.2 0.733
                                    229.91
                                           95.7
4.27
                                                     15.40 36.0
                                           95.7
                                                385.1
     40.0 1536.0 220.1 226.69 37.7
                                    236.87
                              0.756
2.18
                                                322.5 12.90 42.9
                                           95.7
     50.0 1920.0 218.6 236.53 44.8
                              0.788
                                    247.15
1.75
                                                304.1
                                                     12.16 49.0
                                    256.48
                                           95.7
     60.0 2304.0 216.2 245.45 51.2
                               0.818
1.59
                                           95.7
                                                348.0
                                                     13.92 54.6
                               0.846
                                    265.13
     70.0 2688.0 213.4 253.73 57.1
1.76
                                                      6.82 59.8
                                                170.5
                                           95.7
                               0.868
                                    272.24
     80.0 3072.0 209.8 260.53 62.5
 0.84
                                                      5.57 64.4
                                                139.3
                                    278.84
                                           95.6
     90.0 3456.0 205.7 266.69 67.3
                               0.889
 0.67
                                                108.6
                                           95.6
                                                      4.34 68.3
                                    285.51
 0.51 100.0 3840.0 201.3 272.84 71.5
                               0.909
```

COST SUMMARY:

```
Annual Operating Cost @ $0.04 / kwhr = $ 62755.45
8760 hours/year or 100.00%
Total annual operating cost = $ 62755.45
Total kW hours = 1568886.23
```

VARIABLE SPEED OPERATION: (Table 1 of 1)

System suction pressure: 0.00 ft. (0.00 psig)
Best Efficiency Staging is ON

```
HP, in E, d/m, % kWHR
                                                        $/day E, w/w, %
     Q/Qd,% TGPM
                TDH, ft BHP Ep, %
                                RPM
4.01 7.5
                                                  100.2
                                            56.1
                      19.32 13.4 616.9
                                       34.45
     10.0 384.0
                26.7
3.90
                                                        14.91 8.1
                                                  372.7
                                       76.55
                                             60.3
                      46.13 13.4
                                676.4
                 31.9
6.53
     20.0
          768.0
                                                        7.81 19.2
                                             65.3
                                                  195.4
                                772.5
                                       61.36
                40.6 40.08 29.4
     30.0 1152.0
4.27
                                                         5.03 26.4
                                       77.29
                                             70.3
                                                  125.6
                                886.9
                      54.36 37.6
     40.0 1536.0
                52.7
2.18
                                                         5.08 34.0
                                                  126.9
                                             76.1
                                      97.26
     50.0 1920.0 68.3
                      74.06 44.7 1019.6
1.75
                                                         5.91 40.8
                                            79.9
                                                  147.6
                      99.47 51.1 1156.9
                                      124.53
     60.0 2304.0 87.3
 1.59
                                      157.82 82.8
                                                        8.29 47.2
                                                  207.1
      70.0 2688.0 109.8 130.63 57.0 1303.3
 1.76
                                                  124.0
                                                         4.96 53.2
                                             85.2
      80.0 3072.0 135.7 168.72 62.4 1449.7
                                      197.99
 0.84
                                                         4.97 58.0
                                      248.60
                                            86.2
                                                  124.2
      90.0 3456.0 165.1 214.37 67.2 1605.3
 67
                                                         4.68 62.4
                                             87.2
                                                  117.1
 0.51 100.0 3840.0 198.0 268.44 71.5 1751.7
                                      307.92
Annual Operating Cost @ $0.04 / kwhr = $ 23958.38
   8760 hours/year or 100.00%
```

Total kW hours = 598959.47

COST SUMMARY:

tion Pressure : 0.0 psig

ercent of Year : 100% : 8760 Hours/Year

Annual Operating Cost: \$23958.38

Total hours/year = 8760 Total annual operating cost = \$23958.38

ECO NAME:

Controls For Supply CHW Regulation/Reset Temperature

ECO NUMBER:

30

TYPE: BLDG SYSTEM:

Bldg. 25330 Cooling

EXISTING CONDITIONS:

Although the chillers are set to maintain a constant chilled water supply temperature, the temperature actually varies because some water is bypassed through non-operating chillers. The system is set to operate at a constant supply water temperature of approximately 42°F.

PROPOSED CHANGE:

Wire the chilled water supply setpoint to existing EMCS controls so that the chilled water temperature setpoint can be used to vary the flow as required by the system load and the temperature reset be adjusted as conditions require. This will allow the temperature to vary upwards, and the savings of 1.5% of the chiller usage can be obtained for every 1° of reset temperature. Although the savings are available to be had, it is recommended that the ECO 24 in this Project no. 2, variable speed pumping, be implemented so that the temperature maintains the same 42°F. The variable flow to save energy is a better idea because each building will then have the full humidity control.

CALCULATION & COST METHODOLOGY

Total chiller usage is determined by the hours each bin of capacity is shown on Table 3A.

160 tons x 1152 hours x .75 = 138,240 KW hours 320 tons x 2536 hours x .75 = 608,640 KW hours 480 tons x 1680 hours x .75 = 604,800 KW hours 640 tons x 759 hours x .75 = 381,600 KW hours 800 tons x 671 hours x .75 = 402,600 KW hours 960 tons x 611 hours x .75 = 439,920 KW hours 1120 tons x 581 hours x .75 = 488,040 KW hours 1280 tons x 367 hours x .75 = 352,320 KW hours 1440 tons x 183 hours x .75 = 197,640 KW hours 1600 tons x 184 hours x .75 = 220,800 KW hours 3,834,600 KW per year

For the available savings,

Multiply 1.5% of 3,834,600 \times 50% for all temperatures above 43°F Multiply 1.5% \times 3,834,600 \times 20% for all temperatures above 44°F Multiply 3,834,600 \times 10% for all temperatures above 45°F

Total = 46,015 KW or 157.05 Million Btu's per year.

Above 43°F 28759.5 KWH
Above 44°F 11503.8 KWH
Above 45°F 5751.9 KWH

 $\frac{1}{46015.2}$ KWH x $\frac{3413}{1000}$ = 157.05 Million Btu's/yr.

 10^{6}

Cost:

Controls:

Materials

\$5,000

Labor

\$5,000

Location: A Arch/Engr: H mmary: E	FORT GORDON ENERGY STUD AUGUSTA, GEORGIA HARRISON AND SPENCER, INC ECO #30 - TEMP RESET TEM IPTION		timator:	н. тоив		BLDG 25330			
Location: A Arch/Engr: H mmary: E	HARRISON AND SPENCER, INC ECO #30 - TEMP RESET TEM	Es QUANTITY	MATERIAL	H. TOUB	CODE:	BLDG 25330			
nmary: E	ECO #30 - TEMP RESET	Es QUANTITY	MATERIAL	H. TOUB		BLDG 25330			
mmary: E	ECO #30 - TEMP RESET	Es QUANTITY	MATERIAL	H. TOUB		CODE: BLDG 25330			
DESCRI	TEM				Checked:				
			I UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL		
CONTROLS						5000	040 000 00		
		1 LS	5000	5000	5000	5000	\$10,000.00		
				-					
		des reside							
			-						
		*							
		SUBTOTAL		5000		5000			
		5% SAL	FS TAX	\$250.00	1	0000			
		17% LAB		\		\$850.00			
		SUBTOTALS		\$5,250.00		\$5,850.00	\$11,100.00		
		-	(GC ONLY)				\$2,220.00		
		SUBTOTAL G					\$13,320.00		
							640,000,00		
		SUBTOTAL(C				\$13,320.00			
			S PROFIT				#000 DD		
		TOTAL	NTINGENCY				\$666.00 \$13,986.00		

ECO NAME:

Common Manifolding of Cooling Towers

ECO NUMBER:

44

TYPE: BLDG SYSTEM: Bldg. 25330 Cooling

EXISTING CONDITIONS:

All four chillers are 500 ton capacity and each is piped to its own cooling tower.

PROPOSED CHANGE:

Cross-connect cooling tower piping for maintenance work and to allow greater cooling tower capacity to reduce the approach to the ambient wet bulb temperature.

CALCULATION & COST METHODOLOGY:

Maintenance costs can be reduced by better maintenance scheduling. The life of the chillers is extended one year in 20 by allowing maintenance work to be accomplished when it is required not only when the chiller is available. Cooling tower life can also be extended for one year in twenty for the same reasons.

The efficiency of the chillers can be increased by 1% for every 2°F reduction in the condenser water temperature. For an average load on the chillers of 600 tons for five months the usage is:

600 tons x .78 KW/ton x 5 mo. x 30 days/mo x 24 hrs/day = 1,684,800 KW/yr. At 1 % savings

 $.01 \times 1,684,800 = 16,848 \text{ KW savings}$ $16,848 \times \frac{3413}{10^6} = 57.5 \text{ Million Btu's/yr.}$

Maintenance savings only - \$2,000/yr

Cost:

Piping:

Material

\$12,000

Labor

\$10,000

The chiller energy savings is offset by the additional pumping cost of the condenser water. The cost of additional pumping is estimated at 21KW/hr for all the time the cooling tower is saving the 1%.

 $2KWH \times 5 \text{ mo. } \times 30 \text{ days/mo. } \times 24 \text{ hrs/day} = 7,200 \text{ KW/yr.}$

The net savings is therefore the difference of 16,848 - 7,200 = 9,648 KW $9,648 \text{KW} \times \frac{3,413}{10^6} = 32.9 \text{ million BTU's/year}$

CONSTRU	CTION COST ESTIMATE				DATE:	23 SEPT 94	SHEET	I OF 1		
Project:	FORT GORDON ENERGY STUD	Υ								
Location:	AUGUSTA, GEORGIA					PROJ. NO.				
Arch/Engr:	HARRISON AND SPENCER, INC					CODE: 25330				
nmary:	ECO #44 - COMMON MANIFOLDIN	Est	H. TOUB	Checked:						
	ITEM RIPTION	QUANTI	ΤΥ	MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL		
PIPING MAT	TERIALS	1	LS	12000	12000	10000	10000	\$22,000.00		
							1			
		A44_* 11*								
		CURTOT	· A I		12000		10000			
		SUBTOT		S TAX	\$600.00		10000			
				R TAX	\$555.55		\$1,700.00			
		SUBTO			\$12,600.00		\$11,700.00	\$24,300.00		
		20%	OH (GC ONLY)				\$4,860.00		
		SUBTOT	AL GO	S'S WORK				\$29,160.00		
		SUBTO	TAL(G	C & SUBS)				\$29,160.00		
				PROFIT						
				TINGENCY				\$1,458.00		
		TOTAL						\$30,618.00		

ECO NAME:

Cooling Tower Water Treatment

ECO NUMBER:

48

TYPE: BLDG SYSTEM:

Bldg. 25330 Cooling

EXISTING CONDITIONS:

There is currently water treatment based on a conductivity meter of the cooling tower water, but biocide is added manually by the scoopful only as needed.

PROPOSED CHANGE:

This cooling tower chemical feed is adequate except for the method of feeding biocides. Proper maintenance and observation of the cooling towers is insufficient without the addition of new equipment. The equipment cost is \$1,000 in materials and \$300 for labor to measure and alarm when water is in need of treatment to reduce algea build-up.

CALCULATION & COST METHODOLOGY:

Because chemicals are now being added, there is no increased cost of chemicals. Any improvements in the cooling water chemical treatment will be positive and can reduce maintenance by \$2,000/year total. The life of the cooling tower is extended for two years so that with treatment the life of the cooling tower is 20 years, but without treatment it is 18 years. The cost of a new cooling tower is \$18,000 in materials and \$3,600 in labor for each of four towers in Building 25330 for a total of $21,600 \times 4 = $86,400$.

The efficiency improvements of the chillers will be 1% of the yearly chiller operating cost of 3,834,600KW per year as shown in ECO No. 30. This savings is 3,834,600KW x 1% x 3,413 = 130.87 million BTU's/yr.

 10^{6}

CONSTRU	CTION COST ESTIMATE		DATE:	31 JAN 95	SHEET1	OF 1			
Project:	FORT GORDON ENERGY STUD	Υ							
Location:	AUGUSTA, GEORGIA					PROJ. NO. 2			
Arch/Engr:	HARRISON AND SPENCER, INC	: .				CODE:	BLDG 25330		
mmary:	ECO #48 COOLING TOWER WATER 1	REATM	H. TOUB	Checked:					
	ITEM RIPTION	QUANTI QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL	
CHEMICAL I	FEED	1	LS	1,000	1000	300	300	\$1,300.00	
		SUBTOT			1000	1	300		
				S TAX OR TAX	\$50.00		\$51.00		
		SUBTO		I IAX	\$1,050.00		\$351.00	\$1,401.00	
				GC ONLY)				\$280.20	
				'S WORK				\$1,681.20	
				& SUBS)		\$1,681.20			
				PROFIT TINGENCY				\$84.06	
		TOTAL	00,1					\$1,765.26	

ECO NAME:

Chilled Water Storage

ECO NUMBER:

54

TYPE: BLDG SYSTEM:

Bldg. 25330 Cooling

EXISTING CONDITIONS:

From Table 2B in ECO 20, the highest available tonnage at any particular time is in June at 1700 hours where the load gets up to 1543.3 tons for that hour. This high rate occurs when the maximum demand at the base occurs and will cause the electric bill to be based on a higher demand.

PROPOSED CHANGE:

Provide an aboveground chilled water storage tank with a capacity equal to approximately 450,000 gallons. This will supply 3,100 ton hours of cooling, which will allow the chiller to operate at a maximum of 900 tons throughout the summer. During the month of June the calculated tonnage is as follows:

HOUR	TONNAGE COMPUTED	STO	RAGE (Tonnage - 900) COMPUTATION
1400	960.1		60.1
1500	994.9		94.9
1600	999.6		99.6
1700	1543.3		643.3
1800	1486.2		586.2
1900	1376.4		476.4
2000 •	1378.3		378.3
2100	1176.8		276.8
2200	1119.2		219.2
2300	1058.2		158.2
2400	983.1		83.1
		Total	3076.1

The aboveground storage tank is sized based on chilled water 42°F, using it until it gets to 52°F with 10° \(^{\text{t}}\). Therefore 1,200 pounds of water is required per ton hour.

3.076.1 ton hrs x 1,200 lbs/ton hr = 442,604 gal. required

8.34 lbs/gal

3,076.1 ton hrs. x 1,200 lbs/ton hr. = 59,156 cu. ft. required

Rough sizing of the tank to try to make the diameter equal to the height results in a diameter of 44 ft. and a height of 39 ft. Piping will be shown as depicted in the sketch included with the Project No. 2 write-up.

CALCULATION & COST METHODOLOGY:

The cost of a 3,100 ton hour chilled water storage at \$60/ton hr. is \$186,000

Material

\$146,000

Labor

\$40,000

Savings is computed based on demand savings, which is \$106.20/KW/Yr. for demand reduction. Since there is an interruptible rate effective at Fort Gordon, there is an additional \$45/KW they will receive for reducing demand during the peak period, which is the purpose of the chilled water storage. Therefore, the total amount saved is \$151.20/KW of demand. The peak chilling capacity occurs in June and is 1,543.3 tons. If the chiller generated capacity is limited to 900 tons, this would save 643.3 tons.

 $643.3 \text{ tons } \times .78 \text{ KW/ton} = 501.77 \text{ KW demand savings}$ $501.77 \times \$151.20 = \$75,868.23 \text{ savings in demand}$

CONSTRUC	TION COST ESTIMATE			DATE:	23 SEPT 94	SHEET	1 OF 1
Project:	FORT GORDON ENERGY STUD	Υ					
cation:	AUGUSTA, GEORGIA				PROJ. NO.	2	
h/Engr:	HARRISON AND SPENCER, INC	.			CODE:	BLDG 25330	
Summary:	ECO #54 - CHILLED WATER STORAGE		imator:	H. TOUB	Checked:		
	ITEM CRIPTION	QUANTITY QUAN UNIT	MATERIAL	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
UNDERGROU	IND CHILLED WATER STORAGE TANK	1 LS	146000	146000	40000	40000	\$186,000.00
		SUBTOTALS	1	\$146,000.00		\$40,000.00	\$186,000.00
		5% SALE		\$7,300.00			\$7,300.00
		17% LAB				\$6,800.00	\$6,800.00
		SUBTOTALS		\$153,300.00		\$46,800.00	\$200,100.00
			H & PROFIT				\$40,020.00
	SUB-CONTRACTORS	SUBTOTAL G	C WORK				\$240,120.00
		TOTAL SUB \					
			SUB PROFIT	N IOD			\$12,006.00
		5% CON	ITINGENCY O	A JOR			\$12,006.00

ECO NAME:

EMCS Controls for Chilled Water South System

ECO NUMBER:

87

TYPE: BLDG SYSTEM:

Bldg. 25330 Cooling

EXISTING CONDITIONS:

Existing automatic or manual controls that are within the plant are not remotely operable by the EMCS by design. The EMCS office which is manned 24 hours a day has very few, if any, instrumentation readouts from the plant, and no control of the plant with the EMCS. Because EMCS personnel are aware of what is happening in many buildings, they are also aware of conditions and demands in the chilled water system. Currently, the boiler operators are making boiler pressure changes, HTW changes, bringing on and off chillers, cooling towers, and many manual valving operations. However, they are not performing the functions that an EMCS office can to control energy and to improve the operating efficiency of the plant.

PROPOSED CHANGE:

New equipment installed in other ECO's in this Project No. 2 shall be connected to the EMCS system for instrumentation readout and for control of equipment, pumps, etc.

Required EMCS Controls and Instrumentation for the Chilled Water System at Building 25330

<u>DESCRIPTION</u>	<u>POINTS</u>	<u>AMOUNT</u>
Chiller efficiency software	10	\$10,000
Flow meter and temperatures at distribution	8	10,000
pipe locations Operating controls for chiller pumps, condenser	8	4,000
pumps, etc.		
Temperatures for chilled water, condenser water, etc.	8	1,600
Chiller amps	4	2,000
Variable speed and switch controls		1,600
Pressures for chilled water return, supply and storage	6	1,800
		\$31,000

CALCULATION & COST METHODOLOGY:

The cost of the equipment is as shown in the Proposed Change above. The cost estimate sheet is based on percentages of estimates used in ECO 86 of Project No. 1 to arrive at labor rates. These are additional costs only to wire the existing controls to the new controls identified in other ECO's. The only thing that is not included in other ECO's is the distribution system flow meters and temperature sensors because that did not work out as a viable ECO for Project No. 2 as it did for Project No. 1. Those flow meters and temperature sensors in the distribution pipe will be included in this ECO.

Savings: Hours per year operating at 900 tons of chiller capacity of 49 hours based on Table 2B in ECO 20. The remaining hours in the year the average load is 400 tons/hr. 49 x 30 days/mo. = $1,470 \, \text{hrs/yr}$. x 900 tons x .78 KW/ton = $1,031,940 \, \text{KWH}$

(8,760 - 1470) hours per year x 400 tons avg. x .76 KW/ton = 2,274,480 KWH Total = 3,306,420 KWH

3,306,420 KWH x \$.052/KW = \$171,933.84 x .03 = \$5,158.02

3,306,420 KWH x .03 x 3,413 = 338.54 Million Btu's/yr.

This is the savings obtained by 3% improvement in the operating efficiency of the chillers.

CONSTRUC	TION COST ESTIMATE				DATE:	11 JAN 95	SHEET1	OF 1					
Project:	FORT GORDON ENERGY STUD	Υ											
ocation:	AUGUSTA, GEORGIA					PROJ. NO.	2						
ch/Engr:	HARRISON AND SPENCER, INC	·.				CODE:	BLDG 25330						
Summary:	ECO #87 - EMCS CONTROLS		Est	imator:	H. TOUB	Checked:							
	ITEM	QUANTI		MATERIAL		LABOR							
DESC	RIPTION	QUAN	UNIT	UNIT COST	EXTENSION	UNIT COST	EXTENSION	TOTAL					
OUIL ED EE	TENOV COET MARE	1	1.0			10000	10000	\$10,000.00					
	FIENCY SOFT WARE R & TEMP DISTRIBUTION SYSTEM		LS LS	6500	6500	3500	3500	\$10,000.00					
			LS	2500	2500	1500	1500	\$4,000.00					
	ATING CONTROLS		LS	600	600	1000	1000	\$1,600.00					
TEMPERATU CHILLER AM			LS	1000	1000	1000	1000	\$2,000.00					
	PEED & SWITCH CONTROL		LS	600	600	1000	1000	\$1,600.00					
	S - CHW, SUPPLY, RETURN AND STOR		LS	900	900	900	900	\$1,800.00					
		-	SALE	S TAX	\$12,100.00 \$605.00		\$18,900.00 \$3,213.00	\$31,000.00 \$605.00 \$3,213.00					
		SUBTO	TALS 2		\$12,705.00		\$22,113.00	\$34,818.00					
		20%	GC O	H & PROFIT				\$6,963.60					
	SUB-CONTRACTORS	SUBTO	TAL GO	WORK				\$41,781.60					
		TOTAL SUB WORK											
		10% GC SUB PROFIT											
		5% CONTINGENCY ON JOB											
		TOTAL			\$43,870.68								

COOLING PROFILE BUILDING 25330

JANUARY

DAY		BUILDING TYPE														
HOUR	31	31 A	32	33	34	35	36	97	38	39	40	41	42	43	44	TOTAL
1		0.7			15.3								***********			16.
2					12.1											12.
3					9.7											9.
4				1	7.6		1									7.6
5				1	116.0											116.0
6					133.4											133.4
7					144.8		1									144.8
8 9					153.0				4.0							153.0
	1			1	159.3				4.0						1	167.3
10 11					164.5 168.8				10.2			4.0	0.4			184.9 196.0
12					172.4		1		12.4 14.4			1.0 4.2	3.9			
13					175.3				16.0			4.6	4.6			213.5 221.1
14				0.9	177.6		1		17.2			6.1	5.1			233.8
15	0.9			1.4	179.5				18.4		1.3	7.6	5.4			249.7
16	1.6			1.5	184.6			4.0	19.2		2.6	7.9	5.5		0.3	272.8
17	14.1			1.5	187.4			7.4	19.3		1.9	7.7	2.2		0.9	345.5
18	15.0			1.4	83.1		l	6.1	18.7		1.2	6.4	1.2		0.1	230.7
19	15.0			1.2	66.9				7.2	1.2	0.4	5.4	0.5			175.2
20	14.1			1.1	56.2	5.4	1		4.9			4.6			ł	183.6
21	13.4	3.8		0.2	37.4	5.2			3.1							150.4
22	12.0	12.2			31.1	5.0			1.4							208.3
23	11.1	11.5		1	24.2	4.6			0.2							180.2
24	10.0	10.8			19.0	4.4	2.4					!				153.0

FEBRUARY

DAY								BUILD	ING	TYPE						
HOUR	31	AIE	32	33	34	35	36	37	38	39	40	41	42	43	44	TOTAL
1		2.4			15.5									***************************************		26.3
2 3	1.2				12.5											12.5
					9.9 7.8											9.9 7.8
4 5 6 7					116.3											116.3
- 6					133.5				i i							133.5
	1				144.7											144.7
8		:			152.7						-					152.7
9					158.9				4.6							168.1
10					164.1				9.5							183.1
11					168.5				11.4			0.4			1	192.1
12 13					172.0				13.2			3.8 4.4	3.5 4.4			209.5
10				0.3	174.9 177.4				15.1 16.6			5.2	4.4			219.8 231.4
15	0.4			1.2	179.5				17.9			7.5	5.4			243.7
16	1.4	·		1.4	181.0			0.3	18.4		0.8	7.9	5.5			254.5
17	14.5			1.5	183.2			7.2	18.6		1.7	7.9			0.1	335.3
18	16.5			1.5	84.4			7.0	18.4	1.5	1.2	7.4	1.4		0.2	245.7
19	16.4			1.4	68.0	0.3		1.1	7.2	1.4	0.6	6.2				190.4
50	16.2			1.3	56.6	5.9	,		4.9			5.5	0.1			200.4
21	16.0	16.0		0.4	42.1	5.9	7.2		3.1				-			305.7
22	15.5	15.9		0.1	32.4	5.9	6.5		1.7							278.5
23	15.1	15.8			25.3	5.7	5.9		0.7							256.5
24	14.3	15.2			19.3	5.6	5.2									232.8

MARCH

DAY	BUILDING TYPE															
HOUR	31	AIE	32	33	34	35	36	37	38	39	40	41	42	43	44	TOTAL
7	8.8	7.5			16.9	2.0	1.3		0.7							108.8
2	5.5	4.1			12.9	0.9										54.0
3	3.2	1.9			10.3						j					30.1
4	1.7				8.3											16.8
5		1			117.1	ĺ	i									117.1
6					134.5			1								134.5
7					145.7				0.2							146.1
8	0.8	1			153.8				8.9							175.6
9	2.4				160.2				10.4							193.0
10	4.1	1			165.5		l		12.1			1.6				213.4
11	6.4	1		1.0	169.9				14.4			5.6	4.2	0.3		246.9
12	7.9	- 1		1.6	173.6				16.8			7.7	5.3	0.7		270.1
13	8.8			1.8	178.7			10.7	18.6		0.2	9.7	6.0	1.7	1.5	309.9
14	10.5			2.0	190.3			13.6	20.4	4.4	4.4	10.8	6.7	2.7	2.3	351.2
15	11.4	- 1		2.2	191.2	1		14.6	21.3	3.5	2.2	11.5	6.9	3.4	2.5	359.7
16	12.8		4.3	2.4	191.1			15.5	21.7	3.3	2.1	11.9	7.1	3.9	2.7	375.0
17	26.2	21.2	4.0	2.5	191.2			16.0	21.9	4.4	1.9	12.1	3.3		2.8	487.4
18	27.9	26.1	3.5	2.5	95.3	6.5	13.8	15.7	21.7	4.1	1.5	11.5	2.5		1.4	652.4
19	27.4	26.2	2.7	2.3	80.3	9.3	14.7	6.7	9.5	3.7	1.2	10.2	1.7		0.8	617.9
20	26.8	26.1	2.0	2.3	69.7	9.4	14.3	4.2	7.1	1.2	0.4	9.2	1.1		0.4	582.9
21	25.7	25.5	1.3	0.9	46.1	9.4	13.5	2.3	5.4	0.7	0.1	2.3	0.7		0.1	511.1
22	25.2	25.4	0.7	0.6	35.5	9.5	12.7	1.2	3.9	0.3		1.3	0.3			476.6
23	23.9	24.8	0.2	0.4	27.8	9.1	11.8		2.7			0.4				436.9
24	22.2	23.4		0.2	21.8	8.5	10.7		1.7					l	L	395.5

APRIL

DAY		BUILDING TYPE														
HOUR	31	31A	35	33	34	35	36	37	38	39	40	41	42	43	44	TOTAL
1	15.8	11.9	0.7	0.4	18.5	3.7	4.9	0.8	0.7	0.3		0.7				224.4
2	13.2	8.4	0.3	0.3	14.6	2.6	2.9									158.3
3	10.8	6.1		0.2	11.3	1.7	1.6									112.7
4	9.3	4.1			8.7	0.9	0.3									73.3
5	7.8	2.4			118.8	0.3						į				164.4
6	7.0	1.3			136.2			. 1								173.8
7	6.6	0.7			147.4				0.2							182.2
8	7.7	1.5			155.7		l		8.9							215.0
9	8.9	2.4		0.8	162.1			0.7	10.4			0.8		2.3		241.5
10	11.8	4.2		1.7	169.7			11.7	12.1			6.4	3.1	3.4		312.5
11	13.6	5.3	0.9	2.1	178.9		1.3	14.6	14.4		1	9.7	5.2	5.6	2.5	396.6
12	15.1	5.5	4.3	2.4	188.5	1.0	3.4	16.9	16.8	5.5		11.5	6.4	7.2	3.0	481.8
13	16.4	5.8	5.4	2.6	196.3	1.1	3.8	18.6	18.6	7.8	3.3	12.6	7.4	10.0	3.5	528.0
14	18.2	6.6	6.4	2.9	203.8	1.6	4.8	20.7	20.4	9.0	4.4	13.6	8.0	13.2	4.0	586.5
15	20.8	8.0	7.4	3.1	196.2	2.3	6.6	22.7	21.3	5.1	2.5	14.6	8.5	14.7	4.4	635.1
16	21.6	7.9	7.6	3.2	194.8	2.5	7.1	23.1	21.7	4.7	2.3	14.8	8.4	15.2	4.4	648.7
17	38.5	30.8	5.5	3.3	194.6	10.6	20.1	23.3	21.9	6.1	2.1	14.9	3.9	3.4	4.5	1007.5
18	38.4	35.9	5.1	3.3	105.7	12.4	22.5	22.8	21.7	5.9	1.8	14.6	3.1	3.3	2.3	953.7
19	37.8	36.8	4.4	3.1	90.7	12.8	21.9	11.4	9.5	5.5	1.5	13.2	2.3	2.8	1.6	871.6
20	37.2	36.7	3.5	3.0	79.9	12.9	20.6	8.0	7.1	2.3	0.8	12.0	1.7	2.1	1.1	814.1
21	37.3	36.9	2.8	1.3	48.3	12.9	20.5	6.0	5.4	1.7	0.6	4.6	1.2	1.6	0.7	745.5
22	36.3	37.0	2.2	1.0	36.9	12.6	19.5	4.2	3.9	1.3	0.3	3.4	8.0	1.1	0.5	698.2
23	34.8	35.3	1.6	0.7	29.1	12.3	18.1	3.0	2.7	1.0	0.1	2.6	0.5	0.4	0.3	645.1
24	32.4	33.7	1.1	0.6	23.2	11.5	16.4	1.8	1.7	0.6	0.0	1.6	0.3		0.1	583.6

MAY

DAY	BUILDING TYPE															
HOUR	31	31A	32	33	34	35	36	37	38	39	40	41	42	43	44	TOTAL
•	21.2	15.2	1.8	0.7	19.6	5.1	7.6	3.4	2.1	1.0	0.2	2.7	0.5	1.4	0.3	327.8
2	20.0	11.7	1.4	0.5	15.6	4.0	5.6	2.4	1.3	0.8		1.8	0.3	0.9	0.2	265.5
3	17.3	9.1	1.0	0.4	12.4	3.0	4.0	1.4	0.6	0.4		1.1	0.1	0.3	0.0	205.1
- 4	15.0	7.3	0.6	0.3	9.6	2.2	2.8	0.7		0.2		0.3			0.0	158.7
5	13.0	5.6	0.3	0.2	119.1	1.5	1.6		1			0.1			0.0	229.8
6	11.1	4.2		0.1	136.9	1.0	0.5								0.0	214.8
7	12.1	4.7	0.2	0.2	149.0	0.9	1.2		7.5						0.0	258.5
8	13.6	5.4	0.9	0.3	161.8	1.1	2.2	6.7	11.3	0.1		0.3			0.0	319.3
9	14.6	5.9	1.9	1.3	171.6	1.3	3.1	10.7	12.9	1.2		7.6	2.3	5.4	2.1	407.2
10	16.7	7.9	3.4	1.9	175.9	1.8	4.9	14.9	14.7	1.9		10.0	4.8	9.7	2.6	488.8
11	19.0	8.9	5.0	2.4	179.5	2.2	5.9	17.8	16.9	2.6		11.8	5.9	12.4	3.2	550.5
12	21.0	9.0	6.4	2.8	194.0	2.4	6.2	20.5	18.9	7.4	2.1	13.4	7.0	14.8	3.9	612.9
13	23.2	9.4	7.8	3.1	204.5	2.5	6.6	23.5	20.8	9.4	` 4.5	15.0	8.1	18.2	4.6	672.2
14	26.8	10.2	9.0	3.6	213.2	3.0	7.7	26.6	22.2	11.0	5.9	16.3	9.1	21.6	5.3	748.3
15	30.2	11.6	10.4	4.0	199.2	3.6	9.4	29.0	23.5	6.4	3.3	17.4	9.6	22.4	5.7	793.5
16	30.6	12.2	11.0	4.1	197.8	4.1	10.2	29.7	23.8	5.9	3.0	17.9	9.7	22.5	5.8	814.6
17	48.2	40.4	7.0	4.2	197.0	13.8	26.4	29.8	23.9	7.7	2.9	18.1	4.4	6.4	5.8	1237.0
18	48.3	46.5	0.7	4.2	115.7	16.0	28.9	30.1	23.7	7.7	2.7	17.8	3.7	6.1	3.0	1188.8
19	48.0	47.0	6.1	4.1	101.4	16.2	28.6	15.3	11.1	7.4	2.4	16.7	3.0	5.7	2.2	1110.5
20	47.6	47.4	5.1	3.9	93.3	16.2	27.1	10.9	8.4	3.5	1.4	15.0	2.3	4.9	1.7	1048.7
21	49.5	49.2	4.5	1.8	50.4	16.8	27.6	8.7	6.6	2.6	1.0	6.9	1.8	4.2	1.3	989.0
22	47.0	48.0	3.8	1.3	38.3	16.3	26.0	6.9	5.1	2.2	0.7	5.6	1.4	3.5	1.1	919.2
23	44.5	44.7	3.2	1.0	30.4	15.3	23.8	5.6	4.1	1.8	0.6	4.6	1.1	2.7	0.8	840.5
24	41.8	42.9	2.6	8.0	24.4	14.5	22.1	4.4	3.0	1.4	0.4	3.6	0.8	2.1	0.6	775.8

JUNE

DAY		BUILDING TYPE														
HOUR	31	31A	32	33	34	35	36	37	38	39	40	41	42	43	44	TOTAL.
1	29.5	18.2	3.1	0.9	20.5	6.2	9.8	5.5	3.2	1.7	0.5	4.3	1.0	3.8	8.0	435.6
2	30.1	14.6	2.7	0.7	16.7	5.0	7.8	4.6	2.5	1.4	0.4	3.5	0.8	3.1	0.6	381.3
3	27.1	12.3	2.3	0.6	13.4	4.2	6.2	3.6	1.8	1.1	0.3	2.8	0.6	2.6	0.5	322.0
4	24.9	10.2	2.0	0.5	10.7	3.3	5.1	2.8	1.1	0.9	0.1	2.1	0.4	2.1	0.3	274.3
5	22.7	8.5	1.7	0.4	121.4	2.6	3.8	2.2	0.5	0.6		1.7	0.2	1.7	0.2	341.1
6	22.0	7.4	1.5	0.4	139.7	2.2	3.0	1.8		0.5		1.4	0.1	1.3	0.1	335.3
7	23.5	7.6	3.9	0.4	163.0	2.2	3.7	2.6	10.7	0.5	0.2	1.3	0.2	1.5	0.3	404.3
8	25.4	8.6	5.3	0.6	179.5	2.4	4.9	13.7	12.7	1.8	0.4	2.6	0.6	1.8	3.1	507.3
g	27.4	10.0	6.8	2.3	191.4	2.7	5.9	20.9	14.4	2.5	0.7	11.2	4.8	21.5	4.3	628.3
10	31.1	11.5	8.6	3.3	181.5	3.3	7.9	25.4	16.4	3.3	1.2	13.8	7.0	23.5	4.8	708.0
11	32.8	12.5	10.0	3.8	183.9	3.6	8.9	28.2	18.0	4.1	1.8	15.9	8.4	25.3	5.5	764.8
12	34.7	12.7	11.3	4.1	212.6	3.8	9.2	30.6	20.1	11.1	6.4	17.5	9.3	27.3	6.1	843.4
13	36.1	13.1	12.4	4.3	222.5	4.0	9.6	32.4	21.9	13.1	7.9	18.9	10.2	29.2	6.6	890.7
14	39.6	13.7	14.2	4.8	230.1	4.4	10.4	35.4	23.7	14.5	9.6	20.0	11.0	32.3	7.3	960.1
15	43.5	15.2	16.0	5.2	202.8	5.0	12.1	38.2	25.2	7.9	4.5	21.2	11.6	35.1	7.8	994.9
16	42.4	15.3	15.7	5.2	200.3	5.5	13.0	37.9	25.7	7.2	3.9	21.3	11.5	33.8	7.6	999.6
17	62.3	54.1	9.1	5.3	200.0	18.4	34.4	38.4	26.0	9.7	3.7	21.5	5.0	9.0	7.8	1543.3
18	59.5	60.7	8.5	5.3	129.9	20.7	36.7	38.1	26.1	9.9	3.5	21.2	4.3	8.8	3.8	1486.2
19	59.9	59.8	7.8	5.1	117.0	20.5	35.6	18.7	12.4	9.5	3.2	19.9	3.6	8.5	2.9	1376.4
20	57.6	58.4	6.8	4.8	105.4	19.7	33.5	13.5	9.8	4.5	1.9	17.9	2.9	7.3	2.2	1278.3
21	58.3	58.8	6.0	2.1	52.0	19.8	33.2	10.8	7.8	3.5	1.5	8.6	2.3	6.3	1.8	1176.8
22	56.8	58.6	5.2	1.6	39.4	19.6	31.9	9.2	6.5	2.9	1.1	7.2	1.9	5.6	1.5	1119.2
23	55.1	56.3	4.7	1.2	31.4	18.9	30.4	7.7	5.2	2.4	0.9	6.2	1.6	5.1	1.3	1058.2
24	52.2	54.3	4.0	1.1	25.4	18.0	28.1	6.6	4.2	2.0	0.7	5.2	1.3	4.3	1.1	983.1

JULY

DAY	BUILDING TYPE															
HOUR	31	31A	32	33	34	35	36	37	38	39	40	41	42	43	44	TOTAL
1	28.3	17.2	2.9	0.8	20.2	5.7	8.7	4.8	4.6	1.5	0.4	3.7	0.8	3.2	0.7	405.4
2	29.8	14.0	2.5	0.7	16.3	4.6	7.0	3.9	3.8	1.2	0.3	3.1	0.6	2.7	0.6	363.1
3	27.1	11.4	2.2	0.5	13.2	3.8	5.7	3.1	3.1	1.0	0.2	2.6	0.5	2.2	0.4	309.2
4	24.8	9.7	2.0	0.5	10.6	3.0	4.4	2.4	2.4	0.8	0.1	2.0	0.3	1.8	0.3	261.5
5	23.8	8.1	1.7	0.4	121.7	2.4	3.4	2.1	1.9	0.6		1.5	0.2	1.4	0.2	340.8
6	23.1	7.0	1.6	0.3	140.1	2.0	2.6	1.5	1.4	0.4	i	1.2	0.1	1.2	0.1	334.4
7	24.2	6.9	4.3	0.4	165.8	1.9	3.3	2.3	13.1	0.4	0.2	1.0	0.2	1.4	0.3	405.2
8	27.1	8.3	6.3	0.5	184.4	2.2	4.4	14.3	16.0	1.7	0.4	2.2	0.5	1.7	3.4	521.0
9	29.4	9.4	7.9	2.3	196.2	2.5	5.7	22.1	18.3	2.4	0.8	11.1	4.8	24.6	4.7	655.1
10	32.7	11.0	9.7	3.5	182.6	3.1	7.5	26.7	20.4	3.3	1.3	14.4	7.6	26.0	5.2	729.2
- 11	34.8	12.0	11.1	4.0	184.6	3.4	8.6	29.2	22.3	4.2	1.9	16.2	8.6	27.6	5.8	787.2
12	37.0	12.3	12.7	4.3	218.2	3.6	8.9	31.9	24.1	11.9	6.5	17.7	9.7	30.7	6.5	875.3
13	37.9	12.3	13.8	4.6	228.6	3.8	8.8	33.7	25.6	14.0	8.3	18.9	10.5	32.1	7.0	911.6
14	39.6	12.5	14.6	4.8	232.6	4.1	9.7	35.2	27.2	14.8	8.9	19.8	11.0	33.2	7.3	955.0
15	41.1	13.8	15.4	5.0	202.7	4.6	11.1	36.7	28.9	7.8	4.5	20.5	11.4	33.7	7.5	959.9
16	41.1	13.6	15.5	5.1	200.0	5.0	11.5	37.0	29.2	6.9	4.0	20.5	11.3	34.1	7.5	965.9
17	60.1	49.8	8.7	5.1	199.6	17.0	31.8	36.7	29.3	9.1	3.6	20.2	4.6	7.7	7.4	1469.5
18	57.1	58.5	7.9	5.1	127.6	20.1	35.2	36.3	29.5	9.3	3.3	20.0	3.9	7.6	3.5	1435.8
19	58.6	58.0	7.2	5.0	116.9	19.7	34.1	17.5	14.0	9.0	3.0	18.7	3.2	7.2	2.6	1331.4
20	56.4	57.2	6.2	4.7	103.5	19.5	32.5	12.4	11.0	4.2	1.8	16.8	2.5	6.2	2.1	1246.0
21	56.0	56.9	5.4	2.0	51.4	19.1	31.2	9.5	9.2	3.2	1.3	7.7	2.0	5.6	1.7	1121.7
22	54.1	55.0	4.7	1.4	38.9	18.6	30.0	8.1	7.6	2.6	1.0	6.4	1.7	4.9	1.4	1058.3
23	51.4	53.0	4.1	1.2	30.9	17.7	28.0	6.7	6.3	2.1	0.8	5.4	1.3	4.3	1.2	985.1
24	50.6	52.2	3.5	1.0	24.9	17.2	26.8	5.8	5.3	1.8	0.6	4.5	1.1	3.7	0.9	941.6

AUGUST

DAY								BUILD	ING	TYPE						
HOUR	31	31A	32	33	34	35	36	37	388	39	40	41	42	43	44	TOTAL
1	30.5	17.6	3.1	0.8	20.4	6.0	9.0	5.0	4.1	1.5	0.5	4.0	0.9	3.4	0.8	425.
2	30.8	14.0	2.8	0.7	16.4	4.7	7.3	4.2	3.3	1.2	0.4	3.3	0.7	2.9	0.6	374
3	27.8	11.8	2.4	0.6	13.4	3.9	5.7	3.4	2.8	1.0	0.3	2.7	0.5	2.4	0.5	316
4	25.6	9.7	2.1	0.5	10.7	3.1	4.6	2.7	2.2	8.0	0.2	2.1	0.3	1.7	0.3	269
5	23.6	8.5	1.8	0.4	121.7	2.6	3.7	2.0	1.7	0.6		1.6	0.2	1.3	0.2	345
6	22.1	7.0	1.6	0.3	139.8	2.0	2.9	1.5	1.4	0.4		1.2	0.1	1.1	0.1	333
7	21.9	6.4	3.5	0.3	162.3	1.8	2.8	1.6	13.0	0.3	0.2	0.5		0.9	0.1	374
8	24.0	7.5	4.9	0.4	178.9	2.0	3.9	12.3	16.6	1.4	0.3	1.5	0.3	1.0	2.9	478
9	26.9	8.6	6.4	2.1	190.8	2.4	5.1	19.3	18.9	2.1	0.6	10.3	4.4	21.4	4.1	608
10	28.8	10.6	7.8	3.1	181.1	2.8	6.9	23.6	20.9	3.0	1.1	13.4	6.7	21.2	4.5	673
11	30.2	11.3	9.0	3.5	183.4	3.2	7.8	26.1	22.8	3.9	1.7	15.2	8.1	23.1	5.1	725
12	32.6	11.7	10.7	3.9	211.6	3.4	8.1	28.8	24.7	10.8	5.6	16.8	9.2	26.2	5.8	808
13	35.2	11.6	12.6	4.2	224.4	3.5	8.3	31.6	26.5	13.2	7.5	18.2	10.3	29.5	6.5	867
14	37.7	12.3	13.9	4.6	229.8	4.0	9.2	33.7	27.7	14.3	8.4	19.3	11.0	31.1	6.9	923
15	41.0	13.7	15.4	4.9	202.6	4.6	11.0	36.2	28.6	7.8	4.5	20.5	11.5	33.7	7.4	954
16	41.7	14.3	16.0	5.1	200.1	5.1	11.8	37.0	29.1	7.1	4.0	20.9	11.6	33.1	7.5	976
17	60.7	51.6	9.1	5.2	200.0	17.6	33.1	37.2	29.0	9.4	3.8	20.8	4.9	7.9	7.5	1503
18	59.0	60.8	8.3	5.3	131.9	20.7	36.4	37.4	28.8	9.6	3.5	20.4	4.00	7.8	3.6	1480
19	59.2	58.8	7.4	5.0	118.7	19.8	34.4	17.4	13.7	9.0	3.1	18.7	3.30	7.2	2.6	1342
20	57.7	58.7	6.5	4.8	107.2	19.9	33.2	12.3	10.4	4.1	1.8	17.2	2.60	6.4	2.0	1271
21	58.0	59.2	5.7	2.0	51.7	19.8	32.7	10.0	8.6	3.2	1.3	8.1	2.10	5.7	1.7	1164
22	57.2	58.3	5.1	1.5	39.1	19.4	31.5	8.3	7.0	2.6	1.0	6.8	1.8	5.1	1.4	1109
23	54.5	56.5	4.5	1.2	31.1	18.5	29.6	7.2	6.0	2.2	0.8	5.7	1.5	4.4	1.2	1038
24	52.5	54.5	3.9	1.0	25.2	17.7	27.9	6.0	5.0	1,8	0.7	4.9	1.2	3.9	1.0	97

SEPTEMBER

DAY	BUILDING TYPE															
HOUR	31	31A	32	39	34	35	36	37	38	39	40	41	42	43	44	TOTAL
1	22.8	14.8	1.9	0.6	19.6	4.8	7.0	3.2	3.9	1.0	0.3	2.6	0.6	1.5	0.4	327.9
2	23.4	11.4	1.6	0.5	15.7	3.8	5.1	2.4	3.0	0.7	0.1	2.0	0.4	8.0	0.2	277.3
3	19.9	9.2	1.2	0.4	12.5	2.8	3.8	1.6	2.3	0.4		1.3	0.1	0.3	0.0	218.6
4	18.2	7.2	0.9	0.3	9.9	2.1	2.5	0.8	1.7	0.2	1	0.8			0.0	174.6
5	15.7	5.5	0.6	0.2	120.0	1.6	1.7		1.1			0.2			0.0	248.8
- 6	14.2	4.5	0.3	0.1	137.7	0.8	0.8	1	0.5			0.1			0.0	236.5
7	13.2	3.3	0.6		152.4	0.5			11.3						0.0	251.2
8	15.2	4.3	1.5	0.2	165.6	0.8	1.4	6.0	13.9						0.0	318.3
9	16.9	5.5	2.6	1.4	177.7	1.2	2.7	12.7	16.0	1.0		6.5	2.5	9.9	2.8	436.7
10	19.6	7.0	4.3	2.2	178.1	1.5	4.0	16.9	18.1	1.9		10.3	5.0	14.7	3.1	511.4
- 11	21.5	7.7	5.9	2.8	181.5	1.8	4.9	20.2	20.5	2.7	0.8	12.5	7.0	16.7	3.9	573.4
12	23.2	8.5	7.4	3.1	200.1	2.1	5.4	22.7	23.1	8.4	4.4	14.3	8.2	18.7	4.5	645.5
13	25.3	8.6	8.7	3.4	209.7	2.3	5.9	24.8	25.0	10.3	5.8	15.7	9.1	20.4	5.0	698.0
14	28.6	9.7	10.4	3.8	218.7	2.8	7.2	27.5	27.1	11.8	7.1	17.3	10.1	21.8	5.6	774.7
15	31.5	10.4	11.7	4.1	199.8	3.2	8.3	30.0	28.3	6.4	4.1	18.2	10.5	24.8	6.1	801.6
16	33.4	10.9	12.5	4.3	197.9	3.7	9.4	31.2	28.8	6.0	3.7	18.9	10.6	25.6	6.2	837.2
17	51.9	42.8	7.7	4.4	197.9	14.4	27.3	31.2	28.8	7.9	3.5	18.7	4.6	6.3	6.3	1298.7
18	49.7	49.8	6.9	4.4	121.4	17.2	29.7	30.7	28.6	7.8	3.1	17.6	3.7	5.9	2.9	1244.6
19	50.7	49.5	5.8	4.2	109.6	16.8	28.1	13.5	13.6	7.5	2.6	15.9	2.9	5.1	2.0	1131.3
20	51.1	51.2	5.2	4.2	100.7	17.4	28.4	9.8	10.7	3.2	1.5	15.2	2.3	4.3	1.6	1110.7
21	50.9	51.5	4.5	1.7	50.6	17.3	27.9	7.8	8.7	2.6	1.1	6.6	1.8	3.9	1.3	1009.4
22	48.8	49.8	3.8	1.2	38.2	16.7	26.2	6.5	7.1	2.0	0.8	5.5	1.5	3.3	1.1	939.4
23	46.7	47.1	3.3	0.9	30.4	15.8	24.6	5.2	5.9	1.7	0.6	4.5	1.2	2.6	0.8	873.4
24	44.2	45.5	2.7	0.8	24.4	14.9	22.5	4.1	4.8	1.3	0.4	3.6	0.9	2.1	0.6	804.5

OCTOBER

DAY								BUILD	ING	TYPE						
HOUR	31	AIE	32	33	34	35	36	37	38	39	40	41	42	43	44	TOTAL
1	10.3	8.3		0.1	17.0	2.2	1.5		1.2				************			123.7
2	7.2	4.9			13.0	1.0		1	0.4							65.6
3	5.4	2.4			10.4	0.1										42.8
4	3.5	0.8			8.3											27.4
5	2.4				117.8											129.8
6	1.1				135.2											140.7
7	1.1				146.4				2.3							156.5
8	2.5				154.7			1	10.1							187.4
g	4.8				161.4				11.8					0.7		209.7
10	7.0				166.8				14.2			2.6	0.8	2.9		239.1
11	8.8			1.8	171.3				17.0			6.8	4.9	2.2		279.0
12	10.7			2.0	177.7			10.2	19.3			10.2	6.3	2.8	2.0	345.7
13	11.6			2.2	194.2			15.9	21.2	3.0	3.4	11.3	7.2	3.9	2.9	400.7
14	13.1		2.3	2.4	198.7			16.5	22.5	8.1	4.6	12.2	7.6	4.7	3.2	431.5
15	14.4	2.1	5.6	2.5	194.2			17.5	23.5	4.2	2.8	12.8	7.8	5.2	3.3	442.5
16	15.0	4.1	5.8	2.6	193.2			17.6	23.8	3.8	2.5	13.2	7.7	4.8	3.2	448.8
17	28.0	24.3	4.2		192.5	1.1	4.5	17.2	23.6	4.7	2.1	12.7	3.5	0.0	3.1	614.5
18	28.4	25.5	3.3	2.5	97.8	9.3	15.2	15.8	22.9	4.2	1.7	11.2	2.4	0.9	1.4	710.6
19	29.4	27.7	2.6	2.4	84.5	10.1	15.4	6.4	10.5	3.9	1.2	10.2	1.7	0.5	0.8	661.0
20	31.3	29.8	1.8	2.4	73.9	10.7	15.7	4.1	7.8	1.3	0.5	9.5	1.2		0.5	653.3
21	29.8	29.4	1.2	0.9	46.9	10.5	14.9	2.6	6.1	0.8	0.1	2.4	0.7		0.2	572.3
52	28.1	28.3	0.7	1	35.9	10.0	13.8	1.2	4.6	0.4		1.4	0.3			518.8
23	26.7	27.1	0.3		28.1	9.6	12.8		3.2			0.4				474.9
24	25.6	26.0		0.2	22.0	9.0	11.5		2.1							433.7

NOVEMBER

DAY	BUILDING TYPE															
HOUR	31	31A	32	33	34	35	36	37	38	39	40	41	42	43	44	TOTAL
1	9.2	7.3			16.8	1.8	0.9		1.0	***************************************		0.0				103.7
2	6.0	4.0			13.0	0.6										54.6
3	3.6	1.5			10.4	ļ										31.4
- 4	1.7				8.3	- 1	-							!		16.8
5	0.6				117.7											120.7
6					134.7											134.7
7					145.9	1			0.8							147.5
8					153.9		ĺ		9.2							172.3
9	0.6				160.3	-			10.5							184.3
10	2.6				165.7				12.8							204.3
11	4.0				170.2				15.1			4.7	3.2			233.0
12	5.6			1.5	173.8				17.4			6.9	5.1	0.8		263.8
13	7.5			1.7	178.5			2.2	19.3		2.1	9.2	5.9	2.0	0.8	302.3
14	9.5			1.9	191.7			13.1	20.9	3.2	4.5	10.3	6.5	3.1	2.3	373.0
15	11.4			2.2	191.4			14.3	22.2	3.4	2.5	11.3	7.1	3.9	2.6	392.7
16	12.3		3.2	2.3	191.3			15.2	23.0	3.1	2.3	11.8	7.3	4.2	2.8	406.8
17	24.6	1.1	3.4	2.3	191.0			14.8	22.8	4.0	2.0	11.3	3.1		2.7	459.6
18	25.2	22.9	2.6	2.2	95.5			13.6	22.1	3.7	1.5	10.1	2.2		1.0	387.9
19	25.4	23.7	2.0	2.2	82.2	8.5	9.9	5.0	9.9	6.4	1.0	9.4	1.5		0.6	531.4
20	26.8	25.7	1.4	2.2	72.0	9.3	13.0	2.9	7.3	0.9	0.3	8.9	1.0		0.3	563.4
21	27.5	26.9	0.9	0.7	46.2	9.5	12.8	1.6	5.8	0.6	0.1	2.0	0.6		0.1	511.8
22	26.0	26.3	0.4	0.5	35.5	9.2	12.3	0.4	4.3	0.2		1.0	0.3	l		472.6
23	25.0	25.5		0.3	27.8	8.8	11.5		3.1	1		0.1			1	437.0
24	23.2	23.6		0.1	21.8	8.3	10.5		2.1		<u> </u>		<u> </u>	<u> </u>	<u> </u>	397.0

DECEMBER

DAY								BUILD	ING '	TYPÉ						
HOUR	31	31A	32	33	34	35	36	37	38	39	40	41	42	43	44	TOTAL.
1	3.9	4.0			15.8	0.4										45.7
2	0.9	1.0			12.6											19.1
3					10.1								_			10.1
4					8.1											8.1
5					117.2				1							117.2
5			1		134.4											134.4 145.6
7					145.6				2.9							159.5
8			İ		153.7 160.1				9.6							179.3
10					165.4				11.8							189.0
11	1.0	,			169.9				13.9			2.2	1.6			208.7
12	2.5				173.5				16.2			4.8	4.6			232.6
13	3.5			1.2	176.6				18.0			7.1	5.4	0.7		256.4
14	4.3			1.7	181.7			0.9	19.6		3.8	8.8	6.0	1.2		281.3
15	5.3		İ	1.8	190.7			11.3	20.6		2.7	9.2	6.3	1.4		318.8
16	6.0			1.9	190.3			11.3	21.4	0.3	2.3	9.6	6.3	1.4	0.6	329.5
17	18.2	2		1.9	189.5			10.5	21.1	3.4	1.8	9.0	2.5		1.9	394.1
18	19.0			1.7	88.2			9.3	20.4	2.7	1.2	7.7	1.5		1.8	286.3
19	19.3	3		1.6	71.7	2.7		2.1	8.6	2.2	0.6	6.9	0.9		1.8	245.7
20	19.1	1	1	1.5	59.8	6.8	3.2		6.1	0.1		6.4	0.4		0.5	317.1
21	19.0	1	1	0.4	43.6	6.7	8.1		4.3				l			347.5
22	18.3		1	0.2	33.5	6.7	7.6		2.8							321.8
23	17.8		4		25.9	6.6	7.1		1.6				1			300.2
24	17.0	17.6			20.1	6.3	6.5		0.6						1	276.8

TONNAGE PROFILE BY MONTH

DAY HOUR	JAN	FEB	MAR	APR	MAY	JUN	JUL	AUG	SEP	OCT	NOV	DEC
1	16.7	26.3	108.8	224.4	327.8	435.6	405.4	425.1	327.9	123.7	103.7	45.7
2	12.1	12.5	54.0	158.3	265.5	381.3	363.1	374.0	277.3	65.6	54.6	19.1
3	9.7	9.9	30.1	112.7	205.1	322.0	309.2	316.3	218.6	42.8	31.4	10.1
4	7.6	7.8	16.8	73.3	158.7	274.3	261.5	269.7	174.6	27.4	16.8	8.1
5	116.0	116.3	117.1	164.4	229.8	341.1	340.8	345.9	248.8	129.8	120.7	117.2
6	133.4	133.5	134.5	173.8	214.8	335.3	334.4	333.5	236.5	140.7	134.7	134.4
7	144.8	144.7	146.1	182.2	258.5	404.3	405.2	374.8	251.2	156.5	147.5	145.6
8	153.0	152.7	175.6	215.0	319.3	507.3	521.0	478.3	318.3	187.4	172.3	159.5
9	167.3	168.1	193.0	241.5	407.2	628.3	655.1	608.6	436.7	209.7	184.3	179.3
10	184.9	183.1	213.4	312.5	488.8	708.0	729.2	673.7	511.4	239.1	204.3	189.0
11	196.0	192.1	246.9	396.6	550.5	764.8	787.2	725.5	573.4	279.0	233.0	208.7
12	213.5	209.5	270.1	481.8	612.9	843.4	875.3	808.9	645.5	345.7	263.8	232.6
13	221.1	219.8	309.9	528.0	672.2	890.7	911.6	867.8	698.0	400.7	302.3	256.4
14	233.8	231.4	351.2	586.5	748.3	960.1	955.0	923.2	774.7	431.5	373.0	281.3
15	249.7	243.7	359.7	635.1	793.5	994.9	959.9	954.8	801.6	442.5	392.7	318.3
16	272.8	254.5	375.0	648.7	814.6	999.6	965.9	976.1	837.2	448.8	406.8	329.5
17	345.5	335.3	487.4	1007.5				1503.9		614.5	459.6	394.1
18	230.7	245.7	652.4		1188.8					710.6	387.9	286.3
19	175.2	190.4	617.9			1376.4				661.0	531.4	245.7
20	183.6	200.4	582.9	814.1		1278.3		•		653.3	563.4	317.1
21	150.4	305.7	511.1	745.5		1176.8					511.8	347.5
22	208.3	278.5	476.6	698.2		1119.2			939.4	518.8	472.6	321.8
23	180.2	256.5	436.9	645.1	1	1058.2	985.1	1038.4		474.9	437.0	300.2
24	153.0	232.8	395.5	583.6	775.8	983.1	941.6	977.7	804.5	433.7	397.0	276.8

Table 2B

		BUILDING 2533		V
	PLANI	COOLING	SUMMAR	Y
CAPACITY	% PLANT	BIN	HOURS	HOURSPER
TONS		LIMIT-TONS	PERBIN	REP DAY
1600	10	160	1152	3.16
	20	320	2536	6.95
	30	480	1680	4.60
• ,	40	640	795	2.18
	50	800	671	1.84
	60	960	611	1.67
	70	1120	581	1.59
	80	1280	367	1.01
	90	1440	183	0.50
	100	1600	184	0.50

Table 3B

ROWLAND
01!Fort Gordon
P1CARLTON SHUFORD
P2DSN 780-6376
P3ATZH-DIC-E
/RECALL F 000045554 S 03

ECIP PROJECT 2: UPGRADE CHILLER PLANT BUILDING 25330, FT. GORDON

03A !DESCRIPTION OF PROPOSED CONSTRUCTION

***Upgrade chillers, accessories and the chilled water distribution system at the Central Utility Plant, South side of the Ft. Gordon Installation. Several innovative modifications to the central chilled water system are required to meet current and future cooling requirements for all building on the northern half of the facility. Replacement of obsolete equipment with new high efficiency systems will reduce energy requirements significantly while increasing the net cooling capacity for the barracks, classrooms and administrative buildings.

03B !REMARKS

***This Energy conservation measure to replace the existing chilled water system consists of eight ECO's, which were combined to create one comprehensive ECIP. Each ECO was developed from field studies of the South Side Central Utility Plant. The economics of incorporating all ten ECO's is explained in the economic justification section of this document. The ten ECO's are described below to provide extra insight into the comprehensive approach taken.

ECO NO.	DESCRIPTION
7	Chilled Water Chemical Treatment
20	Replace Chillers
24	Variable Speed Pumping System
30	Temperature Reset System
44	Cooling Tower Manifold
48	Condenser Water Chemical Treatment
54	Chilled Water Storage System
87	EMCS Controls and Instrumentation

ECO DATA COMPILATION

ECO NO.	DESCRIPTION	COST (FROM LCC)	SAVINGS 1ST YEAR	TOTAL DISCOUNT SAVINGS
7	Chem Treatment-CHW	15,510	17,000	361,040
20	Chiller Replacement	412,620	155,632	2,427,680
24	Variable Speed Pumping	318,126	50,436	787,309
30	CHW Temperature Reset	15,596	2,393	37,351
44	Cooling Tower Manifold	34,139	3,037	48,033
48	Condenser Water Chemical Treat.	1,968	4,167	64,061
54	Chilled Water Storage	281,121	75,868	1,118,298
87	EMCS Controls & Instrumentatio		5,158	80,516
	Totals	1,127,997	313,691	4,924,288

Simple Payback: 1,127,997 = 3.64

313,691

SIR: $\frac{4,924,288}{1} = 4.37$

1,127,997

03C PROJECT DESCRIPTION

***This Energy conservation measure provides the plan to design the required upgrade to the Central Utility Plant, South. Removal and replacement of five inefficient chillers with three new ones properly sized to provide incremental increase in the chilled water capacity as the site load varies. The five old chillers being replaced include 3-700 ton units and 2-750 ton units for a combined capacity of 3,600 tons. The three new chillers have capacity of 1-400 ton chiller and 2-1,250 ton chillers for a combined total of 2,900 tons. The new units are sized to match the load change throughout the day, and have the capacity to replenish the chilled water storage system at night. The chilled water storage system will provide the capacity to make up the difference between the older units 3,600 tons and the capacity of the newer unit of 2,900 tons, or 700 tons. Since the peak demand for chilled water occurs over a short t period of time, the chilled water storage system will provide a capacity to meet a peak demand of 4,400 tons of refrigeration. This exceeds current demand by 800 tons and allows for less chiller capacity to meet current and future needs. Repiping of both the chilled water system and condenser water system will provide flexibility in selecting equipment to run. Current piping makes manual selection of equipment difficult and requires excessive manpower to change over as site loads vary. Consequently, it is easier for chilled water to run through all chillers than to try to control valves and pumps to meet load requirements. In addition to providing a new efficient piping design that is easy to operate, variable speed pumps will be introduced to further allow for energy efficient operation under all load conditions. With the addition of instrumentation and control, all chilled water control functions could be handled from a central location reducing the need for plant operators by fifty percent.

03D !REQUIREMENT (Why is it needed now)

****The chilled water system is not meeting current cooling requirements for the buildings served on the north side of the facility. New construction and renovations will increase the capacity on this system to meet current and future requirements. New CFC regulations for chiller refrigerants will require replacement of older chillers, and require system redesign of chilled water distribution by 1997.

If not implemented now, cooling capacity will not meet current or future needs.

03E !CURRENT SITUATION (How is the need currently being met)

***ECO 7

The existing chemical treatment system serves the condenser side of the chilled water system and is feeding a C-6220 chemical from Industrial Maintenance Corporation into the condenser water system. Additionally an A-102 microbicide is added to each cooling tower by the bucket as the algae begins to build up in the cooling towers. There is no chemical feed on the chilled water side of the system. Since there is a fairly large volume of make-up water to the chilled water side, water that is fed into the system is not treated water at this time, nor is there any way to treat the water with the present equipment.

ECO 20

See Figure 1B - Existing Chilled Water Schematic-Building 25330. Chillers 1 and 2 are the oldest chillers. Chillers 3 and 4 are the next in age. All chillers are 500 ton capacity.

ECO 24

This building has one chilled water loop with duplicate constant speed pumps circulating the water throughout this distribution loop. Buildings on the distribution loop all have 3-way valves and some have chilled water pumps within the building. The constant speed pumps have 350 horsepower motors, and the voltage used to drive them is 2300 volts.

ECO 30

Although the chillers are set to maintain a constant chilled water supply temperature, the temperature actually varies because some water is bypassed through non-operating chillers. The system is set to operate at a constant supply water temperature of approximately 42°F.

ECO 44

All four chillers are 500 ton capacity and each is piped to its own cooling tower.

ECO 48

There is currently water treatment based on a conductivity meter of the cooling tower water, but biocide is added manually by the scoopful only as needed.

From Table 2B in ECO 20, the highest available tonnage at any particular time is in June at 1700 hours where the load gets up to 1543.3 tons for that hour. This high rate occurs when the maximum demand at the base occurs and will cause the electric bill to be based on a higher demand.

ECO 87

Existing automatic or manual controls that are within the plant are not remotely operable by the EMCS by design. The EMCS office which is manned 24 hours a day has very few, if any, instrumentation readouts from the plant, and no control of the plant with the EMCS. Because EMCS personnel are aware of what is happening in many buildings, they are also aware of conditions and demands in the chilled water system. Currently, the boiler operators are making boiler pressure changes, HTW changes, bringing on and off chillers, cooling towers, and many manual valving operations. However, they are not performing the functions that an EMCS office can to control energy and to improve the operating efficiency of the plant.

03F !IMPACT IF NOT PROVIDED

***If this project is not accomplished, Fort Gordon will continue to use excessive energy to supply chilled water to the buildings on the north side of the facility. Because of old inefficient chillers and a distribution system that does not respond to reduced load conditions, all equipment must run all the time to provide adequate cooling. The existing system requires high electrical consumption at all times and high demand for electricity during the entire cooling season.

03G !ADDITIONAL

***Not Applicable

03I !RELATED PROJECTS

***ECIP - 45553 - Chilled Water System to Central Utility Plant - Building 25330 North Side

ECIP - 45555 - High Temperature Water Systems North Plant - Building 25910

ECIP - 45556 - High Temperature Water System South Plant - Building 25330 /*

07A !GENERAL JUSTIFICATION DATA

***This ECIP project is required to support the Army wide effort to reduce energy consumption. The project will reduce energy consumption by upgrading the chilled water system at the Central Plant South, Building 25330, Ft. Gordon. The project will replace two old inefficient 500 ton chillers with two new high efficiency chillers, replace two 2300 volt pumps with new 480 volt pumps and add variable speed driver. In addition, new control instrumentation will allow connection to the existing EMCS system.

The project has been coordinated with the installation physical security plan and no security improvements are required.

The project includes eight ECO's combined to provide a comprehensive upgrade to the facility chilled water system. The following overview lists the ECO's along with the economic justification.

PROJECT NO. 2 - CHILLED WATER SOUTH

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TOTAL DISCOUNT SAVINGS	361,040	2,427,680	787,309	37,351	48,033	64,061	1,118,298	80,516	4,924,288
SAVINGS 1st YEAR	17,000	155,632	50,436	2,393	3,037	4,167	75,868	5,158	313,691
DEMAND SAVINGS	0	0	0	0	0	0	75,868	0	75,868
NAT GAS SAVINGS MMBTU/YR	0	0	0	0	0	0	0	0	10
ELECTRICAL SAVINGS MMBTU/YR	0	1,008.60	3,310.36	157.05	32.9	130.87	0	338.54	14,053.32
COST (From LCC)	15.510	412,620	318,126	15,596	34,139	1,968	281,121	48.917	1,127,997
NON- RECURRING DISCOUNTED COST (-) SAVINGS (+)	420.000	00000	0	· C	10 728	3 456	6	0	434,184
ANNUAL RECURRING <u>COST</u>	4 000	2,000	o i	o C	000 6	2,000	000,	> <	2,000
CONSTRUCTION COST	13 910 40	370.062.00	285 314 40	13 986 00	30.585.00	1 765 26	752 126 00	73 870 68	1,011,652.70
ECO DATA COMPLATION ECO DESCRIPTION	THE STATE OF THE S	Chem I reatment-Ch w	Chiller Replacement	Variable Speed Fulliphing	CHW lemperature Keset	Cooling Tower Manifolding	Condenser water Chemical Treatment	Chilled Water Storage	EMCS Controls and instrumentation Totals
ECO NO.	t	- 6	2 2	47 6	30	44	48	54	/ 8

Simpler Payback:

 $\frac{1,127,997}{313,691} = 3.60 \text{ years}$

 $\frac{4,924,288}{1,127,997} = 4.37$

SIR:

07B !TRAFFIC ANALYSIS

*** There will be no changes to pedestrian or vehicular traffic as a result of implementing this ECIP.

/*

08B !PRESENT ACCOMMODATIONS AND DISPOSITION

***The physical plant building 25330 housing the chilled water system is adequate to accommodate the new chillers, once the old chillers are removed. The chilled water storage tank will be located outside in a vacant field adjacent to the cooling towers.

09D !RPMA DISCUSSION

***This ECIP will reduce the amount of Real Property Maintenance Required.

10A !ANALYSIS OF DEFICIENCIES

- ***1) Chemical treatment of makeup water not being performed on the chilled water due to large amount of makeup water required.
- 2) Existing constant speed pumping system is not able to adjust chilled water flow to meet air conditioning load changer. The pumps run continuously so more water is circulated than requiring during off peak load condition. Energy is wasted as a result of the pumping costs.
- 3) The chillers and the chilled water system is currently run manually. There is little instrumentation to assist the operator in scheduling equipment to run at reduced load. Running the plant is labor intensive and susceptible to inefficient operation.
- 4) Excessive makeup water requirements make water treatment impractical and costly. Water losses need to be reduced dramatically.
- 5) All chillers run during peak A/C load condition. Excessive use of electricity causes high demand conditions to exist. These peak loads occur over a relatively short period of time during peak summer conditions.
- 6) Two of the four chillers are at the end of their useful life. They are very inefficient and do not meet the requirements to eliminate CFC refrigerant.

11D !DECISION ANALYSIS

***The following is a detailed cost breakdown of each of the ECO's. Refer to the table in 7A General Justification Data which summarizes these costs.

ECO 7 - LCCA

1.	Investment	
1.	A. Construction Cost	\$ 13,910.00
	B. SIOH	\$ 765.00
	C. Design Cost	\$ 835.00
	D. Total Cost $(1A + 1B + 1C)$	\$ 15,510.00
2.	Energy Savings	\$ -5,994.00
3.	Non Energy Savings	\$ 361,040.00
4.	First Year Dollar Savings	\$ 17,000.00
5.	Simple Payback Period	\$ 1.10 Years
6.	Total Net Discounted Savings	\$ 361,040
7.	Savings to Investment Ratio	\$ 23.28
ECO	20 - LCCA	
1.	Investment	
	A. Construction Cost	\$ 370,062.00
	B. SIOH	\$ 20,354.00
	C. Design Cost	\$ 22,204.00
	D. Total Cost $(1A + 1B + 1C)$	\$ 412,620.00
2.	Energy Savings	\$ 4,090.00
3.	Non Energy Savings	\$ 29,480.00
4.	First Year Dollar Savings	\$ 155,632.00
5.	Simple Payback Period	\$ 2.65 Years
6.	Total Net Discounted Savings	\$ 2,427,680.00
7.	Savings to Investment Ratio	\$ 5.88
ECO	24 - LCCA	
1.	Investment	
	A. Construction Cost	\$ 285,314.00
	B. SIOH	\$ 15,693.00
	C. Design Cost	\$ 17,119.00
	D. Total Cost $(1A + 1B + 1C)$	\$ 318,126.00
2.	Energy Savings	\$ -2,684.00
3.	Non Energy Savings	\$ 0.00
4.	First Year Dollar Savings	\$ 50,436.00
5.	Simple Payback Period	\$ 6.31 Years
6.	Total Net Discounted Savings	\$
7.	Savings to Investment Ratio	\$ 2.47

ECO 30 - LCCA

1.	Investment		
	A. Construction Cost	\$	13,986.00
	B. SIOH	\$	770.00
	C. Design Cost	\$	840.00
	D. Total Cost $(1A + 1B + 1C)$	\$	15,596.00
2.	Energy Savings	\$	-5,837.00
3.	Non Energy Savings	\$	0.00
4.	First Year Dollar Savings	\$	2,393.00
5.	Simple Payback Period	\$	6.52 Years
6.	Total Net Discounted Savings	\$	37,351.00
7.	Savings to Investment Ratio	\$	2.39
ECO	44 - LCCA		
1.	Investment		
	A. Construction Cost	\$	30,618.00
	B. SIOH	\$	1,684.00
	C. Design Cost	\$	1,837.00
	D. Total Cost $(1A + 1B + 1C)$	\$	34,139.00
2.	Energy Savings	\$	-5,961.00
3.	Non Energy Savings	\$	40,208.00
4.	First Year Dollar Savings	\$	3,037.00
5.	Simple Payback Period	\$ \$	11.24 Years
6.	Total Net Discounted Savings		48,033.00
7.	Savings to Investment Ratio	\$	1.41
ECO	48 - LCCA		
1.	Investment		
	A. Construction Cost	\$	1,765.00
	B. SIOH	\$	97.00
	C. Design Cost	\$	106.00
	D. Total Cost $(1A + 1B + 1C)$	\$	1,968.00
2.	Energy Savings	\$	-5,863.00
3.	Non Energy Savings	\$	32,936.00
4.	First Year Dollar Savings	\$	4,167.00
5.	Simple Payback Period	\$.47 Years
6.	Total Net Discounted Savings	\$	64,061.00
7.	Savings to Investment Ratio	\$	32.55

ECO 54 - LCCA

1.	Investment	
	A. Construction Cost	\$ 252,126.00
	B. SIOH	\$ 13,867.00
	C. Design Cost	\$ 15,128.00
	D. Total Cost $(1A + 1B + 1C)$	\$ 281,121.00
2.	Energy Savings	\$ -5,994.00
3.	Non Energy Savings	\$ 0.00
4.	First Year Dollar Savings	\$ 75,868.00
5.	Simple Payback Period	\$ 3.71 Years
6.	Total Net Discounted Savings	\$ 1,118,298.00
7.	Savings to Investment Ratio	\$ 3.98

ECO 87 - LCCA

1.	Investment	
	A. Construction Cost	\$ 43,871.00
	B. SIOH	\$ 2,413.00
	C. Design Cost	\$ 2,633.00
	D. Total Cost $(1A + 1B + 1C)$	\$ 48,917.00
2.	Energy Savings	\$ -5,655.00
3.	Non Energy Savings	\$ 0.00
4.	First Year Dollar Savings	\$ 5,158.00
5.	Simple Payback Period	\$ 9.48 Years
6.	Total Net Discounted Savings	\$ 80,516.00
7 .	Savings to Investment Ratio	\$ 1.65

11E !ECONOMIC ANALYSIS ***ECO 7

ITEM DESCRIPTION	QUAN QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Chemical Feed System Test Coupon	1 1	LS LS	3,500 2,000	3,500 2,000	2,500 2,000	2,500 2,000	\$6,000.00 \$4,000.00
				20% OH (SUBTOTAL G SUBTOTAL (G			\$11,040.00 \$2,208.00 \$13,248.00 \$13,248.00 \$662.40 \$13910.40

ITEM DESCRIPTION	QUANTITY QUAN UNIT	MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
500 Ton Chiller	2 EA	112,000	224,000	25,000	50,000 \$2	74,000.00
			20% OH (SUBTOTAL G SUBTOTAL (G		\$ \$3 \$3 \$	93,700.00 58,740.00 52,440.00 52,440.00 17,622.00 70,062.00
ECO 24						
ITEM DESCRIPTION	QUANTITY QUAN UNIT	MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Materials Piping Controls & EMCS Instr. Variable Speed Drive Vacuum Contractors Transformer 480 Volt Motor Piping Changes Controls Electrical Work	4 EA 1 LS 1 LS 1 LS 1 LS 1 LS 1 LS 1 LS 1 LS	8,000 3,000 15,000 40,300 6,500 11,200 17,700 14,000 3,000 4,000	20% OH (SUBTOTAL G SUBTOTAL (G		1,500 \$ \$ 15,000 \$ \$ 1,500 \$ \$ 1,500 \$ \$ 4,000 \$ \$ 1,500 \$ \$ 2,000 \$ \$ 2,000 \$ \$ 2,000	36,000.00 4,5000.00 30,000.00 41,800.00 \$7,500.00 12,700.00 39,400.00 28,000.00 \$4,500.00 \$6,000.00 45,288.00 71,728.00 1,7280.00 13,586.40 85,314.40
ECO 30						
ITEM DESCRIPTION	QUANTITY QUAN UNIT	MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Controls	1 LS	5,000	5,000	5,000	5,000	\$10,000.00
				SUBTOTAL (GC ONLY) GC'S WORK		\$11,100.00 \$2,220.00 \$13,320.00
			SUBTOTAL (G 5% CON	C & SUBS) TINGENCY TOTAL		\$13,320.00 \$666.00 \$13,986.00

ITEM DESCRIPTION	QUAN' QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Piping Materials	1	LS	12,000	12,000	10,000	10,000	\$22,000.00
					UBTOTAL GC ONLY) C'S WORK		\$24,300.00 \$4,860.00 \$29,160.00
				SUBTOTAL (GO 5% CONT	C & SUBS) INGENCY TOTAL		\$29,160.00 \$1,458.00 \$30,618.00
ECO 47							
ITEM DESCRIPTION	QUAN QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	I TOTAL
Chemical Feed	1	LS	1,000	1,000	300	300	\$1,300.00
					UBTOTAL GC ONLY) C'S WORK		\$1,401.00 \$280.20 \$1,681.20
				SUBTOTAL (G 5% CONT	C & SUBS) TINGENCY TOTAL		\$1,681.20 \$84.06 \$1,765.26
ECO 54							
ITEM DESCRIPTION	QUAN QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	I TOTAL
Underground Chilled Water Storage Tank	1	LS	146,000	146,000	40,000	40,000 \$	\$186,000.00
				5% S 17% LA SU 20% GC OH SUBTOTAL	GC WORK	9	\$186,000.00 \$7,300.00 \$6,800.00 \$200,100.00 \$40,020.00 \$240,120.00
				5% CONT	TOTAL	9	\$12,006.00 \$252,126.00

ITEM DESCRIPTION	QUAN QUAN	TITY UNIT	MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	N TOTAL
Chiller Efficiency Soft Wa	re 1	LS			10,000	10,000	\$20,000.00
Flow Meter & Temp Dist.		LS	6,500	6,500	3,500	3,500	\$10,000.00
Pump Operating Controls	1	LS	2,500	2,500	1,500	1,500	\$4,000.00
Temperatures	1	LS	600	600	1,000	1,000	\$1,600.00
Chiller Amps	1	LS	1,000	1,000	1,000	1,000	\$2,000.00
Variable Speed & Switch	Ctrl. 1	LS	600	600	1,000	1,000	\$1,600.00
Pressures-CHW, Supply							
Return and Storage	1	LS	900	900	900	900	\$1,800.00
				SU	BTOTAL 1		\$31,000.00
					ALES TAX		\$605.00
				17% LA	ABOR TAX		\$3,213.00
				SU	BTOTAL 2		\$34,818.00
				20% GC OH	& PROFIT		\$6,963.60
				SUBTOTAL	GC WORK		\$41,781.60
							** ***
				5% CONT	TINGENCY		\$2,089.08
					TOTAL		\$43,870.68

/*

12A !CRITERIA FOR PROPOSED CONSTRUCTION

***Construction will conform to existing guidelines of architectural design and building construction, specifically the AEI Design Guide (March 1987), the Corps of Engineers Guide Specifications CEGS 13947 thru 13949 for EMCS, and TM 5-812-2.

13B !FURNISHINGS AND EQUIPMENT DISCUSSION

- ***1) Two chillers will be replaced with 2 new chillers.
- 2) Two variable speed pump driver will be added.
- 3) Rerouting of existing pipes to permit better control.
- 4) New sensors and controls will automate operation.
- 5) Chilled water storage tank to be added.

/*

15A !ENVIRONMENTAL DOCUMENTATION

***The refrigerant in four old chillers will need to be reclaimed. Permits will be required. The refrigerants have market value and can be disposed of by selling at current market value. There are no other environmental issues.

15B1 !SUMMARY OF ENVIRONMENTAL CONSEQUENCES

***We have reviewed this project and determined that an environmental impact statement, pursuant to PL

91-190, is not required. We have assessed this project and determined that it will not contribute significantly to air and/or water pollution.

16A1 !EVALUATION OF FLOOD HAZARDS

***The renovation is to an existing plant. No history of flooding has been recorded.

19A !SUMMARY OF ENERGY REQUIREMENTS

***The existing electric utility system in adequate to support the modifications, upgrades and new equipment recommendations. No changes will be required to meet the requirements and modifications. Peak load requirements will actually be reduced. Equipment operation will reflect the changing load requirements throughout the day allowing chillers and pumps to be scheduled more efficiently, thus reducing electric consumption and demand.

The engineering study reports electric consumption reduction to be 15,586,741 KWH and a demand reduction of 2,981.78 from first order effects to reducing equipment use, and chilled water storage.

19B ISUMMARY OF UTILITY SUPPORT

***The central utility plant connected load will be reduced by 15%. The existing electric utilities supplied to the central plant is adequate and will not require additional capacity to be added.

20B !HAZARDS TO HANDICAPPED PERSONS

***Existing conditions within the physical plant is considered hazardous to unauthorized personnel. Signs and warnings are posted to alert unauthorized personnel access is restricted to authorized personnel and visitors with prior approval.

20C !HANDICAP PROVISIONS

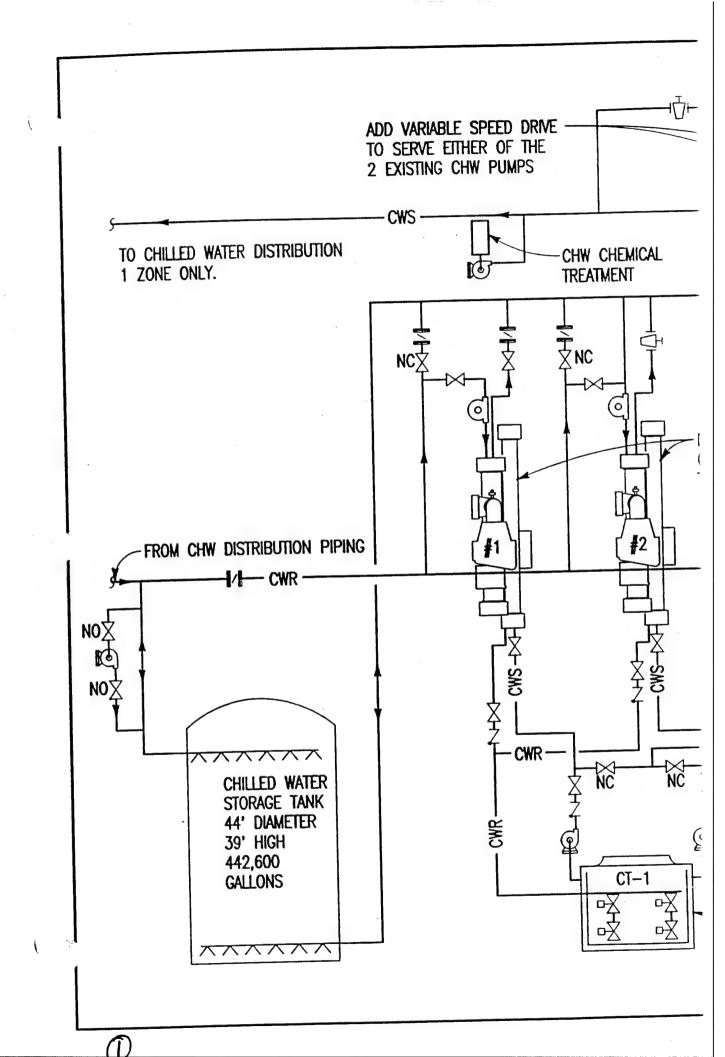
***In accordance with Public Law 90-480, no provisions for the handicapped will be made in the project since the facility is used and operated solely by able bodied personnel. However, the main floor of the facility is at ground level and is handicap accessible.

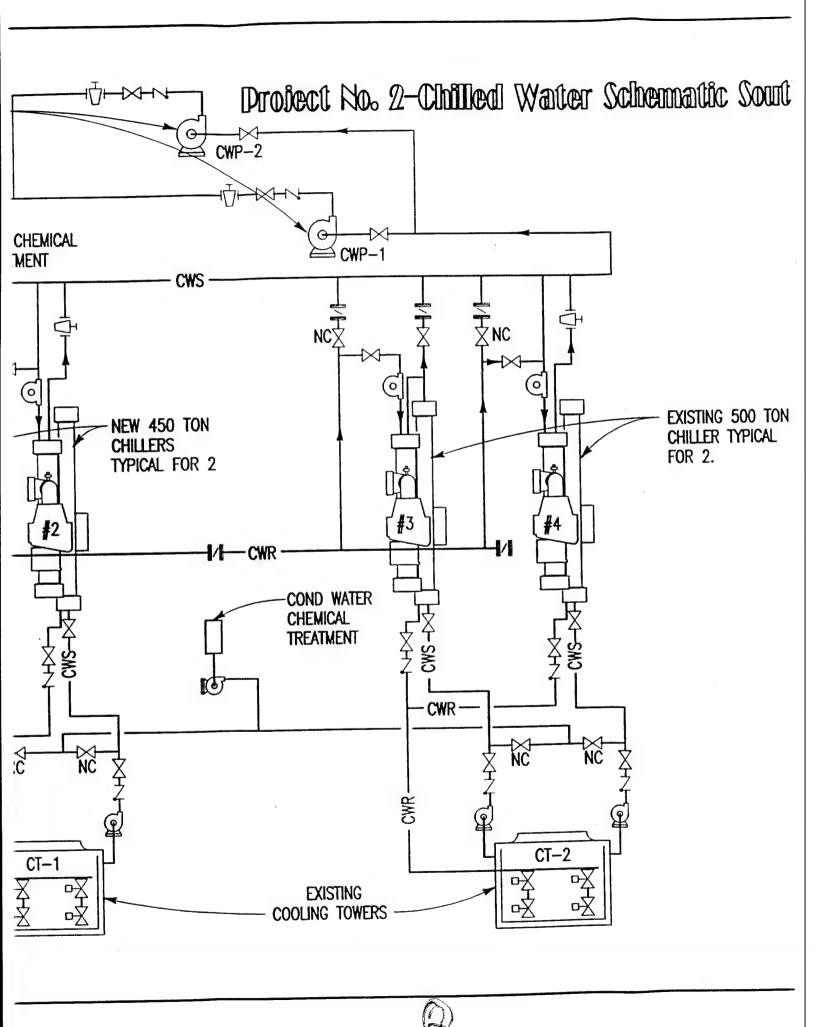
/*

22B !PHYSICAL SECURITY

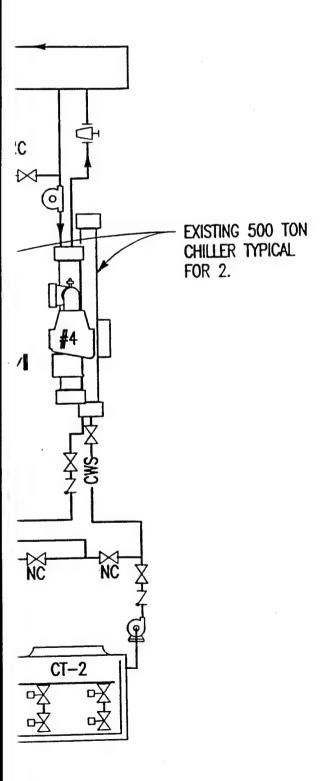
***Project is not considered for commercial activity. The physical plant upgrade to the existing Central Utility Plant will serve the north side of Ft. Gordon. Provisions of DA circular 235-1 are not applicable to this project.

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] Water Schematic South-Bldg. 25330



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INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3
PROJECT NO. & TITLE: 2 CHILLED WATER SOUTH.
FISCAL YEAR 1994 DISCRETE PORTION NAME: CHW CHEMICAL TREATMENT
ANALYSIS DATE: 09-19-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB
1. INVESTMENT
A. CONSTRUCTION COST $
                              13910.
                               765.
B. SIOH
C. DESIGN COST $ 835.
D. TOTAL COST (1A+1B+1C) $ 15510.
E. SALVAGE VALUE OF EXISTING EQUIPMENT $
F. PUBLIC UTILITY COMPANY REBATE $
                                               0.
                                                         15510.
G. TOTAL INVESTMENT (1D - 1E - 1F)
2. ENERGY SAVINGS (+) / COST (-)
DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993
                                                              DISCOUNTED
                                      ANNUAL $ - DISCOUNT
                         SAVINGS
             UNIT COST
                                                   FACTOR (4)
                                                              SAVINGS (5)
                                      SAVINGS (3)
                         MBTU/YR(2)
             S/MBTU(1)
    FUEL
                                                                       0.
                                                      15.61
                                              0.
                              0.
    A. ELECT $ 15.24
                                    ちななななななな
                                                                       0.
                                                      17.56
                                              0.
                              0.
    B. DIST $ 8.82
                                                                       0.
                                                      19.97
                             0.
0.
                                             0.
               2.73
    C. RESID $
                                          0.
0.
0.
0.
                                                                       0.
                                                      20.96
               4.50
    D. NAT G $
                                                                       0.
                          0.
:0.
                                                      17.58
               1.61
    E. COAL $
                                                                        0.
                                                      16.12
               6.34
    F. LPG
                                                                        0.
                                                      14.74
    M. DEMAND SAVINGS
                                                                        0.
                           -5994.
    N. TOTAL
 3. NON ENERGY SAVINGS(+) / COST(-)
                                                                    -4000.
    A. ANNUAL RECURRING (+/-)
                                                       14.74
        (1) DISCOUNT FACTOR (TABLE A)
                                                                   -58960.
        (2) DISCOUNTED SAVING/COST (3A X 3A1)
    B. NON RECURRING SAVINGS(+) / COSTS(-)
                                              DISCOUNTED
                             SAVINGS(+) YR
COST(-) OC
                                                        SAVINGS(+)/
                                               FACTR
                               COST(-)
                ITEM
                                                         COST(-)(4)
                                         (2)
                                               (3)
                                  (1)
                             $6000000. 16
                                                          3660000.
     1. CHW PIPING 16 YRS $6000000.
2. CHW PIPING 20 YRS $-6,000,000
                                                .61
                                                          -3240000.
                                                 .54
                                                             420000.
                             $ 0.
     d. TOTAL
    C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)$ 361040
 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd4/(YRS ECONOMIC LIFE))$
                                                                   17000 •
                                                                   1.10 YE.
 5. SIMPLE PAYBACK PERIOD (1G/4)
                                                                    361040
  6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)
                                                                 23.28
                                        (SIR) = (6 / 1G) =
  7. SAVINGS TO INVESTMENT RATIO
      (IF < 1 PROJECT DOES NOT QUALIFY)
** Project does not qualify for ECIP funding; 4,5,6 for information only.
                                                                 A \setminus N
  8. ADJUSTED INTERNAL RATE OF RETURN (AIRR)
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ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080

LIFE CYCLE COST ANALYSIS SUMMAR:

DIUDI- LCOUT

LIFE CYCLE COST ANALYSIS SUMMARY
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP).

STUDY: ECO020
LCCID 1.080 INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 2 CHILLED WATER SOUTH FISCAL YEAR 1994 DISCRETE PORTION NAME: REPLACE CHILLERS ANALYSIS DATE: 09-19-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1 INVESTMENT A. CONSTRUCTION COST \$ 370062.

B. SIOH \$ 20354.

C. DESIGN COST \$ 22204.

D. TOTAL COST (1A+1B+1C) \$ 412620. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0.

F. PUBLIC UTILITY COMPANY REBATE \$ 0.

G. TOTAL INVESTMENT (1D - 1E - 1F) \$ 412620. 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) FUEL A. ELECT \$ 15.24 10084. \$ 153632. 15.61 \$ 2398200. B. DIST \$ 8.82 0. \$ 0. 17.56 \$ 0. C. RESID \$ 2.73 0. \$ 0. 19.97 \$ 0. D. NAT G \$ 4.50 0. \$ 0. 20.96 \$ 0. E. COAL \$ 1.61 0. \$ 0. 17.58 \$ 0. F. LPG \$ 6.34 0. \$ 0. 16.12 \$ 0. M. DEMAND SAVINGS \$ 0. 16.12 \$ 0. N. TOTAL 4090. \$ 153632. \$ 2398200. 3. NON ENERGY SAVINGS (+) / COST(-) 2000. A. ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) 14.74
(2) DISCOUNTED SAVING/COST (3A X 3A1) (1) DISCOUNT FACTOR (TABLE A) \$ 29480. B. NON RECURRING SAVINGS (+) / COSTS (-) SAVINGS(+) / COSIS(-)

SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4) 0. \$ 0. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS (+) / COST (-) (3A2+3Bd4)\$ 29480. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 155632. 2.65 YEARS 5. SIMPLE PAYBACK PERIOD (1G/4) \$ 2427680. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 5.88 (IF < 1 PROJECT DOES NOT QUALIFY) 12.65 % 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

LIFE CYCLE COST ANALYSIS SUMMARY
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP)

STUDY: ECO024
LCCID 1.080 INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 2 CHILLED WATER SOUTH FISCAL YEAR 1994 DISCRETE PORTION NAME: VARIABLE SPEED PUMPING ANALYSIS DATE: 09-26-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 285314.

B. SIOH \$ 15693.

C. DESIGN COST \$ 17119.

D. TOTAL COST (1A+1B+1C) \$ 318126. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0.
F. PUBLIC UTILITY COMPANY REBATE \$ 0.
G. TOTAL INVESTMENT (1D - 1E - 1F) 318126. 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) A. ELECT \$ 15.24 3310. \$ 50436. 15.61 \$ 787309. B. DIST \$ 8.82 0. \$ 0. 17.56 \$ 0. C. RESID \$ 2.73 0. \$ 0. 19.97 \$ 0. D. NAT G \$ 4.50 0. \$ 0. 20.96 \$ 0. E. COAL \$ 1.61 0. \$ 0. 17.58 \$ 0. E. COAL \$ 1.61 0. \$ 0. 17.58 \$ 0. M. DEMAND SAVINGS \$ 0. 16.12 \$ 0. M. DEMAND SAVINGS \$ 0. 14.74 \$ 0. N. TOTAL -2684. \$ 50436. \$ 787309. 3. NON ENERGY SAVINGS(+) / COST(-) 0. (1) DISCOUNT FACTOR (TABLE A) A. ANNUAL RECURRING (+/-) 14.74 0. (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS (+) / COSTS (-) SAVINGS(+) / COSIS(-)

SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4) ITEM 0. \$ 0. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 0. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 50436. 6.31 YEAR: 5. SIMPLE PAYBACK PERIOD (1G/4) \$ 787309. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 2.47 (IF < 1 PROJECT DOES NOT QUALIFY) 7.88 % 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

LIFE CYC ENERGY CONSER INSTALLATION & LOC PROJECT NO. & TITL FISCAL YEAR 1994 ANALYSIS DATE: 09	E: 2 CHILLED OF DISCRETE PORT	ON REGIOMATER SOUT	ON NOS. 4 H CONTROLS	1 CENSUS:	3
1. INVESTMENT A. CONSTRUCTION CO B. SIOH C. DESIGN COST D. TOTAL COST (1A+ E. SALVAGE VALUE OF. PUBLIC UTILITY G. TOTAL INVESTMEN	F EXISTING EQUI	PMENT \$	0. 0.	\$ 15596	
2. ENERGY SAVINGS DATE OF NISTIR 85- UNIT FUEL \$/MBT	(+) / COST (-) 3273-X USED FOR COST SAVINGS U(1) MBTU/YR(ANNUA 2) SAVIN	L \$ D GS(3) F.	ACTOR (4)	
D. NAT G \$ 4. E. COAL \$ 1. F. LPG \$ 6. M. DEMAND SAVI	-5837.		2393. 0. 0. 0. 0. 0. 2393.	15.61 17.56 19.97 20.96 17.58 16.12 14.74	\$ 37351. \$ 0. \$ 0. \$ 0. \$ 0. \$ 0. \$ 37351.
A. ANNUAL RECUI (1) DISCOUN (2) DISCOUN		: A)	L)	14.74	\$ 0. \$ 0.
		COSTS(-) NGS(+) YF ST(-) OC (1) (2)	R DISCNI C FACTR (3)	SAVI	OUNTED NGS(+)/ (-)(4)
d. TOTAL	\$	0.		1)	0.
C. TOTAL NON E	NERGY DISCOUNTE	SAVINGS (+)/COST(-)	(3A2+3Bd4)\$ 0.
4. FIRST YEAR DOL	LAR SAVINGS 2N3-	+3A+(3Bd1/	(YRS ECONO	OMIC LIFE))\$ 2393.
5. SIMPLE PAYBACK	PERIOD (1G/4)				6.52 YEAR
6. TOTAL NET DISC	OUNTED SAVINGS	(2N5+3C)			\$ 37351.
7. SAVINGS TO INV (IF < 1 PROJE	ESTMENT RATIO CT DOES NOT QUA		R)=(6 / 10	G) =	2.39
8. ADJUSTED INTER	NAL RATE OF RET	URN (AIRR)	:		7.70 %

LIFE CYCLE COST ANALYSIS SUMMARY STUDY: ECO044 ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080 INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 2 CHILLED WATER SOUTH FISCAL YEAR 1994 DISCRETE PORTION NAME: PIPING ANALYSIS DATE: 01-13-95 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUR 1. INVESTMENT A. CONSTRUCTION COST \$ 30618.

B. SIOH \$ 1684.

C. DESIGN COST \$ 1837.

D. TOTAL COST (1A+1B+1C) \$ 34139. 34139. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$
F. PUBLIC UTILITY COMPANY REBATE \$
G. TOTAL INVESTMENT (1D - 1E - 1F) 0. 34139. 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) A. ELECT \$ 15.24 33. \$ 501. 15.61 \$ 7825. B. DIST \$ 8.82 0. \$ 0. 17.56 \$ 0. C. RESID \$ 2.73 0. \$ 0. 19.97 \$ 0. D. NAT G \$ 4.50 0. \$ 0. 20.96 \$ 0. E. COAL \$ 1.61 0. \$ 0. 17.58 \$ 0. F. LPG \$ 6.34 0. \$ 0. 16.12 \$ 0. M. DEMAND SAVINGS \$ 0. 14.74 \$ 0. N. TOTAL -5961. \$ 501. \$ 7825. 3. NON ENERGY SAVINGS (+) / COST (-) 14.74 \$ 29480. A. ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS (+) / COSTS (-) SAVINGS(+) / COSTS(-)

SAVINGS(+) YR DISCNT DISCOUNTED

ITEM COST(-) OC FACTR SAVINGS(+) /

(1) (2) (3) COST(-)(4)

1. CHILLER 19 YRS \$ 450000. 19 .56 252000.

2. CHILLER 20 YRS \$ -450000. 20 .54 -243000.

3. COOL TWRS 19 YRS \$ 86400. 19 .56 48384.

4. COOL TWRS 20 YRS \$ -86400. 20 .54 -46656. \$ 0. d. TOTAL 10728. C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 40208. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd4/(YRS ECONOMIC LIFE))\$ 3037. 11.24 YEARS 5. SIMPLE PAYBACK PERIOD (1G/4) \$ 48033. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 1.41(IF < 1 PROJECT DOES NOT QUALIFY) **** Project does not qualify for ECIP funding; 4,5,6 for information only.

N/A

8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080 INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 2 CHILLED WATER SOUTH FISCAL YEAR 1994 DISCRETE PORTION NAME: WATER TREATMENT ANALYSIS DATE: 01-13-95 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 1765.

B. SIOH \$ 97.

C. DESIGN COST \$ 106.

D. TOTAL COST (1A+1B+1C) \$ 1968. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$
F. PUBLIC UTILITY COMPANY REBATE \$
G. TOTAL INVESTMENT (1D - 1E - 1F) 0. 0. 1968. 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) FUEL A. ELECT \$ 15.24 131. \$ 1994. 15.61 \$ 31125. B. DIST \$ 8.82 0. \$ 0. 17.56 \$ 0. C. RESID \$ 2.73 0. \$ 0. 19.97 \$ 0. D. NAT G \$ 4.50 0. \$ 0. 20.96 \$ 0. E. COAL \$ 1.61 0. \$ 0. 17.58 \$ 0. F. LPG \$ 6.34 0. \$ 0. 16.12 \$ 0. M. DEMAND SAVINGS \$ 0. 16.12 \$ 0. N. TOTAL -5863. \$ 1994. \$ 31125. 3. NON ENERGY SAVINGS(+) / COST(-) \$ 2000. 14.74 \$ 29480. A. ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS(+) / COSTS(-) SAVINGS(+) / COSTS(-)

SAVINGS(+) / R DISCNT DISCOUNTED

ITEM COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4)

1. COOL TWRS 18 YRS \$ 86400. 18 .58 50112.

2. COOL TWRS 20 YRS \$ -86400. 20 .54 -46656. d. TOTAL \$ 0. 3456. C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 32936. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd4/(YRS ECONOMIC LIFE))\$ 4167. .47 YEARS 5. SIMPLE PAYBACK PERIOD (1G/4) 64061. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 32.55 (IF < 1 PROJECT DOES NOT QUALIFY) 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR): 22.71 %

LIFE CYCLE COST ANALYSIS SUMMARY

STUDY: ECO048

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LIFE CYCLE COST ANALYSIS SUMMARY STUDY: EC0054
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080
INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3
PROJECT NO. & TITLE: 2 CHILLED WATER SOUTH
FISCAL YEAR 1994 DISCRETE PORTION NAME: CHW STORAGE
ANALYSIS DATE: 09-19-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUR
1. INVESTMENT
A. CONSTRUCTION COST $ 252126.
B. SIOH $ 13867.
C. DESIGN COST $ 15128.
D. TOTAL COST (1A+1B+1C) $ 281121.
E. SALVAGE VALUE OF EXISTING EQUIPMENT $ 0.
F. PUBLIC UTILITY COMPANY REBATE $ 0.
G. TOTAL INVESTMENT (1D - 1E - 1F)
                                                           281121.
2. ENERGY SAVINGS (+) / COST (-)
DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993
            UNIT COST SAVINGS ANNUAL $ DISCOUNT DISCOUNTED
         $/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5)
    FUEL
   3. NON ENERGY SAVINGS (+) / COST (-)
                                                                         0.
   A. ANNUAL RECURRING (+/-)
       (1) DISCOUNT FACTOR (TABLE A)
        (2) DISCOUNTED SAVING/COST (3A X 3A1)
   B. NON RECURRING SAVINGS (+) / COSTS (-)
                            SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4)
                ITEM
    d. TOTAL
                             $ 0.
                                                                  0.
   C. TOTAL NON ENERGY DISCOUNTED SAVINGS (+) / COST (-) (3A2+3Bd4) $ 0.
4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))$
                                                                     75868.
5. SIMPLE PAYBACK PERIOD (1G/4)
                                                                    3.71 YEAR
                                                          $ 1118298.
6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)
7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) =
                                                                   3.98
    (IF < 1 PROJECT DOES NOT QUALIFY)
                                                                  10.47 %
8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):
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PRO	LIFE CYC ENERGY CONSER TALLATION & LOC DJECT NO. & TITL CAL YEAR 1994 LYSIS DATE: 09	ATION: FT. E: 2 CHII	STMENT PR GORDON LED WATER PORTION N	OGRAM REGIO SOUTI	(ECIP) ON NOS. H CONTROLS	LC 4 CENS	CID 1. US: 3	080
A. B. C. D. E.	INVESTMENT CONSTRUCTION CO SIOH DESIGN COST TOTAL COST (1A+ SALVAGE VALUE O PUBLIC UTILITY TOTAL INVESTMEN	COMPANY REF	EQUIPMENT BATE	. \$	0.	\$ 4	8917.	
2. DAT	ENERGY SAVINGS TE OF NISTIR 85- UNIT FUEL \$/MBT	3273-X USEI	FOR DISC	ΔΙΤΙΛΙΚΔ	T. S	DISCOUN	II DI	SCOUNTED VINGS (5)
	A. ELECT \$ 15. B. DIST \$ 8. C. RESID \$ 2. D. NAT G \$ 4. E. COAL \$ 1. F. LPG \$ 6. M. DEMAND SAVI	82 73 50 61 .34	0. 0. 0. 0.	ው ው ው ው ው ው	5158. 0. 0. 0. 0. 0. 5158.	15.6 17.5 19.5 20.5 17.5 16.5	56 \$ 97 \$ 96 \$ 58 \$	80516. 0. 0. 0. 0. 0. 80516.
3.	NON ENERGY SAVI	RRING (+/-)	TABLE A)	X 3A1		14.	\$ 74 \$	0. 0.
	B. NON RECURRIT		+) / COST SAVINGS(+ COST(-) (1)) YF	C FACTI	2	DISCOUN SAVINGS COST(-)	3(+)/
	d. TOTAL		\$ 0.					0.
	C. TOTAL NON E	NERGY DISCO	OUNTED SAV	INGS (-	+) / COST (-) (3A2+	3Bd4)\$	0.
4.	FIRST YEAR DOL	LAR SAVINGS	2N3+3A+(3Bd1/	(YRS ECO	NOMIC L	IFE))\$	5158.
5.	SIMPLE PAYBACK	PERIOD (10	G/4)					9.48 YEAR
6.	TOTAL NET DISC	OUNTED SAVI	NGS (2N5+	3C)			\$	80516.
7.	SAVINGS TO INV (IF < 1 PROJE	ESTMENT RAT	TIO T QUALIFY)	(SI	R) = (6 /	1G) =		1.65
8.	ADJUSTED INTER	NAL RATE OF	F RETURN ((AIRR)	:			5.70 %

PROJECT NO. 3 HIGH TEMPERATURE WATER NORTH BUILDING 25910

Harrison and Spencer, Inc.

GENERAL PROJECT NO. 3

GENERAL DESCRIPTION:

The concept of the heating plant as a steam generating boiler plant which sparges steam into the high temperature water, which is then pumped through the underground pipe distribution, has changed completely. The new concept is to replace the steam boilers with hot water generators which operate in a primary loop circulating HTW from and to the three existing cascade heaters which will be converted for use as expansion/storage tanks. Variable speed pumps draw water from the expansion/storage tank discharge and pump HTW to the buildings on the distribution system which already have 2 way valves. The expansion/storage tanks will now be pressurized with nitrogen and the pressure on the tank will vary as the water level increases or decreases. The water level will change based on the variable speed pumping changes and water losses in the system. The existing deaerator needs to be modified before any other work is done. The deaerator vessel and storage tank are hopefully reusable, but it is our suspicion that the trays within the deaerator are not operating and need to be replaced entirely. Another item that needs to be done prior to making the switch over from steam to hot water is to add chemical feed tanks and have chemicals fed at the appropriate locations. This should be done in coordination with the chemical supplier, but basically we are adding sulfite and ph control to the make-up water in the deaerator or immediately after the deaerator. Then there is an additional chemical that needs to be added to the distribution system to make sure that the oxygen corrosion is not a problem, and that exposed piping does not corrode. The distribution piping shall also be protected from oxygen pitting and ph imbalance when the make-up water requirement is reduced and the dearator is made to more effectively dearate with less chemicals being added.

Because there is a multiplicity of units available to be converted and to be replaced with new, it is possible that the steam can remain in operation while the new hot water generators are added and one or more of the cascade heaters is converted so that the Plant can serve the needs of the distribution system during the construction period. Then there will be a small shutdown period where steam generation will be converted over to hot water generation. If this can be coordinated with the summer shutdown so that all of the work in the buildings is completed to locally generate domestic water, then the HTW system can be shutdown 4-1/2 months of the summer to make this conversion from steam to hot water generation.

COMPILATION OF DATA:

From the ECO data compilation you will see the total of seven ECO's total a cost of more than \$2,336,238. The simple payback is 6.58 years and the SIR is 2.83 for the total Project No. 3. The LCCD sheet for Project No. 3 shows the same results.

CONCLUSION:

Data for this analysis was based on an assumed existing efficiency of the boilers of 70%. This assumption was made without any accurate information on the efficiencies of the boilers. Recent articles in the ASHRAE Journal and elsewhere indicates that for the Plant as it is now, 70% is probably a very high efficiency for the actual conditions. Even with the payback indicated, we can expect a better payback if the project is well designed and operators develop a concern for energy savings. There are also opportunities to increase the savings if higher efficiency equipment is installed in the buildings on the distribution system. We assumed 80% efficiency for gas combustion, but there are gas-fired heaters that can get into the 90% range. This costs additional money, but may be worthwhile on the basis of dollars saved when the natural gas prices at the time of project completion are compared with high efficiency water heating equipment prices at the same time.

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LIFE CYCLE COST ANALYSIS SUMMARY STUDY: PROJ003 ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080
INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3
PROJECT NO. & TITLE: 3 HTW NORTH
FISCAL YEAR 1994 DISCRETE PORTION NAME: COMPOSITE
ANALYSIS DATE: 02-19-95 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB
1. INVESTMENT
A. CONSTRUCTION COST $ 2095527.
             $ 115254.
OST $ 125732.
B. SIOH
C. DESIGN COST
D. TOTAL COST (1A+1B+1C) $ 2336513.
                                                       0.
E. SALVAGE VALUE OF EXISTING EQUIPMENT $
F. PUBLIC UTILITY COMPANY REBATE $
                                                        0.
                                                                  2336513.
G. TOTAL INVESTMENT (1D - 1E - 1F)
2. ENERGY SAVINGS (+) / COST (-)
DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993
              UNIT COST SAVINGS ANNUAL $ DISCOUNT DISCOUNTED $/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5)
     FUEL
    A. ELECT $ 15.24 1780. $ 27125. 15.61 $ 423426. B. DIST $ 8.82 0. $ 0. 17.56 $ 0. C. RESID $ 2.73 0. $ 0. 19.97 $ 0. D. NAT G $ 4.50 45645. $ 205402. 20.96 $ 4305225. E. COAL $ 1.61 0. $ 0. 17.58 $ 0. F. LPG $ 6.34 0. $ 0. 16.12 $ 0. M. DEMAND SAVINGS $ 0. 14.74 $ 0. N. TOTAL 41431. $ 232527. $ 4728651.
3. NON ENERGY SAVINGS (+) / COST (-)
         (1) DISCOUNT FACTOR (TABLE A)
                                                                           $ 110659.
    A. ANNUAL RECURRING (+/-)
                                                               14.74
                                                                           $ 1631114.
         (2) DISCOUNTED SAVING/COST (3A X 3A1)
    B. NON RECURRING SAVINGS (+) / COSTS (-)
                          SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)/
                                  COST(-)
                  ITEM
                                               (2) (3)
0 1.00
                                 (1)
$ 241500.
                                                                   COST(-)(4)
                                                         1.00
                                                                      241500.
     1. TOTAL
                                                                       241500.
     d. TOTAL
                                 $ 241500.
    C. TOTAL NON ENERGY DISCOUNTED SAVINGS (+) / COST (-) (3A2+3Bd4)$ 1872614.
4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))$ 355261.
                                                                               6.58 YEARS
5. SIMPLE PAYBACK PERIOD (1G/4)
                                                                        $ 6601264.
6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)
7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 2.83
     (IF < 1 PROJECT DOES NOT QUALIFY)
                                                                              8.60 %
8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):
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PROJECT NO. 3 - HIGH TEMPERATURE WATER NORTH

ECO DATA COMPILATION

TOTAL DISCOUNT SAVINGS	245,689	339,832	551,858	1,946,822	3,034,235	37,594	445,267	6,601,297
SAVINGS <u>8 1stYEAR</u>	15,962	19,181	26,829	97,887	172,367	1,793	21,244	355,263
NAT GAS SAVINGS SAVINGS MMBTU/YR 1stYEAR	0	2,040.20	5,587.70	15,736.03	17,161.56	398.58	4,720.81	45,644.88
ELECTRICAL SAVINGS MMBTU/YR	785.13	0	0	0	995.23	0	0	1780.36
COST (From LCC)	179,986	70,597	61,451	1,499,570	448,696	2,056	74,163	2,336,519
NON- RECURRING COST (-) SAVINGS (+)	0	0	0	Items from LCCD on ECO 67	0	0	0	same as ECO 67
ANNUAL RECURRING COST	4,000	10,000	1,684	2	79,795	0	0	110,659
CONSTRUCTION COST	161,421.12	63,315.00	55,112.40	1,344,905.10	402,417.70	1,842.75	66,512.88	2,095,527
DESCRIPTION	Variable Speed Hot Water Pumping	Return Hot Water Temperature Control	Reduce Make-Up Water-Hot Water	Hot Water Generators	Summer Shut Down (1/2) Gas 1/2 Heat Pumns)	Reduce Steam Leaks	FMCS Controls & Instrumentation	Totals
ECO NO.	25	27	; [67	269	71	8	8

Simple Payback: <u>2.336,519</u> = 6.58 years 355,263

 $\frac{6,601.297}{2,336,519} = 2.83$

SIR:

ECO METHODOLOGY FORM

ECO NAME:

Variable Speed HTW Pumping

ECO NUMBER:

25

TYPE: BLDG SYSTEM:

Bldg. 25910 Heating

EXISTING CONDITIONS:

There are three zones leaving Plant 25910. Each has a set of identical pumps serving each zone. Zones 1 and 3 have 50 hp motors rated at 3550 gpm. Zone 2 has the same pump with a 75 hp motor rated at 3550 gpm. The pumps usually operate on the low speed which is 1750 gpm, and the horsepower is 1/4 of that given above at the higher speeds. Pumps in Zone 1 are Dean Brothers pumps sizes 3 x 4 x 9-1/4 impeller, Model No. 8434; the Serial No. on one of the pumps is 148840. The pumps in the other zones are similar. Just upstream of the HTW pumps is the blending station which blends return HTW with water leaving the cascade heater to maintain a setpoint temperature at the blending station for HTW supply water. Water levels in the cascade heaters are effected by the setpoints on the HTW blending stations. By decreasing the temperature setting on Zone 3 Blending Station, it was noted that the HTW return water flow increased and then the level of the cascade heater above Zone 3 went up relative to the water levels in the other cascade heaters. Entering each building at the distribution system is a 2-way valve so that when HTW is not required in the building on the distribution system, the flow ceases to that building.

PROPOSED CHANGE:

To reduce the energy use for pumping to three separate zones, it makes sense to not only combine pumping to one set of two pumps with one pump to backup the other, but to make the pumps variable speed drive so that energy savings can be obtained. Repiping from the cascade heaters into the single pumping station will be required as a part of this Project No. 3. Blending stations will be eliminated. Pump selection shall be 800 gpm at 85 ft. of head and 1750 rpm using a 25 horsepower motor. One variable speed drive will be equipped to operate either 3500 rpm pump motor and will be able to go up to higher head pressures with higher rpms than the 1750 rpm nominal speed. The basis of this selection is the fact that the existing motors and pumps in the three Zones have always run at the low speed and accommodated the heating requirements of the distribution system. Controls will vary the pump speed to maintain a fixed pressure differential between the HTW supply and the HTW return water.

CALCULATION & COST METHODOLOGY:

The savings will be based entirely on the difference between the constant speed of the three motors and one single variable speed drive with the new pump set. Existing motors are two speed and are rated at 50 HP for two sets of pumps and 75 HP for one set of pumps at 3550 rpm. Since one pump is always running on each zone and usually at low speed, the normal power usage is the average for 1750 rpm as follows:

50 hp at 1750 rpm = 12.5 hp75 hp at 1750 rpm = 19 hp

Hp consumed is $(2 \times 12.5) + (1 \times 19) = 44 \text{ hp/hr}$ year round At 800 watts/hp x 44 hp/yr ÷ $\frac{1000 \text{ watts}}{\text{KW}} = 35.2 \text{ KW/hr}$

 $8760 \text{ hrs/yr. } \times 35.2 \text{ KW/hr} = 308,352 \text{ KW/yr.}$

From the B&G Pumping System Analysis on the following page, we see that the new 25 hp pump operating with a variable speed drive will use only 78,310.06 KWH/yr. The savings is therefore 308,352 - 78,310.06 = 230,041.94 KWH/yr. In Million Btu's: 230,041.94 x 3413 = 785.13 Million Btu's/yr.

100

ECO METHODOLOGY FORM

ECO NAME:

Variable Speed HTW Pumping

(Cont'd)

ECO NUMBER:

25

TYPE: BLDG SYSTEM: Bldg. 25910 Heating

CALCULATION & COST METHODOLOGY:

By eliminating the Blending Stations and two sets of pumps, the maintenance cost can be reduced by 4,000/yr. The cost will be based on the following information:

Electrical worl	k		
Materials	\$ 4,000	Labor	\$ 6,000
Piping modific	cations		
Materials	\$20,000	Labor	\$25,000
Demolition			
		Labor	\$15,000
New pumps w	with motors (2)		
Material	\$25,000	Labor	\$ 3,000
TVIATOTIAL	42 5,000		,
Variable speed	d drive (1)		
Materials	\$ 8,500	Labor	\$ 1,000
Switches for n	notor		
Materials	\$4,340	Labor	\$ 1.000
iviateriais	$\psi \rightarrow \mathcal{F} \mathcal{F} \psi$	Luooi	\$ 1,000

B&G Pumping System Analysis: BWG 25910 HEATING

SUMMARY OF INPUT DATA: Office, heating

System peak demand: 800.00 gpm

System discharge pressure: 85.00 ft. (36.82 psig)
Minimum control/Static pressure: 20.00 ft. (8.66 psig)

Standard Efficiency (SE) 60-cycle motor.

1 Pump System:

Pump F: Series 1510 5E, Impeller diameter 9.875" Design RPM = 1750.0, Motor HP = 25.00

CONSTANT SPEED OPERATION:

Q/Qd,% TGPM TDH,ft BHP Ep,% BHP/HP,m HP,in E,mtr,% kWHR \$/day E,w/w,% 87.2 33.6 1.34 20.5 18.77 95.1 16.37 23.5 0.655 20.0 160.0 2.40 1.34 40.9 33.6 18.77 87.2 95.1 16.37 46.9 0.655 40.0 320.0 2.40 50.4 2.02 51.1 87.2 16.37 58.7 0.655 18.77 50.0 400.0 95.1 3.60 2.69 61.2 67.2 0.655 18.77 87.2 60.0 480.0 94.8 16.37 70.2 4.80 2.86 66.3 71.6 17.47 75.9 20.00 87.3 70.0 560.0 93.8 0.699 4.80 1.53 69.5 87.5 38.3 640.0 92.1 18.75 79.3 0.750 21.42 2.40 80.0 40.5 1.62 71.9 22.63 0.794 87.7 19.84 82.1 720.0 89.6 2.40 90.0 21.3 0.85 73.5 23.81 87.6 20.86 83.9 0.834 800.0 86.6 1.20 100.0

OST SUMMARY:

Annual Operating Cost @ \$0.04 / kwhr = \$ 5205.02 8760 hours/year or 100.00% Total annual operating cost = \$ 5205.02 Total kW hours = 130125.59

VARIABLE SPEED OPERATION: (Table 1 of 1)

System suction pressure: 0.00 ft. (0.00 psig)
Best Efficiency Staging is ON

HP, in E, d/m, % kWHR \$/day E, w/w, % Hrs Q/Qd, TGPM TDH, ft BHP Ep, RPM 3.81.69.4 8.6 0.27 24.0 2.65 34.5 855.7 160.0 22.6 2.40 20.0 0.67 26.1 7.12 34.5 995.0 9.42 75.6 16.9 30.4 2.40 40.0 320.0 36.1 1.44 27.3 13.44 79.0 50.0 400.0 36.3 10.61 34.5 1097.6 3.60 1.31 57.6 32.7 9.13 81.2 7.41 71.0 1207.5 480.0 43.4 4.80 60.0 1.65 63.5 83.8 41.4 560.0 51.8 9.68 75.7 1339.5 11.55 4.80 70.0 1.05 67.8 26.3 85.4 12.55 79.3 1464.1 14.69 2.40 80.0 640.0 61.6 1.34 70.8 33.4 16.12 82.0 1603.4 18.67 86.3 720.0 72.7 2.40 90.0 0.84 73.0 20.51 83.7 1735.3 23.52 87.2 21.0 800.0 85.0 1.20 100.0 3132.40 Annual Operating Cost @ \$0.04 / kwhr = \$

8760 hours/year or 100.00%

Total kW hours = 78310.06

COST SUMMARY:

Suction Pressure : 0.0 psig Percent of Year : 100%

Percent of Year Hours/Year : 8760

nual Operating Cost: \$3132.40

Total hours/year = 8760 Total annual operating cost = \$3132.40

CONSTRU	CTION COST ESTIMATE				DATE:	23 SEPT 94	SHEET 1	I OF 1
Project:	FORT GORDON ENERGY STUD	ΟY						
_ocation:	AUGUSTA, GEORGIA					PROJ. NO.	3	
	HARRISON AND SPENCER, INC).	***			CODE:	BLDG 25910	
nmary:	ECO #25 - VARIABLE HTW PUMPII		Est	imator:	H. TOUB	Checked:		
minary.	ITEM	QUANTI		MATERIAL		LABOR		
DESC	RIPTION	QUAN	UNIT	UNIT COST	EXTENSION	UNIT COST	EXTENSION	TOTAL
FLECTRICA	I WORK	1	LS	4000	4000	6000	6000	\$10,000.00
ELECTRICA PIPING	LVVORK		LS	20000	20000	25000	25000	\$45,000.00
DEMOLITIO	N		LS	20000	20000	15000	15000	\$15,000.00
NEW PUMP			EA	12500	25000	3000	6000	\$31,000.00
VARIABLES	SPEED DRIVE		LS	8500	8500	1000	1000	\$9,500.00
SWITCHES	, LLD DINVL		LS	4340	4340	1000	1000	\$5,340.00
		SUBTOT		STAX	61840 \$3,092.00		54000	
				OR TAX	\$3,092.00		\$9,180.00	
		SUBTO		71. 17.0	\$64,932.00		\$63,180.00	\$128,112.00
				GC ONLY)	,			\$25,622.40
		-		C'S WORK				\$153,734.40
		SUBTO	ΓAL(G	C & SUBS)				\$153,734.4
				PROFIT				
		5%	CON	TINGENCY				\$7,686.72
		TOTAL		2100-4-1011				\$161,421.12

ECO NAME: Controls For Return HTW Temperature Regulation

ECO NUMBER: 27

Bldg. 25910 TYPE: BLDG SYSTEM: Heating

HTW is heated in cascade heaters, which is usually maintained at the temperature of the **EXISTING CONDITIONS:** saturation pressure of the boiler, and this boiler pressure is usually maintained except for several times a year when it is changed. At 150 psi, the saturation temperature is 347°F.

When the HTW water leaves the cascade heaters, it passes through a blender that adds unheated HTW return to control the setpoint that maintains the constant HTW supply temperature. Note that as distribution loads vary; less or more HTW water is required, and the HTW return temperature rises and falls depending upon the load. The existing system operates to control the HTW supply water, and does not take into account changes to load

that would effect the overall heating requirements.

PROPOSED CHANGE: Because the existing boilers are now going to be replaced with hot water generators, the

controls in the Control Room will basically have to be changed. The controls will now regulate the high temperature water supply temperature, which will be based on firing the hot water generators to maintain the temperature in the storage tanks. This water will be circulated through the distribution system, and the firing rate of the hot water generators will be maintained based on a setpoint for the high temperature water supply. The HTW supply temperature setpoint will be varied by the EMCS to maintain the lowest acceptable HTW return temperature to adequately serve all buildings on the distribution system. These controls will also be monitored and, in some cases, controlled by the EMCS system so that temperatures in various buildings will establish energy efficient setpoint

temperatures for high temperature water supply in a very short time by this monitoring at the EMCS. Therefore, this ECO, including the cost of new Control Room controls and the tie-ins to the EMCS, will be in the Control Room only. ECO 88 includes new EMCS controls that will cover the cost of any wiring from the Control Room to the EMCS system. The HTW return water temperature will also be monitored at the EMCS. The EMCS

personnel will provide an HTW supply setpoint temperature based on their experience and

time of day usage of high temperature water throughout the distribution system.

CALCULATION & COST METHODOLOGY

Line losses in the HTW distribution piping will be decreased as a percentage of the temperature difference between the trench temperature and the HTW in the piping. If it is assumed that the difference in ground temperature to the pipe temperature is the difference between 325°F and 70°F; the average is now 255°F. After reducing the supply temperature to 300°F, this will reduce the difference to 230°F. This decreases the line loss by .1087. Since the minimum summer month hourly Btu usage is approximately 2,000,000 Btu's, it is reasonably assumed that the line loss is 1,500,000 Btu's per hour. The savings is therefore .1087 x 1.5 million divided by the boiler efficiency of .7 and also divided by 100,000 Btu's per therm. This comes to a savings of 2.329 therms per hour or 0.2329 million Btu/hr. This savings is maintained year round for 8,760 hours per year which totals 2040.204 million Btu's/yr.

The cost of new controls in the Control Room will be mostly for firing and temperature controls to determine hot water temperatures pressures and flows at the following locations as a minimum.

HTW Return Pipes (3) (flow, temp, pressure) HTW Supply Pipes (3) (flow, temp, pressure)

(temp, pressure) Expansion Tanks (3)

Deaerator Tank (temp) Hot Water Leaving Generators (3) (temp)

Hot Water Entering Generators (3) (temp)

ECO NAME:

Controls For Return HTW Temperature Regulation

(Cont'd)

ECO NUMBER:

27

TYPE: BLDG

Bldg. 25910

SYSTEM: Heating

CALCULATION & COST METHODOLOGY:

A Btu meter will total fuel input based on values totaled at the above instrumentation. Remote firing controls will be located in the Control Room also. The many hours that are spent on maintaining the existing boiler controls will be reduced with the new simplified controls. The annual manpower savings will be \$10,000/yr.

CONSTRU	CTION COST ESTIMATE			DATE:	23 SEPT 94	SHEET1	OF 1
Project:	FORT GORDON ENERGY STUD	Υ					
Location:	AUGUSTA, GEORGIA				PROJ. NO.	3	
	HARRISON AND SPENCER, INC		40 PT *1 - *		CODE:	BLDG 25910	
nmary:	ECO #27 - TEMPERATURE CONTR		timator:	H. TOUB	Checked:		
	ITEM	QUANTITY	MATERIAL		LABOR		
DESC	RIPTION	QUAN UNIT	UNIT COST	EXTENSION	UNIT COST	EXTENSION	TOTAL
CONTROLS		1 LS	20000	20000	15000	15000	\$35,000.00
DEMOLITION	OF CONTROL EQUIPMENT	1 LS				10000	\$10,000.00
							· · · · · · · · · · · · · · · · · · ·
						1	
		SUBTOTAL		20000		25000	
		5% SALE		\$1,000.00			
		17% LAB	OR TAX			\$4,250.00	
		SUBTOTALS		\$21,000.00		\$29,250.00	\$50,250.00
			GC ONLY)				\$10,050.00
		SUBTOTAL GO	C'S WORK				\$60,300.00
		SUBTOTAL(G					\$60,300.00
		10% GC'S	PROFIT				AL ALEXANDER OF THE SECOND SEC
			TINGENCY				\$3,015.00
		TOTAL					\$63,315.00

ECO NAME: Reduce Make-Up Water in HTW System

ECO NUMBER: 31

TYPE: BLDG Bldg. 25910 SYSTEM: Heating

EXISTING CONDITIONS: The total number of gallons lost in Building 25910 over the course of 1992 is 2,039,102

gallons. This leakage is caused by pipe failures and operating inefficiencies in the system. The quantity of lost water is based on reports of water meter readings made by the boiler

plant operators.

PROPOSED CHANGE: It is proposed that flow meters and temperature gauges be installed at various locations

throughout the north HTW distribution piping so that actual flows can be measured to determine where water is not being returned from where it is supplied. New flow meters and temperature gauges will be included in the cost of this ECO, and the wiring from them

to the EMCS system will be included in ECO 88 in this Project No. 3.

CALCULATION & COST METHODOLOGY:

The cost is based on locating flow meter and temperature RTD's in various distribution locations throughout the HTW distribution piping. Once they are located in this ECO, ECO 88 for EMCS wiring will absorb the cost to wire them to the nearest building and then go back to the EMCS system. The savings is the heat loss of the water lost from the HTW system, that can be determined and is based on

2,039,102 gallons x 8.34 lb/gal x $(300^{\circ}-70^{\circ}\Delta t) = 3.9114 \times 10^{9}$ Btu/yr = 3,911.4 million Btu's/yr or 39,114 therms Gas to make up loss of heat 39,114

.7 Boiler Eff. = 55,877 therms @ \$.45/therm = \$25,145/yr.

The gas savings is 5587.7 million Btu's/yr.

 $2,039,102 \text{ gal } \times \$.826/1000 \text{ gal} = \$1684.30/\text{yr}$ is the annual recurring cost for purchasing the lost water.

The cost of repairing any water leaks in an ongoing maintenance item that is presently handled with work orders and is not funded in this Project/ECO.

CONSTRU	CTION COST ESTIMATE				DATE:	23 SEPT 94	SHEET	OF 1	
Project:	FORT GORDON ENERGY STUD	Υ							
Location:	AUGUSTA, GEORGIA					PROJ. NO.	3		
	HARRISON AND SPENCER, INC).				CODE:	BLDG 25910		
mmary:	ECO #31 REDUCE HTW MAKE-UP WA		Esti	mator:	H. TOUB	Checked:			
	ITEM	QUANTI	TY	MATERIAL		LABOR			
DESC	RIPTION	QUAN	UNIT	UNIT COST	EXTENSION	UNIT COST	EXTENSION	TOTAL	
FLOW METER	RS	12	EA	1500	18000	10000	12000	\$30,000.00	
TEMP RTD IN	I DISTRIBUTION PIPE	12	EA	300	3600	500	6000	\$9,600.00	

							40000	4	
		SUBTOT			21600		18000	AVA-144-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-	
			SALE		\$1,080.00		*********		
				R TAX	****		\$3,060.00	£42.740.00	
		SUBTO			\$22,680.00		\$21,060.00	\$43,740.00	
				C ONLY)				\$8,748.00	
		SUBTOT	AL GC	'S WORK				\$52,488.00	
						-			
		CURTOT	· A L / C C	e CLIDO)				\$52,488.00	
				& SUBS)				φ02,400.UU	
				PROFIT				\$2,624.40	
		5%	CONT	INGENCY				DZ,024.4L	

ECO NAME:

Replace Existing Boiler with Hot Water Generators

ECO NUMBER:

67

TYPE: BLDG SYSTEM: Bldg. 25910 Heating

EXISTING CONDITIONS:

There are five boilers in Building 25910 heating and cooling plant which have not been tested for combustion efficiency in the studies conducted several years ago because of reported asbestos. These boilers are firing with natural gas and No. 2 oil, but they were originally built for coal firing. 70% combustion efficiency is assumed for this report, but it would not be surprising if, upon conducting tests, this efficiency was found to be lower than 70%. The furnace area is spacious with less heat absorbing tubes than would be in a boiler designed for natural gas firing. The rear section of the boiler is under negative pressure from the high stack and ID fans allow air leakage into the boiler. From the recorded temperatures leaving the boilers it is reasonable to believe that air leakage is reducing the expected flue gas temperature by 70-100°F. Only three of the five boilers are currently operable in 1994.

PROPOSED CHANGE:

The following change items should occur roughly in the order in which they are listed. The first thing that needs to be done will be the replacement of the existing deaerator internals so that the deaerator performs its intended function, which it is not doing now nor has it been doing in the past seven to eight years that we know about. Secondly, chemical feed tanks shall be added to add ph and sulfites to the deaerator and its storage tank. A chemical feed tank shall be added as an oxygen absorber for pipe protection to the circulating water system at the HTW return water piping. Thirdly, a nitrogen storage system with piping to the cascade heaters that will be converted to expansion/ storage tanks should be put in place. Fourthly, an effort should be made to make the cascade heaters into thermal expansion tanks/storage tanks. These tanks will be used for a circulating hot water system vs. their current use as a cascade heater which mixes steam with HTW water. These four revisions shall take place so that the steam boiler system can maintain its operation while the changes are being made to prepare for the new hot water generators to start their function. Fifthly, existing steam boilers that are not in use shall be demolished and removed from the building. As the system is converted from steam to high temperature water systems, the remaining boilers shall be demolished. Sixthly, three HTW zones shall be repiped so that one zone will be all that is required, and that one zone will come out of the one pump which will be driven with a variable speed drive. The pump is part of this project, but is listed in another ECO 25. The common piping for the supply and return is part of this ECO. Seventh is the installation of three new hot water generators. They will be sized for 35,000,000 Btu's per hour each output. Two of them will be required to handle the full load and the third one will be a back-up. The generator price includes controls and an economizer on the stack which will be part of the generator purchase. The unit will not have any ID fans, and the breeching and flue that is existing from the outlet of the boilers to the stack, and including the stack, will be abandoned in place.

CALCULATION & COST METHODOLOGY:

The Proposed Change will result in savings due to the increased efficiency of hot water generator combustion over that of the existing steam boilers. It will result in a deaerator operating properly so that the new equipment's life is considerably longer than the life of the steam boilers now and the very short life of the existing economizer in the stack. Simplicity of the system will also reduce the hours required to maintain the existing controls and the boiler firing equipment by 600 man hours or \$15,000 per year. For non-recurring costs, compare the existing non-deaerated boiler with five boilers with a 10-year life (when treated) and an economizer with a 2-year life with three hot water generators with a 20-year life when treated as defined in this ECO. Also, the plant piping will last only fifteen years with existing treatment, and will last 20 years with the new treatment recommended.

ECO NAME:

Replace Existing Boiler with Hot Water Generators

(Cont'd)

ECO NUMBER:

67

TYPE: BLDG

Bldg. 25910

SYSTEM:

Heating

CALCULATION & COST METHODOLOGY:

Savings are shown as 10% based on 70% efficiency for existing boilers and 80% efficiency for the new hot water generators.

.10 x $\underline{152,777 \text{ MCF} \times 1,030,000 \text{ Btu/MCF}} = 157,360 \text{ therms} = 15,736.03 \text{ Million Btu/yr.}$

100,000 Btu/therms

At \$.45/therm = \$70,812/yr savings

Maintenance manhours saved at Plant 600 manhours @, \$25 = \$15,000/yr

Cost:

Materials \$750,000 Labor \$100,000 Repiping of Cascade Heaters (3) Tanks Materials \$9,000 Labor \$12,000 Repiping to combine three zones into one for hot water Materials \$20,000 Labor \$30,000 Demolition: Labor \$35,000 Deaerator repair Materials \$5,000 Labor \$7,500 Chemical feed tanks (3) Materials \$7,500 Labor \$1,500	Hot water generator 3 @ \$	\$250,000		
Materials \$ 9,000 Labor \$ 12,000 Repiping to combine three zones into one for hot water Materials \$ 20,000 Labor \$ 30,000 Demolition: Labor \$ 35,000 Deaerator repair Materials \$ 5,000 Labor \$ 7,500 Chemical feed tanks (3)		· ·	Labor	\$100,000
Materials \$ 9,000 Labor \$ 12,000 Repiping to combine three zones into one for hot water Materials \$ 20,000 Labor \$ 30,000 Demolition: Labor \$ 35,000 Deaerator repair Materials \$ 5,000 Labor \$ 7,500 Chemical feed tanks (3)	De l'eleccif Constallinat	(2) T1		
Repiping to combine three zones into one for hot water Materials \$ 20,000 Labor \$ 30,000 Demolition: Labor \$ 35,000 Deaerator repair Materials \$ 5,000 Labor \$ 7,500 Chemical feed tanks (3)	110	1 7		# 10 000
Materials \$ 20,000 Labor \$ 30,000 Demolition: Labor \$ 35,000 Deaerator repair Materials \$ 5,000 Labor \$ 7,500 Chemical feed tanks (3)	Materials	\$ 9,000	Labor	\$ 12,000
Materials \$ 20,000 Labor \$ 30,000 Demolition: Labor \$ 35,000 Deaerator repair Materials \$ 5,000 Labor \$ 7,500 Chemical feed tanks (3)	Renining to combine three	zones into one for hot water	r	
Demolition: Labor \$ 35,000 Deaerator repair Materials \$ 5,000 Labor \$ 7,500 Chemical feed tanks (3)				\$ 30,000
Deaerator repair Materials \$ 5,000 Labor \$ 7,500 Chemical feed tanks (3)	Materials	\$ 20,000	Laudi	\$ 30,000
Deaerator repair Materials \$ 5,000 Labor \$ 7,500 Chemical feed tanks (3)				
Deaerator repair Materials \$ 5,000 Labor \$ 7,500 Chemical feed tanks (3)	Demolition:		Labor	\$ 35,000
Materials \$ 5,000 Labor \$ 7,500 Chemical feed tanks (3)	Donie de la constante de la co			. ,
Chemical feed tanks (3)	Deaerator repair			
Chemical feed tanks (3)	•	\$ 5,000	Labor	\$ 7,500
Materials \$ 7,500 Labor \$ 1,500	Chemical feed tanks (3)			
	Materials	\$ 7,500	Labor	\$ 1,500
Nitrogen storage and piping	Nitrogen storage and pipir	ng		
Materials \$ 10,000 Labor \$ 7,000	Materials	\$ 10,000	Labor	\$ 7,000

CONSTRUC	TION COST ESTIMATE				DATE:	23 SEP 94	SHEET	1 OF 1
Project:	FORT GORDON ENERGY STUD	Υ						
Location:	AUGUSTA, GEORGIA					PROJ. NO.	3	
	HARRISON AND SPENCER, INC					CODE:	BLDG 25910	
Summary:	ECO #67 - H.W. GENERATOR S		Est	imator:	H. TOUB	Checked:		
Janimary.	ITEM	QUANTI	ΤΥ	MATERIAL		LABOR		
DESC	RIPTION	QUAN	UNIT	UNIT COST	EXTENSION	UNIT COST	EXTENSION	TOTAL
HOT WATER (CENEDATOR	3	EA	250000	750000	LUMP SUM	100000	\$850,000.00
	CASCADE HEATER		TON	3000	9000	4000	12000	\$21,000.00
	ZONE FROM 3 ZONES		LS	20000	20000	30000	30000	\$50,000.00
DEMOLITION	ZONE I NOW 3 ZONES		LS	20000	20000	35000	35000	\$35,000.00
DEARATOR R	EDAID		LS	5000	5000	7500	7500	\$12,500.00
	ED EQUIPMENT		EA	2500	7500	500	1500	\$9,000.00
	FORAGE & PIPING		LS	10000	10000	7000	7000	\$17,000.00
			SALE	S TAX	\$801,500.00 \$40,075.00		\$193,000.00	\$994,500.00 \$40,075.00 \$32,810.00
		SUBTO			\$841,575.00		\$225,810.00	
				H & PROFIT				\$213,477.00
	SUB-CONTRACTORS	SUBTO	TAL G	WORK				\$1,280,862.00
		TOTAL	CLIDIA	IODK	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,			
		TOTAL						
		-		UB PROFIT TINGENCY ON	LIOB			\$64,043.10
		5%	CON	LINGENCT ON	1000			404,040.10

ECO NAME: Summer Shutdown of HTW System

ECO NUMBER: 69

TYPE: BLDG North Distribution

SYSTEM: Heating

EXISTING CONDITIONS: Space heating is not required from mid-May through the end of September, but a boiler

must be in operation to handle domestic water needs and cooking requirements in some

cases with the HTW distribution system.

PROPOSED CHANGE: Provide onsite water heaters at each building for domestic water usage. Water heaters

should be about 10% more efficient than the boiler plant, i.e., 80%. Use of water heaters should also eliminate the heat loss in the distribution line during this 4-1/2 month period. It will also eliminate supervision of the boilers for 4-1/2 months. The HTW system should either be left full of water or pressurized with nitrogen to avoid corrosion during the period of non-use. The buildings will have hot water generating equipment, which will be heat pumps or gas-fired equipment. The heat pump operates at a COP of 3±. Cool air generated by the heat pump can be used in the buildings to cool air spaces that would not now be cooled or that can be cooled depending on domestic water demand rather than space conditions, i.e., Laundry Room, Hallways, or unused Classroom areas. In some buildings, the cool air generated by the heat pumps controlled to make domestic hot water can be used to supplement the large air handling units so that less chilled water from the CHW distribution system will be required. When this is done, warm air must always be available for domestic water heating regardless of the demand for space cooling in the building. Gas-fired equipment will be more expeditious where there is no use for the chilled air in the building being converted. Each building type should be evaluated with a life cycle cost analysis to see if the higher initial cost of the heat pump and associated

equipment results in enough extra energy savings to warrant the extra cost.

CALCULATION & COST METHODOLOGY:

Methodology for computing the savings for the summer shutdown is based on taking the total amount of gas used during the summer months, May through September, and subtracting from that the estimated hot water consumption in all of the buildings on the distribution system, heat loss in the hot water storage tanks in all of the buildings. Since there is no space heating during these months, the difference between the domestic water heat use and the total HTW heating will be the amount of line loss in the distribution system for HTW. In addition to the savings of line loss of the HTW distribution system, the individual equipment that will be put in the distribution system buildings will have an 80% efficiency whether it is gas-fired equipment or heat pumps that we calculate to have an equal operating cost to gas-fired equipment. Therefore, the calculations become the same. Taking an 80% efficiency for gas-fired equipment and a 2.7 COP for heat pump operation, and using the cost available we calculate below to see that the same cost is derived for both systems per Btu. Because the cost of a Btu is the same, we can therefore easily calculate the savings with gas-fired equipment, and will assume the heating with a heat pump is going to cost the same. Therefore, it comes to the same value for the energy saved. The total savings of the higher efficiency equipment is then added to the line loss which will be saved by shutting down the Main Plant, which gives a total savings in gas over the 4-1/2 month period in which the Main Plaint will be shut down. In addition to the energy savings, the manpower at the Plant can be reduced by one man for 4-1/2 months at \$25/hour. We have added back in some money for shutting down the Plant and isolating the piping which will not be used during the HTW shut down. Separately, heat pumps are compared with natural gas-fired water heaters for the summer heating in each of the buildings. The heat pumps are creating hot water, as well as cold air, so the cold air is free because the heating with the heat pumps is exactly equivalent to the heating with natural gas. Cost of gas heaters in each of the buildings is then worked up, and the cost of the heat pumps is worked up.

ECO NAME:

Summer Shutdown of HTW System

(Cont'd)

ECO NUMBER:

69

TYPE: BLDG SYSTEM: North Distribution

Heating

CALCULATION & COST METHODOLOGY:

Three life cycle cost analyses are shown with this ECO. ECO 69A is worked up for using heat pumps only in all the 96 buildings that need to be modified for summer usage. ECO 69B is worked up for gas used to generate hot water in all of the 96 buildings. ECO 69C is taking the cost of both of the two options and dividing it by two, thereby assuming half the buildings will require heat pumps and half the buildings will require gas. The savings for ECO 69C will be full savings of natural gas which will be shutting down the Plant, and half of the savings allocated to the free cooling will be derived by using heat pumps. Heat pumps vs. gas-fired equipment will be determined by looking at each individual building and determining if there is the possibility of using heat pumps to generate cooling so that they can decrease the cooling load and also take advantage of the fact that we got this cooling as a by-product by producing hot water in the summer time. The purpose of this calculation assumes that half of the buildings qualify for heat pumps and half of the buildings qualify for gas-fired equipment.

From weather data TM 5-785 it appears heat would not be needed for half of May and all of June, July, August, and September which is 4-1/2 months.

From 1992 Boiler Logs Heating Plant Gas Consumption for Months:

```
May - 7190 MCF x 0.5 = 3595 MCF

June - 5690 MCF = 5690 MCF

July - 4771 MCF = 4771 MCF

Aug - 5456 MCF = 5456 MCF

Sept - 5048 MCF = 5048 MCF

24560.5 MCF
```

Estimated Hot Water Consumption = 53,382 GPD

```
Q = 1 BTU/LB \dot{x} 53,382 gal \dot{x} 8.34 lb/gal \dot{x} 60°F (BTU/LB) = 27,000 MBTU/day
```

Tank Losses:

Tank area = 100 sq. ft. with 2-inch insulation

```
Q<sub>L</sub> = 7.5 Btu/Hr. Sf. 100 Sf. x 24 hr = 18000 Btu/day
x 83 bldgs. = 1494 MBtu/day
```

Total domestic hot water usage per day = 27,000 + 1494 = 28,494 MBtu/day With 70% Boiler $\eta = 40,705$ MBtu/day CF Gas = 40,705 MBtu = 40,705 CF/day 1000 Btu/CF

For 30 day month = 1221.2 MCF

Gas needed to generate and maintain the domestic hot water requirement from central plan 1221.2 MCF

Lowest recorded gas consumption by Central Plant = July, 1992 4771 MCF

Deduce that the difference is the system and line loss:

4771 - 1221.2 = 3549.8 = 3550 MCF/month

ECO NAME:

Summer Shutdown of HTW System

(Cont'd)

ECO NUMBER:

69

TYPE: BLDG SYSTEM:

North Distribution

Heating

CALCULATION & COST METHODOLOGY:

> Conversion of buildings to on-site generation of hot water would eliminate Central Plant systems and line losses

> > 3550 MCF/month

Water heaters would have 80% efficiency in lieu of 70% at Central Plant

28,494 MBtu = 35,617.5 MBtu/day

35,618 CF/day

0.8

35,617.5 x 30 days/mo

1068.5 MCF/mo

Savings to increase efficiency = 1221.2 - 1068.5 = 152.7 MCF

Total Gas Savings Over 4-1/2 Months:

Line/system losses = 3550 MCF x 4.5 months 15,975 MCF

= 152.7 MCF x 4.5 months 687 MCF Increased Eff. = 16,662 MCF

Annual Cost Savings: Fuel For Operation Only

17,161.86 MBtu Fuel: 16,662 MCF x 1.03 Million Btu/mcf

@ \$0.45/therm \$77,228.37

Annual Additional Costs:

Labor shut down, isolate and reactivate Plants annually

1 hr per building: 81 manhours @ \$25/mh \$2,025

Plant Manpower Savings

4.5 mo x 1 man at \$25/hr x 30 days/mo x 24 hr/day \$81,000

Net Manhour Savings - (Annual Curring)

\$79,975

Domestic Water Heater Calculations (Gas Vs. Heat Pump)

Heat pump - at 2.7 COP (minimum)

Electricity cost:

= \$.0000056/Btu \$.052/KW 3413 Btu/hr x 2.7 COP

Natural Gas Cost:

\$.45/100,000 Btu = \$.0000056/Btu

.80 Eff

Therefore, cost of energy at Fort Gordon is the same for gas heating at 80% efficiency or with an electric heat pump at a 2.7 COP. But with heat pump, free cooling of space is:

 $30,000 \text{ Btuh} = 2.5 \text{ ton } \times .75 \text{ KW/ton } \times \$.052/\text{KWH} = \$.0975/\text{hr}$

12,000 Btu/ton

At 4-1/2 months x 30 days/month x 24 hrs/day x 0.0975/hr = 315.90/yr

ECO NAME:

Summer Shutdown of HTW System

(Cont'd)

ECO NUMBER:

69

TYPE: BLDG SYSTEM:

North Distribution

Heating

CALCULATION & COST METHODOLOGY:

For 96 buildings:

Total savings is 96 x \$315.90 = \$30,326/yr. This savings would offset the additional cost of heat pumps vs. gas in buildings where heat pumps can be used to serve a useful

purpose.

Savings on cooling load is therefore:

96 bldgs. x 2.5 tons x .75 KW/ton x 3413 Btu/KW \div 10⁶ Btu/Million Btu = .614 Million

Btu/hr

For 4.5 months x 30 days/mo. x 24 hours/day $.614 \times 4.5 \times 30 \times 24 = 1990.46 \text{ Million Btu/yr.}$

Cost for Heat Pump Installation: (ECO 69A)

Cost of Heat Pumps in Buildings:

2-1/2 Ton Heat Pump

\$24,000 Labor Materials \$192,000

Piping and Pumps (2) To Existing Domestic Hot Water Storage Tanks

\$48,000 Labor \$40,000 Materials

FCU in Building

Labor \$20,000 \$30,000 Materials

Electrical Work

\$12,000 Labor Materials \$12,000

Cost for Gas Heater Installation: (ECO 69B)

Gas Piping x 96 Buildings

\$60,000 Materials \$30,000 Labor

Combustion Air Ventilation 96 Buildings

\$ 9,600 Labor \$ 5,000 Materials

Gas-Fired Water Heater (96) x

\$12,400 Labor \$20,000 Materials

Piping To Existing Storage Tanks

\$25,000 Materials \$30,000 Labor

Pumps 1 x 96

Labor \$ 5,000 \$ 9,600 Materials

ECO NAME:

Summer Shutdown of HTW System

(Cont'd)

ECO NUMBER:

69

TYPE: BLDG

North Distribution

SYSTEM: Heating

CALCULATION & COST METHODOLOGY:

ECO 69C:

Because each type of building on the distribution system that is not yet equipped to generate domestic water heating in the cooling season must be individual analyzed for life

cycle cost of heat pump vs. gas. This ECO must be analyzed three ways:

ECO 69A:

Summer shutdown with heat pumps installed in 96 buildings that

require individual domestic water heat generating equipment.

ECO 69B:

Summer shutdown with gas-fired domestic water heaters installed in 96

buildings requiring local domestic water heating equipment.

ECO 69C:

Since paybacks are similar for ECO 69A and ECO 69B, this ECO will

take one half the cost of each and use the savings that would be derived

if this is done.

Cost of ECO 69C - 514,609.20 + 290,226.20 = \$402,417.70

2

Savings:

Gas

17,161.56 Million Btu/yr.

Electric for cooling

1990.46 = 995.23 Million Btu/yr.

(1/2 computed value)

2

CONSTRUC	TION COST ESTIMATE				DATE:	23 SEP 94	SHEET	1 OF 1
Project:	FORT GORDON ENERGY STUD	Υ	-					
cation:	AUGUSTA, GEORGIA					PROJ. NO.	3	
	HARRISON AND SPENCER, INC	.				CODE:	NORTH DIST	RIBUTION
Summary:	ECO69a - SHUTDOWN W/ HEAT PL		Est	imator:	H. TOUB	Checked:		
	ITEM CRIPTION	QUANTI QUAN	TY	MATERIAL	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
	AT DUMP (OO DUU DINGO)	1	LS	192000	192000	24000	24000	\$216,000.00
2-1/2 TON HE	AT PUMP (96 BUILDINGS) MPS TO EXIST TANKS		LS	48000	48000	40000	40000	\$88,000.00
FCU IN BUILD			LS	30000		20000	20000	\$50,000.00
ELECTRICAL			LS	12000	12000	12000	12000	\$24,000.00
		011770	TAL 0.4		#202 000 00		\$96,000.00	\$378,000.00
		SUBTO			\$282,000.00		\$90,000.00	\$14,100.00
				S TAX OR TAX	\$14,100.00		\$16,320.00	\$16,320.00
		SUBTO			\$296,100.00		\$112,320.00	\$408,420.00
				H & PROFIT				\$81,684.00
	SUB-CONTRACTORS			CWORK				\$490,104.00
		TOTAL	SUB V	VORK				
		109	GC S	SUB PROFIT				
		5%	6 CON	TINGENCY OF	N JOB			\$24,505.20
		TOTAL					1.00	\$514,609.2

CONSTRUC	TION COST ESTIMATE				DATE:	23 SEP 94	SHEET1	OF 1
Project:	FORT GORDON ENERGY STUD	Υ						
ecation:	AUGUSTA, GEORGIA					PROJ. NO.	3	
ch/Engr:						CODE:	NORTH DIST	RIBUTION
Summary:	ECO69b - SHUTDOWN W/ GAS		Esti	mator:	H. TOUB	Checked:		
Juninary.	ITEM SAS	QUANTIT	Υ	MATERIAL		LABOR		
DESC	RIPTION	QUAN	UNIT	UNIT COST	EXTENSION	UNIT COST	EXTENSION	TOTAL
GAS PIPING (9	DE BLDGS)	1	S	30000	30000	60000	60000	\$90,000.00
COMPLISTION	I AIR VENTILATION (96 BLDGS)	1		5000		9600	9600	\$14,600.00
GAS FIRED W	ATER HEATER (96 BLDGS)	1		20000	20000	12400	12400	\$32,400.00
PIPING TO EX	ISTING STORAGE TANK	1	LS	30000	30000	25000	25000	\$55,000.00
PUMPS (96 BL		1	LS	9600	9600	5000	5000	\$14,600.00
			SALE	S TAX	\$94,600.00 \$4,730.00		\$112,000.00 \$19,040.00	\$206,600.0 \$4,730.0 \$19,040.0
		SUBTOT	ALS 2	2	\$99,330.00		\$131,040.00	\$230,370.0
		20%	GC C	H & PROFIT				\$46,074.0
	SUB-CONTRACTORS	SUBTOT	AL G	WORK				\$276,444.0
		TOTAL		(OBK	1			
		TOTAL S						
				TINGENCY O	I IOD			\$13,822.2
		: E0/	CON	TIMELNEY OF	M II IH			D 1-7 OZZ

ECO NAME:

Reduce Steam Leaks

ECO NUMBER:

71

TYPE: BLDG SYSTEM:

Bldg. 25910 Heating

EXISTING CONDITIONS:

Steam is leaking in some valves and through holes drilled in the cascade heaters. The total steam leakage is approximated at 50 lbs per hour, which is the equivalent of a half-inch

hole at 14,000 ft. per minute steam flow.

PROPOSED CHANGE:

Weld the holes in the existing cascade heaters closed and replace the packing in leaking valve stems. Any other steam leak shall also be repaired. Even though we are using HTW only, leaks will still flash to steam.

CALCULATION & COST METHODOLOGY:

Estimated steam loss is:

 $\frac{50 \text{ lbs/hr} \times 24 \text{ hr/day} \times 365 \text{ days/yr} \times 910 \text{ Btus/lb}}{100,000 \text{ Btus/therm}} = 3,985.8/\text{therms}$ or 398.58 Million Btu/Yr

 $.45/\text{therm } \times 3,985.8/\text{therms} = 1,793.61/\text{yr}$

Cost of Repairs:

50 hrs @ \$25 = \$1,250

CONSTRUC	TION COST ESTIMATE			DATE:	23 SEP 94	SHEET1	OF 1
Project:	FORT GORDON ENERGY STU	OY '					
Location:	AUGUSTA, GEORGIA				PROJ. NO.	3	
	HARRISON AND SPENCER, INC	3.			CODE:	BLDG 25910	
	ECO71 - REDUCE STEAM LEAF		Estimator:	H. TOUB	Checked:		
Summary.	ITEM	QUANTITY	MATERIAL		LABOR		
DESC	CRIPTION	QUAN U	NIT UNIT COST	EXTENSION	UNIT COST	EXTENSION	TOTAL
REPAIR STEA	MIEAKS	50 HF	RS		25	1250	\$1,250.00
I LET THE OTE							
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							4.80
		-					
		SUBTOTAL	S 1			\$1,250.00	\$1,250.00
			ALES TAX				
			ABOR TAX			\$212.50	\$212.50
		SUBTOTAL				\$1,462.50	\$1,462.50
			C OH & PROFIT				\$292.50
	SUB-CONTRACTORS	-	GC WORK				\$1,755.00
	dob dollinatorica						
		TOTAL SU	B WORK				
		10% G	C SUB PROFIT				
			ONTINGENCY C	N JOB			\$87.75
		TOTAL					\$1,842.75

ECO NAME:

EMCS Controls of Boiler and Chiller vs. Manual Control

ECO NUMBER:

88

TYPE: BLDG SYSTEM:

Bldg. 25910 Heating

DESCRIPTION

EXISTING CONDITIONS:

Existing automatic or manual plant controls are located within the plant only with no EMCS tie-in for control. The EMCS office which is manned 24 hours a day has very few, if any instrumentation readouts from the plant, and no control of the Plant with the EMCS. Because EMCS personnel are aware of what is happening in many buildings, they are also aware of conditions and demands on the high temperature water system. Currently, the boiler operators are making boiler pressure changes, HTW changes, bringing on and off boilers, and many manual valving operations. However, they are not performing the functions that an EMCS office can to reduce the energy consumed and to improve the operating efficiency of the plant.

PROPOSED CHANGE:

Connect most instrumentation and automatic controls and setpoint adjustments to the computerized EMCS system that is existing. EMCS personnel can then adjust HTW temperatures and temperature setpoints, and all new controls that may be added under other ECOs. All temperature, pressure and flow readings of new and existing instrumentation should be readable at the EMCS terminals. The individual that attends the Plant and that is not an EMCS operator shall have access to the readouts, but shall basically do maintenance most of the time, and turn on and off the equipment as required by the EMCS people.

CALCULATION & COST METHODOLOGY:

Required EMCS controls and instrumentation for the high temperature water system at Building 25910 with new hot water generators.

NO. POINTS

DOLLARS

Fuel flow	6	\$ 9,000
Explosion tank temperatures and pressures	6	3,000
Combustion air and flue gas	6	2,000
HTW pump operation/temperature, pressure, flow	10	7,000
Make-up water temperature, pressure, flow	3	3,500
Nitrogen storage - level, temperature, pressure	4	3,600
Valve Positions	10	3,000
Btu computation		2,500
Chemical feed	6	1,800
Hot water generator controls	6	3,000
Hot water generator combustion efficiency		1,200
Gauges and dials	15	8,000
Total	15	\$47,600
Total		Ψ17,000

This assumes that no additional manpower will be required by EMCS personnel, nor will there be any reduction of personnel in the plant to operate the valves. However, the change that will take place will be that the EMCS personnel will actually have either physical control or the ability to tell people in the Plant to change valve positions to start or stop equipment.

The savings for this ECO is 3% of the total gas consumption used in Building 25910. This overall efficiency improvement is based on the fact that there will be better regulation of HTW temperatures. The hot water generator firing rate can be adjusted for predicted loads which the EMCS people will monitor and record, and also pumping speed regulation will be controlled by EMCS so that all buildings will be adequately served to get the required amount of HTW with a minimum amount of pumping energy used. Another savings would be the combustion controls regulations so that by monitoring the air flows and the oxygen

ECO NAME:

EMCS Controls of Boiler and Chiller vs. Manual Control

(Cont'd)

ECO NUMBER:

88

TYPE: BLDG SYSTEM: Bldg. 25910

Heating

CALCULATION & COST METHODOLOGY:

in the flue gases some in the flue gases some regulation of the combustion of the new hot water generators will be available to be made by EMCS people either directly or by calling

in the operator that is available in the Plant.

Calculation is $\underline{.03 \times 152,777 \text{ mcf} \times 1,030,000 \text{ Btu's/mcf}} = 4,720.81 \text{ Million Btu's/yr.}$ $10^6 \text{ Btu's/Million Btu's}$

CONSTRUC	TION COST ESTIMATE				DATE:	23 SEP 94	SHEET1	OF 1
Project:	FORT GORDON ENERGY STUD	Υ						
Location:	AUGUSTA, GEORGIA					PROJ. NO.	4	
	HARRISON AND SPENCER, INC	· · · · · · · · · · · · · · · · · · ·				CODE:	BLDG 25330	
	ECO88 - EMCS CONTROLS - HEAT		Fst	imator:	H. TOUB	Checked:		
Summary:	ITEM	QUANTI	1	MATERIAL	11. 1005	LABOR		
DESC	CRIPTION	QUAN		UNIT COST	EXTENSION	UNIT COST	EXTENSION	TOTAL
FUEL FLOW		1	LS	4000	4000	2000	2000	\$6,000.00
EXPANSION T	ANK		LS	1400	1400	600	600	\$2,000.00
HTW PIPING			LS	2300	2300	2700	2700	\$5,000.00
MAKE-UP WA	TER		LS	2000	2000	1500	1500	\$3,500.00
NITROGEN			LS	1000	1000	1500	1500	\$2,500.00
VALVE POSIT			LS	700	700	1300	1300	\$2,000.00
BTU COMPUT			LS	500		2000	2000	\$2,500.00
CHEMICAL FE			LS	900	900	900	900	\$1,800.00
HW GENERAT	TOR PUMPS CONTROLS		LS	2000		1000	1000	\$3,000.00 \$1,200.00
HW GENERAT	TORS COMBUSTION EFFICIENCY		LS LS	600 2000		600 2000	600 2000	\$4,000.00
		SUBTO	TALS	1	\$17,400.00		\$16,100.00	\$33,500.00
		5%	SALE	ES TAX	\$870.00			\$870.00
		-		OR TAX			\$2,737.00	\$2,737.00
		SUBTO			\$18,270.00		\$18,837.00	\$37,107.00
				OH & PROFIT	V10,270.00			\$7,421.40
								\$44,528.40
	SUB-CONTRACTORS	SOBIO	TAL G	C WORK				Ψ11,020.10
		TOTAL	SUB \	WORK				
		-		SUB PROFIT				
				ITINGENCY OF	N JOB			\$2,226.4
		TOTAL						\$46,754.8

HEATING REOUIREMENTS DATA SUMMARY - BUILDING 25910:

INTRODUCTION:

Heat load requirements for the North Central Utility Plant were determined from field survey data. The data was analyzed using the Trane Trace 600 Load calculation program. The data reported in Tables 3A, 3B, and 3C are the results of the analysis. The data files produced from the Trace 600 program are contained in Appendix I. Load calculations were run for the 36 building types that represent all the building types serviced by the North Central Plant. These building types represent 86 total buildings serviced on the north side of the base from Building 25910. The following commentary explains the data contained in each of the tables.

Table 3A - Heating Profile - Building Types serviced by North Central Utility Plant-Building 25910

Each building type (36 total), as defined in the field survey, is listed across the top of the table. Values are recorded for every hour for twenty four hours. There are twelve sections to the table, one for each month of the year. Each entry is in thousands of BTU/hr. Table 3A therefore contains heating requirements for each building type for every hour of the day for all twelve months of the year in thousands of BTU's per hour (MBTUH). The last column on the right contains the total MBTUH values for each building type for a particular hour. The data shows that the loads are highest during the winter months of December, January, and February. As you proceed into spring, loads diminish and the hours requiring heat become less. As you proceed into the summer months you may see some shall loads reported. Keeping in mind that we are reporting loads in thousands of BTU's, the values are very small and are dropped in later calculations.

Table 3B - Heating Profile - Total of All Buildings Serviced By North Central Utility Plant-Building 25910

Some of the building types surveyed are representative of multiple buildings of the same type. Table 3B accounts for multiple buildings by building type. The totals column therefore is representative of the true hourly loads for each month. Building types representing more than one building are: Type 1A-6 buildings, Type 1B-3 buildings, Type 3A-9 buildings, Type 3B-3 buildings, Type 4A-17 buildings, Type 4B-10 buildings, Type 7-2 buildings, Type 8-2 buildings, Type 9-3 buildings, and Type 12-2 buildings. All the rest of the building types represent a single building each. There are a total of 84 buildings serviced by the Central Utility Plant Building 25910.

Table 3C - Heat Load Requirement Summary - North Utility Plant

This table is a compilation of the totals columns taken from Table 3B for each month. This Table provides a means to estimate plant heating load requirements on the hot water generating equipment at the North Plant.

SUMMARY:

All the data recorded in Table 3 (A, B & C) was derived from field survey information and the Trace 600 load calculations. See Appendix I for a complete printout of all generated data. The values appearing in Table 3A were taken directly from the Trace output data.

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	23		283	284	280	271	280	246	240	731	212	199	182	165	149	136	127	121	118	122	134	153	178	206	233	257	274
	 92		448	467	483	483	200	7 0 0	404	487	480	475	166	452	433	310	254	224	189	184	192	213	241	281	331	374	408
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6.	G	1079	1163	1230	1285	1321	1341	1329	1276	1184	1065	830	793	964	566	496	483	464	487	540	611	669	792	892
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TONNAGE PROFILE BY MONTH - BUILDINGS SERVICED BY NORTH CENTRAL UTILITY PLANT - BUILDING 25910

DAY	JAN	FEB	MAR	APR	MAY	JUN	JUL	AUG	SEP	OCT	NOV	DEC
HOUR	36795	30011	14289	484	372	0	0	0	236	10263	13647	24260
1	38316	32106	17449	833	639	0	0	0	484	13123	17070	26461
3	39235	34619	20314	2335	1050	0	45	0	822	16853	20017	28600
100000000000000000000000000000000000000	39768	36120	22824	4307	276	151	133	108	526	18968	22271	30118
4 5	40055	38261	24394	5588	531	257	203	217	407	20964	24232	31675
6	39771	39520	26107	8004	997	319	245	314	442	22875	26057	32764
7	39082	40726	26657	9428	1761	233	167	367	849	23589	27288	33350
8	38253	41011	26071	12022	1674	53	0	235	1145	22236	27680	32833
9	35813	39541	24148	10731	1357	0	0	23	768	19272	25373	30443
10	32675	37151	21001	7658	439	0	0	0	158	14845	21580	26848
11	29203	34358	16784	4196	36	0	0	0	0	10112	17054	17376
12	26212	31148	12714	1686	0	0	0	0	0	5511	11973	17844
13	22683	27072	8730	29	0	0	0	0	0	2857	7518	13857
14	19278	23149	5288	18	0	0	0	0	0	1237	4175	10748
15	16871	19865	3147	0	0	0	0	0	0	51	1981	8745
16	15048	17764	1580	0	0	0	0	0	0	22	666	7400
17	14577	16445	719	0	0	0	0	0	0	33	406	7515
18	16216	16399	525	0	0	0	0	0	0	66	519	8344
19	18277	17498	795	0	0	0	0	0	0	201	1080	9974
20	21370	19088	1569	0	0	0	0	0	0	499	2157	12307
21	24481	20784	2701	140	0	0	0	0	0	1175	3332	14568
22	28251	22901	4393	359	0	0	0	0	0	2185	5276	16930
23	31292	25215	7163	697	0	0		0	0	3591	7318	19556
24	34452	27449	11025	449	30	0	0	0	10	6114	10011	21775

Table 3C

ROWLAND 01!Fort Gordon P1CARLTON SHUFORD P2DSN 780-6376 P3ATZH-DIC-E /RECALL F 000045555 S 03

ECIP PROJECT 3: UPGRADE BOILER PLANT BUILDING 25910, FT. GORDON

03A !DESCRIPTION OF PROPOSED CONSTRUCTION

***The concept of the heating plant as a steam generating boiler plant which sparges steam into the high temperature water, and is then pumped through the underground pipe distribution has changed completely. The new concept is to replace the steam boilers with hot water generators operating in an auxiliary loop circulating HTW water system from and to the three existing cascade heaters that will be converted for use as expansion/storage tanks. Those tanks will now be pressurized with nitrogen and the pressure on the tank will vary as the water level increases or decreases. The water level will change based on the variable speed pumping and losses in the system. The existing deaerator needs to be modified before any other work is done. The deaerator vessel and storage tank are hopefully reusable, but is our suspicion that the trays within the deaerator are not operating or need to be replace entirely. Another item that needs to be done prior to making the switch over from steam to hot water is to add chemical feed tanks and have chemicals feed at the appropriate locations. This should be done in coordination with the chemical supplier, but basically we are adding sulfite and PH control to the make-up water in the deaerator or immediately after the deaerator. Then there is an additional chemical that needs to be added to the distribution system to make sure that the oxygen corrosion is not an additional problem, and that exposed piping does not corrode. The distribution piping shall also be protected from oxygen pitting and PH imbalance when the make-up water requirement is reduced.

Because there is a multiplicity of units available to be converted and to be replaced with new, it is possible that the steam can remain in operation while the new hot water generators are added and one or more of the cascade heaters is converted so that the plant can serve the needs of the distribution system during the construction period. Then there will be a small shutdown period where you convert over to hot water generation from steam generation. If this can be coordinated with the summer shutdown so that all of the work in the buildings is completed to generate domestic water, then the HTW system can be shutdown 4-1/2 months of the summer to make this conversion from steam to hot water generation.

03B !REMARKS

***Data for this analysis was based on assumed existing efficiency of the boilers of 70%. This was in lieu of not having any accurate information on the efficiencies of the boilers. Recent articles in the ASHRAE Journal and elsewhere indicates that for the Plant as it is now, 70% is probably a very high efficiency for the actual conditions. Even with this payback indicated, we can expect a better payback if the projects are implemented. There are also opportunities to increase the savings if higher efficiency equipment is installed in the buildings. We assumed 80% efficiency for gas combustion, but there are gas-fired heaters that can get into the 90's. This costs additional money, but they may be worthwhile on the basis of dollars they save when the current natural gas prices are compared with high efficiency water heating equipment prices.

The energy conservation measure to upgrade the Heating Plant in Building 25910 includes seven ECO's developed during the extensive engineering study that was conducted. The following describes the ECO's that are included in this ECIP.

ECO NO.	DESCRIPTION
25	Variable Speed Hot Water Pumping
27	Return Hot Water Temperature Control
31	Reduce Make-Up Water-Hot Water
67	Hot Water Generators
69	Summer Shut Down (1/2 Gas, 1/2 Heat Pumps)
71	Reduce Steam Leaks
88	EMCS Controls & Instrumentation

ECO DATA COMPILATION

ECO NO. DESCRIPTION	COST (FROM LCC)	SAVINGS 1ST YEAR	TOTAL DISCOUNT SAVINGS
25 Variable Speed Hot Water Pumping	179,986	15,962	245,689
27 Return Hot Water Temperature Control	70,597	19,181	339,832
31 Reduce Make-Up Water-Hot Water	61,451	26,829	551,858
67 Hot Water Generators	1,499,570	97,887	1,946,822
69 Summer Shut Down (1/2 Gas, 1/2 Heat Pur	, ,	172,367	3,034,235
71 Reduce Steam Leaks	2,056	1,793	37,594
88 EMCS Controls & Instrumentation	74,163	21,244	445,267
Totals	2,336,519	355,263	6,601,297

03C PROJECT DESCRIPTION

***This Energy conservation measure provides the plan to design the required conservation and upgrade to the heating system in building 25910 - Central Utility Plant - North. The scope of this effort includes addition of two new variable speed pumps, additional control for hot water return temperature regulation, reduction of make-up water required and replacement of five low efficiency steam boilers with three hot water generators. In addition the piping distribution system will be redesigned into three distribution systems and hot water/steam leaks will be reduced or eliminated.

To maximize energy savings, new EMCS controls will be added to permit control of the HTW system from the Energy Management Control System. This system will permit optimization of how water temperature set point, time of day scheduling and summer shut down of the system. This function will support minimizing staffing requirements.

03D !REQUIREMENT (Why is it needed now)

****The existing steam heating plant is antequated and inefficient. The study showed that the boilers are

operating at about 70% efficiency, large quantities of make-up water is required to overcome leaks in the existing system. Recent building renovations to the hot water systems in the Barracks, classrooms and administrative office have increased demand for heating capacity.

By implementing the energy conservation improvement now, annual savings of \$354,008 can be realized, reducing the cost of operation for the entire facility.

03E !CURRENT SITUATION (How is the need currently being met)

***ECO 25

There are three zones leaving Plant 25910. Each has a set of identical pumps serving each zone. Zones 1 and 3 have 50 hp motors rated at 3550 rpm. Zone 2 has the same pump with a 75 hp motor rated at 3550 rpm. The pumps usually operate on the low speed which is 1750 rpm, and the horsepower is 1/4 of that given above at the higher speeds. Pumps in Zone 1 are Dean Brothers pumps sizes 3 x 4 x 9-1/4 impeller, Model No. 8434; the Serial No. on one of the pumps is 148840. The pumps in the other zones are similar. Just upstream of the HTW pumps is the blending station which blends return HTW with water leaving the cascade heater to maintain a setpoint temperature at the blending station for HTW supply water. Water levels in the cascade heaters are effected by the setpoints on the HTW blending stations. By decreasing the temperature setting on Zone 3 Blending Station, it was noted that the HTW return water flow increased and then the level of the cascade heater above Zone 3 went up relative to the water levels in the other cascade heaters. Entering each building at the distribution system is a 2-way valve so that when HTW is not required in the building on the distribution system, the flow ceases to that building.

ECO 27

HTW is heated in cascade heaters, which is usually maintained at the temperature of the saturation pressure of the boiler, and this boiler pressure is usually maintained except for several times a year when it is changed. At 150 psi, the saturation temperature is 347°F. When the HTW water leaves the cascade heaters, it passes through a blender that adds unheated HTW return to control the setpoint that maintains the constant HTW supply temperature. Note that as distribution loads vary; less or more HTW water is required, and the HTW return temperature rises and falls depending upon the load. The existing system operates to control the HTW supply water, and does not take into account changes to load that would effect the overall heating requirements.

ECO 31

The total number of gallons lost in Building 25910 over the course of 1992 is 2,039,102 gallons. This leakage is caused by pipe failures and operating inefficiencies in the system and the quantity of lost water is based on reports of water meter readings made by the boiler plant operators.

ECO 67

There are five boilers in Building 25910 heating and cooling plant which have not been tested for combustion efficiency in the studies conducted several years ago because of reported asbestos. These boilers are firing with natural gas and No. 2 oil, but they were originally built for coal firing. 70%

combustion efficiency is assumed for this report, but it would not be surprising if, upon conducting tests, this efficiency was found to be lower than 70%. The furnace area is spacious with less heat absorbing tubes than would be in a boiler designed for natural gas firing. The rear section of the boiler is under negative pressure from the high stack and ID fans so air leakage into the boiler is expected. From the recorded temperatures leaving the boilers it is reasonable to believe that air leakage is reducing the expected flue gas temperature by 70-100°F. Only three of the five boilers are currently operable in 1994.

ECO 69

Space heating is not required from mid-May through the end of September, but a boiler must be in operation to handle domestic water needs and cooking requirements in some cases with the HTW distribution system.

ECO 71

There are steam leaks in some valves and in holes drilled in the cascade heaters. The total steam leakage is approximated at 50 lbs per hour, which is the equivalent of a half-inch hole at 14,000 ft. per minute steam flow.

ECO 88

Existing plant controls are automatic or manual within the plant only with no EMCS tie-in for control. EMCS office which is manned 24 hours a day has very few, if any instrumentation readouts from the plant, and no controllability of the Plant with the EMCS. Because EMCS personnel are aware of what is happening in many buildings, they are also aware of what is happening on the high temperature water system pertaining to conditions and demands. Currently, the boiler operators are making boiler pressure changes, HTW changes, bringing on and off boilers, and many manual valving operations. However, they are not performing the functions that an EMCS office can to reduce the energy consumed and to improve the operating efficiency of the plant.

03F !IMPACT IF NOT PROVIDED

***If this project is not implemented, Fort Gordon will continue to waste excessive quantities of energy. Use of antiquated, inefficient and potentially hazardous boilers will continue to require full staffing of boiler rooms and preclude the possibility of reducing energy waste and reducing staffing requirements. The lack of instrumentation on the current system assures energy waste and ultimately high maintenance costs due to inefficient use of the boiler system.

Annual discounted savings has been determined to be \$6,574,981 with a simple payback of 6.6 years with a savings to investment (SIR) of 2.81.

heating loads will be unevenly distributed and buildings currently not being provided adequately heating will continue to be cold in the winter.

03G !ADDITIONAL

***New construction and renovation projects on the base will increase demand on the boiler plant to respond to new loading conditions.

03I !RELATED PROJECTS

***ECIP - 45553 - Chilled Water System - Building 25910

ECIP - 45554 - Chilled Water System to Central Utility Plant - Building 25330 South Side

ECIP - 45556 - High Temperature Water System South Plant - Building 25330 /*

07A !GENERAL JUSTIFICATION DATA

***This ECIP project is required to support the army wide effort to reduce energy waste. The project will provide new efficient high temperature hot water boilers and variable speed pumps to reduce energy consumption and increase efficiency. New instrumentation will permit better control and provide a means to reduce staffing requirements.

This ECIP consists of seven ECO's identified during an energy study that constitute a cost justifiable solution to deficiencies in the current operation. The following justification overview lists the ECO's along with their economic justification.

PROJECT NO. 1 - BOLLER/HOT WATER SYSTEM NORTH

	r		EAR SAVINGS		81 339,832		87 1,946,822		57 3,034,235			445,267	63 6,601,297
	c	SAVINGS SAVINGS	J/YR <u>1stY</u>]			26,829			172,367		•	21,244	355,263
	F	SAVING	MMBT	O	2,040.00	5,587.70	15,736.03		17,161.56	000	398.58	4,720.81	45,644.88
		SAVINGS	MMBTU/YR	785.13	0	0	0		995.23	C	0	0	1780.36
		COST	(From LCC)	179,986	70,597	61,451	1,499,570		448,696		2,056	74,163	2,336,519
	NON-	RECURRING COST (-)	SAVINGS (+)	0	0	0	Items from LCCD	on ECO 67	0	•	0	0	Same as ECO 67
000000000000000000000000000000000000000		ANNUAL	COST	4,000	10,000	1,684	S		79,795	,	0	0	110,659
		CONSTRUCTION	COST	161,421.12	63,315.00	55,112.40	1,344,905.10		402,417.70		1,842.75	66,512.88	2,095,527
	ECO DATA COLLECTION		DESCRIPTION	Variable Sneed Hot Water Pumping	Return Hot Water Temperature Control	Reduce Make-Up Water-Hot Water	Hot Water Generators		Summer Shut Down	(1/2 Gas, 1/2 Heat Pumps)	Reduce Steam Leaks	EMCS Controls & Instrumentation	Totals
	ECO	ECO	NO.	25	27	7	19		269		71	00	

 $\frac{2,336,519}{355,263}$ = 6.58 years Simple Payback:

Simple Payback:

 $\frac{6,601,297}{2,336,519} = 2.83$

SIR:

07B !TRAFFIC ANALYSIS

***There will be no changes to pedestrian or vehicular traffic as a result of implementing this ECIP.
/*

08B !PRESENT ACCOMMODATIONS AND DISPOSITION

***The physical plant building 25910 housing the boiler plant is adequate to accommodate the new boilers and other modifications once the old boilers are removed. Five Steam boilers are being replaced with three high temperature hot water boilers.

09D !RPMA DISCUSSION

***This ECIP will reduce the amount of Real Property Maintenance Activity because the number of boilers will be reduced, the equipment will be new and deficiencies in the existing miscellaneous equipment such as pipes, valves, strainers, heat exchangers, deaerator vessels and expansion tanks will be replaced or refurbished to provide optimal efficiency. The new equipment will be easier to operate requiring less manual operation and attendance.

10A !ANALYSIS OF DEFICIENCIES

- ***1) The HW pumps are constant volume pumps and run continuously to supply hot water to the north side of the base. This causes excess power to be consumed even during periods of reduced demand. It is more efficient to have a variable speed pumping capability to off load the pumps, reducing their flow and energy consumption during moderate temperature conditions.
- 2) Boiler temperature settings are currently set at a constant value regardless of the load requirements. The new system will regulate supply temperature necessary to meet the load requirements. Current control methods set and keep the temperature constant regardless of the requirements, thus wasting energy by overgenerating HTHW.
- 3) Five old coal fired boilers, converted to using No. 2 oil or natural gas are currently in use. The boilers are inefficient because of the heat chamber is designed for goal firing and have fewer tubes than boilers designed for oil or natural gas. Air leakage into the boiler has reduced the stack temperatures by 70 to 100 F, resulting in inefficient transfer of heat. Only three of the five boilers is currently operational.
- 4) Existing plant controls are not connected to the energy management control system (EMCS) that is controlling many of the existing facilities. The controls require constant supervision by maintenance personnel. The controls are antiquated and the calibration is questionable, thus creating the conditions for energy waste.

 /*

11D !DECISION ANALYSIS

***The following is a detailed breakdown of each of the ECO's. Refer to the table in 7A General Justification Data which summarizes these costs.

ECO 25 - LCCA

1.	Investment		
	A. Construction Cost	\$	161,421.00
	B. SIOH	\$	8,879.00
	C. Design Cost	\$	9,686.00
	D. Total Cost $(1A + 1B + 1C)$	\$	179,986.00
2.	Energy Savings	\$	- 5,209.00
3.	Non Energy Savings	\$	58,960.00
4.	First Year Dollar Savings	\$	15,962.00
5 .	Simple Payback Period	\$	11.28 Years
6.	Total Net Discounted Savings	\$	245,689.00
7.	Savings to Investment Ratio	\$	1.37
ECO	27 - LCCA		
1.	Investment		
	A. Construction Cost	\$	63,315.00
	B. SIOH	\$	3,483.00
	C. Design Cost	\$	3,799.00
	D. Total Cost $(1A + 1B + 1C)$	\$	70,597.00
2.	Energy Savings	\$ \$	-3,954.00
3.	Non Energy Savings	\$	147,400.00
4.	First Year Dollar Savings	\$	19,181.00
5.	Simple Payback Period	\$	3.68 Years
6.	Total Net Discounted Savings	\$ \$	339,832.00
7.	Savings to Investment Ratio	\$	4.81
ECO	31 - LCCA		
1.	Investment		
	A. Construction Cost	\$	55,112.00
	B. SIOH	\$	3,032.00
	C. Design Cost	\$	3,307.00
	D. Total Cost $(1A + 1B + 1C)$	\$	61,451.00
2.	Energy Savings	\$	-406.00
3.	Non Energy Savings	\$	24,827.00
4.	First Year Dollar Savings	\$	26,829.00
5.	Simple Payback Period	\$	2.29 Years
6.	Total Net Discounted Savings	\$	551,858.00
7.	Savings to Investment Ratio	\$	8.98

ECO 67 - LCCA

1.	Investment		
1.	A. Construction Cost	\$	1,344,905.00
	B. SIOH	\$	73,970.00
	C. Design Cost	\$	80,695.00
	D. Total Cost (1A + 1B + 1C)	\$	1,499,570.00
2.	Energy Savings	\$	9,742.00
3.	Non Energy Savings	\$	462,600.00
4.	First Year Dollar Savings	\$	97,887.00
5.	Simple Payback Period	\$	15.32 Years
6.	Total Net Discounted Savings	\$	1,946,822.00
7.	Savings to Investment Ratio	\$	1.30
7.	Savings to investment Ratio	Ψ	1.50
ECO 6	59A - LCCA		
1.	Investment		
	A. Construction Cost	\$	514,609.00
	B. SIOH	\$	15,730.00
	C. Design Cost	\$	17,160.00
	D. Total Cost $(1A + 1B + 1C)$	\$	547,499.00
2.	Energy Savings	\$	13,158.00
3.	Non Energy Savings	\$	1,178,832.00
4.	First Year Dollar Savings	\$	187,530.00
5.	Simple Payback Period	\$	2.92 Years
6.	Total Net Discounted Savings	\$	3,270,933.00
7.	Savings to Investment Ratio	\$	5.97
ECO 6	59B - LCCA		
	•		
1.	Investment	Φ	290,266.00
	A. Construction Cost	\$ \$	15,965.00
	B. SIOH	\$	17,416.00
	C. Design Cost	\$	323,647.00
•	D. Total Cost $(1A + 1B + 1C)$	\$	11,168.00
2.	Energy Savings	\$	1,178,832.00
3.	Non Energy Savings		157,203.00
4.	First Year Dollar Savings	\$ \$	2.06 Years
5.	Simple Payback Period	\$	2,797,538.00
6.	Total Net Discounted Savings	\$ \$	8.64
7.	Savings to Investment Ratio	Φ	0.04

ECO 69C - LCCA

1.	Investment	
	A. Construction Cost	\$ 402,418.00
	B. SIOH	\$ 22,133.00
	C. Design Cost	\$ 24,145.00
	D. Total Cost $(1A + 1B + 1C)$	\$ 448,696.00
2.	Energy Savings	\$ 12,163.00
3.	Non Energy Savings	\$ 1,178,832.00
4.	First Year Dollar Savings	\$ 172,367.00
5.	Simple Payback Period	\$ 2.60 Years
6.	Total Net Discounted Savings	\$ 3,034,235.00
7.	Savings to Investment Ratio	\$ 6.76
ECO	71 - LCCA	
1.	Investment	
	A. Construction Cost	\$ 1,843.00
	B. SIOH	\$ 102.00
	C. Design Cost	\$ 111.00
	D. Total Cost $(1A + 1B + 1C)$	\$ 2,056.00
2.	Energy Savings	\$ -5,874.00
3.	Non Energy Savings	\$ 0.00
4.	First Year Dollar Savings	\$ 538.00
5.	Simple Payback Period	\$ 3.82 Years
6.	Total Net Discounted Savings	\$ 11,278.00
7.	Savings to Investment Ratio	\$ 5.49
ECO	88 - LCCA	
1.	Investment	
	A. Construction Cost	\$ 66,513.00
	B. SIOH	\$ 3,659.00
	C. Design Cost	\$ 3,991.00
	D. Total Cost $(1A + 1B + 1C)$	\$ 74,163.00
2.	Energy Savings	\$ -1,273.00
3.	Non Energy Savings	\$ 0.00
4.	First Year Dollar Savings	\$ 21,244.00
5.	Simple Payback Period	\$ 3.49 Years
6.	Total Net Discounted Savings	\$ 445,267.00
7.	Savings to Investment Ratio	\$ 6.00

11E !ECONOMIC ANALYSIS ***ECO 25

ITEM DESCRIPTION	QUANTI QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Electrical Work Piping Demolition New Pumps Variable Speed Drive Switches	1 1 1 2 1	LS LS LS EA LS	4,000 20,000 12,500 8,500 4,340	4,000 20,000 25,000 8,500 4,340	6,000 25,000 15,000 3,000 1,000	25,000 15,000	\$10,000.00 \$45,000.00 \$15,000.00 \$31,000.00 \$9,500.00 \$5,340.00
					UBTOTAL GC ONLY) C'S WORK		\$128,112.00 \$25,622.40 \$153,734.40
				SUBTOTAL (GO 5% CONT	C & SUBS) INGENCY TOTAL		\$153,734.40 \$7,686.72 \$161,421.12
ECO 27							
ITEM DESCRIPTION	QUANTI QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Controls Demolition of Control Equip.	1	LS LS	20,000	20,000	15,000	15,000 10,000	\$35,000.00 \$10,000.00
					UBTOTAL GC ONLY) C'S WORK		\$50,250.00 \$10,050.00 \$60,300.00
				SUBTOTAL (G 5% CONT	C & SUBS) TINGENCY TOTAL		\$60,300.00 \$3,015.00 \$63,315.00
ECO 31							
ITEM DESCRIPTION	QUANT QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Flow Meters Temp ROD In Distribution	12 12	EA EA	1,500 300	18,000 3,600	1,000 500	12,000 6,000	\$30,000.00 \$9,600.00
					SUBTOTAL (GC ONLY) GC'S WORK		\$43,740.00 \$8,748.00 \$52,488.00
				SUBTOTAL (G 5% CON	C & SUBS) TINGENCY TOTAL		\$52,488.00 \$2,624.40 \$55,112.40

ECO 67

ITEM DESCRIPTION	QUANT QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSIO	n total	
Bisselli Holl	QOIL.	01111	01111 0001					
Hot Water Generator	3	EA	250,000	750,000	Lump Sum	100,000	\$850,000.00	
Repiping of Cascade Heater	3	Ton	3,000	9,000	4,000	12,000	\$21,000.00	
Piping For 1 Zone From 3 Zone	1	LS	20,000	20,000	30,000	30,000	\$50,000.00	
Demolition	1	LS			35,000	35,000	\$35,000.00	
Deaerator Repair	1	LS	5,000	5,000	7,500	7,500	\$12,500.00	
Chemical feed Equipment	3	EA	2,500	10,000	500	1,500	\$9,000.00	
Nitrogen Storage & Piping	1	LS	10,000	10,000	7,000	7,000	\$17,000.00	
				SU	JBTOTAL 1		\$994,500.00	
					SALES TAX		\$40,075.00	
					ABOR TAX		\$32,810.00	
					JBTOTAL 2		\$1,067,385.00	
					I & PROFIT		\$213,477.00	
					GC WORK	\$1,280,862.00		
				5% CON	TINGENCY		\$64,043.10	
				5,0001	TOTAL		\$1,344,905.10	
ECO 69A								
ITEM	QUAN'	TITY	MATERIAL		LABOR			
DESCRIPTION	QUAN		UNIT COST	EXTENSION	UNIT COST	EXTENSIO	ON TOTAL	
2-1/2 Ton Heat pump (96 Bldg	g) 1	LS	19,200	19,200	24,000	24,000	\$216,000.00	

48,000

30,000

12,000

40,000

20,000

12,000

TOTAL

SUBTOTAL 1 5% SALES TAX

SUBTOTAL 2

17% LABOR TAX

20% GC OH & PROFIT

SUBTOTAL GC WORK

5% CONTINGENCY

LS

LS

LS

1

1

1

Piping & Pumps to Exist Tanks

FCU In Building

Electrical Work

48,000

30,000

12,000

40,000

20,000

12,000

\$88,000.00

\$50,000.00

\$378,000.00

\$14,100.00 \$16,320.00

\$408,420.00

\$81,684.00

\$24,505.20

\$514,609.20

\$490,104.00

24,000.00

ECO 69B

ITEM DESCRIPTION	QUAN QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Gas Piping (96 Bldgs) Combustion Air Ventilation (9 Gas Fired Water Heater (96 Bl Piping To Existing Storage Tar Pumps (96 Bldgs)	dg) 1	LS LS LS LS	30,000 5,000 20,000 30,000 9,600	30,000 5,000 20,000 30,000 9,600	60,000 9,600 12,400 25,000 5,000	60,000 9,600 12,400 25,000 5,000	\$90,000.00 \$14,600.00 \$32,400.00 \$55,000.00 \$14,600.00
				5% S. 17% LA		5	\$206,600.00 \$4,730.00 \$19,040.00 \$230,370.00 \$46,074.00 \$276,444.00
ECO 71				5% CONT	INGENCY TOTAL		\$13,822.20 \$290,266.20
ITEM DESCRIPTION	QUAN QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Repair Steam Leaks	50	HRS			25	1,250	\$1,250.00
				5% S 17% LA			\$1,250.00 \$212.50 \$1,462.50 \$292.50 \$1755.00
				5% CONT	TINGENCY TOTAL		\$87.75 \$1,842.75

ECO 88

ITEM	QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
DESCRIPTION	QUAN	UNII	UNII COST	EXTENSION	ONII COSI	EXTENSION	IOIAL
Fuel Flow	1	LS	6,000	6,000	3,000	3,000	\$9,000.00
Expansion Tank Temp & Press	ure 1	LS	2,000	2,000	1,000	1,000	\$3,000.00
Combustion Air & Flue Gas	1	LS	1,000	1,000	1,000	1,000	\$2,000.00
HTW Pump Operation (T,P,F)	1	LS	3,000	3,000	4,000	4,000	\$7,000.00
Make-Up Water (T,P,F)	1	LS	2,000	2,000	1,500	1,500	\$3,500.00
Nitrogen Storage (Level, T,P)	1	LS	1,200	1,200	2,400	2,400	\$3,600.00
Valve Positions	1	LS	1,000	1,000	2,000	2,000	\$3,000.00
BTU Computation	1	LS	500	500	2,000	2,000	\$2,500.00
Chemical Feed	1	LS	900	900	900	900	1,800.00
HW Generator Pumps Controls	1	LS	2,000	2,000	1,000	1,000	\$3,000.00
HW Generator Combustion Eff		LS	600	600	600	600	\$1,200.00
Gauges & Dials	1	LS	4,000	4,000	4,000	4,000	\$8,000.00
				SU	BTOTAL 1		\$47,600.00
				5% S	ALES TAX		\$1,210.00
				17% LA	ABOR TAX		\$3,978.00
				SU	BTOTAL 2		\$52,788.00
				20% GC OH	& PROFIT		\$10,557.60
				SUBTOTAL	GC WORK		\$63,345.60
				5% CON	TINGENCY		\$3,167.28
				2.03011.	TOTAL		\$66,512.88

12A !CRITERIA FOR PROPOSED CONSTRUCTION

***Construction will occur inside the confines of the existing Building 25910. No additions to the exterior shell is required. Inside renovation work will conform to existing guidelines of architectural design and building construction, specifically the AEI Design Guide (March 1987), the Corps of Engineers Guide Specifications CEGS 13947 thru 13949 for Power Plant and EMCS requirements.

13B !FURNISHINGS AND EQUIPMENT DISCUSSION

- ***This ECIP consists of the following renovations and additions;
- 1) Replace 5 steam boilers with 3 HTHW boilers,
- 2) Add Variable Speed Drives for two pumps, and eliminate the need for a third existing pump,
- 3) Install new instrumentation and controls that will interface to the existing EMCS system at the base.

15A !ENVIRONMENTAL DOCUMENTATION

***There will be no environmental impact to the modification, renovations and upgrades to the central utility plant heating system. Boilers being replaced will be dismantled and new high efficiency boilers, pumps and heat. The addition of chemical treatment system will be handled in accordance with state and federal regulations.

15B1 !SUMMARY OF ENVIRONMENTAL CONSEQUENCES

***We have reviewed this project and determine that an environmental impact statement, pursuant to PL 91-190, is not required. We have assessed this project and determined that it will not contribute significantly to air and/or water pollution.

16A1 !EVALUATION OF FLOOD HAZARDS

***The renovation is to an existing plant. No history of flooding has been recorded.

19A !SUMMARY OF ENERGY REQUIREMENTS

***Current Electrical oil and gas services are adequate to support the required upgrades to the heating system for the Central Utility Plant, Building 25910. There will be no changes or increased requirements for additional services. The demand for utility service will be reduced as the changes are implemented. See the cost and savings analysis for details.

19B !SUMMARY OF UTILITY SUPPORT

***No additional service will be required.

/RECALL F 000045555 S 20 20B !HAZARDS TO HANDICAPPED PERSONS

***Existing conditions within the physical plant is considered hazardous to unauthorized personnel. Signs and warnings are posted to alert unauthorized personnel access is restricted to authorized personnel and visitors with prior approval.

20C !HANDICAP PROVISIONS

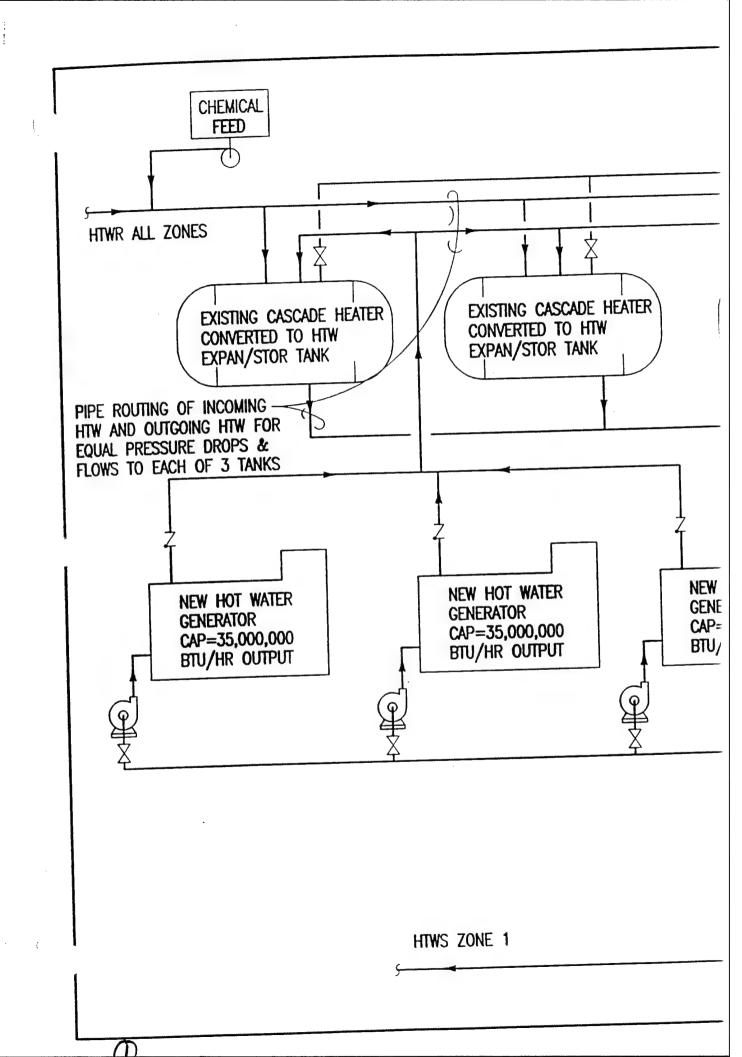
***In accordance with Public Law 90-480, no provisions for the handicapped will be made in the project since the facility is used and operated solely by able bodied personnel. However, the main floor of the facility is at ground level and is handicap accessible.

/*

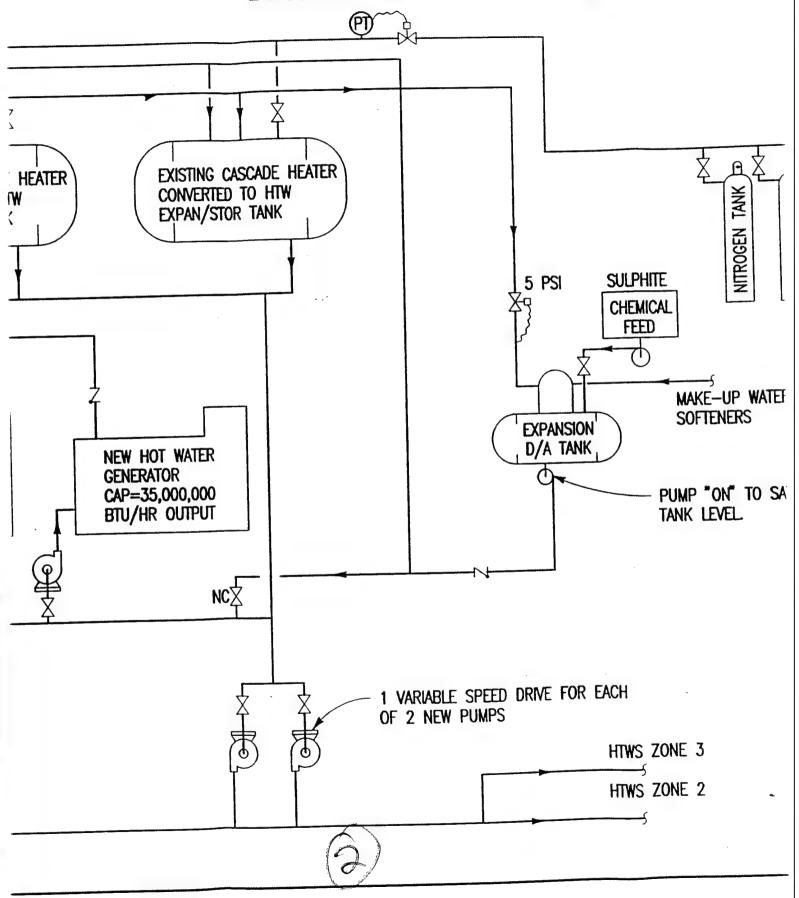
22B !PHYSICAL SECURITY

***Project is not considered for commercial activity. The physical plant upgrade to the existing Central Utility Plant will serve the north side of Ft. Gordon. Provisions of DA circular 235-1 are not applicable to this project.

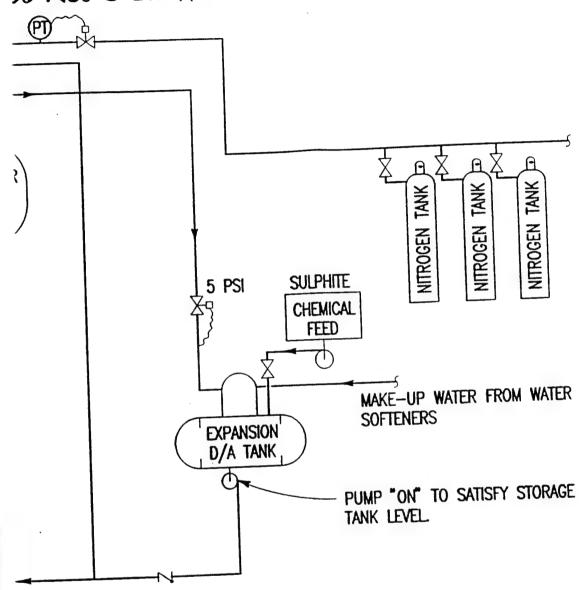
/*



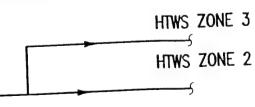
Project No. 3 HTW Schematic North-



it No. 3 MTW Schematic North-Bldg. 25910



1 VARIABLE SPEED DRIVE FOR EACH OF 2 NEW PUMPS



LIFE CYCLE COST ENERGY CONSERVATION INSTALLATION & LOCATION: PROJECT NO. & TITLE: 3 FISCAL YEAR 1994 DISCE ANALYSIS DATE: 09-21-94	INVESTMENT PR FT. GORDON HTW NORTH	OGRAM (EC) REGION NO	IP) DS. 4 CE ABLE SPEE	LCCID NSUS: 3 D PUMP:	1.080 3 ING
1. INVESTMENT A. CONSTRUCTION COST B. SIOH C. DESIGN COST D. TOTAL COST (1A+1B+1C) E. SALVAGE VALUE OF EXIST F. PUBLIC UTILITY COMPANY G. TOTAL INVESTMENT (1D	\$ 179986. TING EQUIPMENT TREBATE	\$	0. 0. \$	179986	
2. ENERGY SAVINGS (+) / C DATE OF NISTIR 85-3273-X UNIT COST FUEL \$/MBTU(1)	USED FOR DISC SAVINGS MBTU/YR(2)	ANNUAL \$ SAVINGS (3) FACTO	OR (4)	DISCOUNTED SAVINGS(5)
A. ELECT \$ 15.24 B. DIST \$ 8.82 C. RESID \$ 2.73 D. NAT G \$ 4.50 E. COAL \$ 1.61 F. LPG \$ 6.34 M. DEMAND SAVINGS N. TOTAL	0. 0. 0. 0.	\$ 11962 \$ 0 \$ 0 \$ 0 \$ 0 \$ 0 \$ 11962	19. 19. 19. 19. 19. 19. 19. 19. 19. 19.	5.61 7.56 9.97 0.96 7.58 6.12 4.74	\$ 186729. \$ 0. \$ 0. \$ 0. \$ 0. \$ 0. \$ 0. \$ 186729.
3. NON ENERGY SAVINGS(+) A. ANNUAL RECURRING (X 3A1)	1	4.74	\$ 4000. \$ 58960.
B. NON RECURRING SAVI	NGS(+) / COST SAVINGS(+ COST(-)	S(-)	DISCNT FACTR	SAVI	OUNTED NGS (+) / (-) (4)
d. TOTAL	\$ 0.				0.
C. TOTAL NON ENERGY I	DISCOUNTED SAV	'INGS(+)/C	OST(-)(3 <i>I</i>	A2+3Bd4)\$ 58960.
4. FIRST YEAR DOLLAR SA	/INGS 2N3+3A+(3Bd1/(YRS	ECONOMIC	C LIFE))\$ 15962.
5. SIMPLE PAYBACK PERIOR) (1G/4)				11.28 YEAR
6. TOTAL NET DISCOUNTED	SAVINGS (2N5-	+3C)			\$ 245689.
7. SAVINGS TO INVESTMENT (IF < 1 PROJECT DOE	T RATIO S NOT QUALIFY)	(SIR) = (6 / 1G)=		1.37
8. ADJUSTED INTERNAL RA	TE OF RETURN	(AIRR):			4.72 %

LIFE CYCLE COST ANALYSIS SUMMARY

ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP)

LCCID 1.080 LIFE CYCLE COST ANALYSIS SUMMARY INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 3 HTW NORTH FISCAL YEAR 1994 DISCRETE PORTION NAME: CONTROLS ANALYSIS DATE: 09-21-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 63315.
B. SIOH \$ 3483.
C. DESIGN COST \$ 3799.
D. TOTAL COST (1A+1B+1C) \$ 70597. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$
F. PUBLIC UTILITY COMPANY REBATE \$ 0. 0. G. TOTAL INVESTMENT (1D - 1E - 1F) 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNTED FUEL \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) 3. NON ENERGY SAVINGS(+) / COST(-) \$ 10000. 14.74 \$ 147400. (1) DISCOUNT FACTOR (TABLE A) A. ANNUAL RECURRING (+/-) (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS(+) / COSTS(-) SAVINGS(+) / COSTS(-)

SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4) ITEM 0. \$ 0. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 147400. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 19181. 3.68 YEAR: 5. SIMPLE PAYBACK PERIOD (1G/4) \$ 339832. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 4.81 (IF < 1 PROJECT DOES NOT QUALIFY) 11.53 % 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

LIFE CYCLE COST ENERGY CONSERVATION INSTALLATION & LOCATION: PROJECT NO. & TITLE: 3 FISCAL YEAR 1994 DISCH ANALYSIS DATE: 09-21-94	FT. GORDON HTW NORTH PETE PORTION NA	REGION NOS.	4 CENSUS:	3	
1. INVESTMENT A. CONSTRUCTION COST B. SIOH C. DESIGN COST D. TOTAL COST (1A+1B+1C) E. SALVAGE VALUE OF EXIST F. PUBLIC UTILITY COMPANY G. TOTAL INVESTMENT (1D	S 61451. FING EQUIPMENT FREBATE	Ş 0.		1.	
2. ENERGY SAVINGS (+) / CONTROL OF NISTIR 85-3273-X UNIT COST FUEL \$/MBTU(1)	USED FOR DISC SAVINGS	ANNUAL \$	DISCOUNT		OUNTED NGS (5)
A. ELECT \$ 15.24 B. DIST \$ 8.82 C. RESID \$ 2.73 D. NAT G \$ 4.50 E. COAL \$ 1.61 F. LPG \$ 6.34 M. DEMAND SAVINGS N. TOTAL	0. 0. 0. 5588. 0. 0.	\$ 0. \$ 0. \$ 0. \$ 25145. \$ 0. \$ 0. \$ 25145.	15.61 17.56 19.97 20.96 17.58 16.12 14.74	\$ \$ \$	0. 0. 0. 527032. 0. 0. 0. 527032.
3. NON ENERGY SAVINGS(+)	/ COST(-)				
A. ANNUAL RECURRING ((1) DISCOUNT FACT (2) DISCOUNTED SA	+/-) OR (TABLE A) VING/COST (3A	х за1)	14.74	\$ \$	1684. 24827.
B. NON RECURRING SAVI	NGS(+) / COSTS	S(-) YR DISC OC FACT	CNT DISC	COUNTE INGS (+ I (-) (4	+)/
d. TOTAL	\$ 0.			0	•
C. TOTAL NON ENERGY I	DISCOUNTED SAV	INGS(+)/COST	(-) (3A2+3Bd	4)\$	24827.
4. FIRST YEAR DOLLAR SAY	VINGS 2N3+3A+(3Bd1/(YRS EC	ONOMIC LIFE))\$	26829.
5. SIMPLE PAYBACK PERIO	O (1G/4)			-	2.29 YEAR:
6. TOTAL NET DISCOUNTED	SAVINGS (2N5+	3C)		\$	551858.
7. SAVINGS TO INVESTMENT (IF < 1 PROJECT DOE	T RATIO S NOT QUALIFY)	(SIR) = (6 /	1G) =		8.98
8. ADJUSTED INTERNAL RA	TE OF RETURN (AIRR):		1	.5.06 %

LIFE CYCLE COST ANALYSIS SUMMARY STUDY: ECO067
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP)

LCCID 1.080 INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3. PROJECT NO. & TITLE: 3 HTW NORTH FISCAL YEAR 1994 DISCRETE PORTION NAME: REPLACE BOILERS ANALYSIS DATE: 09-21-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 1344905.
B. SIOH \$ 73970.
C. DESIGN COST \$ 80695.
D. TOTAL COST (1A+1B+1C) \$ 1499570. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$
F. PUBLIC UTILITY COMPANY REBATE \$ 0. 0. 1499570. G. TOTAL INVESTMENT (1D - 1E - 1F) 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) 0. 0. 0 \$ 1484222. 0. 0. 0 \$ 1484222 3. NON ENERGY SAVINGS (+) / COST (-) 15000 (1) DISCOUNT FACTOR (TABLE A) A. ANNUAL RECURRING (+/-) 14.74 221100 (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS(+) / COSTS(-)

SAVINGS(+) YR DISCNT

ITEM COST(-) OC FACTR

(1) (2) (3) COST(-) (4)

1. 5 BOILERS 10 YRS \$ 550000. 10 .74 407000.

2. 3 HW GEN 20 YRS \$-750000. 20 .54 -405000.

3. EXST ECON 2 YRS \$ 250000. 2 .94 235000.

4. PLT PIPG 15 YRS \$ 50000. 15 .63 31500.

5. PLT PIPG 20 YRS \$ -50000. 20 .54 -27000. B. NON RECURRING SAVINGS(+) / COSTS(-) 241500. \$ 50000. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 46260 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd4/(YRS ECONOMIC LIFE))\$ 97887 15.32 Y 5. SIMPLE PAYBACK PERIOD (1G/4) \$ 194682 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 1.30 (IF < 1 PROJECT DOES NOT QUALIFY) 4.45 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

3 - 62

LIFE CYCLE COST ANALYSIS SUMMARY

ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP)

INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3

PROJECT NO 6 TITLE: 3 HIGH NORTH

PROJECT NO. & TITLE: 3 HTW NORTH

FISCAL YEAR 1994 DISCRETE PORTION NAME: SUMMER SHUTDOWN-HEAT PUMPS ANALYSIS DATE: 09-21-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB

1. INVESTMENT A. CONSTRUCTION COST B. SIOH C. DESIGN COST D. TOTAL COST (1A+1B+1C) E. SALVAGE VALUE OF EXIST F. PUBLIC UTILITY COMPAN G. TOTAL INVESTMENT (1D	Y REBATE	\$ 0. \$ 0.	\$ 54749	9.		
2. ENERGY SAVINGS (+) / DATE OF NISTIR 85-3273-X UNIT COST FUEL \$/MBTU(1)	USED FOR DISC	ANNUAL S	DISCOONI	DIS SAV	COUNTED INGS (5)	
A. ELECT \$ 15.24 B. DIST \$ 8.82 C. RESID \$ 2.73 D. NAT G \$ 4.50 E. COAL \$ 1.61 F. LPG \$ 6.34 M. DEMAND SAVINGS N. TOTAL 3. NON ENERGY SAVINGS(+) A. ANNUAL RECURRING (1) DISCOUNT FACT (2) DISCOUNTED SA	1990. 0. 0. 17162. 0. 0. 13158. / COST(-) (+/-) TOR (TABLE A) AVING/COST (3A	\$ 30326. \$ 0. \$ 77228. \$ 0. \$ 0. \$ 0. \$ 107555.	15.61 17.56 19.97 20.96 17.58 16.12 14.74	\$ \$ \$	473395. 0. 0. 1618707. 0. 0. 2092102. 79975.	
B. NON RECURRING SAV	SAVINGS (+ COST (-)	S(-)) YR DISC OC FACT (2) (3)	TR SAV	COUN' INGS I(-)	(+)/	
d. TOTAL	\$ 0.				0.	
C. TOTAL NON ENERGY	DISCOUNTED SAV	INGS(+)/COST	(-) (3A2+3Bd	4)\$	1178832.	
4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$						
5. SIMPLE PAYBACK PERIOD (1G/4)						
6. TOTAL NET DISCOUNTED		-3C)		\$	3270933.	
7. SAVINGS TO INVESTMEN (IF < 1 PROJECT DOE	T RATIO	(SIR) = (6 /	1G) =		5.97	

8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

12.74 %

LIFE CYCLE COST ANALYSIS SUMMARY STUDY: EC0069B ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080 INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 3 HTW NORTH FISCAL YEAR 1994 DISCRETE PORTION NAME: SUMMER SHUTDOWN-GAS ANALYSIS DATE: 09-21-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 290266.

B. SIOH \$ 15965.

C. DESIGN COST \$ 17416.

D. TOTAL COST (1A+1B+1C) \$ 323647. 0. 0. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$
F. PUBLIC UTILITY COMPANY REBATE \$ \$ 323647. G. TOTAL INVESTMENT (1D - 1E - 1F) 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED FUEL \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) 3. NON ENERGY SAVINGS(+) / COST(-) \$ 79975. A. ANNUAL RECURRING (+/-) 14.74 (1) DISCOUNT FACTOR (TABLE A) (2) DISCOUNTED SAVING/COST (3A X 3A1) \$ 1178832. B. NON RECURRING SAVINGS (+) / COSTS (-) SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4) ITEM 0. \$ 0. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 1178832. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 157203. 2.06 YEAF 5. SIMPLE PAYBACK PERIOD (1G/4) \$ 2797538. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 8.64 (IF < 1 PROJECT DOES NOT QUALIFY) 14.84 % 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

LIFE CYCLE COST ANALYSIS SUMMARY
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP)

STUDY: ECO069C
LCCID 1.080 INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 3 HTW NORTH FISCAL YEAR 1994 DISCRETE PORTION NAME: SUMMER SHUTDOWN-1/2 GAS, 1/2 HP ANALYSIS DATE: 09-21-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 402418.

B. SIOH \$ 22133.

C. DESIGN COST \$ 24145.

D. TOTAL COST (1A+1B+1C) \$ 448696. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0.

F. PUBLIC UTILITY COMPANY REBATE \$ 0.

G. TOTAL INVESTMENT (1D - 1E - 1F) \$ 448696. 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNTED FUEL \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) A. ELECT \$ 15.24 995. \$ 15163. 15.61 \$ 236697.

B. DIST \$ 8.82 0. \$ 0. 17.56 \$ 0.

C. RESID \$ 2.73 0. \$ 0. 19.97 \$ 0.

D. NAT G \$ 4.50 17162. \$ 77228. 20.96 \$ 1618707.

E. COAL \$ 1.61 0. \$ 0. 17.58 \$ 0.

F. LPG \$ 6.34 0. \$ 0. 16.12 \$ 0.

M. DEMAND SAVINGS \$ 0. 14.74 \$ 0.

N. TOTAL 12163. \$ 92392. \$ 1855404. 3. NON ENERGY SAVINGS(+) / COST(-) ANNUAL RECURRING (+/-) \$ 79975.

(1) DISCOUNT FACTOR (TABLE A) 14.74

(2) DISCOUNTED SAVING/COST (3A X 3A1) \$ 1178832. \$ 79975. A. ANNUAL RECURRING (+/-) B. NON RECURRING SAVINGS(+) / COSTS(-) (+) / COSTS(-)
SAVINGS(+) YR DISCNT DISCOUNTED
COST(-) OC FACTR SAVINGS(+)/
(1) (2) (3) COST(-)(4) ITEM \$ 0. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 1178832. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 172367. 2.60 YEAR 5. SIMPLE PAYBACK PERIOD (1G/4) \$ 3034235. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 6.76 (IF < 1 PROJECT DOES NOT QUALIFY) 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR): 13.44 %

LIFE CYCLE COST ANALYSIS SUMMARY STUDY: ECENTRIC CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 3 HTW NORTH FISCAL YEAR 1994 DISCRETE PORTION NAME: STEAM LEAKS ANALYSIS DATE: 01-13-95 ECONOMIC LIFE 20 YEARS PREPARED BY: HA	1.080
1. INVESTMENT A. CONSTRUCTION COST \$ 1843. B. SIOH \$ 102. C. DESIGN COST \$ 111. D. TOTAL COST (1A+1B+1C) \$ 2056. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0. F. PUBLIC UTILITY COMPANY REBATE \$ 0. G. TOTAL INVESTMENT (1D - 1E - 1F) \$ 2056.	
2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT	AVINGS (5)
C. RESID \$ 2.73	0. 0. 0. 37594. 0. 0. 0. 37594.
3. NON ENERGY SAVINGS(+) / COST(-)	
A. ANNUAL RECURRING (+/-) \$ (1) DISCOUNT FACTOR (TABLE A) 14.74 (2) DISCOUNTED SAVING/COST (3A X 3A1) \$	
B. NON RECURRING SAVINGS(+) / COSTS(-) SAVINGS(+) YR DISCNT DISCOUNT COST(-) OC FACTR SAVINGS (1) (2) (3) COST(-)	SS(+)/
d. TOTAL \$ 0.	0.
C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$	0.
4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$	1794.
5. SIMPLE PAYBACK PERIOD (1G/4)	1.15 YEARS
6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) \$	37594.
7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = (IF < 1 PROJECT DOES NOT QUALIFY)	18.29
8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):	19.22 %

LIFE CYCLE COST ANALYSIS SUMMARY ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 3 HTW NORTH FISCAL YEAR 1994 DISCRETE PORTION NAME: EMCS CONTROLS/INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: INTRUMANALYSIS DATE: 09-27-94 ECONOMIC LIFE 20 YEARS PREPARED BY: 09-27-94 ECONOMIC LIFE 20 YEARS PR	3 MENTATION
1. INVESTMENT A. CONSTRUCTION COST \$ 66513. B. SIOH \$ 3659. C. DESIGN COST \$ 3991. D. TOTAL COST (1A+1B+1C) \$ 74163. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0. F. PUBLIC UTILITY COMPANY REBATE \$ 0. G. TOTAL INVESTMENT (1D - 1E - 1F) \$ 74163	•
UNIT COST DAVITOS INTEREST	DISCOUNTED SAVINGS(5)
A. ELECT \$ 15.24	\$ 0. \$ 0. \$ 0. \$ 445267. \$ 0. \$ 0. \$ 445267.
3. NON ENERGY SAVINGS(+) / COST(-) A. ANNUAL RECURRING (+/-)	\$ 0.
A. ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) (2) DISCOUNTED SAVING/COST (3A X 3A1)	\$ 0.
ITEM COST(-) OC FACTR SAVIN	DUNTED NGS (+) / (-) (4)
d. TOTAL \$ 0.	0.
C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)	0.
4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))	\$ 21244.
5. SIMPLE PAYBACK PERIOD (1G/4)	3.49 YEARS
6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)	\$ 445267.
7. SAVINGS TO INVESTMENT RATIO (SIR)=(6 / 1G)= (IF < 1 PROJECT DOES NOT QUALIFY)	6.00
8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):	12.77 %

PROJECT NO. 4

HIGH TEMPERATURE WATER SOUTH

BUILDING 25330

Harrison and Spencer, Inc.

GENERAL PROJECT NO. 4

GENERAL DESCRIPTION:

This project is intended to improve high temperature water (HTW) operating efficiency at the south distribution and its supply in Building 25330. Existing Plant Building 25330 supplies HTW year round to the south distribution system as opposed to chilled water from Building 25330 which is only supplied in the summer time. The HTW system serves barracks, offices, and recreational facilities. The existing boilers in the Plant are higher efficiency than those in Building 25910. As a means of comparison, the load is a lot less, although the two boilers in Building 25330 are equal in capacity to each of the five boilers in Building 25910. The difference is that the boilers in Building 25330 are made for gas-firing and are therefore more efficient than the converted Building 25910 boilers. However, in the interest of saving energy, we will replace those with a high temperature water system using hot water generators. When loads are calculated, the maximum load on the building is in the neighborhood of 7,000 lbs/hr. Factoring in the line loss and other things makes us want to select the 15,000,000 Btu per hour output for each generator. One generator will be used for the maximum load and the other will be used as a back-up. The hot water generator shall be on a loop which is taken out of the high temperature water fed from the bottom of the expansion/storage tanks going to the pumps and the loop returns to the top of the expansion/storage tank. The expansion tanks will be the existing cascade heaters converted for the new use. There will be nitrogen tanks supplying nitrogen that will keep a varying pressure on the tanks dependent on the water level within them. When make-up water is required because of a low level in the storage tank, the existing deaerator will process the water using high temperature water expanded to 5 psi which will then flash to steam. In this deaerator we will add sulphite to absorb any remaining oxygen, as well as chemicals to control the ph. That make-up water will then be fed either into the high temperature return line or to the water entering the hot water generators to make up the existing deficit in the storage tanks.

SUMMARY:

There are seven ECO's that comprise Project 4. As you can see from the data compilation on the next page, the payback is less than 5 years, and the SIR is a very good 3.71. All of the ECO's identified have an SIR greater than 1 except for ECO 68 which is the new hot water generators. It is necessary to keep ECO 68 in the project because the savings obtained by simplifying and improving temperature control in the system are all conditional upon having the hot water system rather than a steam system. Also, the life of the Plant in general will be much longer with hot water generators where steam treatment is not required and corrosion will be reduced even if the equipment is not treated properly, as is the present case with the equipment at Fort Gordon.

COMPILATION OF DATA:

The following two (2) pages show the ECO's that make up Project No. 4 and the life cycle cost analysis considering all ECO's as components of one (1) project.

CONCLUSION:

The summer shutdown is handled very much as it was handled in Project 3. There are many buildings that need to be modified to generate their own domestic water in the summer time so that the Plant can be shutdown thereby saving the line loss in the underground piping. To do this, we are not identifying which buildings need to be converted, but we have allowed for half of them to have gas domestic water heating and half to have heat pumps. Although heat pumps cost more, it is still a better choice where we can use the chilled air to offset some of the energy being used by the chilled water system now. We have put calculations in the report with all gas heating, and with all heat pumps, but we have selected the values for the ECO with half heat pumps and half gas for the summer domestic water heating.

```
LIFE CYCLE COST ANALYSIS SUMMARY STUDY: PROJ004
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080
INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3
PROJECT NO. & TITLE: 4 HTW SOUTH
FISCAL YEAR 1994 DISCRETE PORTION NAME: COMPOSITE
ANALYSIS DATE: 02-21-95 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB
1. INVESTMENT
A. CONSTRUCTION COST $ 1105659.

B. SIOH $ 60812.

C. DESIGN COST $ 66340.

D. TOTAL COST (1A+1B+1C) $ 1232811.
                                                        0.
0.
E. SALVAGE VALUE OF EXISTING EQUIPMENT $
F. PUBLIC UTILITY COMPANY REBATE $
G. TOTAL INVESTMENT (1D - 1E - 1F)
                                                                   $ 1232811.
2. ENERGY SAVINGS (+) / COST (-)
DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993
     UNIT COST SAVINGS ANNUAL $ DISCOUNT DISCOUNTED

FUEL $/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5)
     A. ELECT $ 15.24 908. $ 13831. 15.61 $ 215899.
B. DIST $ 8.82 0. $ 0. 17.56 $ 0.
C. RESID $ 2.73 0. $ 0. 19.97 $ 0.
D. NAT G $ 4.50 29156. $ 131202. 20.96 $ 2749992.
E. COAL $ 1.61 0. $ 0. 17.58 $ 0.
F. LPG $ 6.34 0. $ 0. 16.12 $ 0.
M. DEMAND SAVINGS $ 0. 14.74 $ 0.
N. TOTAL 24070. $ 145033. $ 2965891.
3. NON ENERGY SAVINGS (+) / COST(-)
                                                                               $ 91286.
         (1) DISCOUNT FACTOR (TABLE A) 14.74
(2) DISCOUNTED SAVING/COST (3A X 3A1) $ 1345556.
        ANNUAL KECUKKING (+/-)
(1) DISCOUNT FACTOR (TABLE A)
    A. ANNUAL RECURRING (+/-)
    B. NON RECURRING SAVINGS (+) / COSTS (-)
                          SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4)
                    ITEM
                                                                               0.
     d. TOTAL
                                     $ 0.
    C. TOTAL NON ENERGY DISCOUNTED SAVINGS (+) / COST (-) (3A2+3Bd4) $ 1345556.
4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))$ 236319.
                                                                                   5.22 YEARS
5. SIMPLE PAYBACK PERIOD (1G/4)
                                                                               $ 4311447.
6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)
7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) =
     (IF < 1 PROJECT DOES NOT QUALIFY)
8. ADJUSTED INTERNAL RATE OF RETURN (AIRR): 9.76 %
```

PROJECT NO. 4 - HOT WATER SOUTH

ECO DATA COMPILATION

TOTAL DISCOUNT SAVINGS	980,06	296,079	294,814	587,085	2,760,665	18,797	263,811	4,311,334
SAVINGS 1st YEAR	5,771	14,304	14,351	30,977	157,426	897	12,586	236,312
NAT GAS SAVINGS MMBTU/YR	0	3,045.32	2,975.50	4,662.00	15,477.00	199.00	2,796.98	29,155.80
ELECTRICAL SAVINGS MMBTU/YR	379	0	0	0	529	0	0	806
TOTAL COST (From LCC)	26.738	54,160	51,209	774,748	272,389	1.439	52,133	1,232,816
NON-RECURRING COST (-) SAVINGS (+)	0	0	C	0) C	0	0	0
ANNUAL RECURRING COST	C	909	961	10 000	79.725		0	91,286
CONSTRUCTION COST	23 980 00			607.870.00	247,640.00	1 290 00	754.82	1,105,659.00
DESCRIPTION		Variable Speed Fumping	Keturn Hot water Terriperature Control	Keduce Make-up water	Hot water Generators	Summer Shurdown (1/2 gas, 1/2 hp)	Keduce Steam Leaks	EMCS Controls/instrumentation Totals
ECO NO.	ì	26	28	32	89	70c	7.5	68

Simple Payback: 1,232,816 = 5.22 yrs. 236,312

 $\frac{4,311,334}{1,163,554} = 3.50$

SIR:

4 - 3

ECO METHODOLOGY FORM

ECO NAME:

Variable Speed HTW Pumping

ECO NUMBER:

26

TYPE: BLDG SYSTEM: Bldg. 25330 Heating

EXISTING CONDITIONS:

HTW water leaving Building 25330 is pumped with only one set of two identical pumps. The pumps are Ingersol-Rand 4 x 9A with a Louis Allis motor with a serial number of 5111871001 on one motor, and 5111871002 on the other. Type C004NB, 460 volts, 1.15 service factor, 4040 TS frame and the rating is 100 hp at 3550 rpm or 25 hp at 1776 rpm. One or the other of these pumps always operate at low speed. All buildings in the distribution system are equipped with 2-way valves so that when HTW is not required, the flow ceases to that building. Just upstream of the pump there is a blending station that mixes hot water return water before it gets heated with the heated HTW to control the temperature of the HTW leaving the Plant.

PROPOSED CHANGE:

Install one variable speed drive with switching so that either pump can be operated to supply the HTW needs of the distribution system. Using the existing pumps will require only one variable speed drive to be connected with switching to either one of the existing pumps with its existing motors. The Blending Station will be eliminated. Pumping speed will be varied to maintain a constant supply pressure, but as the total flow decreases with block valves closing the pump speed, the total developed head will decrease.

CALCULATION & COST METHODOLOGY

Because the pump always operates at low speed in the actual conditions, we will select the low speed information from the pump curve, which is 450 gpm at 70 ft. of head when using the existing motor which is 25 horsepower rated at 1750 rpm. Running the Bell & Gossett program using a heating profile, we can determine how often the pump will run at the various 10% increments of speed required to satisfy the south distribution HTW system. From the program run on the following pages we note that the pump on constant speed uses the same hp at all flows. But that hp is only .61 times the motor size. Since the motors were originally sized for 100 hp at high speed, it is NOT reasonable to assume at low speed, where only 25 hp is available, that 13.82 hp is actually consumed. Therefore, the full hp at low speed is assumed for constant speed operation. The power consumed is:

 $1 \text{ KW} \times 800 \text{ KW/hp} \times 25 \text{ hp} \times 24 \text{ hrs/day} \times 365 \text{ days/yr} = 175,200 \text{ KWH/yr} \times 1000 \text{ watts}$

From the program printout the variable speed pump consumes only 64,218.95 KWH/yr.

The savings is the difference: 64.218.98 = 11

175,200 - 64,218.98 = 110,981.02 KWH or $\frac{110,981.02}{10^6}$ x 3413 = 378.78 Million Btu/hr

Cost:

Variable speed drive

Materials \$11,000

Labor

Necessary switches at the motor (2)

Materials

\$ 4,340

Labor

\$1,000

\$1,500

CONSTRU	CTION COST ESTIMATE				DATE:	23 SEPT 94	SHEET 1	OF 1	
Project:	FORT GORDON ENERGY STUD	Y				-			
Location:	AUGUSTA, GEORGIA						4		
	HARRISON AND SPENCER, INC				CODE:				
nmary:	ECO #26 - VARIABLE HTW PUMPING		Est	imator:	H. TOUB	Checked:			
	ITEM RIPTION	QUANTI QUAN	ΓΥ	MATERIAL	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL	
VARIABLE SF	PEED DRIVE	1	LS	11,000	11,000	1,500	1,500	\$12,500.00	
SWITCHES		1	LS	4,340	4,340	1,000	1,000	\$5,340.00	
		SUBTOT	AL		15,340		2,500		
		5% SALES TAX 17% LABOR TAX		\$767.00					
						\$425.00			
		SUBTO			\$16,107.00		\$2,925.00	\$19,032.00	
		20% OH (GC ONLY)						\$3,806.40	
		SUBTOT	AL GO	C'S WORK				\$22,838.40	
		SUBTOTAL(GC & SUBS)						\$22,838.40	
		10% GC'S PROFIT						04 444 00	
	5% CONTINGENCY						\$1,141.92		
		TOTAL						\$23,980.32	

B&G Pumping System Analysis: BLDG 25330 HEATING

SUMMARY OF INPUT DATA: Office, heating

System peak demand: 450.00 gpm

System discharge pressure: 70.00 ft. (30.32 psig)
Minimum control/Static pressure: 20.00 ft. (8.66 psig)

Standard Efficiency (SE) 60-cycle motor.

1 Pump System:

Pump 1: Series 1510 5BC, Impeller diameter 8.875" Design RPM = 1750.0, Motor HP = 20.00

CONSTANT SPEED OPERATION:

Q/Qd,% TGPM TDH,ft BHP Ep,% BHP/HP,m HP,in E,mtr,% kWHR \$/day E, w/w, % Hrs 0.99 11.8 24.7 13.82 88.3 72.0 12.20 13.4 0.610 90.0 2.40 20.0 24.7 0.99 23.7 88.3 12.20 26.8 0.610 13.82 72.0 2.40 180.0 40.0 37.1 1.48 29.6 13.82 88.3 0.610. 225.0 72.0 12.20 33.5 3.60 50.0 1.98 35.5 88.3 49.5 13.82 0.610 12.20 40.3 4.80 60.0 270.0 72.0 49.5 1.98 41.5 88.3 13.82 70.0 315.0 72.0 12.20 47.0 0.610 4.80 24.7 0.99 47.3 12.20 53.6 0.610 13.82 88.3 360.0 71.9 80.0 2.40 0.99 53.1 88.3 24.7 12.20 60.2 0.610 13.82 71.8 90.0 405.0 2.40 13.5 0.54 53.8 0.665 15.08 88.2 1.20 100.0 450.0 71.5 13.30 61.0

COST SUMMARY:

Annual Operating Cost @ \$0.04 / kwhr = \$ 3626.57 8760 hours/year or 100.00% Total annual operating cost = \$ 3626.57 Total kW hours = 90664.32

VARIABLE SPEED OPERATION: (Table 1 of 1)

System suction pressure: 0.00 ft. (0.00 psig)
Best Efficiency Staging is ON

HP, in E, d/m, % kWHR \$/day E, w/w, % Hrs Q/Qd, % TGPM TDH, ft BHP Ep, % RPM 90.0 22.0 2.11 23.7 965.9 2.84 74.3 5.1 0.20 17.6 2.40 20.0 12.2 0.49 18.6 6.83 78.7 40.0 180.0 28.0 5.38 23.7 1087.0 2.40 80.5 26.0 1.04 19.1 9.68 3.60 50.0 225.0 32.5 7.80 23.7 1176.3 1.90 19.6 60.0 270.0 38.0 10.94 23.7 1278.3 82.6 47.4 13.25 4.80 1.23 41.3 30.7 8.58 84.6 7.26 48.8 1380.3 70.0 315.0 44.5 4.80 0.75 45.3 10.43 85.6 18.7 8.93 52.9 1495.0 2.40 52.0 80.0 360.0 22.4 0.90 49.3 86.4 12.54 10.83 57.1 1609.8 90.0 405.0 60.5 2.40 0.54 53.1 13.4 14.97 87.1 13.04 61.0 1724.5 1.20 100.0 450.0 70.0 Annual Operating Cost @ \$0.04 / kwhr = \$ 2568.76

8760 hours/year or 100.00% Total kW hours = 64218.98

COST SUMMARY:

: 0.0 psig Suction Pressure

Percent of Year : 100% : 8760 Hours/Year

Annual Operating Cost: \$2568.76

al hours/year = 8760 Total annual operating cost = \$2568.76

ECO NAME:

Controls For Return HTW Temperature Regulation

O NUMBER:

28

TYPE: BLDG SYSTEM: Bldg. 25330 Heating

EXISTING CONDITIONS:

HTW is heated in cascade heaters, which is usually maintained at the temperature of the saturation pressure of the boiler, and this boiler pressure is usually maintained except for several times a year when it is changed. At 150 psi, the saturation temperature is 347°F. When the HTW water leaves the cascade heaters, it passes through a blender that adds unheated HTW return to controls with setpoint that maintains the constant HTW supply temperature. Note that as distribution loads vary; less or more HTW water is required, and the HTW return temperature rises and falls depending upon the load. The existing system operates to control the HTW supply water, and does not take into account changes to load that would effect the overall heating requirements.

PROPOSED CHANGE:

Because the existing boilers are now going to be replaced with hot water generators, the controls in the Control Room will basically have to be changed. The controls will now regulate the high temperature water supply temperature, which will be based on firing the hot water generators to maintain the temperature in the storage tanks. This water will be circulated through the distribution system, and the firing rate of the hot water generators will be maintained based on a setpoint for the high temperature water supply. The HTW supply temperature set point will be varied by the EMCS to maintain the lowest acceptable HTW return temperature to adequately serve all buildings on the distribution system. These controls will also be monitored and, in some cases, controlled by the EMCS system so that temperatures in various buildings will establish energy efficient setpoint temperatures for high temperature water supply in a very short time by this monitoring at the EMCS. Therefore, this ECO, including the cost of new Control Room controls and the tie-ins to the EMCS, will be in the Control Room only. ECO 89 that includes new EMCS controls will cover the cost of any wiring from the Control Room to the EMCS system. The HTW return water temperature will also be monitored at the EMCS. The EMCS personnel will provide an HTW supply setpoint temperature based on their experience and time of day usage of high temperature water throughout the distribution system.

CALCULATION & COST METHODOLOGY:

Using the calculation method shown for ECO 27 in Project No. 3 for the line loss and knowing that the summer time gas usage is almost equal in both distribution systems (North and South), the line loss is calculated using the same ratios used in Project No. 3.

Savings: Line loss is reduced from an average of 255°F to 230°F (.1087 reduction). Since the minimum summer HTW usage is 4968 MCF of gas per month which is actually higher than the longer north distribution system it is assumed that the line loss is 60% or this total instead of the 75% assured in Project No. 3. The boiler efficiencies are 78% so the savings are:

 $\frac{4968 \, \text{MCF} \times 1000 \, \text{CF/MCF} \times 1030 \, \text{Btu/CF} \times .75 \, \text{Boiler Eff}}{24 \, \text{hrs/day} \times 30 \, \text{days/month}} = 5,330,250 \, \text{Btu/Hr}$

At 60% line loss:

 $.6 \times 5{,}330{,}250 \text{ Btu/Hr} = 3{,}198{,}150 \text{ Btu/Hr} \text{ or } 3.198 \text{ Million Btu/Hr}$

The reduction in line loss is:

 1087×3.326 Million Btu/hr = .3476 Million Btu/hr

Line loss at 8760 Hrs/Year the Total Savings is 3045.32 Million Btu's/yr.

Cost:

Controls:

Materials

\$20,000

Labor

\$15,000

Since the plant has new controls with computerized readout, the boiler controls simplifications suggest by this ECO will reduce maintenance time by only \$600/yr.

CONSTRUCTIO	N COST ESTIMATE				DATE:	23 SEPT 94	OF 1		
	RT GORDON ENERGY STUD	Υ							
	GUSTA, GEORGIA					PROJ. NO.	4		
	RRISON AND SPENCER, INC	÷.				CODE:	BLDG 25330		
	#28 - TEMPERATURE CONTROL		Est	imator:	H. TOUB	Checked:	NO. 4 BLDG 25330 ed: FR		
ITEN	1	QUANTI	TY	MATERIAL		LABOR	EXTENSION	TOTAL	
DESCRIPTI	ON	QUAN	UNIT	UNIT COST	EXTENSION	UNIT COST	EXTENSION	IOIAL	
CONTROLS		1	LS	20,000	20,000	15,000	15,000	\$35,000.00	
	10.00								
		1							
					00.000		45,000		
		SUBTO			20,000		15,000		
				STAX	\$1,000.00		\$2,550,00		
1		SUBTO		OR TAX	\$21,000.00			\$38 550 00	
		-		GC ONLY)	\$21,000.00		417,000.00		
				S'S WORK					
		00510	712 00	- TOTAL					
		1					-		
		-							
		SUBTO	TAL(G	C & SUBS)				\$46,260.00	
				PROFIT					
			CON	TINGENCY				\$2,313.00	
		TOTAL						\$48,573.00	

ECO NAME:

Reduce Make-Up Water in HTW System

ECO NUMBER:

32

TYPE: BLDG SYSTEM:

Bldg. 25330 Heating

EXISTING CONDITIONS:

The total number of gallons lost in Building 25330 over the course of 1992 averages 43,663 gallons per month except for September where the very high recorded leakage is suspect. This leakage is caused by pipe failures and operating inefficiencies in the system. The quantity of lost water is based on reports of water meter readings made by the boiler operators.

PROPOSED CHANGE:

It is proposed that flow meters and temperature gauges be installed at various locations throughout the HTW distribution piping so that actual flows can be measured to determine where water is not being returned from where it is supplied. New flow meters and temperature gauges will be included in the cost of this ECO, and the wiring from them to the EMCS system will be included in ECO 89 in this Project No. 4.

CALCULATION & COST METHODOLOGY:

The cost is based on locating flow meter and temperature RTD's in various distribution locations throughout the HTW distribution piping. Once they are located in this ECO, ECO 89 for EMCS wiring will absorb the cost to wire them to the nearest building and then go back to the EMCS system. Savings is the heat loss of the water lost from the HTW system that can be determined and is based on the following:

Make-Up Water From Log Sheets

r	0	Gallons
January		56,451
February		19,400
March		57,910
April		30,430
May		23,900
June		16,640
July		20,110
August		45,420
September		683,080
October		80,310
November		67,630
December		62,100
	Total	1,163,381gal/yr
	Total Not Including Sept.	480,301gal/yr

1,163,381 gal. x 8.34 lb/gal x $(300^{\circ}-70^{\circ}\Delta t) = 2.2316 \times 10^{9}$ Btu/yr or 22316 therms/yr

Gas to make up loss of heat:

22316 Therms

.75 Boiler Eff. = 29,755 therms or 2,975.5 Million Btu/yr. @ \$.45/therm = \$13,389.60/yr

Also, 1,163,381 gal x \$.826/1000 gal = \$960.95 yr. is the annual recurring cost savings available for the water purchase cost to replace the leaked water.

CONSTRUCTION COST ESTIMATE	,			DATE:	23 SEPT 94	SHEET1	ET1 OF 1		
Project: FORT GORDON ENERGY STUI	ΣΥ								
Location: AUGUSTA, GEORGIA					PROJ. NO.	4	•		
Arch/Engr: HARRISON AND SPENCER, INC	C.				CODE:				
mmary: ECO #32 - REDUCE MAKE-UP WATE		Esti	imator:	H. TOUB	Checked:				
ITEM DESCRIPTION	QUANTIT QUAN	ſΥ	MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL		
FLOW METERS	10	FA	1,500	15,000	1,000	10,000	\$25,000.00		
TEMP RTD IN DISTRIBUTION PIPE	10		300	3,000	500	5,000	\$8,000.00		
			A :						
	SUBTOTA			18,000	!	15,000			
			S TAX R TAX	\$900.00		\$2,550.00			
	SUBTOT		K IAX	\$18,900.00		\$17,550.00	\$36,450.00		
			C ONLY)	\$10,000.00		V ,ess.es	\$7,290.00		
			'S WORK				\$43,740.00		
			& SUBS)			\$43,740.00			
			PROFIT						
		CON	TINGENCY	1.00000			\$2,187.00		
	TOTAL						\$45,927.0		

ECO NAME:

Replace Existing Boilers with Hot Water Generators

ECO NUMBER:

68

TYPE: BLDG SYSTEM: Bldg. 25330 Heating

EXISTING CONDITIONS:

Existing boilers are gas-fired with oil back-up. The steam generators are operating as intended. Efficiency testing that was reported by Gee Jenson shows the boilers in Building 25330 operate at approximately 75% efficiency at 100% - 25% capacity.

PROPOSED CHANGE:

The existing boilers will be removed and replaced with 15,000,000 Btu's/hr output hot water generators. The hot water generators shall be piped as shown on the drawing for Project No. 4 included in this project write-up. The project shall be such that the cascade heaters will be converted to expansion/storage tanks with the nitrogen pressure above. Water will flow down from the storage tanks into the existing pumps that will now be variable speed driven. Off of that line going down to the pumps will be a loop that goes through the hot water generators. The generators will have their own pumps to circulate HTW back into the expansion/storage tanks so that the hot water generators will come on only to heat the water in the storage tanks. The water will then leave the expansion tanks as required by either the hot water generators or the variable speed pumps. This means that the supply HTW temperature will be the controlling item for the variable speed pumping and the controls that are addressed in ECO 28 will assure that the return temperature is adequate to supply heat to all users. The existing deaerator can be reused. HTW water will have its pressure reduced to 5 psi which will allow it to flash to steam. That steam will be used to remove oxygen in the deaerator as the deaerator now operates. Additionally, there will be a sulphite chemical storage tank which will add sulphite to the deaerator process to remove any remaining oxygen at that point. An additional chemical storage pump and tank will be used to control the PH in the system at the deaerator tank and there will be a chemical feed tank that supplies a pipe preservative-type chemical for the distribution system, which will be pumped into the HTW return water.

The proposed system will have to be installed piece-meal so that the system operates as it currently does on steam. Converting one new hot water generator with one cascade heater at a time will allow the system to be converted over to hot water generation rather than steam generation with a relatively short shutdown period. Part of Project No. 4 allows for a summer shutdown of the Plant by installing hot water generating equipment at the various buildings. If this is done, there will be a longer shutdown to allow the Plant to be converted to hot water generation. The hot water generators selected for this project are those of the type produced by the International Boiler Company. These are truly hot water generators and not steam boilers that are converted for hot water generation use. Converted steam boilers will be less expensive, but they do not have the life nor are they specifically designed for the generation of the hot water. These new hot water generators are rated presently by International Boiler Company at 80% efficiency.

CALCULATION & COST METHODOLOGY:

The new high temperature hot water generator will produce hot water at 80% efficiency as rated by the company that supplies them. Calculations done by Gee Jensen indicate that the existing boilers are 75% efficiency at the expected capacities they are running now which is in the neighborhood of 20% to 25%. As unbelievable as these figures may be, we still use them to determine the savings. Because of these low savings, the payback on this particular ECO does not appear to be as good as the other ECO's, but it is important that this ECO be implemented because other savings will be generated with controls changes and with a system that allows us to reduce operating temperatures in the plant and the distribution piping. The use of direct circulating hot water generators in lieu of steam at higher than necessary temperatures allows total savings that justify the entire Project No. 4.

ECO NAME:

Replace Existing Boilers with Hot Water Generators

(Cont'd)

ECO NUMBER:

68

TYPE: BLDG SYSTEM:

Bldg. 25330 Heating

CALCULATION & COST METHODOLOGY:

Savings is shown as 80% - 75% = 5%

 $90,517 \text{ MCF} \times 1,030,000 \text{ Btu/MCF} \times .05 = 46,616.26 \text{ therms} = 4,661.63 \text{ Million Btu/yr}.$

100,000 Btu/therms

46,616.63 therms @ \$.45/therm = \$20,977.32/yr

Maintenance manhour savings are \$10,000/yr at 400 hrs x \$25/hr.

Cost:

Hot water generators (2) Materials	\$175,000 ea.	Labor	\$ 65,000
Repiping of Cascade Heat Materials	ters \$ 6,000	Labor	\$ 8,000
Controls for hot water ger Materials	erator \$ 25,000	Labor	\$ 20,000
Demolition		Labor	\$ 15,000
Chemical Feed Equipment Materials	st (3) \$ 7,500	Labor	\$ 1,500
Nitrogen Storage and Pip Materials	ing \$ 8,000	Labor	\$ 6,000

CONSTRUCTION COST ESTIMATE			DATE:	23 SEPT 94	SHEET	1 OF 1				
Project: FORT GORDON ENERGY STUD	Y									
Location: AUGUSTA, GEORGIA	•			PROJ. NO.	4					
Arch/Engr: HARRISON AND SPENCER, INC	1			CODE: BLDG 25330						
mmary: ECO #68 - H. W. GENERATORS	Est	imator:	H. TOUB	Checked:						
TTEM DESCRIPTION	QUANTITY QUAN UNIT	MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL				
HOT WATER COVERATOR	2 EA	175,000	350000	LUMP SUM	65,000	\$415,000.00				
HOT WATER GENERATOR REPIPING OF CASCADE HEATER	1 LS	6000	6000	8000	8000	\$14,000.00				
CONTROLS FOR HOT WATER GENERATOR	1 LS	25,000	25000	20,000	20000	\$45,000.00				
DEMOLITION	1 LS	25,000	23000	15000	15000	\$15,000.00				
CHEMICAL FEED EQUIPMENT	3 LS	2,500	7500	500	1500	\$9,000.00				
NITROGEN STORAGE & PIPING	1 LS	8,000	8000	6000	6000	\$14,000.00				
	SUBTOTAL 5% SALE	S TAX	396,500 \$19,825.00		115,500					
	17% LAB	OR TAX			\$19,635.00					
	SUBTOTALS		\$416,325.00		\$135,135.00	\$551,460.00				
	20% OH (GC ONLY)				\$110,292.00				
	SUBTOTAL GO					\$661,752.00				
						0.00				
	SUBTOTAL(GO					\$661,752.00				
	10% GC'S					4				
	-	TINGENCY				\$33,087.60				
	TOTAL					\$694,839.60				

ECO NAME:

Summer Shutdown of HTW System

ECO NUMBER:

70

TYPE: BLDG

South Distribution

SYSTEM:

Heating

EXISTING CONDITIONS:

Space heating is not required from mid-May through the end of September, but a boiler must be in operation to handle domestic water needs and cooking requirements in some cases with the HTW distribution system.

PROPOSED CHANGE:

Provide onsite water heaters at each building for domestic water usage. Water heaters should be about 10% more efficient than the boiler plant, i.e., 80%. Use of water heaters should also eliminate the heat loss in the distribution line during this 4-1/2 month period. It will also eliminate supervision of the boilers for 4-1/2 months. The HTW system should either be left full of water or pressurized with nitrogen to avoid corrosion during the period of non-use. The buildings will have hot water generating equipment, which will be heat pumps or gas-fired equipment. The heat pump operates at a COP of 3±. Cool air generated by the heat pump can be used in the buildings to cool air spaces that would not now be cooled or that can be cooled depending on domestic water demand rather than space conditions, i.e., Laundry Room, Hallways, or unused Classroom areas. In some buildings, the cool air generated by the heat pumps controlled to make domestic hot water can be used to supplement the large air handling units so that less chilled water from the CHW distribution system will be required. When this is done, warm air must always be available for domestic water heating regardless of the demand for space cooling in the building. Gas-fired equipment will be more expeditious where there is no use for the chilled air in the building being converted. Each building type should be evaluated with a life cycle cost analysis to see if the higher initial cost of the heat pump and associated equipment results in enough extra energy savings to warrant the extra cost.

CALCULATION & COST METHODOLOGY:

Methodology for computing the savings for the summer shutdown is based on taking the total amount of gas used during the summer months, May through September, and subtracting from that the estimated hot water consumption in all of the buildings on the distribution system, including heat loss in the hot water storage tanks in all of the buildings. Since there is no space heating during these months, the difference between the domestic water heat use and the total HTW heating will be the amount of line loss in the distribution system for HTW. In addition to the savings of line loss of the HTW distribution system, the individual equipment that will be put in the distribution system buildings will have an 80% efficiency whether it is gas-fired equipment or heat pumps that we calculate to have an equal operating cost to gas-fired equipment. Therefore, the calculations become the same. Taking an 80% efficiency for gas-fired equipment and a 2.7 COP for heat pump operation, and using the cost available we calculate below to see that the same cost is derived for both systems per Btu. Because the cost of a Btu is the same, we can therefore easily calculate the savings with gasfired equipment, and will assume the heating with a heat pump is going to cost the same. Therefore, it comes to the same value for the energy saved. The total savings of the higher efficiency equipment is then added to the line loss which will be saved by shutting down the Main Plant, which gives a total savings in gas over the 4-1/2 month period in which the Main Plaint will be shut down. In addition to the energy savings, the manpower at the Plant can be reduced by one man for 4-1/2 months at \$25/hour. We have added back in some money for shutting down the Plant and isolating the piping which will not be used during the HTW shut down. Separately, heat pumps are compared with natural gas-fired water heaters for the summer heating in each of the buildings. The heat pumps are creating hot water, as well as cold air, so the cold air is for free because the heating with the heat pumps is exactly equivalent to the heating with natural gas. Cost of gas heaters in each of the buildings is then worked up, and the cost of the heat pumps is worked up.

ECO NAME:

Summer Shutdown of HTW System

(Cont'd)

ECO NUMBER:

70

TYPE: BLDG SYSTEM:

South Distribution

Heating

CALCULATION & COST METHODOLOGY:

Three life cycle cost analyses are shown with this ECO. ECO 70A is worked up for using heat pumps only in all the 96 buildings that need to be modified for summer usage. ECO 70B is worked up for gas used to generate hot water in all of the 96 buildings. ECO 70C is taking the cost of both of the two options and dividing it by 2, assuming half the buildings will require heat pumps and half the buildings will require gas. The savings for ECO 70C will be full savings of natural gas which will be shutting down the Plant, and half of the savings allocated to the free cooling will be derived by using heat pumps. Heat pumps vs. gas-fired equipment will be determined by looking at each individual building and determining if there is the possibility of using heat pumps to generate cooling so that they can decrease the cooling load and also take advantage of the fact that we got this cooling as a byproduct by producing hot water in the summer time. The purpose of this calculation assumes that half of the buildings qualify for heat pumps and half of the buildings qualify for gas-fired equipment.

From weather data TM 5-785 it appears heat would not be needed for half of May and all of June, July, August, and September which is 4-1/2 months.

From 1992 Boiler Logs Heating Plant Gas Consumption for Months:

```
MCF
               4878 \text{ MCF } \times 0.5 = 2439
May
                                = 4877
                                          MCF
June
                                          MCF
                                = 4335
July
                                = 4261
                                           MCF
Aug
                                = 4137
                                          MCF
Sept
                                          MCF
                                  20,049
```

Estimated Hot Water Consumption = 40,708 GPD

```
Q = 1 BTU x 40,708 gal x 8.34 lb/gal x 60°F = 20,370 MBTU/day
```

Tank loss (from 25910 calculation) = 18,000 Btu/day x 51 Bldgs. = 918 MBtu/day Total net/day = 20,370 + 918 = 21,288 MBtu/day With $\eta = 0.75 = 28,384$ MBtu/day

```
CF Gas = 28,384 x 1.03 = 29,236 CF/day
30 day/mo = 877.1 MCF/mo
```

Lowest recorded gas consumption, SCFT = 4137 MCF

Line and system loss = lowest record - est. HW consumption =

4137 MCF - 877.1 MCF = 3260 MCF

Gas savings due to increased η

```
21288 MBtu/day = 36.610 MBtu/day
.80
x 30 days/mo = 798.3 MCF/mo
```

Savings due to increased η

877.1 - 798.3 = 78.8 MCF

Total savings for 4-1/2 month period
Line/system losses = 3260

Line/system losses = 3260 x 4.5 = 14,671 MCF Increased η = 78.8 x 4.5 = 355 MCF 15,026 MCF

ECO NAME:

Summer Shutdown of HTW System

(Cont'd)

ECO NUMBER:

70

TYPE: BLDG SYSTEM: South Distribution

Heating

CALCULATION & COST METHODOLOGY

Annual Savings:

- Fuel: 15026 MCF = 154,768 therms @ 1,030 Million Btu/CF (15,476.8 Million Btu/yr) @ \$0.45/therm = \$69,645

- Operator Hrs Saved: 3240 hrs @ \$25/hr = \$81,000 (1 man x 24 hrs/day x 30 day/mo x 4.5 hrs)

Additional Annual Cost:

- Labor to shut down, 1500 Ft and reactivate plant annually

@ 1.0 hrs per building

.51 hrs @ \$25/hr = \$ 1,275 Net annual labor savings = 81,000 - 1275 \$79,725

Domestic Water Calculations (Gas vs. Heat Pump)

Heat Pump at 2.7 COP (Min)

Electricity Cost is <u>\$.052/KW</u> = \$.0000056/Btu 3413 Btu/Hr x 2.7COP

80 Eff

Natural Gas Cost is <u>\$.45/100,000 Btu</u> = \$.0000056/Btu

Additional Savings for Heat Pump Cooling:

Therefore, cost of energy at Fort Gordon is the same for gas heating at 80% efficiency or with an electric heat pump at a 2.7 COP. But with heat pump we get free cooling of space at

30,000 Btuh = 2.5 ton x .75 KW/ton x \$.052/KWH = \$.0975/hr

12,000 Btu/ton 2.5 tons x .75 KW/ton x 51 bldgs x 24 hr/day x 30 days/mo x 4.5 mo/yr = 309,825.0 KWH/yr or 309,825 KW x 3413 Btu/KW = 1057.4327 Million Btu/yr.

 10^{6}

ECO 70A:

Consider heat pumps in all 51 buildings. The cost of the modifications is a percentage of the costs used for ECO 69A in Project No. 3 except that a higher cost for fan coil units is inserted because some modifications are already made to buildings in the North distribution system.

The savings are the line loss in the HTW distribution, plus the higher efficiency of the local equipment when compared to the HTW Plant equipment. This savings value is 15,476.8 million Btu/yr for gas. There is an electrical savings also for heat pumps because we get space cooling that will reduce the Btu's distributed from the Plant. This savings is 1057.43 million Btu/yr.

ECO 70B:

Consider gas-fired domestic water heating equipment in all 51 buildings. The gas savings will be the same as in ECO 70A, but there will not be the electric savings because we get no free cooling as we do with heat pumps. The cost of equipment is a pro rata cost difference from that figured for ECO 69B on the North HTW distribution loop in Project No. 3.

ECO NAME:

Summer Shutdown of HTW System

(Cont'd)

ECO NUMBER:

70

TYPE: BLDG SYSTEM: South Distribution

Heating

CALCULATION & COST

METHODOLOGY

Cost for Gas Heater:

Gas Piping x 51 Buildings

Materials \$16,000 Labor \$32,000

Combustion Air Ventilation 51 Buildings

Materials \$ 2,600 Labor \$ 5,000

Gas-Fired Water Heater (51) x

Materials \$11,000 Labor \$ 7,000

Piping To Existing Storage Tanks

Materials \$17,000 Labor \$14,000

Pumps 1 x 96

Materials \$ 5,000 Labor \$ 3,000

ECO 70C:

This ECO is a composite of ECO 70A and ECO 70B and it is the values that will be used for this Project No. 4. We will use an average cost of gas and heat pumps and we will use the same savings for line loss of the HTW, but will use only 1/2 of the free cooling savings for heat pumps because the basis of this ECO 70C is that 1/2 the buildings on the distribution system will use gas for domestic water heating and 1/2 will use heat pumps. The criteria for whether gas or heat pumps will be selected will depend on the existing equipment in each building on the HTW distribution system and whether there is a use for the free cooling that heat pumps can supply, but at a greater initial cost.

Cost:

Gas 158,193.00 Heat pumps 330,296.40

 $488.489.40 \div 2 = 244,294.20$

Savings:

Electric 1.057.43 = 528.72 Million Btu/yr

2

Gas 15,476.8 Million Btu/yr

CONSTRUC	CTION COST ESTIMATE	DATE:	DATE: 23 SEPT 94 SHEET									
Project:	FORT GORDON ENERGY STUD	Υ										
	AUGUSTA, GEORGIA					PROJ. NO.	4					
	HARRISON AND SPENCER, INC					CODE:	SOUTH DIST	RIBUTION				
	ECO #70a - SHUTDOWN W/HEAT PUN		Est	imator:	H. TOUB	Checked:						
	ITEM RIPTION	QUANTI		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL				
2 1/2 TON HE	AT DUMP (51 BUILDINGS)	1	LS	102,000	102,000	13,000	13,000	\$115,000.00				
PIPING & PUN	AT PUMP (51 BUILDINGS) MPS TO EXIST TANKS		LS	25500	25,500	21500	21,500	\$47,000.00				
FCU IN BUILD			LS	40,000	40,000	25,000	25,000	\$65,000.00				
ELECTRICAL \		1	LS	7500	7,500	7500	7,500	\$15,000.00				
		SUBTOT	ΔΙ		175,000		67,000					
				S TAX	\$8,750.00		0.,000					
				OR TAX	ψο,700.00		\$11,390.00					
		SUBTO		// ////	\$183,750.00		\$78,390.00	\$262,140.00				
				GC ONLY)	V 1001100100			\$52,428.00				
				C'S WORK				\$314,568.00				
		SUBTOT	AL(G	C & SUBS)				\$314,568.00				
		10% GC'S PROFIT										
		5%	CON	TINGENCY				\$15,728.40				
		TOTAL						\$330,296.40				

CONSTRUCTION COST ESTIMATE				DATE:	23 SEPT 94	SHEET	Γ1 OF 1		
Project: FORT GORDON ENERGY STU	DY								
ocation: AUGUSTA, GEORGIA					PROJ. NO.	4	•		
Arch/Engr: HARRISON AND SPENCER, IN	C.				CODE:	RIBUTION			
mmary: ECO #70b - SHUTDOWN W/ GAS		Est	imator:	H. TOUB	Checked:				
ITEM	QUANTI	ΓY	MATERIAL		LABOR				
DESCRIPTION	QUAN	UNIT	UNIT COST	EXTENSION	UNIT COST	EXTENSION	TOTAL		
GAS PIPING (51 BLDGS)	1	LS	16,000	16,000	32,000	32,000	\$48,000.00		
OMBUSTION AIR VENTILATION (51 BLDGS)		LS	2600	2,600	5000	5,000	\$7,600.00		
GAS FIRED WATER HEATER (51 BLDGS)	1	LS	11,000	11,000	7,000	7,000	\$18,000.00		
IPING TO EXISTING STORAGE TANK	1	LS	17000	17,000	14000	14,000	\$31,000.00		
PUMPS (51 BLDGS)	1	LS	5000	5,000	3000	3,000	\$8,000.00		
	SUBTOT		CTAV	51,600 \$2,580.00		61,000			
			STAX	\$2,560.00		640.270.00			
			OR TAX	\$54,180.00		\$10,370.00 \$71,370.00	\$125,550.0		
	SUBTO1		GC ONLY)	\$54,160.00		\$71,570.00	\$25,110.0		
			C'S WORK				\$150,660.0		
			C & SUBS)				\$150,660.0		
	10%								
		CON	TINGENCY		100000		\$7,533.0		
	TOTAL						\$158,193.0		

ECO NAME:

Reduce Steam Leaks

ECO NUMBER:

72

TYPE: BLDG SYSTEM:

Bldg. 25330 Heating

EXISTING CONDITIONS:

There are steam leaks at steam valves and one hole was found in the cascade heaters. There are less

leaks in this building than in Building 29510.

PROPOSED CHANGE:

Weld holes closed and replace packing in leaking valve stems. High pressure water will flash to

steam at leaks to atmospheric pressure.

CALCULATION & COST

Estimated steam loss is:

METHODOLOGY: 25 lbs/hr x 24 hr/day x 365 c

25 lbs/hr x 24 hr/day x 365 days/yr x 910 Btus/lb = 1,992.9 therms = 199.3 Million Btu/yr

100,000 Btus/therm

.45/therm x 1,992.9/therms = \$896.811/yr

Cost of Repairs:

35 hrs @ \$25 = \$875

CONSTRUC	TION COST ESTIMATE			DATE:	23 SEP 94	SHEET	SHEET1 OF 1		
Project:	FORT GORDON ENERGY STUD	Υ							
Location:	AUGUSTA, GEORGIA				PROJ. NO.	3			
	HARRISON AND SPENCER, INC	.			CODE:	BLDG 25330			
Summary:			stimator:	H. TOUB	Checked:				
	ITEM CRIPTION	QUANTITY QUAN UN	MATERIAL	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL		
REPAIR STEA	M LEAKS	35 HR	3		25	875	\$875.00		
		SUBTOTALS				\$875.00	\$875.00		
	,		LES TAX			24.075	04.40.75		
			BOR TAX			\$148.75	\$148.75		
		SUBTOTAL				\$1,023.75	\$1,023.75 \$204.75		
	SUB-CONTRACTORS	SUBTOTAL	OH & PROFIT GC WORK				\$1,228.50		
		TOTAL SUE	WORK						
			SUB PROFIT			4.0			
			NTINGENCY O	N JOB			\$61.43		
		TOTAL					\$1,289.93		

ECO NAME:

EMCS of Boiler and Chiller Controls vs. Manual Control

ECO NUMBER:

89

TYPE: BLDG

Bldg. 25330 Heating

EXISTING CONDITIONS:

SYSTEM:

Existing automatic or manual controls are within the plant only with no EMCS tie-in for control. The EMCS office which is manned 24 hours a day has very few, if any instrumentation readouts from the plant, and no control of the plant with the EMCS. Because EMCS personnel are aware of what is happening in many buildings, they are also aware of conditions and demands on the high temperature water system. Currently, the boiler operators are making boiler pressure changes, HTW changes, bringing on and off boilers, and many manual valving operations. However, they are not performing the functions that an EMCS office can to control the energy consumed and to improve the operating efficiency of the Plant. The controls in Building 25330 have recently been upgraded and additions for EMCS points and new points are more readily available than in other places. Therefore, the amount of points necessary to be added is minimal. There is a computer existing that can currently read out large quantities of information.

PROPOSED CHANGE:

Connect most instrumentation and automatic controls and setpoint adjustments to the computerized EMCS system that is existing. EMCS personnel can then adjust HTW temperatures and temperature setpoints, and all new controls that may be added under other ECOs. All temperature, pressure and flow readings of new and existing instrumentation should be readable at the EMCS terminals. The individual that attends the plant but is not an EMCS operator shall have access to the readouts, but shall basically do maintenance most of the time, and turn on and off the equipment as required by the EMCS people. In addition to EMCS controls, there are also temperature gauges and dials that will be added so that Plant personnel can read exactly what is happening at any given time. Prior to actual designing this system, a thorough investigation should be made of the new controls system that has been added to see how much of that information could be fed directly into the EMCS and how much needs to be modified with in-house software to be installed in the computer within Building 25330.

CALCULATION & COST METHODOLOGY:

Required EMCS controls and instrumentation for the high temperature water system at Building 25330 with new hot water generators.

DESCRIPTION	NO. POINTS	DOLLARS
Fuel flow	4	\$ 6,000
Expansion Tank (temperature and pressure)	4	2,000
HTW pump operation (temperature, pressure, flow)	10	5,000
Make-up water (temperature, pressure, flow)	3	3,500
Nitrogen (level, temperature, pressure)	. 3	2,500
Valve positions	7	2,000
Btu computation		2,500
Chemical feed	8	1,800
Hot water generator pump controls	6	3,000
Hot water generator combustion efficiency		1,200
Gauges and dials		4,000
Total		\$33,500

This assumes that no additional manpower will be required by EMCS personnel, nor will there be any reduction of personnel in the plant to operate the valves. However, the change that will take place will be the EMCS personnel will actually have either physical control or the ability to tell people in the Plant to change valve positions or start equipment.

ECO NAME:

EMCS Controls of Boiler and Chiller vs. Manual Control

(Cont'd)

ECO NUMBER:

89

TYPE: BLDG SYSTEM: Bldg. 25330 Heating

CALCULATION & COST METHODOLOGY:

Gas consumption used in Building 25330 is 90,517 mcf. A 3% overall efficiency improvement is based on the fact that there will be better regulation of HTW temperatures. The hot water generator firing rate can be adjusted for predicting of loads which the EMCS people will monitor and record, and also pumping speed regulation will be controlled by EMCS so that all buildings will be adequately served to get the required amount of HTW with a minimum amount of pumping energy used. Another savings would be the combustion controls regulations so that by monitoring the air flows and the oxygen in the flue gases some regulation of the combustion of the new hot water generators will be available to be made by EMCS people either directly or by calling in the operator that is available in the Plant.

Calculation is:

 $.03 \times 90,517 \text{ mcf} \times 1,030,000 \text{ Btu's/mcf} = 2,796.98 \text{ Million Btu's/yr.}$ $10^6 \text{ Btu's/Million Btu's}$

CONSTRU	CTION COST ESTIMATE	DATE:	23 SEPT 94	SHEET1 OF 1				
Project:	FORT GORDON ENERGY STUD	Υ						
Location:	AUGUSTA, GEORGIA					PROJ. NO.	4	•
Arch/Engr:	HARRISON AND SPENCER, INC).				CODE:	BLDG 25330	
nmary:	ECO #89 - EMCS - HTW SOUTH		Est	imator:	H. TOUB	Checked:		
	ITEM	QUANTI		MATERIAL		LABOR		
DESC	RIPTION	QUAN	UNIT	UNIT COST	EXTENSION	UNIT COST	EXTENSION	TOTAL
EUEL ELOVA		1	LS	4000	4000	2000	2000	\$6,000.00
FUEL FLOW EXPANSION	TANK		LS	1400		600	600	\$2,000.00
HTW PIPING			LS	2300	2300	2700	2700	\$5,000.00
MAKE-UP WA			LS	2000		1500	1500	\$3,500.00
NITROGEN	TIEN	1	LS	1000		1500	1500	\$2,500.00
VALVE POST	TONS		LS	700	700	1300	1300	\$2,000.00
BTU COMPU			LS	500	500	2000	2000	\$2,500.00
CHEMICAL F			LS	900	900	900	900	\$1,800.00
	ATOR PUMPS CONTOLS		LS	2000	2000	1000	1000	\$3,000.00
	ATOR COMBUSTION EFFICIENCY		LS	600		600	600	\$1,200.00
GAUGES & D			LS	2000	2000	2000	2000	\$4,000.00
		+	SALE	ES TAX DR TAX	17400 \$870.00 \$18,270.00		16100 \$2,737.00 \$18,837.00	\$37,107.00
		20%	OH (GC ONLY)				\$7,421.40
		SUBTOT	AL GO	C'S WORK				\$44,528.40
		SUBTOT	AL(G	C & SUBS)				\$44,528.40
				PROFIT				, , , , , , , , , , , , , , , , , , , ,
		-		ITINGENCY				\$2,226.42
			CON	TINGENCY				\$46,754.82
		TOTAL						\$40,734.82

HEATING REQUIREMENTS DATA SUMMARY - BUILDING 25330

INTRODUCTION:

Heat load requirements for the South Central Utility Plant were determined from field survey data. The data analyzed using the Trane Trace 600 Load calculation program. The data reported in Tables 4A, 4B, and 3C are the results of the analysis. The data files produced from the Trace 600 program are contained in Appendix I Load calculations were run for the 36 building types that represent all the building types serviced by the South Central Plant. These building types represent 86 total buildings serviced on the south side of the base from Building 25330. The following commentary explains the data contained in each of the tables.

Table 4A - Heating Profile - Building Types Serviced By South Central Utility Plant - Building 25330

Each building type (36 total), as defined in the field survey, is listed across the top of the table. Values are recorded for every hour for twenty four hours. There are twelve sections to the table, one for each month of the year. Each entry is in thousands of BTU/hr. Table 4A therefore contains heating requirements for each building type for every hour of the day for all twelve months of the year in thousands of BTU's per Hour (MBTUH). The last column on the right contains the total MBTUH values for each building type for a particular hour. The data shows that the loads are highest during the winter months of December, January, and February. As you proceed into spring, loads diminish and the hours requiring heat become less. As you proceed into the summer months you may see some small loads reported. Keeping in mind that we are reporting loads in thousands of BTU's, the values are very small and are dropped in later calculations.

Table 4B - Heating Profile - Total of All Buildings Serviced By South Central Utility Plant - Building 25330

Some of the building types surveyed are representative of multiple buildings of the same type. Table 4B accounts for multiple buildings by building type. The totals column therefore is representative of the true hourly loads for each month. Building types representing more than one building are: Type 31-5 buildings, Type 31A-2 buildings, Type 33-5 buildings, Type 35-6 buildings, Type 36-15 buildings, Type 37-2 buildings, Type 38-2 buildings, Type 41-2 buildings, and Type 44-8 buildings. All the rest of the building types represent a single building each. There are a total of 53 buildings serviced by the Central utility Plant Building 25330.

Table 4C - Heat Load Requirement Summary - South Utility Plant Building 25330

This table is a compilation of the totals column taken from Table 4B for each month. This Table provides a means to estimate plant heating load requirements on the hot water generating equipment at the South Plant.

SUMMARY:

All the data recorded in Table 4 (A, B & C) was derived from field survey information and the Trace 600 load calculations. See Appendix II for a complete printout of all generated data for buildings serviced by the South Utility Plant. The values appearing in Table 4A were taken directly from the Trace output data in Appendix II.

JANUARY

TOTAL	1799	1832	1858	1837	1828	1787	1722	1643	1459	1279	1107	666	890	794	706	646	654	745	856	1011	1149	1311	1474	1607
44	41	45	45	41	41	40	38	36	32	9	26	24	21	19	18	18	19	21	24	27	99	34	37	39
43	64	65	99	99	67	89	99	99	57	52	47	43	41	36	34	32	34	35	36	4	45	51	55	61
42	113	115	116	114	114	112	108	102	88	75	99	44	32	24	19	11	24	37	49	61	74	86	96	105
41	101	104	108	108	109	109	107	104	88	72	53	42	32	23	17	14	18	33	45	26	99	92	84	60
40	82	84	86	88	88	68	68	88	87	85	83	79	74	2	65	61	29	57	28	61	64	69	73	78
Ħ	77	78	77	75	72	89	63	28	53	84	42	37	32	28	25	24	25	29	36	44	25	109	68	7
38	92	8	82	8	8 6	06	88	87	78	69	5.2	35	19	00)				ıc	26	9 6	67	80	9
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HEATING PROFILE - BUILDING SERVICED BY SOUTH CENTRAL UTILITY PLANT - BUILDING 25330

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31		895	1015	1040	1050	1085	1065	915	805	685	290	520	465	385	355	375	455	525	290	640	720	780
DAY			¢σ	-	40	φι		, 4	. 0	•	Ç		**	*2	91					ı Ŧ		8

Table 4B - 6

TONNAGE PROFILE BY MONTH - BUILDINGS SERVICED BY SOUTH CENTRAL UTILITY PLANT - BUILDING 25330

DAY	JAN	FEB	MAR	APR	MAY	JUN	JUL	AUG	SEP	OCT	NOV	DEC
HOUR												
1	6851	5261	2716	5	2	0	0	0	0	1303	2648	4426
2	6899	5701	3236	40	81	0	0	0	51	2467	3120	4815
3	7035	6080	3709	104	374	0	0	0	274	3084	3555	5115
4	6932	6383	4129	167	334	0	0	0	226	3437	11669	5324
5	6985	6828	4378	345	42	0	0	0	21	3794	4296	5498
- 6	6881	6957	4585	461	124	0	0	0	32	4080	4548	5720
7	6695	7138	4608	508	98	0	0	0	100	4070	4716	5863
- 8	6422	7024	4124	774	62	0	0	0	54	3479	4627	5720
9	5706	6381	3404	1213	24	0	0	0	24	2641	3928	4922
10	5120	5849	2697	278	0	0	0	0	0	1875	3201	4210
11	4514	5390	1858	32	0	0	0	0	0	1080	2606	3546
12	4199	4974	1263	0	0	0	0	0	0	529	1999	2977
13	3826	4482	934	0	0	0	0	0	0	120	1436	2566
14	3463	3925	333	0	0	0	0	0	0	23	750	2117
15	3035	3274	103	0	0	0	0	0	0	0	126	1766
16	2690	2886	7	0	0	0	0	0	0	0	19	1419
17	2622	2535	2	0	0	0	0	0	0	0	21	1436
18	2966	2478	2	0	0	0	0	0	0	0	107	1781
19	3388	2952	10	0	0	0	0	0	0	0	286	2137
20	3949	3327	63	0	0	0	0	0	0	10	489	2470
21	4537	9174	340	32	0	0	0	0	0	72	658	2812
22	5207	4100	681	60	0	0	0	0	0	338	939	3205
23	5716	4449	988	184	0	0	0	0	0	785	1710	3596
24	6244	4584	1372	221	8	0	0	0	0	977	2181	3943

Table 4C

ROWLAND 01!Fort Gordon P1CARLTON SHUFORD P2DSN 780-6376 P3ATZH-DIC-E /RECALL F 000045556 S 03

ECIP PROJECT 4: UPGRADE HIGH TEMPERATURE WATER SOUTH BUILDING 25330, FT. GORDON

03A IDESCRIPTION OF PROPOSED CONSTRUCTION

***The concept of the heating plant as a steam generating boiler plant which sparges steam into the high temperature water, and is then pumped through the underground pipe distribution has changed completely. The new concept is to replace the steam boilers with hot water generators operating in an auxiliary loop circulating HTW water system from and to the three existing cascade heaters that will be converted for use as expansion/storage tanks. Those tanks will now be pressurized with nitrogen and the pressure on the tank will vary as the water level increases or decreases. The water level will change based on the variable speed pumping and losses in the system. The existing deaerator needs to be modified before any other work is done. The deaerator vessel and storage tank are hopefully reusable, but is our suspicion that the trays within the deaerator are not operating or need to be replace entirely. Another item that needs to be done prior to making the switch over from steam to hot water is to add chemical feed tanks and have chemicals feed at the appropriate locations. This should be done in coordination with the chemical supplier, but basically we are adding sulfite and PH control to the make-up water in the deaerator or immediately after the deaerator. Then there is an additional chemical that needs to be added to the distribution system to make sure that the oxygen corrosion is not an additional problem, and that exposed piping does not corrode. The distribution piping shall also be protected from oxygen pitting and PH imbalance when the make-up water requirement is reduced.

Because there is a multiplicity of units available to be converted and to be replaced with new, it is possible that the steam can remain in operation while the new hot water generators are added and one or more of the cascade heaters is converted so that the plant can serve the needs of the distribution system during the construction period. Then there will be a small shutdown period where you convert over to hot water generation from steam generation. If this can be coordinated with the summer shutdown so that all of the work in the buildings is completed to generate domestic water, then the HTW system can be shutdown 4-1/2 months of the summer to make this conversion from steam to hot water generation.

03B !REMARKS

***Data for this analysis was based on assumed existing efficiency of the boilers of 70%. This was in lieu of not having any accurate information on the efficiencies of the boilers. Recent articles in the ASHRAE Journal and elsewhere indicates that for the Plant as it is now, 70% is probably a very high efficiency for the actual conditions. Even with this payback indicated, we can expect a better payback if the projects are implemented. There are also opportunities to increase the savings if higher efficiency equipment is installed in the buildings. We assumed 80% efficiency for gas combustion, but there are gas-fired heaters that can get into the 90's. This costs additional money, but they may be worthwhile on the basis of dollars they save when the current natural gas prices are compared with high efficiency water heating equipment prices.

The energy conservation measure to upgrade the Heating Plant in Building 25910 includes seven ECO's developed during the extensive engineering study that was conducted. The following describes the ECO's that are included in this ECIP.

ECO NO.	DESCRIPTION			
26	Variable Speed Hot Water Pumping System			
28	Return Hot Water Temperature Control			
32	Reduce Make-up Hot Water			
68	Hot Water Generators System			
70	HTW System			
72	Reduce Steam Leaks			
89	EMCS Controls and Instrumentation			

ECO DATA COMPILATION

ECO NO.	DESCRIPTION	COST (FROM LCC)	SAVINGS 1ST YEAR	TOTAL DISCOUNT SAVINGS
26	Variable Speed Pumping	26,738	5,771	90,086
28	Return Hot Water Temp. Control	54,160	14,403	296,079
32	Reduce Make-up Water	51,209	14,351	294,814
68	Hot Water Generators	774,748	30,977	587,085
70c	Summer Shutdown (1/2 gas, 1/2)	hp) 272,389	157,426	2,760,665
72	Reduce Steam Leaks	1,439	897	18,797
89	EMCS Controls & Instrumentation	12,586	263,811	
	Totals	1,232,816	236,312	4,311,334

Simple Payback: 1,232,816 = 5.22

236,312

SIR: 4,311,334 = 3.50

1,163,554

03C !PROJECT DESCRIPTION

***This Energy conservation measure provides the plan to design the required conservation and upgrade to the heating system in building 25910 - Central Utility Plant - North. The scope of this effort includes addition of two new variable speed pumps, additional control for hot water return temperature regulation, reduction of make-up water required and replacement of five low efficiency steam boilers with three hot water generators. In addition the piping distribution system will be redesigned into three distribution systems and hot water/steam leaks will be reduced or eliminated.

To maximize energy savings, new EMCS controls will be added to permit control of the HTW system from

the Energy Management Control System. This system will permit optimization of how water temperature set point, time of day scheduling and summer shut down of the system. This function will support minimizing staffing requirements.

03D !REQUIREMENT (Why is it needed now)

****The existing steam heating plant is antequated and inefficient. The study showed that the boilers are operating at about 70% efficiency, large quantities of make-up water is required to overcome leaks in the existing system. Recent building renovations to the hot water systems in the Barracks, classrooms and administrative office have increased demand for heating capacity.

By implementing the energy conservation improvement now, annual savings of \$354,008 can be realized, reducing the cost of operation for the entire facility.

03E !CURRENT SITUATION (How is the need currently being met)

***ECO 26

HTW water leaving Building 25330 is pumped with only one set of two identical pumps. The pumps are Ingersol-Rand 4 x 9A with a Louis Allis motor with a serial number of 5111871001 on one motor, and 5111871002 on the other. Type C004NB, 460 volts, 1.15 service factor, 4040 TS frame and the rating is 100 hp at 3550 rpm or 25 hp at 1776 rpm. One or the other of these pumps always operate at low speed. All buildings in the distribution system are equipped with 2-way valves so that when HTW is not required, the flow ceases to that building. Just upstream of the pump there is a blending station that mixes hot water return water before it gets heated with the heated HTW to control the temperature of the HTW leaving the Plant.

ECO 28

HTW is heated in cascade heaters, which is usually maintained at the temperature of the saturation pressure of the boiler, and this boiler pressure is usually maintained except for several times a year when it is changed. At 150 psi, the saturation temperature is 347°F. When the HTW water leaves the cascade heaters, it passes through a blender that adds unheated HTW return to controls with setpoint that maintains the constant HTW supply temperature. Note that as distribution loads vary; less or more HTW water is required, and the HTW return temperature rises and falls depending upon the load. The existing system operates to control the HTW supply water, and does not take into account changes to load that would effect the overall heating requirements.

ECO 32

The total number of gallons lost in Building 25330 over the course of 1992 averages 43,663 gallons per month except for September where the very high recorded leakage is suspect. This leakage is caused by pipe failures and operating inefficiencies in the system. The quantity of lost water is based on reports of water meter readings made by the boiler operators.

ECO 68

Existing boilers are gas-fired with oil back-up. The steam generators are operating as intended. Efficiency testing that was reported by Gee Jenson shows the boilers in Building 25330 operate at approximately 75% efficiency at 100% - 25% capacity.

ECO 70

Space heating is not required from mid-May through the end of September, but a boiler must be in operation to handle domestic water needs and cooking requirements in some cases with the HTW distribution system.

ECO 72

There are steam leaks at steam valves and one hole was found in the cascade heaters. There are less leaks in this building than in Building 29510.

ECO 89

Existing automatic or manual controls are within the plant only with no EMCS tie-in for control. The EMCS office which is manned 24 hours a day has very few, if any instrumentation readouts from the plant, and no control of the plant with the EMCS. Because EMCS personnel are aware of what is happening in many buildings, they are also aware of conditions and demands on the high temperature water system. Currently, the boiler operators are making boiler pressure changes, HTW changes, bringing on and off boilers, and many manual valving operations. However, they are not performing the functions that an EMCS office can to control the energy consumed and to improve the operating efficiency of the Plant. The controls in Building 25330 have recently been upgraded and additions for EMCS points and new points are more readily available than in other places. Therefore, the amount of points necessary to be added is minimal. There is a computer existing that can currently read out large quantities of information.

03F !IMPACT IF NOT PROVIDED

***If this project is not implemented, Fort Gordon will continue to waste excessive quantities of energy. Use of antiquated, inefficient and potentially hazardous boilers will continue to require full staffing of boiler rooms and preclude the possibility of inefficient high temperature hot water system requiring minimum staffing. The lock of instrumentation on the current system assures energy waste and ultimately high maintenance costs.

Annual discounted savings has been determined to be \$6,574,981 with a simple payback of 6.6 years with a savings to investment (SIR) of 2.81.

Heating loads will be unevenly distributed and buildings currently not being provided adequately heating will continue to be cold in the winter.

03G !ADDITIONAL

***New construction and renovation projects on the base will increase demand on the boiler plant to respond to new loading conditions.

03I !RELATED PROJECTS

***ECIP - 45553 - Chilled Water System to Central Utility Plant - Building 25330 North Side

ECIP - 45554 - Chilled Water System to Central Utility Plant - Building 25330 South Side

ECIP - 45555 - High Temperature Water Systems North Plant - Building 25910

07A !GENERAL JUSTIFICATION DATA

This ECIP project is required to support the army wide effort to reduce energy waste. The project will provide new efficient high temperature hot water boilers and variable speed pumps to reduce energy consumption and increase efficiency. New instrumentation will permit better control and provide a means to reduce staffing requirements.

This ECIP consists of six ECO's identified during an energy study that constitute a cost justifiable solution to deficiencies in the current operation. The following justification overview lists the ECO's along with their economic justification.

PROJECT NO. 4 - HOT WATER SOUTH

ECO DATA COMPILATION

TOTAL DISCOUNT SAVINGS	90,086 296,079 294 814	587,085 2,760,665 18,797	<u>263,811</u> 4,311,334
SAVINGS 1st YEAR	5,771 14,304 14,351	30,977 157,426 897	12,586 236,312
NAT GAS SAVINGS MMBTU/YR	0 3,045.32 2,975.50	4,662.00 15,477.00 199.00	2,796.98 29,155.80
ELECTRICAL SAVINGS MMBTU/YR	379	529 0 0	0 806
TOTAL COST (From LCC)	26,738 54,160	21,203 774,748 272,389 1,439	52,133 1,232,816
NON-RECURRING COST (-) SAVINGS (+)	000	000) o o
ANNUAL RECURRING <u>COST</u>	009	961 10,000 79,72 5 0	91,286
CONSTRUCTION COST		45,927.00 694,840.00 244,294.00 1,290.00	46,754.82 1,105,659.00
DESCRIPTION	Variable Speed Pumping Return Hot Water Temperature Control	Reduce Make-up Water Hot Water Generators Summer Shutdown (1/2 gas, 1/2 hp)	Reduce Steam Leaks EMCS Controls/Instrumentation Totals
ECO NO.	26 28	32 68 70c	68

 $\frac{1,232,816}{236,312} = 5.22 \text{ yrs.}$

 $\frac{4,311,334}{1,163,554} = 3.50$

SIR

07B !TRAFFIC ANALYSIS

***There will be no changes to pedestrian or vehicular traffic as a result of implementing this ECIP.
/*

08B !PRESENT ACCOMMODATIONS AND DISPOSITION

***The physical plant building 25910 housing the boiler plant is adequate to accommodate the new boilers and other modifications once the old boilers are removed. Five Steam boilers are being replaced with three high temperature hot water boilers.

09D IRPMA DISCUSSION

***This ECIP will reduce the amount of Real Property maintenance activity because new high efficiency boilers and a new variable speed driver will be installed. Pipes, valves, strainers, heat exchangers and deaeration vessels will be replaced with new equipment.

10A !ANALYSIS OF DEFICIENCIES

- ***1) High temperature water is pumped from the boiler plant with one of two available pumps. One of the pumps runs on slow speed to meet site requirements. All buildings serviced with HTW have two way valves in the HTW lines. When the buildings do not require heat, they close and HTW bypasses that building. As more buildings close, the valves pressure builds in the HTW supply line. This design wastes energy when demand for HTW is low.
- 2) High temperature water is supplied at a constant temperature, even when HTW demand is low. This wastes energy because the water temperature remains higher than required to meet site requirements.
- 3) Make up water requirements are high. A better means of detecting and locating sources of water leaks and excessive use is required.
- 4) The existing steam boilers operate inefficiently. The entire hot water generating system including piping, valves and expansion/storage tanks are inefficiently designed. The system locks the necessary instrumentation and controls to assist operators in running and maintaining the system efficiently. Boilers must be run all year to meet requirements for domestic hot water.
- 5) Steam leaks primarily around valves and cascade feedwater heaters cause energy waste.

 /*

11D !DECISION ANALYSIS

***The following is a detailed cost breakdown of each of the ECO's. Refer to the table in 7A General Justification Data which summarizes these costs.

ECO 26 - LCCA

1.	Investment		
1.	A. Construction Cost	\$	23,980.00
	B. SIOH	\$	1,319.00
	C. Design Cost	\$	1,439.00
	D. Total Cost $(1A + 1B + 1C)$	\$	26,738.00
2.	Energy Savings	\$	-5,615.00
3.	Non Energy Savings	\$	0.00
4.	First Year Dollar Savings	\$	5,771.00
5.	Simple Payback Period	\$	4.63 Years
6.	Total Net Discounted Savings	\$	90,086.00
7.	Savings to Investment Ratio	\$	3.37
ECO	28 - LCCA		
1	Turingtonomt		
1.	Investment A. Construction Cost	\$	48,573.00
	B. SIOH	\$	2,672.00
	C. Design Cost	\$	2,915.00
	D. Total Cost (1A + 1B + 1C)	\$	54,160.00
2.	Energy Savings	\$	-2,949.00
3.	Non Energy Savings	\$	8,844.00
4.	First Year Dollar Savings		14,304.00
5.	Simple Payback Period	\$ \$	3.79 Years
6.	Total Net Discounted Savings	\$	296,079.00
7.	Savings to Investment Ratio	\$	5.47
ECO	22. LCCA		
ECO	32 - LCCA		
1.	Investment	Φ.	45 007 00
	A. Construction Cost	\$	45,927.00
	B. SIOH	\$	2,526.00
	C. Design Cost	\$	2,756.00
	D. Total Cost $(1A + 1B + 1C)$	\$	51,209.00
2.	Energy Savings	\$	-3,019.00 14,164.00
3.	Non Energy Savings	\$ \$	14,351.00
4.	First Year Dollar Savings	\$ \$	3.57 Years
5.	Simple Payback Period	\$ \$	294,814.00
6.	Total Net Discounted Savings	\$ \$	5.76
7.	Savings to Investment Ratio	Ф	5.70

ECO 68 - LCCA

1.	Investment	
1.	A. Construction Cost	\$ 694,840.00
	B. SIOH	\$ 38,217.00
	C. Design Cost	\$ 41,691.00
	D. Total Cost (1A + 1B + 1C)	\$ 774,748.00
2.	Energy Savings	\$ -1,332.00
3.	Non Energy Savings	\$ 147,400.00
4.	First Year Dollar Savings	\$ 30,977.00
5.	Simple Payback Period	\$ 25.01 Years
6.	Total Net Discounted Savings	\$ 587,085.00
7.	Savings to Investment Ratio	\$.76
ECO	70A - LCCA	
1.	Investment	
1.	A. Construction Cost	\$ 330,296.00
	B. SIOH	\$ 18,167.00
	C. Design Cost	\$ 19,818.00
	D. Total Cost (1A + 1B + 1C)	\$ 368,281.00
2.	Energy Savings	\$ 10,540.00
3.	Non Energy Savings	\$ 1,175,147.00
4.	First Year Dollar Savings	\$ 165,479.00
5.	Simple Payback Period	\$ 2.23 Years
6.	Total Net Discounted Savings	\$ 2,886,362.00
7.	Savings to Investment Ratio	\$ 7.84
ECO	70B - LCCA	
ECO	70B - Ecch	
1.	Investment	150 100 00
	A. Construction Cost	\$ 158,193.00
	B. SIOH	\$ 8,701.00
	C. Design Cost	\$ 9,492.00
	D. Total Cost $(1A + 1B + 1C)$	\$ 176,386.00
2.	Energy Savings	\$ 9,483.00
3.	Non Energy Savings	\$ 1,175,147.00
4.	First Year Dollar Savings	\$ 149,371.00
5.	Simple Payback Period	\$ 1.18 Years
6.	Total Net Discounted Savings	\$ 2,634,918.00
7.	Savings to Investment Ratio	\$ 14.94

ECO 70C - LCCA

1.	Investment	
	A. Construction Cost	\$ 244,294.00
	B. SIOH	\$ 13,437.00
	C. Design Cost	\$ 14,658.00
	D. Total Cost $(1A + 1B + 1C)$	\$ 272,389.00
2.	Energy Savings	\$ 10,012.00
3.	Non Energy Savings	\$ 1,175,147.00
4.	First Year Dollar Savings	\$ 157,426.00
5.	Simple Payback Period	\$ 1.73 Years
6.	Total Net Discounted Savings	\$ 2,760,665.00
7.	Savings to Investment Ratio	\$ 10.14
ECO	72 - LCCA	
1.	Investment	
	A. Construction Cost	\$ 1,290.00
	B. SIOH	\$ 71.00
	C. Design Cost	\$ 78.00
	D. Total Cost $(1A + 1B + 1C)$	\$ 1,439.00
2.	Energy Savings	\$ -5,795.00
3.	Non Energy Savings	\$ 0.00
4.	First Year Dollar Savings	\$ 897.00
5.	Simple Payback Period	\$ 1.60 Years
6.	Total Net Discounted Savings	\$ 18,797.00
7.	Savings to Investment Ratio	\$ 13.06
ECO	89 - LCCA	
1.	Investment	
	A. Construction Cost	\$ 46,755.00
	B. SIOH	\$ 2,572.00
	C. Design Cost	\$ 2,806.00
	D. Total Cost $(1A + 1B + 1C)$	\$ 52,133.00
2.	Energy Savings	\$ -3,197.00
3.	Non Energy Savings	\$ 0.00
4.	First Year Dollar Savings	\$ 12,586.00
5.	Simple Payback Period	\$ 4.14 Years
6.	Total Net Discounted Savings	\$ 263,811.00
7.	Savings to Investment Ratio	\$ 5.06

11E !ECONOMIC ANALYSIS ***ECO 26

ITEM DESCRIPTION	QUANTIT QUAN U		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Variable Speed Drive Switches	1	LS LS	11,000 4,340	11,000 4,340	1,500 1,000	1,500 1,000	\$12,500.00 \$5,340.00
				20% OH (0 SUBTOTAL G SUBTOTAL (GO			\$19,032.00 \$3,806.00 \$22,838.40 \$22,838.40 \$1,141.92 \$23,980.32
ECO 28							
ITEM DESCRIPTION	QUANTIT QUAN U		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL
Controls	1	LS	20,000	20,000	15,000	15,000	\$35,000.00
				20% OH (SUBTOTAL G SUBTOTAL (G			\$38,550.00 \$7,710.00 \$46,260.00 \$46,260.00 \$2,313.00 \$48,573.00
ECO 32							
ITEM DESCRIPTION	QUANTIT QUAN U		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	N TOTAL
Flow Meters Temp RTD in Distr. Pipe	10 10	EA EA	1,500 300	15,000 3,000	1,000 500	10,000 5,000	\$25,000.00 \$8,0000.00
				SUBTOTAL \$36,450.00 20% OH (GC ONLY) \$7,290.00 SUBTOTAL GC'S WORK \$43,740.00 SUBTOTAL (GC & SUBS) \$43,740.00 5% CONTINGENCY \$2,187.00 TOTAL \$45,927.00			

ECO 68

ITEM DESCRIPTION	QUANTITY QUAN UNIT	MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSIO:	n total
Hot Water Generator	2 EA	175,000	,	UMP SUM		\$415,000.00
Repiping of Cascade Heat	er 1 LS	6,000	6,000	8,000	8,000	\$14,000.00
Controls for Hot Water Ge		25,000	25,000	20,000	20,000	\$45,000.00
Demolition	1 LS			15,000	15,000	\$15,000.00
Chemical Feed Equipment		2,500	7,500	500	1,500	\$9,000.00
Nitrogen Storage & Piping		8,000	8,000	6,000	6,000	\$14,000.00
			S	UBTOTAL		\$551,460.00
			20% OH (GC ONLY)		\$110,292.00
			SUBTOTAL G			\$661,752.00
			SUBTOTAL (GO	C & SUBS)		\$661,752.00
				INGENCÝ		\$33,087.60
				TOTAL		\$694,839.60
ECO 70A						
ECO 70A						
ITEM	QUANTITY	MATERIAL		LABOR		
DESCRIPTION	QUAN UNIT		EXTENSION	UNIT COST	EXTENSIO	N TOTAL
2-1/2 Ton Heat Pump (51		102,000	102,000	13,000	13,000	\$115,000.00
Piping & Pumps to Exist.	Tank 1 LS	25,500	25,500	21,500	21,500	\$47,000.00
FCU in Building	1 LS	40,000	40,000	25,000	25,000	\$65,000.00
Electrical Work	1 LS	7,500	7,500	7,500	7,500	\$15,000.00
			S	SUBTOTAL		\$262,140.00
				GC ONLY)		\$52,428.00
			SUBTOTAL G			\$314,568.00
						#21 4 5 CD 00
			SUBTOTAL (G			\$314,568.00
			5% CONT	TINGENCY		\$15,728.40
				TOTAL		\$330,296.40
ECO 70B						
		3.64 (WYD) 1.4 T		LADOD		
ITEM	QUANTITY	MATERIAL	PATENICIONI	LABOR	EXTENSIO	N TOTAL
DESCRIPTION	QUAN UNIT	UNIT COST	EXTENSION	UNIT COST	EXTENSIC	M TOTAL
Gas Piping (51 Bldgs)	1 LS	16,000	16,000	32,000	32,000	\$48,000.00
Combustion Air Vent. (5	1 B) 1 LS	2,600	2,600	5,000	5,000	\$7,600.00
Gas Fired Water Heater (11,000	11,000	7,000	7,000	\$18,000.00
Piping to Exist. Storage T		17,000	17,000	14,000	14,000	\$31,000.00
Pumps (51 Buildings)	1 LS		5,000	3,000	3,000	\$8,000.00
				SUBTOTAL		\$125,550.00
				(GC ONLY)		\$25,110.00
			SUBTOTAL C			\$150,660.00
			GI TOTOTALI (C	AC 6 CITON		\$150 660 00
			SUBTOTAL (G			\$150,660.00 \$7,533.00
			5% CON	TINGENCY TOTAL		\$158,193.00
				101/10		4.20,100

ECO 72

/*

ITEM DESCRIPTION	QUAN QUAN		MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL	
Repair Steam Leaks	35	HRS			25	875	\$875.00	
				17% LA			\$875.00 \$148.75 \$1,023.75 \$204.75 \$1,228.50	
				5% CONT	INGENCY TOTAL		\$61.43 \$1,289.93	
ECO 89	ECO 89							
ITEM DESCRIPTION	QUAN QUAN	TITY UNIT	MATERIAL UNIT COST	EXTENSION	LABOR UNIT COST	EXTENSION	TOTAL	
Fuel Flow Expansion Tank HTW Piping Make-up Water Nitrogen Valve Positions BTU Computations Chemical Feed HW Generator Pumps Con HW Gen. Combust. Efficit Gauges and Dials		LS LS LS LS LS LS LS LS	4,000 1,400 2,300 2,000 1,000 700 500 900 2,000 600 2,000	5% S 17% LA			\$6,000.00 \$2,000.00 \$5,000.00 \$3,500.00 \$2,500.00 \$2,500.00 \$1,800.00 \$1,200.00 \$4,000.00 \$33,500.00 \$470.00 \$2,737.00 \$37,107.00 \$7,421.40 \$4,528.40	
				5% CONT	TINGENCY TOTAL		\$2,226.42 \$46,754.82	

12A !CRITERIA FOR PROPOSED CONSTRUCTION

***Construction will occur inside the confines of the existing Building 25910. No additions to the exterior shell is required. Inside renovation work will conform to existing guidelines of architectural design and building construction, specifically the AEI Design Guide (March 1987), the Corps of Engineers Guide Specifications CEGS 13947 thru 13949 for Power Plant and EMCS requirements.

13B !FURNISHINGS AND EQUIPMENT DISCUSSION

- ***This ECIP consists of the following renovations and additions
- 1) Replace 2 steam boilers with HTW boilers.
- 2) Add variable speed drive pumps.
- 3) Install new instrumentation to automate the plant.

15A !ENVIRONMENTAL DOCUMENTATION

***There will be no environmental impact to the modification, renovations and upgrades to the central utility plant heating system. Boilers being replaced will be dismantled and new high efficiency boilers, pumps and heat. The addition of chemical treatment system will be handled in accordance with state and federal regulations.

15B1 !SUMMARY OF ENVIRONMENTAL CONSEQUENCES

***We have reviewed this project and determine that an environmental impact statement, pursuant to PL 91-190, is not required. We have assessed this project and determined that it will not contribute significantly to air and/or water pollution.

16A1 !EVALUATION OF FLOOD HAZARDS

***The renovation is to an existing plant. No history of flooding has been recorded.
/*

19A !SUMMARY OF ENERGY REQUIREMENTS

***Current Electrical oil and gas services are adequate to support the required upgrades to the heating system for the Central Utility Plant, Building 25910. There will be no changes or increased requirements for additional services. The demand for utility service will be reduced as the changes are implemented. See the cost and savings analysis for details.

19B !SUMMARY OF UTILITY SUPPORT

***The existing electric utilities supplied to the central plant is adequate and will not require additional capacity to be added.

20B !HAZARDS TO HANDICAPPED PERSONS

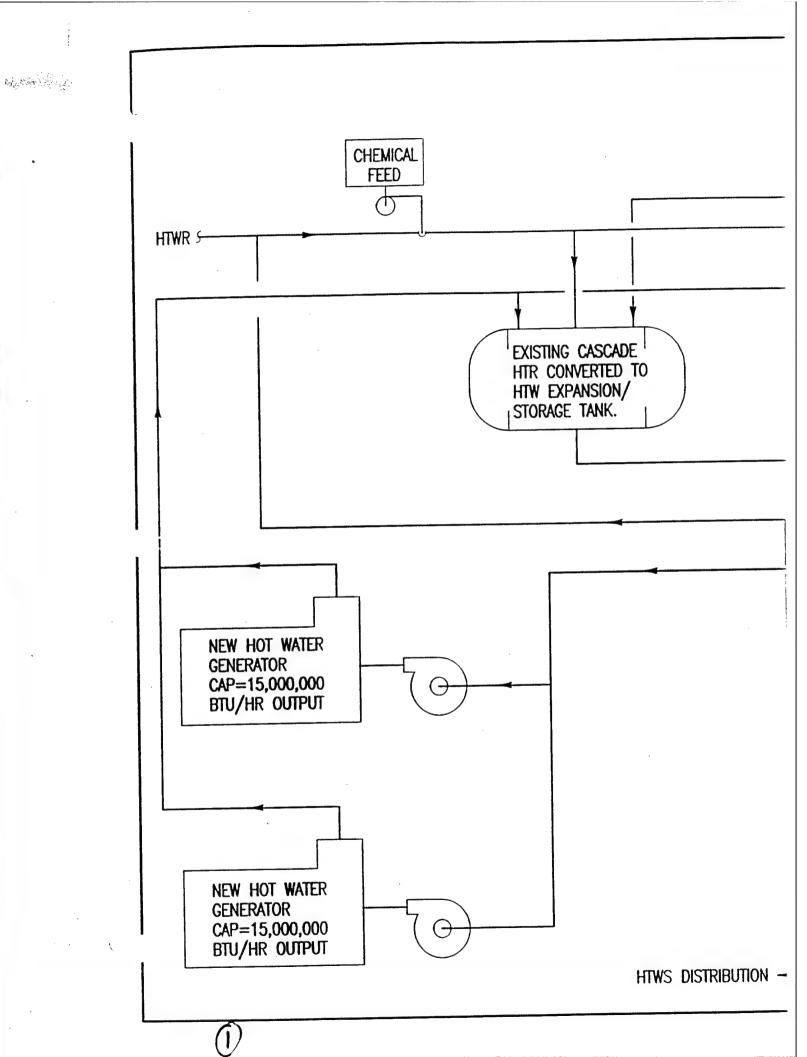
***Existing conditions within the physical plant is considered hazardous to unauthorized personnel. Signs and warnings are posted to alert unauthorized personnel access is restricted to authorized personnel and visitors with prior approval.

20C !HANDICAP PROVISIONS

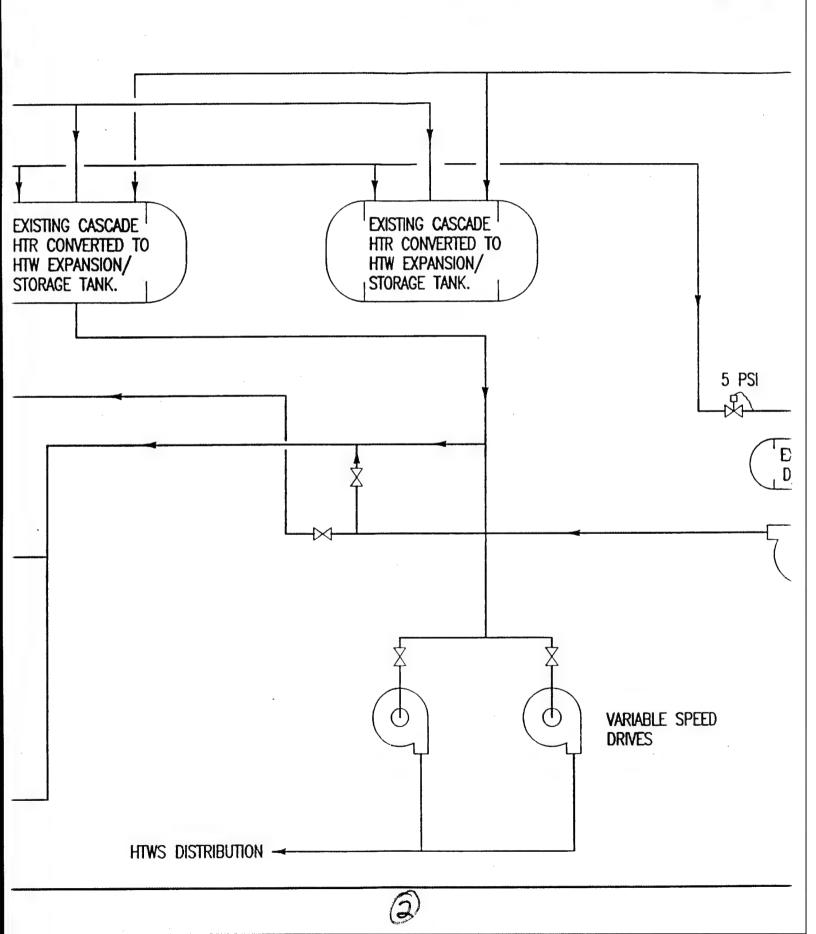
***In accordance with Public Law 90-480, no provisions for the handicapped will be made in the project since the facility is used and operated solely by able bodied personnel. However, the main floor of the facility is at ground level and is handicap accessible.

22B !PHYSICAL SECURITY

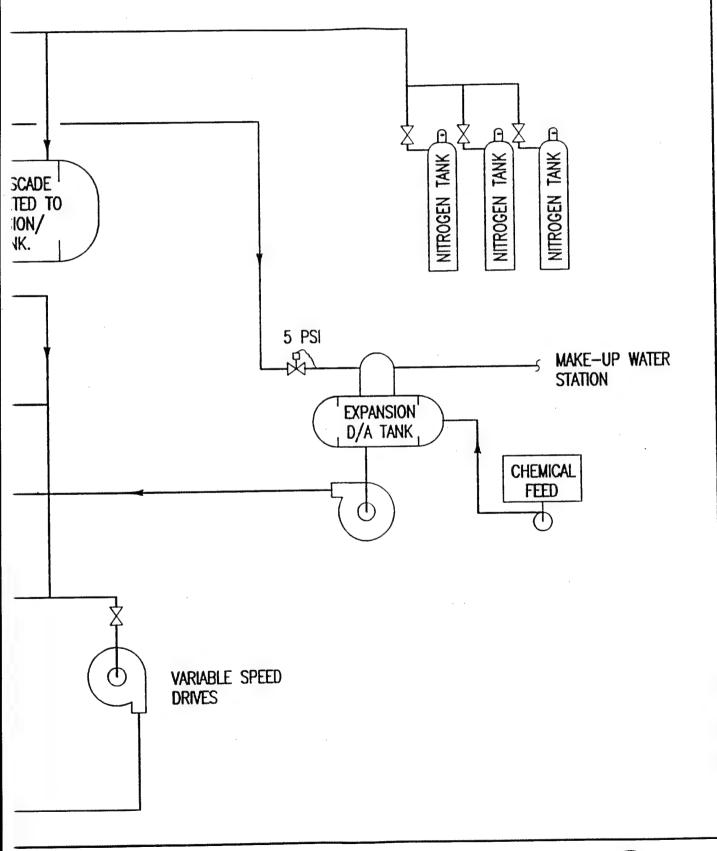
***Project is not considered for commercial activity. The physical plant upgrade to the existing Central Utility Plant will serve the north side of Ft. Gordon. Provisions of DA circular 235-1 are not applicable to this project. /*



Project No. 4 - HTW Schemai



No. 4 - IHTW Schematic-South Bldg. 25330



LIFE CYCLE COST ENERGY CONSERVATION INSTALLATION & LOCATION: PROJECT NO. & TITLE: 4 FISCAL YEAR 1994 DISCI ANALYSIS DATE: 09-22-94	FT. GORDON HTW SOUTH RETE PORTION	REGION NAME: VA	NOS. ARIABLE	4 CENSUS: SPEED PUM	3 PING	••
1. INVESTMENT A. CONSTRUCTION COST B. SIOH C. DESIGN COST D. TOTAL COST (1A+1B+1C) E. SALVAGE VALUE OF EXIS' F. PUBLIC UTILITY COMPAN G. TOTAL INVESTMENT (1D	\$ 1439 \$ 26738 TING EQUIPMENTY REBATE	NT \$ \$	0. 0.	\$ 2673	8.	
2. ENERGY SAVINGS (+) / DATE OF NISTIR 85-3273-X UNIT COST FUEL \$/MBTU(1)	COST (-) USED FOR DI SAVINGS MBTU/YR(2)	ANNUAL	Ş	DISCOUNT		COUNTED INGS (5)
A. ELECT \$ 15.24 B. DIST \$ 8.82 C. RESID \$ 2.73 D. NAT G \$ 4.50 E. COAL \$ 1.61 F. LPG \$ 6.34 M. DEMAND SAVINGS N. TOTAL	379. 0. 0. 0. 0. 0.	· ቀ ቀ ቀ ቀ ቀ ቀ	771. 0. 0. 0. 0. 0. 0. 771.	17.56 19.97	ው ው ው ው ው ው ው ው	90086. 0. 0. 0. 0. 0. 90086.
3. NON ENERGY SAVINGS(+) A. ANNUAL RECURRING ((+/-) OR (TABLE A)	A X 3A1)		14.74	\$ \$	0. 0.
B. NON RECURRING SAVI	SAVINGS (COST (-	STS(-) (+) YR -) OC (2)	FACT	R SAV	COUNT INGS T(-)	(+)/
d. TOTAL	\$ ().			(0.
C. TOTAL NON ENERGY I	DISCOUNTED SA	AVINGS (+)	/COST(-) (3A2+3Bd	4)\$	0.
4. FIRST YEAR DOLLAR SA	VINGS 2N3+3A-	+ (3Bd1/(YRS ECO	NOMIC LIFE))\$	5771.
5. SIMPLE PAYBACK PERIO	D (1G/4)					4.63 YEAR
6. TOTAL NET DISCOUNTED	SAVINGS (2N	5+3C)			\$	90086.
7. SAVINGS TO INVESTMENT (IF < 1 PROJECT DOE	T RATIO S NOT QUALIF	-)=(6 /	1G) =		3.37
8. ADJUSTED INTERNAL RA	TE OF RETURN	(AIRR):				9.56 %

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LIFE CYCLE COST ANALYSIS SUMMARY STUDY: EC0028
-ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) .. LCCID 1.080
INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3
PROJECT NO. & TITLE: 4 HTW SOUTH
FISCAL YEAR 1994 DISCRETE PORTION NAME: CONTROLS
ANALYSIS DATE: 01-13-95 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB
1. INVESTMENT
A. CONSTRUCTION COST $ 48573.

B. SIOH $ 2672.

C. DESIGN COST $ 2915.

D. TOTAL COST (1A+1B+1C) $ 54160.
                                                 0.
0.
E. SALVAGE VALUE OF EXISTING EQUIPMENT $
F. PUBLIC UTILITY COMPANY REBATE $
G. TOTAL INVESTMENT (1D - 1E - 1F)
                                                         $ 54160.
2. ENERGY SAVINGS (+) / COST (-)
DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993
    UNIT COST SAVINGS ANNUAL $ DISCOUNT DISCOUNTED $/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5)
    3. NON ENERGY SAVINGS (+) / COST (-)
        NNUAL RECURRING (+/-) $ 600.

(1) DISCOUNT FACTOR (TABLE A) 14.74

(2) DISCOUNTED SAVING/COST (3A X 3A1) $ 8844.
       (1) DISCOUNT FACTOR (TABLE A)
   A. ANNUAL RECURRING (+/-)
   B. NON RECURRING SAVINGS (+) / COSTS (-)
                  SAVINGS(+) / COSTS(-)

SAVINGS(+) YR DISCNT DISCOUNTED

TEM COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4)
                 ITEM
                     $ 0.
                                                                   0.
    d. TOTAL
   C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)$ 8844.
4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))$ 14304.
                                                                       3.79 YEARS
5. SIMPLE PAYBACK PERIOD (1G/4)
                                                             $ 296079.
6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)
7. SAVINGS TO INVESTMENT RATIO (SIR)=(6 / 1G)=
                                                                       5.47
    (IF < 1 PROJECT DOES NOT QUALIFY)
                                                                    12.24 %
8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):
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LIFE CYCLE COST ANALYSIS SUMMARY STUDY: EC0032
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080
INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3
PROJECT NO. & TITLE: 4 HTW SOUTH
FISCAL YEAR 1994 DISCRETE PORTION NAME: REDUCE WATER
ANALYSIS DATE: 01-13-95 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB
1. INVESTMENT
A. CONSTRUCTION COST $ 45927.

B. SIOH $ 2526.

C. DESIGN COST $ 2756.

D. TOTAL COST (1A+1B+1C) $ 51209.
                                               0.
0.
E. SALVAGE VALUE OF EXISTING EQUIPMENT $
F. PUBLIC UTILITY COMPANY REBATE $
G TOTAL INVESTMENT (1D - 1E - 1F)
G. TOTAL INVESTMENT (1D - 1E - 1F)
2. ENERGY SAVINGS (+) / COST (-)
DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993
    UNIT COST SAVINGS ANNUAL $ DISCOUNT DISCOUNTED FUEL $/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5)
    3. NON ENERGY SAVINGS(+) / COST(-)
        NNUAL RECURRING (+/-) $ 961.

(1) DISCOUNT FACTOR (TABLE A) 14.74

(2) DISCOUNTED SAVING/COST (3A X 3A1) $ 14164.
       (1) DISCOUNT FACTOR (TABLE A)
 A. ANNUAL RECURRING (+/-)
    B. NON RECURRING SAVINGS (+) / COSTS (-)
                 SAVINGS(+) YR DISCNT DISCOUNTED

ITEM COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4)
                               $ 0.
    d. TOTAL
    C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)$ 14164.
 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))$
                                                                      3.57 YEARS
 5. SIMPLE PAYBACK PERIOD (1G/4)
                                                             $ 294814.
 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)
 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) =
                                                                      5.76
    (IF < 1 PROJECT DOES NOT QUALIFY)
                                                              12.53 %
 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):
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LIFE CYCLE COST ANALYSIS SUMMARY STUDY: EC0068
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080 INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 4 HTW SOUTH FISCAL YEAR 1994 DISCRETE PORTION NAME: REPLACE BOILERS ANALYSIS DATE: 02-21-95 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 694840. B. SIOH \$ 38217.
C. DESIGN COST \$ 41691.
D. TOTAL COST (1A+1B+1C) \$ 774748. 0. 0. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ F. PUBLIC UTILITY COMPANY REBATE \$ G. TOTAL INVESTMENT (1D - 1E - 1F) 774748. 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) FUEL 3. NON ENERGY SAVINGS (+) / COST (-) \$ 10000. 14.74 \$ 147400. A. ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS (+) / COSTS (-) SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4) ITEM Ο. \$ 0. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS (+) / COST (-) (3A2+3Bd4) \$ 147400. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 30977. 25.01 YEARS 5. SIMPLE PAYBACK PERIOD (1G/4) \$ 587085. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = .76

8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

(IF < 1 PROJECT DOES NOT QUALIFY)

Project does not qualify for ECIP funding; 4,5,6 for information only.

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LIFE CYCLE COST ANALYSIS SUMMARY ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) · · LCCID 1 INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 4 HTW SOUTH	.080
FISCAL YEAR 1994 DISCRETE PORTION NAME: SUMMER SHUTDOWN-HEAT ANALYSIS DATE: 09-22-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HA	RVEY TOUB
1. INVESTMENT A. CONSTRUCTION COST \$ 330296. B. SIOH \$ 18167. C. DESIGN COST \$ 19818. D. TOTAL COST (1A+1B+1C) \$ 368281. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0. F. PUBLIC UTILITY COMPANY REBATE \$ 0. G. TOTAL INVESTMENT (1D - 1E - 1F) \$ 368281.	
2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DI FUEL \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(3)	ISCOUNTED AVINGS(5)
B. DIST \$ 8.82	251491. 0. 0. 1459725. 0. 0. 1711216.
(1) DISCOUNT FACTOR (TABLE A) 14.74	79725. 1175147.
B. NON RECURRING SAVINGS(+) / COSTS(-) SAVINGS(+) YR DISCNT DISCOUNT ITEM COST(-) OC FACTR SAVINGS (1) (2) (3) COST(-)	S(+)/
d. TOTAL \$ 0.	0.
C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$	1175147.
4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$	165479.
5. SIMPLE PAYBACK PERIOD (1G/4)	2.23 YEAR!
6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) \$	2886362.
7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = (1F < 1 PROJECT DOES NOT QUALIFY)	7.84
8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):	14.28 %

LIFE CYCLE COS ENERGY CONSERVATION INSTALLATION & LOCATION: PROJECT NO. & TITLE: 4 FISCAL YEAR 1994 DISC ANALYSIS DATE: 09-22-94	FT. GORDON HTW SOUTH RETE PORTION 1	REGION NOS.	4 CENSUS: SHUTDOWN-GA	3 S
1. INVESTMENT A. CONSTRUCTION COST B. SIOH C. DESIGN COST D. TOTAL COST (1A+1B+1C) E. SALVAGE VALUE OF EXIS F. PUBLIC UTILITY COMPAN G. TOTAL INVESTMENT (1D	TING EQUIPMENT Y REBATE	\$ 0.		6.
2. ENERGY SAVINGS (+) / DATE OF NISTIR 85-3273-X UNIT COST FUEL \$/MBTU(1)	USED FOR DISC	COUNT FACTORS ANNUAL \$ SAVINGS(3)	OCT 1993 DISCOUNT FACTOR(4)	DISCOUNTED SAVINGS (5)
A. ELECT \$ 15.24 B. DIST \$ 8.82 C. RESID \$ 2.73 D. NAT G \$ 4.50 E. COAL \$ 1.61 F. LPG \$ 6.34 M. DEMAND SAVINGS N. TOTAL	0.	\$ 0. \$ 0. \$ 0. \$ 69646. \$ 0. \$ 0. \$ 69646.	15.61 17.56 19.97 20.96 17.58 16.12 14.74	\$ 0. \$ 0. \$ 0. \$ 1459772. \$ 0. \$ 0. \$ 1459772.
A. ANNUAL RECURRING (1) DISCOUNT FACT (2) DISCOUNTED SE	(+/-)	X 3A1)	14.74	\$ 79725. \$ 1175147.
B. NON RECURRING SAV	INGS(+) / COST SAVINGS(+ COST(-) (1)	OC FAC	rr savi	COUNTED INGS (+) / I (-) (4)
d. TOTAL	\$ 0.			0.
C. TOTAL NON ENERGY	DISCOUNTED SAV	'INGS(+)/COST	(-) (3A2+3Bd	1)\$ 1175147.
4. FIRST YEAR DOLLAR SA	VINGS 2N3+3A+(3Bd1/(YRS EC	ONOMIC LIFE))\$ 149371.
5. SIMPLE PAYBACK PERIO	D (1G/4)			1.18 YEARS
6. TOTAL NET DISCOUNTED	SAVINGS (2N5+	-3C)		\$ 2634918.
7. SAVINGS TO INVESTMEN (IF < 1 PROJECT DOE	T RATIO S NOT QUALIFY)	(SIR) = (6 /	1G) =	14.94
8. ADJUSTED INTERNAL RA	TE OF RETURN	(AIRR):		18.02 %

LIFE CYCLE COST ANALYSIS SUMMARY ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 4 HTW SOUTH FISCAL YEAR 1994 DISCRETE PORTION NAME: SUMMER SHUTDOWN-1/2 GANALYSIS DATE: 09-22-94 ECONOMIC LIFE 20 YEARS PREPARED BY: HAM	AS 1/2HP
1. INVESTMENT A. CONSTRUCTION COST \$ 244294. B. SIOH \$ 13437. C. DESIGN COST \$ 14658. D. TOTAL COST (1A+1B+1C) \$ 272389. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0. F. PUBLIC UTILITY COMPANY REBATE \$ 0. G. TOTAL INVESTMENT (1D - 1E - 1F) \$ 272389.	
FOEL 3/FB10(1) 1B10/11(1)	SCOUNTED VINGS (5)
A. ELECT \$ 15.24	125746. 0. 0. 1459772. 0. 0. 0. 1585518.
3. NON ENERGY SAVINGS(+) / COST(-) A. ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) (2) DISCOUNTED SAVING/COST (3A X 3A1) \$	79725. 1175147.
B. NON RECURRING SAVINGS(+) / COSTS(-) SAVINGS(+) YR DISCNT DISCOUN ITEM COST(-) OC FACTR SAVINGS (1) (2) (3) COST(-)	S(+)/
d. TOTAL \$ 0.	0.
C. TOTAL NON ENERGY DISCOUNTED SAVINGS (+)/COST(-)(3A2+3Bd4)\$	1175147.
4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$	157426.
5. SIMPLE PAYBACK PERIOD (1G/4)	1.73 YEAR
6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) \$	2760665.
7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = (IF < 1 PROJECT DOES NOT QUALIFY)	10.14
8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):	15.76 %

LIFE CYCLE COST ENERGY CONSERVATION INSTALLATION & LOCATION: PROJECT NO. & TITLE: 4 FISCAL YEAR 1994 DISCI ANALYSIS DATE: 09-22-94	INVESTMENT P FT. GORDON HTW SOUTH	ROGRAM REGIO	(ECIP) ON NOS. STEAM LE	4 CENSUS	: 3	80
1. INVESTMENT A. CONSTRUCTION COST B. SIOH C. DESIGN COST D. TOTAL COST (1A+1B+1C) E. SALVAGE VALUE OF EXIS F. PUBLIC UTILITY COMPAN G. TOTAL INVESTMENT (1D	\$ 71. \$ 78. \$ 1439. TING EQUIPMEN Y REBATE		0. 0.	\$ 14	39.	
2. ENERGY SAVINGS (+) / DATE OF NISTIR 85-3273-X UNIT COST FUEL \$/MBTU(1)	USED FOR DIS		1. 5	DISCOUNT	שובטע	COUNTED INGS (5)
A. ELECT \$ 15.24 B. DIST \$ 8.82 C. RESID \$ 2.73 D. NAT G \$ 4.50 E. COAL \$ 1.61 F. LPG \$ 6.34 M. DEMAND SAVINGS N. TOTAL	0. 0. 199. 0.	\$ \$ \$ \$	0. 0. 0. 897. 0. 0. 897.	17.56 19.97	₩₩₩₩₩	0. 0. 18797. 0. 0. 18797.
3. NON ENERGY SAVINGS (+) A. ANNUAL RECURRING (1) DISCOUNT FACT (2) DISCOUNTED SA	(+/-) FOR (TABLE A)	а х за:	1)	14.74	\$ \$	o. o.
B. NON RECURRING SAV	INGS(+) / COS SAVINGS(COST(- (1)	+) YI	R DISC	R SA	SCOUNT VINGS (ST(-)(+)/
d. TOTAL	4).				
C. TOTAL NON ENERGY	DISCOUNTED SA	VINGS (+)/COST	(-) (3A2+3E	d4)\$	0.
4. FIRST YEAR DOLLAR SA	VINGS 2N3+3A+	(3Bd1/	(YRS ECC	ONOMIC LI	'E))\$	897.
5. SIMPLE PAYBACK PERIO	D (1G/4)					1.60 YEAR
6. TOTAL NET DISCOUNTED	SAVINGS (2N	5+3C)			\$	18797.
7. SAVINGS TO INVESTMEN (IF < 1 PROJECT DOE	T RATIO S NOT QUALIF		(R) = (6 /	1G) =	:	13.06
8. ADJUSTED INTERNAL RA	TE OF RETURN	(AIRR)	:		Ċ	17.24 %

LIFE CYCLE COST ANALYSIS SUMMARY
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP)

LCCID 1.080 INSTALLATION & LOCATION: FT. GORDON REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 4 HTW SOUTH FISCAL YEAR 1994 DISCRETE PORTION NAME: CONTROLS ANALYSIS DATE: 02-19-95 ECONOMIC LIFE 20 YEARS PREPARED BY: HARVEY TOUB 1. INVESTMENT A. CONSTRUCTION COST \$ 46755. B. SIOH \$ 2572. C. DESIGN COST \$ 2806. D. TOTAL COST (1A+1B+1C) \$ 52133. 0. 0. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ F. PUBLIC UTILITY COMPANY REBATE \$ \$ 52133. G. TOTAL INVESTMENT (1D - 1E - 1F) 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) FUEL 0. 0. 0. \$ 263811. 0. 0. 0. 263811. 3. NON ENERGY SAVINGS (+) / COST (-) 0. A. ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) 0. (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS (+) / COSTS (-) SAVINGS(+) YR DISCNT DISCOUNTED

COST(-) OC FACTR SAVINGS(+)/

(1) (2) (3) COST(-)(4) ITEM 0. d. TOTAL \$ 0. C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 0. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 12586. 4.14 YEARS 5. SIMPLE PAYBACK PERIOD (1G/4) \$ 263811. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 5.06 (IF < 1 PROJECT DOES NOT QUALIFY) 11.81 % 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

LIFE CYCLE COS ENERGY CONSERVATION INSTALLATION & LOCATION: PROJECT NO. & TITLE: 4 FISCAL YEAR 1994 DISC ANALYSIS DATE: 01-13-95	FT. GORDON HTW SOUTH RETE PORTION 1	REGION NOS. NAME: EMCS-HI	. 4 CENSUS:	3
1. INVESTMENT A. CONSTRUCTION COST B. SIOH C. DESIGN COST D. TOTAL COST (1A+1B+1C) E. SALVAGE VALUE OF EXIS F. PUBLIC UTILITY COMPAN G. TOTAL INVESTMENT (1D	TING EQUIPMEN' Y REBATE	T \$ 0 .	\$ 5213	3.
FUEL \$/MBTU(1)	USED FOR DIS SAVINGS MBTU/YR(2)	ANNUAL \$ SAVINGS(3)	DISCOUNT FACTOR(4)	SAVINGS(5)
A. ELECT \$ 15.24 B. DIST \$ 8.82 C. RESID \$ 2.73 D. NAT G \$ 4.50 E. COAL \$ 1.61 F. LPG \$ 6.34 M. DEMAND SAVINGS N. TOTAL	0. 0. 0. 2797. 0. 0.	\$ 0. \$ 0. \$ 0. \$ 12586. \$ 0. \$ 0. \$ 12586.	15.61 17.56 19.97 20.96 17.58 16.12 14.74	\$ 0. \$ 0. \$ 0. \$ 263811. \$ 0. \$ 0. \$ 263811.
3. NON ENERGY SAVINGS(+) / COST(-)				
A. ANNUAL RECURRING ((1) DISCOUNT FACT (2) DISCOUNTED SA	OR (TABLE A)	X 3A1)	14.74	\$ 0. \$ 0.
B. NON RECURRING SAVI	SAVINGS(+ COST(-)	YR DIS	TR SAVI	COUNTED INGS (+) / I(-) (4)
d. TOTAL	\$ 0.			0.
C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 0.				
4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 12586.				
5. SIMPLE PAYBACK PERIOD (1G/4)				4.14 YEARS
6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)				\$ 263811.
7. SAVINGS TO INVESTMENT RATIO (SIR) = (6 / 1G) = 5.06 (IF < 1 PROJECT DOES NOT QUALIFY)				
8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):			11.81 %	